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รายงานผลการปฏิบัติตามมาตรการป้องกันและแก้ไขผลกระทบสิ่งแวดล้อม และมาตรการติดตามตรวจสอบผลกระทบสิ่งแวดล้อม
โครงการในพื้นที่จังหวัดกำแพงเพชร
ฉบับเดือนมกราคม - ธันวาคม พ.ศ. 2566

ภาคผนวกที่ 30

เอกสารแสดงการจัดทำ Hazardous Area Classification



PTT Exploration and Production Public Company Limited

Hazard and Operability (HAZOP) Study Guideline

Document Code: 12147-GDL-SSHE-401/00/03-R03

September 2022



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Approval Register

Document Subject	Hazard and Operability (HAZOP) Study Guideline
Document Code	12147-GDL-SSHE-401/00/03-R03
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Effective Date	September 2022

Review and Approve

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Document Custodian			29-Aug-2022
Technical Reviewer			08-Sep-2022
			08-Sep-2022
			06-Sep-2022
Document Owner			08-Sep-2022
Approval Authority			12-Sep-2022

THIS DOCUMENT WILL BE REVIEWED EVERY 5 YEARS FROM THE DATE OF APPROVAL OR REVISED EARLIER IF NECESSARY.

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INTRODUCTION

1. PURPOSE

This corporate guideline provides PTTEP approach to conducting Hazard and Operability (HAZOP) studies. It is intended for relevant stakeholders such as a HAZOP facilitator, scribe, team members, project management, and asset owner to understand how to organize an effective HAZOP.

The objective of HAZOP studies is to scrutinize design information such as Process & Instrumentation Diagrams (P&IDs), Cause and Effects Diagrams, ESD Logic Diagrams, etc., by using guidewords in order to identify potential deviations from the design intent that could lead to hazardous situations or operability problems. Identifying such issues allow design modifications before a plant or facility is installed or as a part of a proactive Process Safety Management (PSM) through Management of Change (MOC), where field modifications are typically requested for existing facilities. Even though a HAZOP is not appropriate in all circumstances (see IEC 61882:2016 section 5.3 for HAZOP study limitations), one of the major benefits is that it can be used to identify significant operability problems and can thus provide a clear return on the investment beyond the reduction in hazards.

This Hazard and Operability (HAZOP) Study Guideline is part of the SSHE Risk Management Standard (Document code: 11038-STD-SSHE-401) and the Project Realisation Process (PREP) Standard, Safety, Security, Health and Environment Management (Document code: 10008-STD-3-PRP-004), Section 8.6 Mandatory SSHE Activities.

2. SCOPE

This document applies to all operating assets within PTTEP and subsidiaries. It may also be utilized, as agreed by Jointed Operated Assets or Non-operated Joint Venture Assets.

Overview of HAZOP studies throughout Project life-cycle based on PTTEP PREP					
Phase 1 Identify/ Assess	Phase 2 Select	Phase 3 Define/ Develop	Phase 4 Execute	Phase 5 Operate/ Evaluate	Abandonment
-	Coarse HAZOP	HAZOP	HAZOP HAZOP for MOC	HAZOP for MOC Re-HAZOP	-

HAZOP studies shall be performed on all PTTEP projects and plant modifications that change process, equipment, instrument, setpoint, and piping in P&IDs. Modifications that are like-for-like replacements of equipment and piping specifications do not require a HAZOP study. Any department can propose a HAZOP to be held.

REQUIREMENTS

3. HAZARD AND OPERABILITY (HAZOP) STUDY REQUIREMENT

Hazard and Operability (HAZOP) Studies involve critical sequences of information gathering and application of a decision-making process. Team members should be selected based on their knowledge of the technical and operational aspects relevant to the facility/installation being studied as per Section 3.3. In addition, basis information, documentation, and methodology as per Section 3.2.1 are to be provided for an effective HAZOP study. below shows the Simplified HAZOP Study Process.

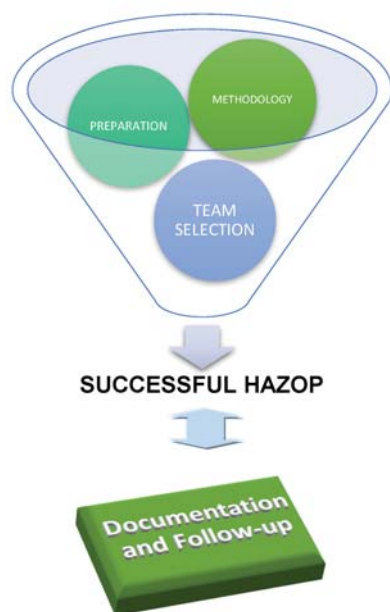


Figure 1: Simplified HAZOP Study Process

3.1 HAZOP APPLICATION THROUGHOUT PROJECT LIFE-CYCLE

This topic aims to give an overview of HAZOP application for each stage of the project life-cycle, to understand the concept, function of HAZOP, and stakeholders' responsibilities throughout the project life cycle.

Phase 2: SELECT - Conceptual and Pre-Project

At this phase, a coarse HAZOP should be conducted using the Process Flow Diagrams (PFDs) since little information is available. The same methodology with a regular HAZOP can be applied. Typically, the PFDs are segregated into a small number (of larger) nodes appropriately for an early design development stage. The intention of a coarse HAZOP at this early stage of the project life cycle is to allow the ability to change the design, operating, and maintenance strategy without any significant adverse effects on the project.

The coarse HAZOP plays a significant role in the facility siting and safeguarding studies of the chosen design concept. Changes to the design at this stage are generally feasible and economical.

Phase 3: DEFINE - Basic Engineering

When the basic engineering is almost completed (approximately 60% of overall project progress when most required information is available), a HAZOP study shall be carried out on the P&IDs. The design should be mature enough to avoid "design review" and provide meaningful answers to questions raised in the HAZOP. At this point, it is still possible to change the design without major costs. The objective of HAZOP at this stage is the assurance of the safety of the current design ('Will it work?') rather than making radical recommendations for change.

A HAZOP report and HAZOP action report shall be generated, and these shall be parts of the Project deliverables.

The Project Manager (or his/her delegation) is responsible for initiating the request for arranging, budgeting, allocating resources, and coordinating with the VP/SSHE Manager for any needed HAZOP studies. It is the responsibility of the Project Manager to ensure all HAZOP recommendations are closed out in a timely manner.

Phase 4: EXECUTE - Detailed Engineering, Commissioning, and Start-Up

A detailed HAZOP study shall be held toward the end of the detailed engineering design stage when drawings are ready for Approved for Construction (AFC). It shall include equipment vendor or package details. Unless a major change is introduced in the detailed engineering work, the study focuses on changes since the previous HAZOP in the define phase rather than reviewing the agreed design. It is possible that vendor information for utilities or auxiliary systems may be available at a much later stage in the detailed design phase. In this case, additional HAZOP studies can be arranged, ensuring that all systems are included.

After the main HAZOP finishes, any changes to the design are subject to go through the MOC process, and the Re-HAZOP would be required. A mini-HAZOP is generally organized to review the proposed changes. The key aspect here is to look at the original node and associated nodes upstream and downstream.

The Project Manager is responsible for arranging and allocating resources for the (Mini) HAZOP study. The risks during start-up are well known in the hydrocarbon industry, and great care shall be made to minimize that risk from changes during this project phase to ensure the adequacy of the safety barriers.

When all HAZOP recommendations have been closed out, a final HAZOP close-out report shall be generated. This document is part of the project deliverables.

Phase 5: OPERATE - Operation

Problems, concerns, and changes in operating methods and design may emerge over time once operations have begun. Modifications and Plant Changes to facilities shall be raised to resolve the problems. The company's MOC process shall be applied. Any changes other than like-for-like replacement of the original piping, equipment, process sequence, and integrity operating windows shall require a HAZOP study. This means revisiting the HAZOP report and the safety case and performing a mini-HAZOP. HAZOP study provides value at this stage by assessing any potential change impact prior to implementation.

All Brownfield major installation/process changes shall follow the PREP requirements (Safety, Security, Health, and Environment Management, Document code: 10008-STD-3-PRP-004) to ensure all SSHE aspects are taken into consideration. For any acquired assets where the existing HAZOP studies are not placed, the asset must put in place a plan to complete the HAZOP within the timeframe complying with local regulations. In case of no legal requirement, the asset must agree with Corporate Process Safety and Assurance department to complete the HAZOP as soon as possible.

Over the course of the operation phase, the HAZOP will be repeated (as a part of SSHE Risk Management Standard 11038-STD-SSHE-401 requirement) throughout the life of a facility, and the finding of significant issues is likely to decrease during each subsequent HAZOP. This is to be expected from the rigorous application of a robust, systematic, and well-established technique. However, there are subtle changes that may be difficult to detect and monitor using conventional HAZOP study. These changes, known as "Creeping Changes," can lead to "normalization in deviance" and potentially be devastating.

Therefore, to understand the creeping changes to the process that have occurred and ensure that the risks associated with them have been understood and addressed, it was necessary to look at the process differently. It is recommended that for any HAZOP revalidations, the guidelines and approaches suggested in the IChemE Safety Centre Guidance - Effective revalidation of risk assessments Delta HAZOP should be consulted. Appendix E to G provides the suggested information, topics for discussion, and explanation which should be adopted during the revalidation study workshop.

It is recommended that the revalidation should focus on the changes (i.e. process, equipment, methodology, operating personnel, etc.) rather than starting from the clean sheet. In order to allocate resources and time to identify any potential creeping changes that are sometimes difficult to detect and monitor.

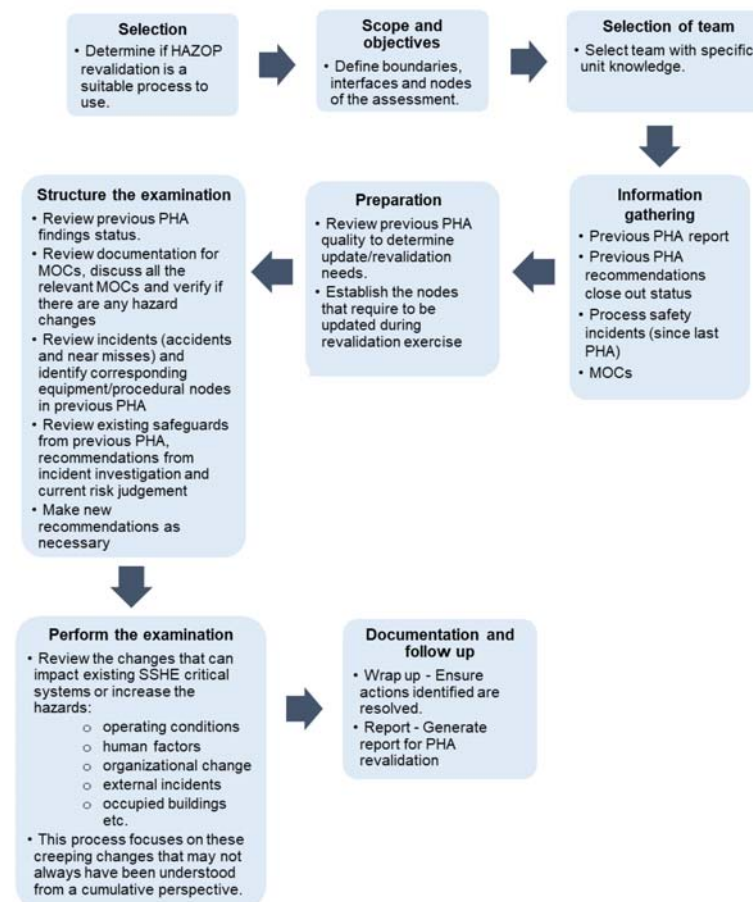


Figure 2: HAZOP Revalidation Process (Ref. IChemE Safety Center Guidance – Effective Revalidation of Risk Assessments)

The Brownfield Project Manager/Asset Manager or his/her delegate is responsible for initiating the request for any needed HAZOP studies and coordinating with the SSHE Manager/VP for the HAZOP arrangement. In the case of International assets, they may also do their own HAZOP studies if they have competent personnel to organize/participate in the workshops based on team selection criteria in section 3.3.

3.2 PREPARATION FOR A HAZOP STUDY

To conduct a HAZOP study effectively, up-to-date P&IDs and relevant information are essential before the HAZOP can be held. These should be supported by operating instructions or philosophy, Cause and Effects Diagrams, ESD Logic Diagrams, Process Flow Diagrams (PFD), plant layouts, and other relevant documents. It should be available and distributed at least one week before the HAZOP to allow team members to study them. It should be marked "Issued for HAZOP". Such documents should be gone through an interdisciplinary check prior to the HAZOP in order to avoid the HAZOP becoming predominantly a design review meeting. The HAZOP facilitator/leader will select and mark up lines or "nodes" from the P&IDs before the study begins.

So, before the commencement of the HAZOP study, the following steps should be studied and completed:

Terms of Reference (TOR)

TOR should be prepared and agreed upon with budget holders such as site/asset/project management for the study scope, schedule, tariff cost, traveling cost, etc. This is particularly useful for large-scope HAZOP, which can have a long duration or where cost allocation is required.

The HAZOP Terms of Reference (TOR) need to be generated and agreed upon between a HAZOP requester and a HAZOP provider. It can be initiated, typically by the requester, to ensure that a successful HAZOP study will be achieved. It should be agreed upon at least two weeks in advance. However, it depends on the scope and complexity of the HAZOP study. Generally, its content should contain the list as follows, but not limited to:

- a) Project Background/Description
- b) Project Objectives
- c) Methodology
- d) Scope of Work
- e) Documents for Review
- f) Activities and Schedule
- g) Venue
- h) Deliverables
- i) Resources

3.2.1 Required Documents for HAZOP Study

The HAZOP facilitator/leader should ensure, with assistance from relevant disciplines, that appropriate documentation is available before the HAZOP is conducted. These should consist of:

Basis Information

Typically, the following documentation is required and should be available before performing the HAZOP:

- 1) **P&IDs and/or PFDs (Mandatory)**
- 2) **System description (Mandatory)**
- 3) Outline the project constraints
- 4) Appropriate background information and studies collated, such as historical incident/equipment failure records.
- 5) Plot plans/ Layouts/ Module layouts of the site/installation
- 6) (UFDs)
- 7) Process control narrative and design basis
- 8) Start-up and emergency shut-down procedures, Cause and Effects Diagrams, and ESD Logic Diagrams.
- 9) Previous HAZOP and Risk Assessment Studies (if any)
- 10) Data of material or fluid properties
- 11) Standard Operating Procedures (SOP – The current revision for an existing operation, operating instructions)
- 12) The environmental conditions

It is strongly recommended to put the HAZOP study on hold until the mandatory and other agreed documents are available.

For the effectiveness of HAZOP study, all required design documentation shall be clearly and uniquely identified, updated, and approved. The information should be provided to the HAZOP team members and HAZOP facilitator/leader at least one week before the workshop. This allows preparations to be made, such as preparing a list of work steps for critical review. In addition, HAZOP team members should familiarize themselves with the information provided prior to the workshop and note any important issues to be discussed.

Selection of HAZOP Node and Node Mark Up

In order to save time during the HAZOP study, the HAZOP facilitator/leader and scribe should pre-select and mark up the nodes. A node represents a section of a process. Generally, during HAZOP study, full-sized P&IDs with the marked-up nodes are shown in the meeting room. These marked-up P&IDs will be the point for the team discussions and will serve as the official record of the discussions.

The node's design intention defines how the process is expected to perform, and it should be recorded for all plant operating cases. It is important to give the full range of operating and design conditions.

Before the HAZOP workshop, a Process Engineer should review and/or provide process operating and design condition in HAZOP worksheet. During the study, he/she should give a brief description of the process and its design intent at the beginning of each node. This will be recorded in the HAZOP worksheet. Similarly, the operation representative should give a brief step-by-step description of operating modes associated with the node being discussed, such as start-up, standby, normal operation, normal shutdown, and emergency shutdown before these topics are addressed.

Operating Modes

All potential operating modes should be identified and included in the study. Each mode may impose different maxima in the operating envelope, and some nodes are used for different purposes under the various operating modes for the plant. For example, flow rates and directions may change in wellhead lines during well killing or injection. Process conditions may also change significantly during start-up or upset conditions, e.g. ESD and blowdown. Maintenance isolation of individual trains or equipment sections may have significant effects on other parts of the process by changing the flow rates or temperatures/pressures/phases within the surrounding sections.

HAZOP Deviation

In the preparation stage of a HAZOP study, the HAZOP facilitator/leader should propose an initial list of guidewords to be used for the HAZOP Session. Some examples of Guidewords and their associated parameters and causes are given in APPENDIX A: HAZOP GUIDEWORDS. The selected guidewords should be considered carefully, specified, and focused on the HAZOP study topic. The HAZOP facilitator/leader should test the proposed guidewords against the system and confirm their adequacy.

HAZOP Work Sheet and HAZOP Action Sheet

During the HAZOP study, the HAZOP Work Sheet is used by the HAZOP Scribe to record all discussions, including recommendations and classifications, actions, etc. to present the results of the study and generate the final report as detailed in Section 3.5.1. The example HAZOP Work Sheet and HAZOP Action Sheet are given in APPENDIX B: EXAMPLE OF HAZOP WORK SHEET and APPENDIX C: EXAMPLE OF HAZOP ACTION SHEET.

Risk Assessment Matrix (RAM)

A RAM defines the various levels of risk comprising of the probability of occurrence of deviation and the severity of each identified hazard. This is a simple mechanism to increase the visibility of risks and assist management in decision making. When using the risk matrix, HAZOP Facilitator shall ensure that the HAZOP Study complies with SSHE Risk Management Standard (Document code: 11038-STD-SSHE-401).

3.2.2 HAZOP Study Location

In case of the onsite workshop, the HAZOP study location should be in a conference room large enough to comfortably accommodate the number of team members from a multi-discipline such as asset, project, PTTEP Corporate, and external parties. HAZOP teams vary in size; however, groups of 6 - 10 team members are usual and recommended.

The location should be well ventilated with adequate lighting. All computer support and projection equipment must be able to operate and be easily accessible. Dual projectors are recommended and should be arranged when possible. One shows the HAZOP worksheet, and another shows the marked-up P&ID. Otherwise, it is recommended to tape P&IDs on the wall so that the team can examine them readily during the study.

It is typical to provide felt tip color pens or highlighter pens to identify piping/vessel sections on the P&IDs or "nodes", for the team to better understand what part of the process is being studied.

3.2.3 HAZOP Study Duration

The duration of a HAZOP session depends on the project development scale and complexity of the P&IDs to be reviewed and the competency/experience of the participants in the HAZOP study sessions. For the workshop's effectiveness, it is recommended to limit the duration of each session to not more than six (6) hrs./day to avoid fatigue and distraction, which can negatively affect the quality of the discussion.

3.3 TEAM SELECTION

The success of a HAZOP predominantly depends on the quality of the team members. All participants should be competent in their discipline and understand the process and overview.

3.3.1 HAZOP Team Facilitator/Leader

The choice of the HAZOP team facilitator or leader is critical to the success of the study. A nominated person as HAZOP facilitator/leader will be reviewed/approved by Technical Safety Technical Authority (TA). However, the HAZOP facilitator/leader could be an external specialist/consultant who is approved by Technical Safety TA and/or Project Owner. The team facilitator/leader should be independent from the project or asset concerned. The facilitator/leader should be a competent and experienced engineer trained in HAZOP study methodology e.g. Process Hazard Analysis (PHA) training and PHA Leader training with many years of process industry experience.

For internal facilitator, the required qualifications are:

- A minimum of 5 years of experience in hazard analysis.
- Has scribed in at least five (5) reports.
- More experience years are required for a capital project.

For the external facilitator, the required qualifications are:

- A minimum of 10 years of experience in hazard analysis tools
- A minimum of 8 years of experience in HAZOP leader.
- The experience shall be relevant to the study scope and process technology.

3.3.2 HAZOP Scribe

The HAZOP is made more efficient by having a HAZOP scribe to assist the HAZOP facilitator/leader. The HAZOP scribe should ensure that all computer equipment is operable before the study begins. She/he should be able to record all the discussions on the HAZOP worksheets (see APPENDIX B: EXAMPLE OF HAZOP WORK SHEET) with minimum aid from the HAZOP facilitator/leader. HAZOP Scribe shall have at least 4 years of experience in the Oil & Gas industry or Petroleum process, be approved by the Technical Safety TA, and be trained in HAZOP study methodology.

3.3.3 HAZOP Team Members

A multi-disciplinary team should be appointed of competent personnel from relevant disciplines. Team members should be familiar with the processes under study. The HAZOP team should be defined first by agreement between HAZOP facilitator/leader, Technical Safety TA, and Project Owner. A representative from technical safety, competent personnel from an international asset, or a chosen contractor can be acted as HAZOP facilitator/leader and coordinate with team members from relevant disciplines. An interdisciplinary team is desirable and usually consists of no more than 6 – 10 people. HAZOP team member role will depend on the scope of the HAZOP. Typical team members include:

- Process Design Engineer
- Operation Representative
- SSHE Engineer
- Project Engineer – see note below
- Experienced Plant Operation/Maintenance personnel – see note below

Note: Actual number of engineers from each discipline depends on the scope and complexity of the HAZOP. However, the recommended number of people in the HAZOP team should not exceed 10.

Study personnel that may be added on an as needed basis:

- Discipline Engineer e.g. Mechanical, Corrosion, Instrument, Electrical Engineer, etc.
- Other Specialists as needed
- Vendor suppliers of packaged skid mounted processes

It is important that team members are competent personnel and can provide information on behalf of their department/function; otherwise, reaching conclusions will be difficult if a reference has to be made back to management.

3.4 HAZOP WORKSHOP METHODOLOGY

3.4.1 Beginning A HAZOP Study

Before conducting a HAZOP, an opening or kick-off meeting shall be led by a HAZOP facilitator/leader. The following information should be discussed, but not limited to:

- Starting with SSHE Moment
- Discussion of the location of fire exits
- Request that all cell phones be turned off and locations of smoking shelters
- Introduction of HAZOP team members
- Scope of the HAZOP
- HAZOP objective and methodology
- HAZOP schedule with anticipated date and time of the closing / debrief meeting
- Possible site visit

A presentation is then given by the Process Engineer responsible for the project/modification, giving an outline of the process and operating modes, including pressure temperatures and piping/vessel specifications. This helps the team understand since they may not be familiar with the process.

3.4.2 Conducting A HAZOP Study

A HAZOP facilitator/leader will conduct the HAZOP study as per Figure 3 below. However, it should be noted that HAZOP team members are engineers and may be tempted to try and solve problems in long discussions and debates. While this is good for the study, unless a ready solution is discussed, the problem should be noted for further study by the relevant engineering group, and the HAZOP team facilitator/leader should move the study along.

There might be a serious argument or debate; the HAZOP facilitator/leader should ask the HAZOP scribe to note the disagreement and move on.

System description: At the commencement of the HAZOP, the complete system of assets, materials, human activities, and process operations within the boundaries of the study should be clearly defined and understood, considering the original design, subsequent changes, and current conditions. Typically, the system should be divided into distinct, separate components or sections to enable manageable quantities of information to be handled at each stage.

3.4.3 HAZOP Software

It is recommended to adopt Process Hazard Analysis software for HAZOP study as it is believed to enhance the effectiveness of the risk assessment undertaken by reducing time consumption and preventing human error.

The recommended software is PHAPro® by Sphera or other compatible software that can be imported into the PHAPro® environment.

3.4.4 Execution

During a HAZOP study, a team of experienced engineers from various disciplines uses a systematic approach to identify and record hazards and operability problems that result from deviations from the intended design of the process and its safe operating ranges. The team facilitator/leader systematically leads the team through the Process and Instrument Diagrams (P&ID) by applying HAZOP Guidewords in Appendix A. The guidewords are applied to specific process sections or "nodes". It is normal practice to record HAZOP study results in a HAZOP Worksheet (see Appendix B) which included guideword parameters, deviations, causes of the deviation, consequences, safeguards, recommendations, and groups assigned to follow up on the recommendation generated.

HAZOP studies concentrate on identifying hazards and operability problems. While the HAZOP study is intended to identify hazards, it is typical that more than 80% of the recommendations generated will be about solving operability problems.

To help understand the difference, here are the definitions of "Hazard" and "Operability":

Hazard

Any operations that could possibly cause a catastrophic release of toxic, flammable, or explosive materials or any actions that could result in an injury to personnel.

Operability

Any operations that could cause a process upset or shutdown could lead to violating safety, environmental, or health regulations or negatively impacting profitability.

Parameter

For example, the guideword parameter "Pressure" combines with the process guideword "More" results in a discussion about the causes of "More Pressure" from the design intent. Sometimes the team facilitator/leader will use checklists, industry experience, or loss history analysis to help the team in its discussion. A suggested list of parameters is given in Appendix A.

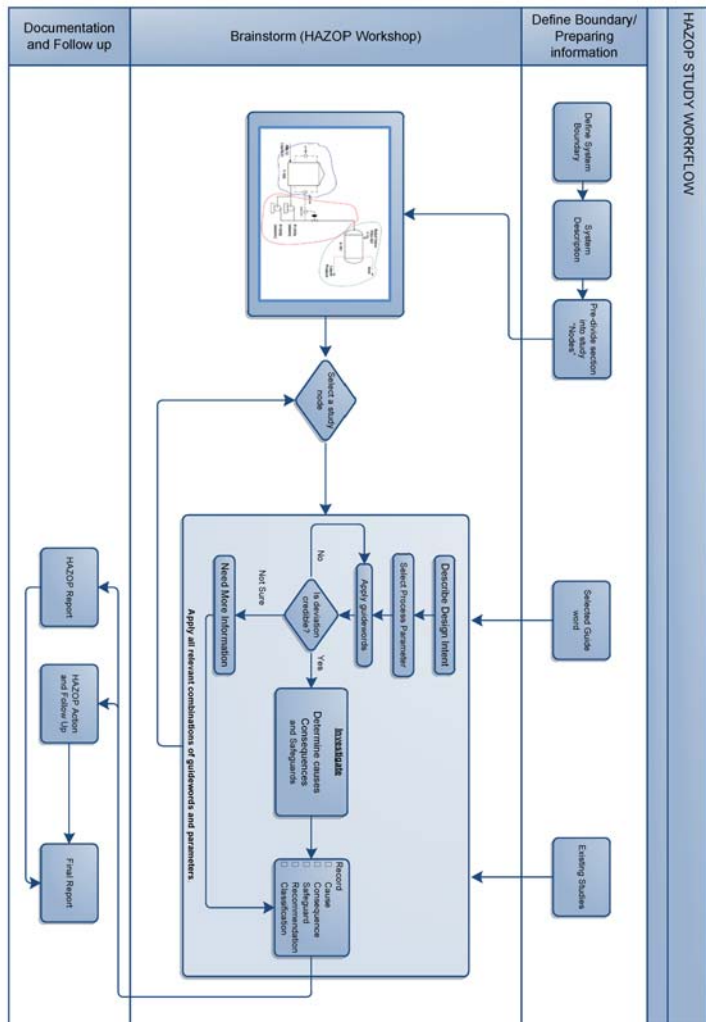


Figure 3: HAZOP Study Workflow

Guidewords

The following gives the definitions of the deviation guidewords:

Guideword	Meaning
No	Complete negation of design intent
More	Quantitative increase
Less	Quantitative decrease
As well as	Quantitative modification/increase
Part of	Quantitative modification/decrease
Reverse	Logical opposite of design intent
Other than	Complete substitution
Early/Late	Relative to the clock time
Before/After	Relating the order or sequence
Where else	Applicable for flows, transfers, sources, and destinations
Faster/Slower	The step is done/not done with the right timing

Causes

The team studies the effects of the deviation from design intent and lists all the realistic causes of the deviation. In APPENDIX A: HAZOP GUIDEWARDS show good examples of causes, parameters, deviations, and realistic causes.

Note: PTTEP uses a single jeopardy approach to discussing causes during HAZOP studies. In other words, a single-point failure would be listed as a cause. "Level transmitter plugged" is an example of a single point failure which may have the consequence of low level in a vessel. Although double jeopardy is generally not considered, care should be taken before ruling out a failure, which could undergo undetected and become a "pre-condition" to the other failure e.g. unrevealed misoperation, heat exchanger tube failure. The HAZOP is not capable of identifying all the double jeopardy scenarios. However, the discussion should be made and recorded on those that appear to be credible.

Consequences

Next, the team will determine all the possible consequences for each cause listed. The consequences of the deviations may be minor or severe; however, an attempt should be made to focus on the severe issues such as pipeline rupture, vessel explosion, significant environmental releases, etc. If the consequences cannot be fully determined e.g. effect of significant gas release on third parties, the team could recommend additional risk assessment studies to be performed, such as toxic gas dispersion studies or explosion modeling.

For determination of consequence severity, the ultimate consequence shall be addressed clearly without consideration of safeguards. It should be quantified e.g. full production at 130 MMscfd, worst case 8 hrs., 1 MM USD if no production for 1 day, 100 condensates bbl of the spill, etc.

Safeguards

Next, the team will list the available safeguards and determine if they are adequate to prevent deviations and consequences from occurring. Safeguards usually are:

- Process systems and equipment, engineered designs, and written procedures that help prevent a catastrophic release of hazardous or flammable material e.g. emergency shutdown systems, pressure relief valves, flare, and depressurization systems.
- Process systems and equipment that is designed and installed to detect and give warning following the immediate release of hazardous or flammable materials e.g. flow/pressure/temperature/level alarm indicators, smoke, fire, and gas detection systems.
- Fire protection systems and equipment or written procedures that help to mitigate the consequences of a release of hazardous or flammable materials e.g. firewater/foam systems and deluge systems.

The HAZOP team should be careful when evaluating safeguards since hazard analysis requires the consequences of the failures of engineering and administrative controls. a HAZOP recommendation shall be generated if the team determines that the safeguards are not adequate,

Risk Evaluation/Risk Ranking (Preferable)

It is preferable to assess the level of risk. Risks could then be ranked as High/Medium/Low according to the PTTEP Risk Assessment Matrix (RAM) in Appendix D of SSHE Risk Management Standard, 11038-STD-SSHE-401.

The level of risk management required will be determined using the RAM to estimate the probability (likelihood) and the impact rating (severity) of the consequence of each identified hazard. The initial risk is a risk without any additional control or mitigation measures in place. Residual Risk is a remaining risk considering the effectiveness of the safeguards that are in place.

After HAZOP team members identified the causes and consequences on the HAZOP Worksheet. The facilitator/leader will ask the HAZOP team members to evaluate the initial frequency of occurrence (likelihood) for each cause on a scale of "A" to "E", where "A" is Rare - Remote or never heard in E&P business while "E" is Frequent - occurred more than one per year in at the same location and consequence for each cause on a scale of "1" to "5" where "1" is minor and "5" is critical. The combination between consequence and likelihood gives an estimation of initial risk. The maximum number of risks, whether on the people, property, environment or reputation, will be noted in the "risk level" column on the HAZOP Worksheet. If any identified risks having a High Risk (red region) of the matrix, such risks are unacceptable, and measures must be taken to eliminate or reduce the identified risk to a Medium or Low Risk with ALARP demonstrated. Those unacceptable initial risk levels, i.e. severity of 5 (Critical), are classified as MAEs.

Residual risk can be determined similarly, considering protective/mitigative safeguards provided (from existing safeguards or proposed additional safeguards). Risk reduction could be relative to the initial risk, such as incorporating a suitable pressure relief valve could reduce the likelihood by two orders of magnitude.

Write the Recommendation (Action)

Recommendations generated during the HAZOP should clearly address:

- What is the problem?
- Where is the problem?
- What is the suggested correction?
- What party is responsible or accountable for the completion of the actions recommended by the team?

The HAZOP team should decide if a partial or full recording is required. The former requires responses to each guideword to be recorded only when an action is identified. The latter requires the recording of responses even if no actions arise.

Recording the HAZOP Recommendation Classifications

PTTEP HAZOP actions usually are classified as follows:

Class 1: for mandatory recommendations that must be done at high priority.

Class 2: for recommendations that should be considered as a possible improvement.

Class 3: for clarification or further review.

Class 4: for document mistake or inconsistency.

HAZOP actions/recommendations should normally be classified using risk ranking or mutual agreement with the experience committee, reference document, previous study, etc. However, the recommendation classification is not mandatory for all HAZOP studies but preferred; it depends on the scope and complexity of the study. The classification allows the design team to focus and prioritize the follow-up & close-out recommendations.

Regarding the current Corporate SSHE action tracking system, severity of the findings/recommendations can be categorized into three (3) levels i.e. High, Medium, and Low. The HAZOP action's classification can be corresponding to those three levels, per the guideline as follows:

HAZOP Action Classification	Severity of Findings (according to Corporate SSHE Action Tracking System)
Class 1	High
Class 2	Medium
Class 3	Medium
Class 4	Low

3.4.5 HAZOP Study Close Out Meeting

HAZOP study close-out meeting should be conducted. The close-out meeting should be held with the site/asset/project or operations and maintenance superintendents to help answer any questions from HAZOP recommendations.

A draft table of HAZOP recommendations can be left with the project, process, or asset team at this close-out meeting for them to begin to address HAZOP recommendations as soon as possible.

3.5 DOCUMENTATION AND FOLLOW UP

Once the HAZOP study is completed, the study outputs and conclusions should be documented. In addition, to ensure that the recommendations from the study are closed-out in a satisfactory manner, recommendation tracking should be established and adopted.

3.5.1 HAZOP Report and HAZOP Action Report

The HAZOP Facilitator/Leader shall issue a complete HAZOP report to the study team, project, asset team, and other relevant parties. The report should include the following topics as a minimum:

- Cover Sheet
- Executive Summary
- Contents
- Introduction
- Scope
- HAZOP Methodology
- HAZOP Review Session (Node, Team members, Location, and Duration)
- Conclusion
- Appendices (such as references to previous studies, associated documents reviewed, marked-up P&IDs, calculation notes, assumptions, HAZOP Worksheets, etc.).

The individual HAZOP action should be registered in the existing SSHE action tracking system. A recommendation from HAZOP study can be followed-up and closed-out offline by using HAZOP action sheet. The action sheet format should be referred to APPENDIX C: EXAMPLE OF HAZOP ACTION SHEET. However, the HAZOP Facilitator/Leader should issue the close-out report to all relevant parties after completing a HAZOP study and action follow-up, and it should be uploaded to the system.

Note: A HAZOP report has been developed based on a HAZOP meeting, the resulting risk register from the meeting, and the consequent follow-up work and discussions. It will be generated after finished the HAZOP session. Any significant changes resulting from the HAZOP findings may not be implemented and contained in the part of the HAZOP report.

3.5.2 HAZOP Recommendation Tracking and Close Out

After the HAZOP facilitator/leader issues the HAZOP report, the project manager shall ensure that responsible parties provide their proposed actions to the team facilitator/leader for review. The remaining findings and recommendations in the HAZOP worksheet should be uploaded and tracked until completion in the SSHE action tracking system, as mentioned in section 3.5.1. The action parties may propose alternative action to satisfy the intent of the findings and the target completion dates for the action. The project manager or delegated person and HAZOP facilitator should follow up on the progress regularly.

3.6 RELATION TO OTHER ANALYSIS TOOLS

According to IEC 61882 Guideline and ISO 17776 Standard, the HAZOP study can be used with other risk identification and analysis methods such as FMEA, FTA, ETA, and LOPA.

For example, LOPA uses the Major Accident Events (MAEs) and High-Risk hazards (Severity level 5) information as identified from hazard identification studies (e.g. HAZOP) and develops the initiating cause and the independent protection layers (IPLs) that demonstrate ALARP of the risk. This can then be used to determine the amount of risk reduction achieved by existing controls and to ascertain whether further preventive/mitigative layer is needed. See Layer of Protection Analysis (LOPA) Guideline (Document code: 12147-GDL-SSHE-401/00/06).

APPENDICES

APPENDIX A: HAZOP GUIDEWORDS

The HAZOP Parameter/Deviation Guidewords and Examples of Causes are available on the [SSHE Intranet > SSHE MS > SSHE MS Documents > Corporate Tools > Appendix – Hazard and Operability \(HAZOP\) Study Guideline](#).



APPENDIX B: EXAMPLE OF HAZOP WORK SHEET

The Example of HAZOP Work Sheet is available on the [SSHE Intranet > SSHE MS > SSHE MS Documents > Corporate Tools > Appendix – Hazard and Operability \(HAZOP\) Study Guideline](#).



APPENDIX C: EXAMPLE OF HAZOP ACTION SHEET

The Example of HAZOP Action Sheet is available on the [SSHE Intranet > SSHE MS > SSHE MS Documents > Corporate Tools > Appendix – Hazard and Operability \(HAZOP\) Study Guideline](#).



APPENDIX D: EXAMPLE OF HAZOP ATTENDANCE SHEET

The Example of HAZOP Attendance Sheet is available on the [SSHE Intranet > SSHE MS > SSHE MS Documents > Corporate Tools > Appendix – Hazard and Operability \(HAZOP\) Study Guideline](#).



APPENDIX E: EXAMPLE OF INFORMATION REQUIRED FOR A HAZOP REVALIDATION

The Example of information required for a HAZOP revalidation and how it can be used are available on the [SSHE Intranet > SSHE MS > SSHE MS Documents > Corporate Tools > Appendix – Hazard and Operability \(HAZOP\) Study Guideline](#).



APPENDIX F: EXAMPLE OF EXECUTION CHECKLIST FOR A HAZOP REVALIDATION

The Example of HAZOP Revalidation Execution Checklist is available on the [SSHE Intranet > SSHE MS > SSHE MS Documents > Corporate Tools > Appendix – Hazard and Operability \(HAZOP\) Study Guideline](#).



APPENDIX G: EXAMPLE OF ISSUES CHECKLIST FOR A HAZOP REVALIDATION

The Example of issues checklist for a HAZOP revalidation and how it can be used are available on the [SSHE Intranet > SSHE MS > SSHE MS Documents > Corporate Tools > Appendix – Hazard and Operability \(HAZOP\) Study Guideline](#).

ROLES AND RESPONSIBILITIES

Roles	Responsibilities
Document Owner	<p>The owner of the Hazard and Operability (HAZOP) Guideline is the VP, Process Safety and Assurance Department, with responsibilities for:</p> <ul style="list-style-type: none"> ■ Issuing the Hazard and Operability (HAZOP) Guideline and its revision. ■ Ensuring effective implementation of the guideline.
Document Custodian	<p>The custodian of the Hazard and Operability (HAZOP) Guideline is the Manager, Technical Safety Section, with responsibilities for:</p> <ul style="list-style-type: none"> ■ Identifying deficiencies or potential improvements. ■ Initiating periodic revision. ■ Maintaining revision history and document status register.
SSHE Managers/VPs	<p>SSHE Managers/VPs should provide support for HAZOP studies by:</p> <ul style="list-style-type: none"> ■ Ensuring HAZOP session is facilitated by competent and trained HAZOP Team Facilitator. ■ Providing experienced and trained HAZOP Team Facilitator/ Team Member and HAZOP Scribe. ■ Reviewing the application of the HAZOP Study Guideline and suggesting improvements.
Project Managers /VPs	<p>Project Managers/VPs should:</p> <ul style="list-style-type: none"> ■ Arrange and Allocate budget and resources (e.g. qualified participants) for HAZOP studies as needed. ■ Assign personnel to provide the reliable and latest information as needed for the HAZOP study e.g. P&ID, layout, Process Control Narrative, ESD logic diagram, etc. ■ Ensure that the HAZOP recommendations in his/her asset are tracked to completion.
HAZOP Facilitator	<p>HAZOP Facilitator/Leader should:</p> <ul style="list-style-type: none"> ■ Competent, experienced, and trained HAZOP Team facilitator/ leader. ■ Coordinate HAZOP study. ■ Prepare pre-HAZOP activities before the HAZOP study e.g. review scope of work, all relevant documents, assign HAZOP Nodes, appoint HAZOP team, etc. ■ Conduct the opening meeting.

Roles	Responsibilities
HAZOP Facilitator (continue)	<ul style="list-style-type: none"> ■ Facilitate/lead the HAZOP team when conducting the study. Ensure that information is distributed to all members. ■ Conduct the debrief/close out meeting. ■ Ensure that the HAZOP recommendations are closed out properly. ■ Ensure the study performance and documentation comply with regulatory and Company requirements.
HAZOP Scribe	<p>HAZOP Scribe should:</p> <ul style="list-style-type: none"> ■ Assist the HAZOP team facilitator/leader. ■ Prepare the HAZOP Report and HAZOP Action Reports. ■ Ensure all facilities, e.g. Print-out document Equipment, Venue etc., are completed before the study begins. ■ Record all the study work, final findings/recommendations in the HAZOP worksheet.
HAZOP Team Members	<p>HAZOP Team Members should:</p> <ul style="list-style-type: none"> ■ Review all relevant documents before the HAZOP study when available. ■ Fully attend and contribute their area of expertise in the HAZOP study e.g. keep side conversations to a minimum, actively participate in the study, etc.

DEFINITIONS AND ACRONYMS

Set out below are common specific terms presented in alphabetical order:

Term	Definition
Asset	Refers to an operating asset, site, or location within a respective Function Group.
Corporate	Refers to the PTTEP business groups hierarchically above asset level, and located in the PTTEP headquarters, Bangkok.
Department	A subgroup within a Function Group, Division or Asset.
Division	A business group may have one or more distinct groups within its hierarchy. These are referred to as Divisions.
Function Group	Refers to a corporate level business group. These may have associated Divisions, Departments, or operational assets within their hierarchy.
As Low As Reasonably Practicable (ALARP)	A term used to define tolerable risk acceptance only where risk reduction is impractical or cost-benefit analysis is carried out and a judgment is made that the cost of further risk reduction is grossly disproportionate when compared to the actual risk reduction that would be achieved.
Barrier	Measure which reduces the probability of releasing a hazard's potential for harm or which reduces its consequences. The hierarchy of barriers is prevention, detection, control, mitigation, and emergency response.
Cause	Anything with the potential to release a hazard.
Consequence	An event or a chain of events that results from the release of a hazard.
Control	The barrier which reduces the probability of releasing a hazard's potential for harm.
Creeping Change	Creeping change is the accumulation of small changes that are gradual in nature, unseen and not planned, but can add up to a significant change. They may be difficult to detect and monitor using conventional hazard identification studies and risk assessments. Creeping change can lead to the "normalization of deviance".

Term	Definition
Design Intent	A detailed explanation of the ideas, concepts, and criteria that are defined by designer. The Design Intent should contain the basic process description and how to meet the project requirement, included design information, material of construction, operation condition, envelop, and basic controls/safeguards.
Deviation	Combination of guideword and parameter, which may or may not constitute meaningful and significant consequence that defines variation from the design intent.
Element	Constituent of a part which serves to identify the part's essential features
Guideword	An action word or phrase that amplifies the parameter to define specific type of deviation from the design intent.
Hazard	A hazard is an intrinsic property of anything with the potential to cause harm. Harm includes ill-health, and injury, damage to property, plant, products or the environment, production losses, or increased liabilities.
Like-for-Like	A like-for-like replacement, i.e. item or component that is replaced by an item of the same specification. Like-for-Like replacement is used interchangeably with In-Kind replacement while Not Like-for-Like or Not In-Kind replacement is the opposite terms.
Major Accident Event (MAE)	Any incident that results in multiple fatalities or equivalent damage, production loss, environmental impact as per the Risk Matrix.
Management Review	A systematic and timely study of a facility's equipment and management systems to help ensure safe operation.
Management System	A structured set of interdependent doctrines, processes, documents, and principles that are intended to ensure that the activities of an organization are directed, planned, conducted, and controlled in such a way to provide reasonable assurance that the objectives of the organization at met.
Node	A section, stage, or step (for batch operation) of which specific and clear design intent can be described.
Parameter	Qualitative or Quantitative property of an element as we consider during HAZOP study e.g. pressure, temperature, flow, etc.

Term	Definition
Qualitative Risk Analysis	This type of risk analysis which does not involve numerical probabilities or predictions of loss. Instead, the qualitative method involves defining the various threats, and determining the extent of vulnerabilities.
Quantitative Risk Analysis	An attempt is made to numerically determine the probabilities of various hazardous events and the likely extent of the losses if a particular event takes place.
Recommendation	An action to reduce a potential to cause a hazard. Any action shall be ensured that it can reduce a risk to ALARP level by considered reducing the Likelihood or Severity/Impact or both of them.
Risk	Risk is a combination of the probability of occurrence of a consequence and the severity of that consequence.
Risk Analysis	An overall process of defining and analyzing the dangers to asset posed by potential hazardous of events, A risk analysis report can be either quantitative or qualitative.
Risk Assessment	An overall process of risk analysis and risk evaluation. Typically includes toxic gas dispersion modeling, blast calculations, thermal radiation studies, etc.
Risk evaluation	The process to involve the establishment of relationship between risks and benefits, involving the complex process of determining the significance of the identified hazards and estimated risks to those organisms or people concerned with or affected by them.
Safeguard	Safeguards are measured to prevent threats from releasing a hazard or to limit the consequences arising from the top event. For safeguard to be valid, they shall be effective, independent, and auditable.
Technical Authority (TA)	PTTEP personnel responsible for technical standards, and providing advice on issues relating to their discipline, including advice on whether proposals to change or to deviate from a standard or from the reliability and integrity envelope should be approved.

Acronyms	Description
AFC	Approved for Construction
ALARP	As Low As Reasonably Practicable
CEN	Environment Management Department
CPA	Process Safety and Assurance Department

Acronyms	Description
CPA/T	Technical Safety Section
CSA	Safety Management Department
CSH	Safety, Security, Health, and Environment Division
ESD	Emergency Shutdown
ETA	Event Tree Analysis
FEED	Front End Engineering Design
FMEA	Failure Mode and Effects Analysis
FTA	Fault Tree Analysis
HAZID	Hazard Identification
HAZOP	Hazard and Operability
IEC	International Electrotechnical Commission
ISO	International Organization for Standardization
LOPA	Layer of Protection Analysis
MOC	Management of Change
P&ID	Process and Instrumentation Diagram
PFD	Process Flow Diagram
PHA	Process Hazard Analysis
PREP	Project Realization Process
PSM	Process Safety Management
RAM	Risk Assessment Matrix
SOP	Safety Operating Procedure
SSHE	Safety, Security, Health, and Environment
TA	Technical Authority
TOR	Terms of Reference
UFD	Utility Flow Diagram

REFERENCES

Document Code	Document Title
PTTEP SSHE Controlling Documents	
11038-STD-SSHE-401	SSHE Risk Management Standard
11038-STD-SSHE-508	Management of Change Standard
Other Reference Documents	
10008-STD-3-PRP-001	PREP Framework for Project Management
10008-STD-3-PRP-004	Safety, Security, Health, and Environment Management
-	Effective revalidation of risk assessments - Delta HAZOP; IChemE Safety Centre; 2021
-	Guidance on Applying A Creeping Change Hazard Identification (CCHAZID) Methodology, First Edition; Energy Institute, UK; 2017
-	HAZOP: Guide to Best Practice; IChemE Safety Centre; 2015
2015-RP-ORM-001 (Rev. 1)	PTT Group Hazard and Operability Study Guideline; PTT; 2015
2015-RP-ORM-002 (Rev. 1)	PTT Group Process Hazard Analysis Guideline; PTT; 2015
IEC 61882:2016	Hazard and operability studies (HAZOP studies) - Application guide; International Electrotechnical Commission (IEC); 2016
ISO 17776:2016	Petroleum and natural gas industries - Offshore production installations - Major accident hazard management during the design of new installations; International Organization for Standardization (ISO); 2016

REVISION HISTORY

Rev.	Description of Revision
0	<p>Authorized by: CEO, Date: December 2010</p> <p>This corporate procedure separates and describes in better detail the PTTEP HAZOP Study Methodology found in the outdated "SSHE Loss Prevention and Risk Management Standard S.PSH.004 Rev. 0, 2004.</p> <p>Changes from the last version are:</p> <ul style="list-style-type: none"> Detailed information on how to prepare for, conduct and generate the HAZOP report. Responsibilities are spelled out in detail. <p>Many examples are found in the appendices to help conduct HAZOPs more effectively and efficiently.</p>
1	<p>Authorized by: CSH, Date: April 2012</p> <p>Changes from the previous version are:</p> <ul style="list-style-type: none"> Changed from document type from a procedure to a guideline. Updated to new standard format to comply with SSHE Documentation Management Standard (SSHE-106-STD-330). Updated the Record and Action Sheet of HAZOP study. Updated HAZOP Guideline information from IEC 61882.
2	<p>Authorized by: CSH, Date: April 2017</p> <p>Changes from the previous version are:</p> <ul style="list-style-type: none"> Added more Terminology and Acronyms. Added more requirements in Term of Reference preparation. Incorporated PTT HAZOP Guideline. Added risk ranking requirement as optional in HAZOP study. Updated HAZOP Facilitator/Scribe qualification. Added requirement of ATS. Revised Appendix B for the worksheet format. Added Appendix D for the Attendance list format.
3	<p>Authorized by: CSH, Date: September 2022</p> <ul style="list-style-type: none"> Added terminology and guidelines for creeping change and like-for-like replacement. Added details of creeping change consideration in Section 3.4 HAZOP Workshop Methodology and Appendices E to G. Added recommended PHA software. Updated guidelines for action tracking and close-out. Revised risk ranking assessment from "Optional" to "Preferable". Updated reference documents numbering and title.



บริษัท ปตท.สผ. สยาม จำกัด

รายงานผลการปฏิบัติตามมาตรการป้องกันและแก้ไขผลกระทบสิ่งแวดล้อม และมาตรการติดตามตรวจสอบผลกระทบสิ่งแวดล้อม
โครงการในพื้นที่จังหวัดกำแพงเพชร
ฉบับเดือนมกราคม - ธันวาคม พ.ศ. 2566

ภาคผนวกที่ 31

การจัดทำ HAZOP ของอุปกรณ์และกระบวนการผลิต



PTT Exploration and Production Public Company Limited

SIRIKIT OIL FIELD (S1) ASSET

Wellsite

Re-HAZOP 2016 Report

Report No. - TPA-2016-AUD-HZP-043

S1 Asset, Thailand
October 2016, Rev. 0



Document Approvals		
	Signature	Date
Prepared by: (Issue for Implementation)		11/10/2016
Checked by: (Engineer, SSHE)		11/10/2016
Approved by: (Section Manager)		12/10/16



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Abbreviations, Acronyms and Definitions

API	American Petroleum Institute
ATS	Action Tracking System
ASME	American Society of Mechanical Engineers
BPD	Barrel Per Day
C&E	Cause and Effect
CAO	Computer Aided Operation
CITHP	Closed-in Tubing Head Pressure
CM	Corrective Maintenance
DCS	Distributed Control System
ESD	Emergency Shutdown
ESP	Electric Submersible Pump
FC	Fail Closed
FO	Fail Open
FW	Fire Water
H ₂ S	Hydrogen Sulphide
HP	High Pressure
IA	Instrument Air
IP	Intermediate Pressure
JT	Joule-Thompson
KO	Knockout Drum
LKU	Lan Kra Bue
LLP	Low Low Pressure
LP	Low Pressure
LPG	Liquefied Petroleum Gas
MAWP	Maximum Allowable Working Pressure
MMSCFD	Million Standard Cubic Feet per Day
MW	Molecular Weight
NPSHa	Net Positive Suction Head Available
NPSHr	Net Positive Suction Head Required
OPM	Operating Manual
OSD	Operational Shutdown
OTR	Operational Technical Review
P&ID	Piping and Instrumentation Diagram
PFD	Process Flow Diagram
PM	Preventive Maintenance
PPE	Personal Protective Equipment
PSV	Pressure Safety Valve
PVV	Pressure Vacuum Valve
PTW	Permit to work
RBI	Risk Based Inspection
RO	Restriction Orifice
RV	Relief Valve
SCADA	Supervisory Control and Data Acquisition

1.0 Executive Summary

A Hazard and Operability (HAZOP) workshop for re-assessment of hazards identification during OPERATION phase at S1 Wellsite was carried out from 20th June to 26th August 2016 at S1 30th Years Building Meeting room 2.

The HAZOP review is a structured guidewords based hazard identification and evaluation based on PTTEP Risk Assessment Matrix from SSHE Risk Management Standard (Doc. No. SSHE-106-STD-400) Rev 5. A list of attendees is shown in Section 5.0.

The findings of the study were recorded on worksheets attached in **Appendix A** of this report. A total of **54 actions** have been raised to be implemented from the HAZOP workshop. **5 recommendations** are classified as High priority, **44 and 5 recommendations** for Medium priority and Low priority respectively.

For action follow up, Action Tracking System (ATS) was introduced to use for audit finding follow up. All action parties shall close out the findings via this system. The ATS will send the email notification to assigned parties. HAZOP ATS are provided in **Appendix C**.

The following High priority findings should be addresses as soon as possible:

- Improve MPF Flare Flash back prevention: (1) Add N2 purge requirement before start-up of MPF-01 to 05 and Liquid seal drum checking before start up MPF-06, 07, 08 in OPM., (2) Carry out study for N2 requirement to ensure safe to ignition flare, record in OPM and train to operator. (ECM/E)
- (1) Review sizing of liquid seal drum (Concerned loss of water). In case sizing problem, MOC shall be raised for downgrade situation. , (2) Review installation of auto filling and source of water supply. (ECM/E)
- Recommend to review equipment in hazardous area that it's suitable for zone classification or not, especially for zone 1. (ECM/E).
- Develop all MPF function test and PM of SCE equipment. (PS1/M)
- Local Dehydration LKU-F, Project to final investigation cause of failure and find out solution to solve problem Desander and liner inefficiency/damage to asset. (ECM/N).

2.0 Introduction

The Sirikit oil field is located in the Central plains of Thailand near Lan Krabue (LKU) town some 400 kilometer North of Bangkok situated in a region with little other industrial activity. The nearest large town with rail and airport facilities is Phitsanulok, which lies 50 kilometres east of the Sirikit Field.

Lan Krabue is situated in an agricultural region of a forest reserve with no significant rivers or streams passing through. There is no history of earthquakes, high winds or other devastating conditions. Flooding during the annual rainy season can occur but generally will only pose a short-term threat to crude/LPG production and evacuation.

The Sirikit Oil field has over 74 well site locations and 12 well site extensions in the S1 concession and a sales gas metering station. The Sirikit Oil field also contains substations and mobile production facilities (MPF) which consist of separation and storage facilities sufficient to accommodate one day's production from the production strings.

Well Site Locations facilities include

- Well
- Oil well
- Gas well
- Water injection well
- Water source well
- Utilities water well
- Process equipment
- Pit & Sump (API, Concrete pit, Well Cellar).
- Drilling Pad
- Flow lines.
- RTU, CAO shade
- LV switch gear shade.

The HAZOP study was carried out in accordance with PTTEP Hazard and Operability (HAZOP) study guideline (Doc. No. SSHE-106-GDL-412 Rev.1).

3.0 Objective and Scope

The overall objective of a HAZOP is to provide assurance that a safe and operable plant is in service.

Specifically the objectives of this HAZOP were to:

- Assess the safety and operational risks of the S1 Wellsite plant given the current plant configuration.
- Identify potential safety and operational issues due to any significant design changes since the EXECUTE phase.
- Assess any significant current proposed modifications and operating modes which have significantly changed from the original operational intent.

4.0 Methodology

The HAZOP study is to identify potential deviations of operating conditions from the design intent which could lead to hazardous situations or operability problems and to determine if the necessary safeguards and operation requirements of the proposed changes had been addressed, and that the

risks to Personnel, Asset, Environment and Reputation are As Low As Reasonably Practicable (ALARP).

After a safety moment, attendees were provided with an introduction to the purpose and methodology of Hazard Identification (HAZOP) Study, which included general meeting rules, objective of the HAZOP review, HAZOP methodology briefing and review schedule.

All audit findings shall be classified as 'High', 'Medium', or 'Low' by applying the PTTEP 'Risk Assessment Matrix' (RAM) ref SSHE-106-STD-400 or the criteria shown in Table 1 below. The determined severity and the related consequence category (i.e. people, asset environment, and reputation) shall be documented in the audit report for each finding.

Table 1: Finding Rating Classification

Finding Rating Definition	Finding Rating Definition
High (H)	The Audit finding is likely to cause a significant undesirable effect on the achievement of the entity's and or PTTEP's objectives and has the potential to have a notable impact on the SSHE objectives of the business, therefore warranting reporting to the entities management and PTTEP senior management.
Medium (M)	The Audit finding is likely to cause an undesirable effect on the achievement of the entity's objective
Low (L)	The weakness is likely to have an insignificant undesirable effect on the achievement of one of the entity's objectives, but its correction would enhance the risk-based control framework

For each node, the Process engineer and operation gave an outline of the process, design intent and operating conditions including pressure, temperature, piping and vessel specifications.

All guidewords have been reviewed in the order as listed in **Table 2**. Only the applicable guidewords were recorded in the worksheet and the non-applicable guidewords were not present in the worksheet.

The HAZOP study was recorded in HAZOP worksheets (refer to Appendix A). For each identified hazard, the following information were recorded:

- Deviation: from the guidewords as listed in **Table 2**.
- Cause: Possible causes that will result in the hazard being realized.
- Consequence: Possible development of the outcome. Note that the ultimate consequence will be determined without consideration of safeguards.
- Initial Risk: Consequence and frequency determination as per PTTEP risk matrix.
- Safeguards: Listing of all existing safeguards or mitigation measures.
- Residual Risk: Consequence and frequency determination as per PTTEP risk matrix.
- Recommendation: If the safeguards are deemed inadequate, a recommendation was generated and recorded in the HAZOP worksheet.

Table 2: HAZOP Guidewords

ID	Guideword	ID	Guideword
1	No Flow	12	Less Composition Change
2	More Flow	13	Less Instrument / control
3	Less Flow	14	Corrosion/Erosion
4	Reverse Flow	15	Maintenance/ Inspection
5	More Pressure	16	Safety Environmental
6	Less Pressure	17	Sampling
7	More Level	18	Effluents
8	Less Level	19	Static Electricity
9	More Temperature	20	Startup / Shutdown
10	Less Temperature	21	Other
11	More Composition Change		

5.0 HAZOP Review Team

The review team comprises of PTTEP multidiscipline engineers, S1 Supervisor, S1 Superintendent, S1 operators, including personnel from Technical Safety Corporate and Asset, detailed below:

Participant's Name	Position	Department	Years of Experiences
Pimol Suriyaprasit	HAZOP Facilitator	TPA/T	26
Aunchalee Saesantivong	HAZOP Scribe	TPA/T	17
Ekkalak Somroop	HAZOP Scribe	TPA/T	9
Charoen Chungthanacharoen	Mgr, Prod. Operations Support Sect.	PNO/O	26
Sarawut Uparawanna	Superintendent, SSHE	PS1/S	17
Anuchit Sangsai	Supervisor, Production	PS1/P	10
Theeraphot Kulthamrong	Supervisor, Production	PS1/P	24
Bancha Srisawad	Supervisor, Production	PS1/P	10
O-Path Komprachaya	Supervisor, Production	PS1/P	26
Sornnarong Theinkaew	Senior Engineer, Process	EET/P	16
Alongkot Thungjitnammakorn	Engineer, Maintenance	PS1/M	10
Dussadee Napredakul	Engineer, Production	PNO/O	9
Nalat Opasiamkajorn	Engineer, Process	ECM/E	2
Nontapong Panudulkitti	Engineer, SSHE	PS1/S	11
Sathaporn Lawan	Engineer, SSHE	PS1/S	4

6.0 Findings

A total of **54 actions** have been raised during the HAZOP session from all potential scenarios discussed.

Findings	Number
High priority	5
Medium priority	44
Low priority	5
Total	54

Full details of the study and each action can be found in the worksheets provided in **Appendix A**.

The Action responsible will ensure that all recommendations from the HAZOP Study are fully addressed and appropriately closed-out as soon as possible. Additionally, the Action responsible shall submit all responses to HAZOP facilitator for review and approval.

For action follow up, Action Tracking System (ATS) was introduced to use for audit finding follow up. All action parties shall close out the findings via this system. The ATS will send the email notification to assigned parties. HAZOP ATS are provided in **Appendix C**.



Appendix A. HAZOP worksheets



Appendix A, Well
site Re-HAZOP Work



Appendix B. Node Marked-Up P&IDs



Wellsite Re-HAZOP
2016 Node Details.p



Node 50
MPF-01.pdf



Node 50
MPF-02.pdf



Node 50
MPF-03.pdf



Node 51
MPF-04.pdf



Node 51
MPF-05.pdf



Node 52
MPF-06.pdf



Node 52
MPF-07.pdf



Node 52
MPF-08.pdf



Node 53 LKU-E.pdf



Node 54 LKU-F.pdf



Node 55 LKU-D.pdf



Node 56 Sucker rod
pump.pdf



Node 57 ESP
System.pdf



Node 58 Flow
line.pdf



Node 59 Gaslift
well.pdf



Node 60 PCP
System.pdf



Node 61 Water
injectioin.pdf



Node 62 Mobile
Test Separator.PDF



Node 63 Sales Gas
Metering Station.pd



Appendix C. HAZOP Action Tracking System (ATS)



Appendix C_Well
site Re-HAZOP Actio



บริษัท ปตท.สผ. สยาม จำกัด

รายงานผลการปฏิบัติตามมาตรการป้องกันและแก้ไขผลกระทบสิ่งแวดล้อม และมาตรการติดตามตรวจสอบผลกระทบสิ่งแวดล้อม
โครงการในพื้นที่จังหวัดกำแพงเพชร
ฉบับเดือนมกราคม - ธันวาคม พ.ศ. 2566

ภาคผนวกที่ 32

รายงานการตรวจประเมินด้านความปลอดภัย อาชีวอนามัย
และสิ่งแวดล้อม (SHE Internal Audit)

รายการตรวจประเมินด้านความปลอดภัยฯ (SSHE Audit)

AUDIT + DELETE

Summary

 Export

 Add Audit

 GRID

Audit Template	Responsible Level	Audit Topic	Title	Audit Level	Audit Type	Date started	Date completed
SSHE MS Audit	PS1/S : S1	Site Inspection	2023 S1 SSHE Committee & Ambassador Monthly walkabout audit at STN-A (October)	Asset/Site Level	Internal Audit	17 October 2023	17 October 2023
SSHE MS Audit	ENX : S1	HAZID Report	GS1-MOD-21037-2023-AUD-HZD-002	Corporate Level	Internal Audit	15 September 2023	15 September 2023
SSHE MS Audit	PS1/S : S1	Site Inspection	2023-08 S1 SSHE committee walkabout audit at NSG-A	Asset/Site Level	Internal Audit	18 September 2023	18 September 2023
SSHE MS Audit	PS1 : S1	SSHE MS Verification (MSV)	S1 SSHE MS Verification 2023	Corporate Level	Internal Audit	12 September 2023	15 September 2023
SSHE MS Audit	ENX : S1	HAZOP Report	GS1-MOD-21037-2023-AUD-HZP-001	Corporate Level	Internal Audit	19 July 2023	8 August 2023
SSHE MS Audit	PS1 : S1	DMF HSE and Waste Management audit	DMF HSE and Waste Management Audit 2023 at S1 Outstation	Corporate Level	External Audit	8 August 2023	10 August 2023
SSHE MS Audit	PS1/S : S1	SSHE MS Audit	2023 S1 SSHE Committee & Ambassador Monthly walkabout audit at LKU-ZB (Flush by Activity, Rig Sinope...	Asset/Site Level	Internal Audit	24 July 2023	24 July 2023
SSHE MS Audit	PS1/S : S1	Site Inspection	2023-06 S1 SSHE Cross Function Audit at LKU-Z EOR4	Asset/Site Level	Internal Audit	30 June 2023	30 June 2023
SSHE MS Audit	ENX : S1	HAZOP Report	GS1-PRO-22005-2023-AUD-HZP-002	Corporate Level	Internal Audit	3 March 2023	30 June 2023
SSHE MS Audit	PS1/S : S1	Other (specify)	2023 S1 Green Office Internal Audit	Asset/Site Level	Internal Audit	27 June 2023	30 June 2023
SSHE MS Audit	PS1/S : S1	MOC Audit	2023 S1 MOC Barrier Audit #01	Asset/Site Level	Internal Audit	30 March 2023	5 April 2023
SSHE MS Audit	ENX : S1	HAZOP Report	GS1-STU-22010-2023-AUD-HZP-001	Corporate Level	Internal Audit	28 June 2023	28 June 2023



บริษัท ปตท.สผ. สยาม จำกัด

รายงานผลการปฏิบัติตามมาตรการป้องกันและแก้ไขผลกระทบสิ่งแวดล้อม และมาตรการติดตามตรวจสอบผลกระทบสิ่งแวดล้อม
โครงการในพื้นที่จังหวัดกำแพงเพชร
ฉบับเดือนมกราคม - ธันวาคม พ.ศ. 2566

ภาคผนวกที่ 33

รายงานการซ่อมแผนฉุกเฉิน และการฝึกซ้อมแผนอพยพ
ปี 2566 โครงการเอส 1



PTTEP

PTT Exploration and Production Public Company Limited

รายงานผลการฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ประจำปี 2566 จังหวัดพิษณุโลก

บริษัท ปตท.สผ.สยาม จำกัด (โครงการเอส 1)

ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ

อำเภอเมืองพิษณุโลก จังหวัดพิษณุโลก

วันที่ 25 ตุลาคม 2566

2023 Major Emergency Exercise at BPR Depot

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บทนำ

เนื่องด้วย กฎกระทรวง กำหนดมาตรฐานในการบริหารและการจัดการด้านความปลอดภัย อาชีวอนามัย และสภาพแวดล้อมในการทำงานเกี่ยวกับการป้องกันและระงับอัคคีภัย พ.ศ. 2555 หมวด 8 การดำเนินการเกี่ยวกับความปลอดภัยจากอัคคีภัยและการรายงาน ข้อ 29 ให้นายจ้างจัดให้ลูกจ้างฝึกซ้อมอพยพหนีไฟอย่างน้อยปีละ 1 ครั้ง

ดังนั้น ทางคณะผู้บริหาร บริษัท ปตท.สผ.สยาม จำกัด (โครงการเอส 1) ได้เห็นถึงความสำคัญในการบริหารทีมตอบโต้ภาวะฉุกเฉิน จึงได้ดำเนินการจัดซ้อมดับเพลิงและอพยพหนีไฟ ประจำปี 2566 ขึ้น ณ บริเวณคลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมืองพิษณุโลก จังหวัดพิษณุโลก ตามที่ได้รับความเห็นชอบแผนและรายละเอียดการฝึกซ้อมดับเพลิงและอพยพหนีไฟจากอธิบดีหรือผู้ซึ่งอธิบดีมอบหมาย ตามหนังสือเห็นชอบการฝึกซ้อมดับเพลิงและอพยพหนีไฟ ประจำปี 2566 เลขที่ พล 0030/1514 ลงวันที่ 20 กันยายน 2566 โดยมี นายนำพล แก้วทอง ตำแหน่งเจ้าหน้าที่ความปลอดภัยในการทำงานระดับวิชาชีพ เป็นผู้ประสานงานดังกล่าว

ซึ่งผลการฝึกซ้อมดับเพลิงและอพยพหนีไฟในปี 2566 นี้ ทางบริษัทฯ ได้ดำเนินการแล้วเสร็จเมื่อวันที่ 25 ตุลาคม 2566 โดยการจัดทำข้อมูลฯ ดังกล่าวสามารถถูกล่วงเป็นอย่างดี

นาย นเรศร์ เกิดทรัพย์
นาย รัชมงคล คะมาลี
นาย นำพล แก้วทอง
ช่างเทคนิคอาวุโส แผนกความปลอดภัย มั่นคง อาชีวอนามัยและสิ่งแวดล้อม
บริษัท ปตท.สผ. สยาม จำกัด (โครงการเอส 1)
ดำเนินการจัดทำรายงาน

ตรวจสอบและอนุมัติเอกสารโดย			
	ชื่อ	ลายเซ็น	วันที่
ตรวจสอบโดย	<div></div> (เจ้าหน้าที่แผนกความปลอดภัย ฯ)	<div></div>	23-11-2023
ผู้มีอำนาจอนุมัติ	<div></div> (หัวหน้าปฏิบัติการแผนกความปลอดภัย ฯ)	<div></div>	3-11-2023

แบบรายงานผลการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟ

๑. ข้อมูลสถานประกอบกิจการ

๑.๑ ชื่อสถานประกอบกิจการ บริษัท ปตท.สผ.สยาม จำกัด (โครงการเอส ๑)

ประเภทกิจการ สํารวจและผลิตปิโตรเลียม

ที่อยู่ เลขที่ ๔๑/๓ หมู่ ๒ ซอย - ถนน - แขวง/ตำบล บึงพระ เขตอำเภอ เมืองพิษณุโลก

จังหวัด พิษณุโลก รหัสไปรษณีย์ ๖๕๐๐๐ โทรศัพท์ ๐๒-๕๓๗๑๑๕๐

๑.๒ จำนวนลูกจ้าง/พนักงาน/ผู้เกี่ยวข้อง รวม ๔๐ คน

๑.๓ ลักษณะที่ตั้งของสถานประกอบกิจการ

☐ เป็นสถานที่ที่มีหลายสถานประกอบกิจการตั้งอยู่ร่วมกัน

ระบุชื่ออาคาร/สถานที่

☒ เป็นสถานประกอบกิจการเดียว (ข้ามไปตอบข้อ ๒)

๑.๔ กรณีเป็นสถานที่ที่มีหลายสถานประกอบกิจการตั้งอยู่ร่วมกัน

☐ ลูกจ้างที่ทำงานอยู่ภายในอาคารเดียวกัน และในวันและเวลาเดียวกันของนายจ้างทุกรายในสถานที่นั้นทำการฝึกซ้อมพร้อมกัน

☐ ลูกจ้างที่ทำงาน ภายในอาคารเดียวกัน และในวันและเวลาเดียวกันของนายจ้างทุกรายในสถานที่นั้นไม่ได้ทำการฝึกซ้อมพร้อมกัน

๒. รายงานผลการดำเนินการ

๒.๑ วัน/เดือน/ปี ที่ทำการฝึกซ้อม ๒๕ ตุลาคม ๒๕๖๖

๒.๒ มีการฝึกซ้อมครั้งที่ผ่านมา เมื่อ (วัน/เดือน/ปี) ๒๕ สิงหาคม ๒๕๖๕

๒.๓ จำนวนผู้ที่เข้าร่วมในการฝึกซ้อม ๑๒๑ คน

๒.๔ ผลการดำเนินการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟ

☐ ไม่ดี ☐ พอใช้ ☒ ดี ☐ ดีมาก

๓. ดำเนินการฝึกซ้อมโดย

☒ ได้รับความเห็นชอบแผนและรายละเอียดการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟจากอธิบดีหรือผู้ซึ่งอธิบดีมอบหมาย

ตามหนังสือเห็นชอบแผนฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟ ประจำปี ๒๕๖๖ เลขที่ กพ ๐๐๓๐/๑๕๑๔

ลงวันที่ ๒๐ กันยายน ๒๕๖๖ โดยได้แนบเอกสารให้ความเห็นชอบมาด้วยแล้ว

☐ ผู้ที่ได้รับใบอนุญาตจากกรมสวัสดิการและคุ้มครองแรงงานดำเนินการฝึกซ้อมให้คือ -

เลขที่ใบอนุญาต - โดยได้แนบสำเนาใบอนุญาตและหนังสือรับรองแสดงการฝึกซ้อม ฯ มาด้วยแล้ว

ลงชื่อ

นายจ้าง

รักษาการ ผจก.อาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส ๑

กำหนดการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟ ประจำปี 2566

เวลา	รายการดำเนินการ	ผู้ดำเนินการ
08:30 - 10:30 น.	ดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟเสมือนจริงบนโต๊ะ (Table Top Exercise)	PS1/S
11:00 - 11:45 น.	ดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟภาคสนาม (Field Exercise)	PS1/S, PS1/P, PS1/O, PTN/A และ หน่วยงานราชการที่เข้าร่วมซ้อมแผน ฯ
11:45 - 12:00 น.	- สรุปผลการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟ - ถ่ายภาพหมู่ร่วมกัน	PS1/S, PS1/P, PS1/O, PTN/A และ หน่วยงานราชการที่เข้าร่วมซ้อมแผน ฯ

วัตถุประสงค์การฝึกซ้อมดับเพลิงและอพยพหนีไฟ

- เพื่อทราบวิธีการปฏิบัติเมื่อเกิดเหตุฉุกเฉิน และเป็นการใช้ทรัพยากรที่มีอยู่ให้เกิดประโยชน์สูงสุดดังนี้
 - ช่วยเหลือผู้ประสบภัยและช่วยชีวิตผู้ที่ได้รับบาดเจ็บ (Protection of People)
 - ส่งผลกระทบต่อสิ่งแวดล้อมน้อยที่สุด (Protection of Environment)
 - เกิดความเสียหายต่อทรัพย์สินน้อยที่สุด (Protection of Property)
 - ปกป้องธุรกิจและชื่อเสียง (Protection of the Business and Reputation)
- เพื่อให้มั่นใจต่อชุมชนและหน่วยงานในพื้นที่ ต่อความพร้อมในการตอบสนองเหตุฉุกเฉินของบริษัทฯ
- เพื่อรับฟังความคิดเห็นและข้อเสนอแนะ ให้เกิดความพร้อมในกรณีเกิดเหตุฉุกเฉิน



ผลิตภัณฑ์ : น้ำมันดิบ

สิ่งที่เกิดขึ้น : ตู้รถไฟบรรทุกน้ำมันดิบพลิกคว่ำขณะเคลื่อนตัวออกจากโรงถ่ายน้ำมันดิบ

สาเหตุ : กลไกการประจักษ์ลึกลับทำให้เกิดการชำรุด

ลักษณะเหตุฉุกเฉิน :

- มีรอยข้าวของผู้บรรพบุรุษน้ำมันดิบ และมีการรื้อไหลของน้ำมันดิบ รวมทั้งมีเพลิงลุกไหม้
- ตอบสนองเหตุโดยทีมตอบโต้ของบริษัทฯ
- ขอความช่วยเหลือจากหน่วยงานท้องถิ่น

ผู้พบเห็นเหตุการณ์ : พนักงานขับห้วงจรจักรของรถไฟ, พนักงานรักษาความปลอดภัยคั้งน้ำมันดิบึงพระ

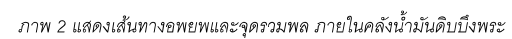
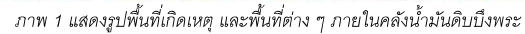
ผู้บาดเจ็บ - ลักษณะการบาดเจ็บ : 1 คน - บาดเจ็บที่ขาทั้ง 2 ข้าง

หน่วยงานเข้าร่วมทำการฝึกซ้อมแผนฯ

1. บริษัท ปตท.สม. สยาม จำกัด
2. องค์การบริหารส่วนตำบลบึงพระ
3. เทศบาลนครพิษณุโลก
4. สถานีตำรวจภูธรวังน้ำคู้
5. โรงพยาบาลกรุงเทพ-พิษณุโลก

หน่วยงานเข้าร่วมทำการสังเกตการฝึกซ้อมแผนฯ

1. บริษัท ปตท.สผ. สยาม จำกัด
2. คลังน้ำมัน ปตท.พิษณุโลก
3. PTT Group Transportation Safety Taskforce
4. ผู้ใหญ่บ้านหมู่ 2 ตำบลบึงพระ
5. สมาคมอนุรักษ์สภาพแวดล้อมของกลุ่มอุตสาหกรรมน้ำมัน (IESG)
6. สวัสดิการและคุ้มครองแรงงานจังหวัดพิษณุโลก
7. สถานีรถไฟบึงพระ
8. สำนักงานพลังงานจังหวัดพิษณุโลก
9. บริษัท BES Energy Resources Co.Ltd
10. บริษัท BRK Intertransport Co.Ltd



ภาพสถานการณ์การฝึกซ้อมแผนฯ



ภาพ 4 แสดงสถานการณ์จำลอง รถไฟบรรทุกน้ำมันดิบตกราง มีพนักงานสับเปลี่ยนรางได้รับบาดเจ็บ และเกิดเหตุเพลิงไหม้



ภาพ 5 แสดงผู้บาดเจ็บขณะหนีออกจากบริเวณที่เกิดเหตุการณ์เพลิงไหม้

ภาพสถานการณ์การฝึกซ้อมแผนฯ



ภาพ 6 เจ้าหน้าที่คลังน้ำมันดิบปีงพระได้รับแจ้งเหตุ กดสัญญาณฉุกเฉิน ทำการนับจำนวนพนักงานและเตรียมพร้อมระงับเหตุ



ภาพ 7 แสดงการเข้าเผชิญเหตุ และการช่วยเหลือผู้บาดเจ็บ (กันพื้นที่น้ำมันดิบหกั่วไหล)

ภาพสถานการณ์การฝึกซ้อมแผนฯ



ภาพ 8 ทีมสนับสนุนเหตุฉุกเฉิน ณ ห้องสั่งการเหตุฯ สถานีผลิตลานกระบือ (ระบบ CCTV มุมมองสถานการณ์)



ภาพ 9 แสดงผู้สั่งการ ณ จุดเกิดเหตุของ ปตท.สผ. รายงานสถานการณ์ให้กับ ท่านนายกองค์การบริหารส่วนตำบลบึงพระเพื่อรับมอบอำนาจผู้อำนวยการเหตุฯ และบัญชาการเหตุร่วมกัน

ภาพสถานการณ์การฝึกซ้อมแผนฯ



ภาพ 10 แสดงเจ้าหน้าที่พยาบาลของโรงพยาบาลกรุงเทพ-พิษณุโลก ถึงที่เกิดเหตุ
เข้ารายงานตัว และช่วยปฐมพยาบาลเบื้องต้นให้กับผู้ได้รับบาดเจ็บ ก่อนนำส่งโรงพยาบาลโรงพยาบาลกรุงเทพ-พิษณุโลก



ภาพ 11 แสดงทีมตอบสนองเหตุฉุกเฉินของ อบต.บึงพระ ถึงที่เกิดเหตุ รายงานตัวต่อผู้อำนวยการเหตุฯ
และเข้าสนับสนุนระงับเหตุฉุกเฉิน

ภาพสถานการณ์การฝึกซ้อมแผนฯ



ภาพ 12 แสดงทีมตอบสนองเหตุฉุกเฉินของเทศบาลนครพิษณุโลก ถึงที่เกิดเหตุ รายงานตัวต่อผู้อำนวยการเหตุ ฯ และเข้าสนับสนุนระงับเหตุฉุกเฉิน



ภาพ 13 แสดงทีมตอบสนองเหตุฉุกเฉินของการท่าอากาศยานพิษณุโลก ถึงที่เกิดเหตุ รายงานตัวต่อผู้อำนวยการเหตุ ฯ และเข้าสนับสนุนระงับเหตุฉุกเฉิน



ภาพ 14 แสดงเจ้าหน้าที่ตำรวจ สภ.วังน้ำคู้ ถึงที่เกิดเหตุ รายงานตัวต่อผู้อำนวยการเหตุ ฯ และเข้าสนับสนุนอำนวยความสะดวกด้านจราจร

ภาพสถานการณ์การฝึกซ้อมแผนฯ



ภาพ 15 แสดงเจ้าหน้าที่ทุกหน่วยงานปฏิบัติงานระงับเหตุ ฯ ร่วมกันแบบบูรณาการ

ภาพสถานการณ์การฝึกซ้อมแผนฯ



ภาพ 16 แสดงเหตุการณ์เข้าสู่สถานการณ์ภายใต้การควบคุม เข้าตรวจสอบเหตุการณ์
โดยผู้อำนวยการเหตุฯ เจ้าหน้าที่ ปตท.สผ. และเจ้าหน้าที่ตำรวจ



ภาพ 17 แสดงหน่วยงานเข้าร่วมฝึกซ้อม

ภาพสถานการณ์การฝึกซ้อมแผนฯ



ภาพ 18 สรุปการประชุมชี้แจงข้อสังเกตจากผู้สังเกตการณ์การฝึกซ้อม

สรุปลำดับเหตุการณ์ที่ปฏิบัติจริง

ลำดับ	เวลา	เหตุการณ์
1	11.02 น.	-เกิดเหตุรถไฟชนถ้ำน้ำมันดิบตกวาง ขณะเคลื่อนตัวออกจากโรงบรรจุน้ำมันดิบ มีน้ำมันรั่วไหล และมีเพลิงไหม้ -เจ้าหน้าที่รักษาความปลอดภัยถ้ำน้ำมันดิบบึงพระที่พบเหตุเพลิงไหม้และพบผู้บาดเจ็บ 1 คน ได้ทำการแจ้งเหตุมายังนายคลังน้ำมันดิบบึงพระ
2	11.05 น.	- นายคลังน้ำมันดิบบึงพระ แจ้งห้องสื่อสาร ปตท.สม. ลานกระบือ เพื่อประสานขอความช่วยเหลือ และกวดสัญญาณอพยพพนักงาน รวมทั้งนับจำนวนพนักงาน ณ จุดรวมพล - เจ้าหน้าที่ห้องสื่อสารประกาศให้ผู้ที่มีส่วนเกี่ยวข้องใช้เครือข่ายวิทยุ ช่องฉุกเฉิน - จัดตั้งศูนย์ควบคุมเหตุฉุกเฉิน ที่สถานีผลิตลานกระบือ แจ้งยังผู้เกี่ยวข้องในทุกแผนก ให้เข้ารวมการช่วยเหลือระดับเหตุ **นายคลังน้ำมันดิบบึงพระ เปลี่ยนบทบาทหน้าที่ในสถานการณ์ฉุกเฉินเป็นผู้สั่งการ ณ จุดเกิดเหตุ**
3	11.10 น.	ผู้สั่งการ ณ จุดเกิดเหตุ นำทีมเข้าระงับเหตุ ฯ และเข้าช่วยเหลือผู้บาดเจ็บ
4	11.12 น.	-ผู้สั่งการ ณ จุดเกิดเหตุ ร้องขอไปยังหัวหน้าศูนย์ควบคุมเหตุฉุกเฉิน ปตท.สม. ขอสนับสนุนโรงพยาบาล เพื่อนำส่งผู้บาดเจ็บไปส่งโรงพยาบาล -เจ้าหน้าที่ห้องสื่อสาร ติดต่อโรงพยาบาลกรุงเทพ-พิษณุโลก ขอสนับสนุนโรงพยาบาล
5	11.14 น.	-หัวหน้าจุดรวมพล รายงานจำนวนพนักงานกับทาง ผู้สั่งการ ณ จุดเกิดเหตุ (ไม่มีผู้สูญหาย, ผู้บาดเจ็บ 1 คน
6	11.17 น.	-น้ำมันหกทั่วไหล และไฟลุกไหม้ต่อเนื่อง ผู้สั่งการ ณ จุดเกิดเหตุ ให้ดำเนินการฉีดน้ำหล่อเย็นไปในจุดที่เกิดเพลิงไหม้ และทำแมงกัณฑ์ทราย เพื่อป้องกันไม่ให้น้ำมันดิบไหลไปสู่พื้นที่โดยรอบ -รพพยาบาลของโรงพยาบาลกรุงเทพ-พิษณุโลก มาถึงที่เกิดเหตุ เข้ารายงานตัวต่อผู้สั่งการ ณ จุดเกิดเหตุ ให้การช่วยเหลือผู้บาดเจ็บ นำขึ้นรพพยาบาลและนำส่งโรงพยาบาล
7	11.20 น.	-ผู้สั่งการ ณ จุดเกิดเหตุ ประเมินสถานการณ์ มีโอกาสส่งผลกระทบวงกว้าง ร้องขอสนับสนุนหน่วยงานท้องถิ่นกับหัวหน้าศูนย์ควบคุมเหตุฉุกเฉิน ปตท.สม. เพื่อเข้าช่วยระงับเหตุ -หัวหน้าศูนย์ควบคุมเหตุฉุกเฉิน ปตท.สม. รับทราบเรื่อง ให้เจ้าหน้าที่ห้องสื่อสารติดต่อ <ul style="list-style-type: none">● เจ้าหน้าที่ตำรวจ สภ. วังนาคู● องค์การบริหารส่วนตำบลบึงพระ● เทศบาลนครพิษณุโลก● การท่าอากาศยานพิษณุโลก เพื่อเข้าสนับสนุนระดับเหตุ
8	11.23 น.	-รองนายกองค์การบริหารส่วนตำบลบึงพระ ถึงที่เกิดเหตุรับรายงานเหตุการณ์จากผู้สั่งการ ณ จุดเกิดเหตุฯ รับมอบอำนาจบัญชาการ โดยรับหน้าที่ผู้อำนวยการเหตุ ฯ

ลำดับ	เวลา	เหตุการณ์
9	11.24 น.	-ระดับเพลิงและเจ้าหน้าที่ดับเพลิง ขององค์การบริหารส่วนตำบลบึงพระ ถึงที่เกิดเหตุ เข้ารายงานตัวต่อ ผู้อำนวยการเหตุ ฯ และเข้าสนับสนุนระดับเหตุ -ระดับเพลิงและเจ้าหน้าที่ดับเพลิง ของการท่าอากาศยานพิษณุโลก ถึงที่เกิดเหตุ เข้ารายงานตัวต่อ ผู้อำนวยการเหตุ ฯ และเข้าสนับสนุนระดับเหตุ
10	11.26 น.	-ระดับเพลิงและเจ้าหน้าที่ดับเพลิง ของเทศบาลนครพิษณุโลก ถึงที่เกิดเหตุ เข้ารายงานตัวต่อ ผู้อำนวยการเหตุ ฯ และเข้าสนับสนุนระดับเหตุ
11	11.28 น.	-เจ้าหน้าที่ตำรวจ สภ. วังนาคู ถึงที่เกิดเหตุ เข้ารายงานตัวต่อ ผู้อำนวยการเหตุ ฯ และเข้าสนับสนุนความเรียบร้อยและการจราจร -หัวหน้าศูนย์ควบคุมเหตุฉุกเฉินรับแจ้ง รพพยาบาลส่งผู้บาดเจ็บถึงโรงพยาบาล
12	11.30 น.	-เจ้าหน้าที่ทุกหน่วยงาน กระจ่ายกำลังเข้าระงับเหตุ โดยการระดมฉีดน้ำหล่อเย็น เพื่อป้องกันรังสีความร้อน และป้องกันการลุกไหม้เพิ่มเติม -ทีมดับเพลิงจากคลังน้ำมันดิบบึงพระ ฉีดโฟมดับเพลิง เพื่อคลุมเชื้อเพลิงเพื่อดับไฟ (ดับไฟได้)
13	11.35 น.	-สามารถดับเพลิงที่ติดอยู่ที่ตู้รถไฟได้ -หัวหน้าทีมดับเพลิง ส่งการฉีดหล่อเย็นต่อไป (สถานการณ์อยู่ภายใต้การควบคุม)
14	11.38 น.	สถานการณ์เข้าสู่สภาวะปกติ -เจ้าหน้าที่ทุกหน่วยงานหยุดฉีดน้ำหล่อเย็น
15	11.41 น.	ทุกหน่วยงานเข้ารายงานกำลังพล ต่อผู้อำนวยการเหตุ ฯ (ไม่มีผู้บาดเจ็บขณะปฏิบัติหน้าที่)
16	11.42 น.	- ผู้อำนวยการเหตุ ฯ เห็นว่าสถานการณ์อยู่ในการควบคุม แจ้งให้ ผู้สั่งการ ณ จุดเกิดเหตุรายงานตามขั้นตอน ปตท.สม. เพื่อยุติการซ้อมแผนฉุกเฉิน -ผู้สั่งการ ณ จุดเกิดเหตุแจ้งไปยังศูนย์ควบคุมเหตุฉุกเฉิน รายงานสถานการณ์ อยู่ในการควบคุม ขอแจ้งยกเลิกการซ้อมแผน
17	11.43 น.	-ผู้อำนวยการเหตุ ฯ ประกาศยกเลิกสถานการณ์ฉุกเฉิน -ผู้สั่งการ ณ จุดเกิดเหตุ (OSC) แจ้งต่อ หัวหน้าศูนย์ควบคุมเหตุฉุกเฉิน ประกาศยกเลิกภาวะฉุกเฉิน -เจ้าหน้าที่ห้องสื่อสารประกาศยกเลิก การซ้อมแผนฉุกเฉิน

หมายเหตุ : หน่วยงานสนับสนุนจากท้องถิ่น ไม่ได้ออกจากสถานที่ปฏิบัติงานจริงขณะทำการฝึกซ้อม เพื่อหลีกเลี่ยงการใช้เส้นทางจราจรที่อาจกระทบชุมชน และเพื่อป้องกันอุบัติเหตุจากการเดินทาง

สรุปประเด็นข้อเสนอแนะจากผู้ปฏิบัติงานและผู้สังเกตการณ์

ลำดับที่	ประเด็นเสนอแนะปรับปรุง	แนวทางการปรับปรุง
1.	ในการฝึกซ้อมแผนฉุกเฉิน มีการใช้ศัพท์เฉพาะของทาง ปตท.สม ซึ่งอาจทำให้เกิดความเข้าใจที่สับสน กับหน่วยงานท้องถิ่น อาจทำให้การประสานร่วมกันติดขัดได้	หาแนวทางการสื่อสาร ที่สามารถสื่อสารกับ หน่วยงานท้องถิ่นเพื่อให้ความเข้าใจที่ตรงกัน
2.	เมื่อรู้ว่ามีผู้บาดเจ็บ ควรมีการประสานงานกับทางสายด่วน 1669 ก่อนที่จะขอความช่วยเหลือจากหน่วยงานอื่น	ในการซ้อมครั้งต่อไป ควรจัดให้มีการซ้อมถึง บทบาทที่มีการติดต่อไปที่สายด่วน 1669 เพื่อให้ เป็นระเบียบปฏิบัติในการแจ้งเหตุของ ปตท.สม
3.	การร้องขอการสนับสนุนจากหน่วยงานท้องถิ่นค่อนข้างล่าช้า ถ้า ประเมินสถานการณ์ได้เร็ว ประสานขอสนับสนุนได้รวดเร็ว จะช่วยลดความรุนแรงของเหตุฉุกเฉินต่อชุมชนได้	จัดให้มีการซ้อมที่ภายในมากขึ้น เพื่อให้พนักงาน ประเมินสถานการณ์ได้รวดเร็ว และดำเนินการร้อง ขอสนับสนุนได้รวดเร็ว (ทำตามขั้นตอนของ สถานการณ์จำลองที่เขียนไว้)
4.	การขนย้ายผู้บาดเจ็บ และการตอบสนองช่วยเหลือผู้บาดเจ็บ ค่อนข้างช้า	จัดอบรมและซักซ้อมการขนย้ายผู้บาดเจ็บให้มี ความถี่มากขึ้น
5.	เนื่องจากในสถานการณ์จริงอาจ มีโอกาสเกิดขึ้นจากการเผาไหม้ จึงควรมีการบอกทิศทางของลมในการการซ้อมแผน เพื่อติดตาม สถานการณ์และอพยพผู้คนไปในที่ที่ปลอดภัย	ในการซ้อมครั้งต่อไป ควรเพิ่มบทบาทผู้สังเกต ณ์ จุดเกิดเหตุ ฯ ถึงการสังเกต ทิศทางลม เพื่อกำหนด สถานการณ์การอพยพต่อไป
6.	เนื่องจากมีชุมชนอยู่ค่อนข้างใกล้ที่เกิดเหตุ เสนอแนะให้ในครั้งต่อไป มีการจำลองสถานการณ์โดยการเชิญตัวแทนจากชุมชนที่ อยู่ใกล้เคียงกับที่เกิดเหตุ เข้าร่วมซ้อมแผนฉุกเฉิน	เชิญตัวแทนชาวบ้านในห้วงคาเรือนใกล้เคียง เพื่อ ร่วมสังเกตการณ์ฝึกซ้อมในครั้งต่อไป
7.	ในช่วงที่มีการอธิบายสถานการณ์การซ้อมแผนในห้องประชุม (Tabletop exercises :TTX) ควรมีโมเดล 3 มิติ ระบุทิศทางของ ที่เกิดเหตุ เพื่อให้ทุกคนหน่วยงานสนับสนุนได้เห็นภาพรวมและ ทำความเข้าใจได้ง่าย	พิจารณาจัดอุปกรณ์ การจำลองเหตุการณ์แบบ โมเดล 3 มิติ มาใช้ฝึกซ้อมในครั้งต่อไป

ภาคผนวก ก 1 รายชื่อผู้เข้าร่วมทำการฝึกซ้อม

ลำดับ	ชื่อ-นามสกุล	ตำแหน่ง	หน่วยงาน
1	นายโรจน์ เพชรนิล	รองนายก	อบต.บึงพระ
2	ส.อ. ทวีลาภ ลิ้มนาถ	จพง. บึงก้านขนง.	อบต.บึงพระ
3	นางสาวสุภารัตน์ ทองรักษา	เลขานุการนายกฯ	อบต.บึงพระ
4	นายฉัตรชัย เล่าทิมย์	พนักงานดับเพลิง	อบต.บึงพระ
5	นายฉัตรชัย เล่าทิมย์	หัวหน้าฝ่ายป้องกัน	อบต.บึงพระ
6	นายอนุชา เทียนทอง	พนักงานขับรถยนต์	อบต.บึงพระ
7	นายอาทิตย์ นันทะสังข์	พนักงานดับเพลิง	อบต.บึงพระ
8	นายอำนาจ สุขสวัสดิ์	ผู้ช่วยเจ้าพนักงานป้องกันฯ	อบต.บึงพระ
9	สืบเอกทวีลาภ ลิ้มนาถ	เจ้าพนักงานป้องกันฯ	อบต.บึงพระ
10	กมลภพ บัวบานแอ้ม	เจ้าหน้าที่กู้ภัยและดับเพลิง	การท่าอากาศยานพิษณุโลก
11	กัมพล ดีโหมด	เจ้าหน้าที่กู้ภัยและดับเพลิง	การท่าอากาศยานพิษณุโลก
12	ณัฏฐาณันต์ จิตวิธาวาณ	หัวหน้ากลุ่มความปลอดภัย	การท่าอากาศยานพิษณุโลก
13	นพพล ลิ้มโพธิ์ศรี	เจ้าหน้าที่กู้ภัยและดับเพลิง	การท่าอากาศยานพิษณุโลก
14	นาย ธนศักดิ์ สิงห์เดช	เจ้าหน้าที่กู้ภัยและดับเพลิง	การท่าอากาศยานพิษณุโลก
15	นาย วีระ มินเดระชา	เจ้าหน้าที่กู้ภัยและดับเพลิง	การท่าอากาศยานพิษณุโลก
16	นายอัคร บุญสวัสดิ์	เจ้าหน้าที่กู้ภัยและดับเพลิง	การท่าอากาศยานพิษณุโลก
17	ปัทมา บัณเฑาะ	นักวิชาการขนส่งปฏิบัติการ	การท่าอากาศยานพิษณุโลก
18	ปัทมา บัณเฑาะ	นักวิชาการขนส่งปฏิบัติการ	การท่าอากาศยานพิษณุโลก
19	ธีรศักดิ์ นันทศิริ	เจ้าหน้าที่กู้ภัยและดับเพลิง	การท่าอากาศยานพิษณุโลก
20	วรวิทย์ บัวอ่อน	นักวิชาการขนส่ง	การท่าอากาศยานพิษณุโลก
21	สุทธกานต์ ศุภธนสินเชษฐ	นักวิชาการขนส่ง	การท่าอากาศยานพิษณุโลก
22	ธีรศักดิ์ ยาวะธรรมโม	พนักงานจ้าง	เทศบาลนครพิษณุโลก
23	นางเข็มทอง ทาหา	เจ้าพนักงานขนส่งชำนาญงาน	ท่าอากาศยานพิษณุโลก
24	นายณัฏฐาณันต์ จิตวิธาวาณ	เจ้าพนักงานขนส่งชำนาญงาน	ท่าอากาศยานพิษณุโลก
25	นายช่ออนันท์ นาคเหล็ก	นักวิชาการขนส่งชำนาญการ	ท่าอากาศยานพิษณุโลก
26	นายธรรมา ทอมจินทร์	ผู้อำนวยการท่าอากาศยานพิษณุโลก	ท่าอากาศยานพิษณุโลก
27	ภานุ คุ้มแพทย	ดับเพลิง	ท่าอากาศยานพิษณุโลก
28	นายเอกพล พรหมสงฆ์	พนักงานดับเพลิง	เทศบาลนครพิษณุโลก
29	นายฤทธิชัย เอี่ยมเย็น	พนักงานจ้างตามภาระกิจ	เทศบาลนครพิษณุโลก
30	นายพิพัฒน์พงษ์ ภูมิระชากุล	เจ้าพนักงานป้องกันฯ ชำนาญงาน	เทศบาลนครพิษณุโลก
31	นายสิทธิโชค อันเอียด	พนักงานดับเพลิง	เทศบาลนครพิษณุโลก
32	นายสุรสิทธิ์ จินใจตรง	เจ้าพนักงานป้องกันและบรรเทาสาธารณภัยปฏิบัติการ	เทศบาลนครพิษณุโลก
33	นายอุเทน ทองเหล็ก	เจ้าพนักงานป้องกันและบรรเทาสาธารณภัยชำนาญงาน	เทศบาลนครพิษณุโลก
34	ทนศักดิ์ มาลาศรี	ผู้ช่วยพยาบาล	โรงพยาบาลกรุงเทพพิษณุโลก
35	นางศิริรัตน์ มิกทิด	หัวหน้าแผนกห้องฉุกเฉิน	โรงพยาบาลกรุงเทพพิษณุโลก
36	นายทนศักดิ์ มาลาศรี	ผู้ช่วยพยาบาล	โรงพยาบาลกรุงเทพพิษณุโลก
37	นายสาธิต จันทศิริ	หัวหน้างานด้านความปลอดภัย ๖๒หัวหน้างาน	โรงพยาบาลกรุงเทพพิษณุโลก
38	นายสิริศักดิ์ มากกุล	เจ้าหน้าที่เวชกิจฉุกเฉินเบื้องต้น	โรงพยาบาลกรุงเทพพิษณุโลก
39	วาทิตย์ แป้งหอม	พยาบาล	โรงพยาบาลกรุงเทพพิษณุโลก
40	สิริศักดิ์ มากกุล	พยา	โรงพยาบาลกรุงเทพพิษณุโลก
41	จ.ส.ด.ธีรศักดิ์ หลวงศิริ	ผบ.หมู่(ป.)	สถานีตำรวจภูธรวังนาคู
42	พ.ต.ท.จรูญ คณานนท์	สว.ญ.สภ.วังนาคู	สถานีตำรวจภูธรวังนาคู
43	ร.ต.อ.ชนะชล ชาญนัธ	รอง.สว.(ป.)สภ.วังนาคู	สถานีตำรวจภูธรวังนาคู
44	ร.ต.อ.ประเทือง โกทา	รองสว.(ป.)	สถานีตำรวจภูธรวังนาคู
45	ส.ต.ท.ศิริดี ภูมิโยธสวัสดิ์สกุล	ผบ.หมู่(ป.)สภ.วังนาคู	สถานีตำรวจภูธรวังนาคู
46	ส.ต.อ.อรรถ เนตรสว่าง	ผบ.หมู่(ป.)สภ.วังนาคู	สถานีตำรวจภูธรวังนาคู
47	ต.ต.ณัฏฐ์วันทนา น้อยบ้านใหม่	ผบ.หมู่(ป.)สภ.วังนาคู	สถานีตำรวจภูธรวังนาคู

เอกสารแนบ 1 ใบลงทะเบียนผู้เข้าร่วมฝึกซ้อมฝึกซ้อมแผนฯ ประจำปี 2566 ณ คัดค้าน้ำมันดับบึงพระ

สังกัดการณื			
ลำดับ	ชื่อ-นามสกุล	ตำแหน่ง	หน่วยงาน
1	Kantorn Inpo	Operation Depot	คลังน้ำมัน ปตท.พิษณุโลก
2	คมกริช ชัยชาวลย์	พนักงานบริการขาย	คลังน้ำมัน ปตท.พิษณุโลก
3	นายปริดา สกุลโต	แผนกปฏิบัติการน้ำมัน	คลังน้ำมัน ปตท.พิษณุโลก
4	นายสมนึก บรรดาศักดิ์	ผ.ว.ส่วนคลังน้ำมันพิษณุโลก	คลังน้ำมัน ปตท.พิษณุโลก
5	ระเบียบ เอี่ยมมี	ประธานหมู่บ้าน	ชุมชน หมู่บ้านวังทองธานี
6	ชัชพงศ์ ศิริอุดมใหญ่	ทีมงาน	PTT Group Transportation Safety Taskforce
7	อนุชา พันธุ์เครือบุตร	ผู้จัดการ	PTT Group Transportation Safety Taskforce
8	ชัชพงศ์ ศิริอุดมใหญ่	ทีมงาน	PTT Group Transportation Safety Taskforce
9	นุรินทร์ วุฒิปญญารัตนกุล	พนักงานบริหารความปลอดภัยและอาชีวอนามัย	PTT Group Transportation Safety Taskforce
10	ชวพงศ์ ชื่นขจร	พนักงานบริหารความปลอดภัย	PTT Group Transportation Safety Taskforce
11	นายบรรดิษฐ์ ไวยมิตรา	ผ.ม.ป.ส.ค. / ว.ป.วิชาชีพ	การรถไฟ (ฝ่ายบริการสินค้า)
12	Kantorn Inpo	Operation Depot	คลังน้ำมัน ปตท.พิษณุโลก
13	คมกริช ชัยชาวลย์	พนักงานบริการขาย	คลังน้ำมัน ปตท.พิษณุโลก
14	นายปริดา สกุลโต	แผนกปฏิบัติการน้ำมัน	คลังน้ำมัน ปตท.พิษณุโลก
15	นายสมนึก บรรดาศักดิ์	ผ.ว.ส่วนคลังน้ำมันพิษณุโลก	คลังน้ำมัน ปตท.พิษณุโลก
16	ศราวุฒิ บุญเกิด	พนักงานคุมประแส	สถานีรถไฟบึงพระ
17	สันต์ คำภูเมือง	ผู้ช่วยนายสถานีบึงพระ	สถานีรถไฟบึงพระ
18	นิยะ ช่างอยู่	พนักงานสับเปลี่ยน	สถานีรถไฟบึงพระ
19	นางอุษุขญา สมศิริ	ผู้ใหญ่นบ้าน	ผู้ใหญ่บ้านหมู่ที่ 2 ตำบลบึงพระ
20	นางระเบียบ เอี่ยมมี	ประธานหมู่บ้านวงศ์ทอง	ผู้ใหญ่บ้านหมู่ที่ 2 ตำบลบึงพระ
21	นางสาริภัทร แซ่เดียว	ผู้ช่วยผู้ใหญ่บ้าน	ผู้ใหญ่บ้านหมู่ที่ 2 ตำบลบึงพระ
22	นางสาวจริภัทร แซ่เดียว	ผู้ช่วยผู้ใหญ่บ้าน	ผู้ใหญ่บ้านหมู่ที่ 2 ตำบลบึงพระ
23	ปภาภัสสร ชัยนิต	Admin Assistant	สมาคมอนุรักษ์สภาพแวดล้อมของกลุ่มอุตสาหกรรมน้ำมัน (IESG)
24	กัทธิญา กิตติวิริยะการ	Admin Assistant	สมาคมอนุรักษ์สภาพแวดล้อมของกลุ่มอุตสาหกรรมน้ำมัน (IESG)
25	นางมิ่งขวัญ กุ้ย	นักวิชาการแรงงานชำนาญการ	สวัสดิการและคุ้มครองแรงงานจังหวัดพิษณุโลก
26	อาภากรณ อ่อนอัน	นิติกรชำนาญการ	สวัสดิการและคุ้มครองแรงงานจังหวัดพิษณุโลก
27	นางสาวกมลชนก สวนจันทร์	วิเคราะห์นโยบายและแผน	สำนักงานพลังงานจังหวัดพิษณุโลก
28	นายภัทรพล อัมภะระวง	วิศวกรชำนาญการ	สำนักงานพลังงานจังหวัดพิษณุโลก
29	นายศุภชัย ภูมิผาเดช	นักวิชาการพลังงานชำนาญการ	สำนักงานพลังงานจังหวัดพิษณุโลก
30	ปณิดา แสงจันทร์	SSHE Officer	BES
31	Sirithorn Wong-Anu	Safety officer	BRK Intertransport Co.,Ltd
32	Sittipong M.	Site Manager	GGI
33	ว่าที่ ร.ต. สอน สอนจันทร์	Security Supervisor	GGI
34	เดวิด เพชรนิล	รปภ	GGI

เอกสารแนบ 1 ใบลงทะเบียนผู้เข้าร่วมฝึกซ้อมฝึกซ้อมแผนฯ ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ (ต่อ)

LKU ECC Member Check-in Sheet

Role	Assigned to	Name-Signature	Check-in Date &Time
ERT Main Duty Group			
ERT Leader	VP, S1 Production Operation		
ERT Duty Officer	Production Superintendent		11:00
Deputy ERT Leader	Production Superintendent ,LKU Flow Station, Office, Well sites, MPFs and PHS Housing Compounds		
	Workshop Superintendent ,Well Service Workshop		
	Oil Movement and Transportation Manager ,BPR Depot and CNS		
	Well Services /Superintendents		
Deputy ERT Leader	Well Services Workshop Duty		
SSHE Duty	SSHE Superintendent		11:02
Event Logger	Production Engineer		11.11
Muster Logger	SSHE Officer, Operational Safety		11.02
On-Call Support Team - Mobilize to ECC in 2 hours			
Maintenance Duty	Maintenance Superintendent		11:00
Logistics Duty	Oil Movement and Transportation Manager		
IT/Telecom Services	IT and Telecommunication Supervisor		11.00
Community & Media Response Team (CMRT)	Public Affairs Manager		11.14
Relative Response Team (RRT)	Operation Training Center Manager		11.02
Construction Duty	Onshore Execution Team Leader		11.24
Land Acquisition, Permits & Operation Services	Land Acquisition, Permits, and Operations Services Manager		11.00
LKU Support Base Duty	Lankrabue Support Base Supervisor		
Well Services Support	Representative		
Drilling Support	Representative		


Note: Reference from the S1 Emergency Response Plan (13247-PDR SSHE 501-08-R03)

SI BCM Co.

Lankrabue T.

เอกสารแนบ 2 ใบลงทะเบียนผู้ปฏิบัติงาน ณ ศูนย์ควบคุมเหตุฉุกเฉิน สถานีผลิตลานกระบือ

ภาคผนวก 2 เอกสารแจ้งและเรียนเชิญหน่วยงานราชการ



PTTEP

บริษัท ปตท.ส.ส.สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-38
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ที่ ปตท.ส.ส.สยาม 13247/00-10418/2023

18 กันยายน 2566

เรื่อง ขอความเห็นชอบการฝึกซ้อมดับเพลิงและอพยพหนีไฟในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566


เรียน สวัสดิการและคุ้มครองแรงงานจังหวัดพิษณุโลก

สิ่งที่ส่งมาด้วย ข้อมูลประกอบเพื่อพิจารณาให้ความเห็นชอบแผนการฝึกซ้อมฯ และรายละเอียดการฝึกซ้อมฯ

ด้วย บริษัท ปตท.ส.ส.สยาม จำกัด ขอนำเสนอแบบแจ้งแผนการฝึกซ้อมดับเพลิงและอพยพหนีไฟในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566 วันพุธที่ 25 ตุลาคม 2566 ณ บริเวณคลังน้ำมันดิบปิโตรเลียม อ.เมือง จ.พิษณุโลก เพื่อให้เป็นไปตามกฎกระทรวง กำหนดมาตรฐานในการบริหารกิจการ และดำเนินการด้านความปลอดภัย อาชีวอนามัย และสภาพแวดล้อมในการทำงานเกี่ยวกับการป้องกันและระงับอัคคีภัย พ.ศ. 2555 ที่ระบุให้แจ้งแผนการฝึกซ้อมดับเพลิงและอพยพหนีไฟ ต่อสำนักงานสวัสดิการและคุ้มครองแรงงานในพื้นที่ก่อนทำการฝึกซ้อมอย่างน้อย 30 วัน เพื่อให้ความเห็นชอบ ดังรายละเอียดในเอกสารแนบมาพร้อมนี้

จึงเรียนมาเพื่อโปรดพิจารณา

ขอแสดงความนับถือ



รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

แนบความปลอดภัย มั่นคง อาชีวอนามัย และสิ่งแวดล้อม ปตท.ส.ส. โครงการเอส 1


ผู้ประสานงาน นายนำพล แก้วทอง

โทรศัพท์ 0 5573 1150 ต่อ 6031

สำเนาเรียน : PS1/O, PS1/P, PS1/S, PTN/A

Sutham D.

เอกสารแนบ 3 หนังสือขอความเห็นชอบการฝึกซ้อมดับเพลิงและอพยพหนีไฟในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566



PTTEP

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ที่ พส ๐๐๓๐/๐๕๖๒

๒๐ กันยายน ๒๕๖๖

เรื่อง เห็นชอบแผนการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟ ประจำปี ๒๕๖๖

เรียน ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส ๑ คลังน้ำมันดิบปิโตรเลียม บริษัท ปตท.ส.ส.สยาม จำกัด


อ้างถึง หนังสือบริษัท ปตท.ส.ส.สยาม จำกัด ที่ ปตท.ส.ส.สยาม ๑๓๒๔๗/๐๐-๑๐๔๑๘/๒๐๒๓ ลงวันที่ ๑๘ กันยายน ๒๕๖๖

ตามหนังสืออ้างถึงบริษัท ปตท.ส.ส.สยาม จำกัด คลังน้ำมันดิบปิโตรเลียม ตั้งอยู่เลขที่ ๘๒/๓ หมู่ที่ ๒ ตำบลบึงพระ อำเภอเมืองพิษณุโลก จังหวัดพิษณุโลก ขอความเห็นชอบแผนการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟ ประจำปี ๒๕๖๖ ต่ออธิบดีกรมสวัสดิการและคุ้มครองแรงงานหรือผู้ซึ่งอธิบดีกรมสวัสดิการและคุ้มครองแรงงานมอบหมาย โดยกำหนดฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟ ประจำปี ๒๕๖๖ ตามแผนในวันที่ ๒๕ ตุลาคม ๒๕๖๖ ระหว่างเวลา ๐๘.๓๐ น. - ๑๐.๓๐ น. ฝึกซ้อมเสมือนจริงบนโต๊ะ และเวลา ๑๑.๐๐ น. - ๑๒.๐๐ น. ฝึกซ้อมภาคสนาม ณ สถานที่ดังกล่าวข้างต้น

สำนักงานสวัสดิการและคุ้มครองแรงงานจังหวัดพิษณุโลก พิจารณาแผนการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟรวมทั้งรายละเอียดเกี่ยวกับการฝึกซ้อมดังกล่าว เห็นว่าแผนการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟสอดคล้องเป็นไปตามกฎกระทรวงกำหนดมาตรฐานในการบริหารและการจัดการด้านความปลอดภัย อาชีวอนามัย และสภาพแวดล้อมในการทำงานเกี่ยวกับการป้องกันและระงับอัคคีภัย พ.ศ. ๒๕๕๕ ข้อ ๓๐ จึงให้ความเห็นชอบการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟ ประจำปี ๒๕๖๖ ของบริษัท ปตท.ส.ส.สยาม จำกัด คลังน้ำมันดิบปิโตรเลียม ดำเนินการฝึกซ้อมฯ ตามวัน เวลา และสถานที่ดังกล่าว ทั้งนี้ เมื่อได้ดำเนินการฝึกซ้อมเสร็จสิ้นแล้วให้ท่านจัดทำรายงานผลการฝึกซ้อมตามแบบที่อธิบดีกำหนดยื่นต่อสำนักงานสวัสดิการและคุ้มครองแรงงานจังหวัดพิษณุโลก ภายในสามสิบวันนับแต่วันที่เสร็จสิ้นการฝึกซ้อม

จึงเรียนมาเพื่อทราบ

ขอแสดงความนับถือ




นักวิชาการแรงงานชำนาญการพิเศษ รักษาการแทน
สวัสดิการและคุ้มครองแรงงานจังหวัดพิษณุโลก

กลุ่มงานสวัสดิการและคุ้มครองแรงงาน

โทร. ๐ ๕๕๒๔ ๘๖๖๙ - ๐ ๕๕๒๔ ๒๑๙๑

E-mail : phitsanulok@labour.mail.go.th

เอกสารแนบ 4 หนังสือเห็นชอบแผนการฝึกซ้อมดับเพลิงและฝึกซ้อมอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566

 **บริษัท ปตท. จำกัด**
PTTEP Siam Limited
A Company of PTTEP Group

(บริษัท ปตท. จำกัด (มหาชน) อาคาร A ชั้น 19-20
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ที่ ปตท.สยาม 13247/00-11246/2023

6 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566
เรียน อธิบดีกรมเชื้อเพลิงธรรมชาติ

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิต
ปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันลิธิกีที่
ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบ
จากสถานีผลิตสถานกระบือสู่คลังน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก
และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก
ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติ
สถานการณ์บริเวณสถานีรถไฟบรรทุกน้ำมันดิบผ่านประแจสับราง กลไกได้เกิดชำรุด เป็นเหตุ
ให้ตู้รถไฟบรรทุกน้ำมันดิบถกวาง 2 ตู้ และเกิดเพลิงลุกไหม้ผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ฝ่ายปฏิบัติการ จำนวน 1-2 ท่าน เข้าร่วม
สังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟ ในวันที่ 25 ตุลาคม 2566 โดยมีรายละเอียด
กำหนดการดังต่อไปนี้

- เวลา 08:30-10:30 น. ประชุมชี้แจงรายละเอียดขั้นตอนและฝึกซ้อมแผนฯ
ตามเหตุการณ์สมมติบนโต๊ะ ณ ห้องประชุมคลังน้ำมันดิบบึงพระ
- เวลา 11:00-12:00 น. ฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ณ คลังน้ำมันดิบ
บึงพระ จังหวัดพิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบ
ตอบรับยืนยันการเข้าร่วม ดังถึง คุณภาพิณล สายสอด อีเมล PaipimonS@pttep.com หรือสแกน
คิวอาร์โค้ดตามเอกสารต้นแบบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566


-2/- จึงเรียนมา...

รณวิมลวรรณ / rana@pttep.com โทร. 0100020000/010

เอกสารแนบ 5 หนังสือแจ้งอธิบดีกรมเชื้อเพลิงธรรมชาติจัดการฝึกซ้อมแผนอพยพและป้องกันระดับอัคคีภัย
ในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566



จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ




ผู้จัดการอาวุโส ฝ่ายพัฒนาปิโตรเลียม โครงการผลิตบนฝั่ง - ประเทศไทย
วิชาการ ผู้ช่วยกรรมการผู้จัดการใหญ่ โครงการผลิตบนฝั่ง - ประเทศไทย

แนบความปลอบขวัญ มั่นคง ธารชีวิตนามัย และสิ่งสวัสดิการ โครงการเขต 1
ผู้ประสานงาน คุณภาพิณล สายสอด
โทรศัพท์ : 0 2537 6136
สำเนาเวียน : PS1, PS1/P, PS1/O, PS1/S, PTN/A
Subhor D.

เอกสารแนบ 5 หนังสือแจ้งอธิบดีกรมเชื้อเพลิงธรรมชาติจัดการฝึกซ้อมแผนอพยพและป้องกันระดับอัคคีภัย
ในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566 (ต่อ)



PTTEP

บริษัท ปตท.สผ. สยาม จำกัด
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ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566

เรียน นายกองัดการบริหารส่วนตำบลบึงพระ

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ.สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และอุทัยธานี ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตตามกระบวนที่สุดถึงน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกส่งน้ำมันดิบผ่านประแจสลักราง กลไกได้เกิดชำรุด เป็นเหตุให้รถบรรทุกน้ำมันดิบตกจาก 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน


ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ฝ่ายปฏิบัติการ เข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ ในวันพุธที่ 25 ตุลาคม 2566 โดยมีรายละเอียดกำหนดการดังต่อไปนี้

- เวลา 08:30-10:30 น. ประชุมชี้แจงรายละเอียดวันตอนและฝึกซ้อมแผนฯ ตามเหตุการณ์สมมติบนโต๊ะ ณ ห้องประชุมคลังน้ำมันดิบบึงพระ
- เวลา 11:00-12:00 น. ฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ณ คลังน้ำมันดิบบึงพระ

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณาออกรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ส่งถึง คุณภาพิมล สายสอด อีเมล PapimonS@pttep.com หรือสแกนคิวอาร์โค้ดตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ




รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

ผู้ประสานงาน คุณภาพิมล สายสอด

โทรศัพท์ : 0 2537 6136 สำเนาเรียน : PS1/P, PS1/O, PS1/S, PTN/A
Subhan G

ร/ค/00000001 / Registration No. 0105020000016

เอกสารแนบ 6 หนังสือขอเชิญนายกองัดการบริหารส่วนตำบลบึงพระ เข้าร่วมประชุมและฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566



PTTEP

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-36
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร กรุงเทพฯ 10900

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ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566

เรียน นายกเทศมนตรีนครพิษณุโลก

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ.สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และอุทัยธานี ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตตามกระบวนที่สุดถึงน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกส่งน้ำมันดิบผ่านประแจสลักราง กลไกได้เกิดชำรุด เป็นเหตุให้รถบรรทุกน้ำมันดิบตกจาก 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน


ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ฝ่ายปฏิบัติการ เข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ ในวันพุธที่ 25 ตุลาคม 2566 โดยมีรายละเอียดกำหนดการดังต่อไปนี้

- เวลา 08:30-10:30 น. ประชุมชี้แจงรายละเอียดวันตอนและฝึกซ้อมแผนฯ ตามเหตุการณ์สมมติบนโต๊ะ ณ ห้องประชุมคลังน้ำมันดิบบึงพระ
- เวลา 11:00-12:00 น. ฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ณ คลังน้ำมันดิบบึงพระ

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณาออกรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ส่งถึง คุณภาพิมล สายสอด อีเมล PapimonS@pttep.com หรือสแกนคิวอาร์โค้ดตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ



รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

ผู้ประสานงาน คุณภาพิมล สายสอด

โทรศัพท์ : 0 2537 6136 สำเนาเรียน : PS1/P, PS1/O, PS1/S, PTN/A
Subhan G

ร/ค/00000001 / Registration No. 0105020000016

เอกสารแนบ 7 หนังสือขอเชิญนายกเทศมนตรีเทศบาลนครพิษณุโลก เข้าร่วมประชุมและฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-36
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร เขตจตุจักร
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ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566
เรียน ผู้อำนวยการโรงพยาบาลกรุงเทพพิษณุโลก

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ


ด้วย บริษัท ปตท.สผ. สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันในสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกถังใส่รถไฟบรรทุกน้ำมันดิบผ่านประจวบสถับราง กลไกได้เกิดชำรุด เป็นเหตุให้ตู้รถไฟบรรทุกน้ำมันดิบตกราง 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ฝ่ายปฏิบัติการ เข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ ในวันพุธที่ 25 ตุลาคม 2566 โดยมีรายละเอียดกำหนดการดังต่อไปนี้

- เวลา 08:30-10:30 น. ประชุมชี้แจงรายละเอียดขั้นตอนและฝึกซ้อมแผนฯ ตามเหตุการณ์สมมติบึงพระ ณ ห้องประชุมคลังน้ำมันดิบบึงพระ
- เวลา 11:00-12:00 น. ฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ณ คลังน้ำมันดิบบึงพระ เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอกรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ดังถึง คุณภาพิณล สายสออด อีเมล PapimonS@pttep.com หรือสแกนคิวอาร์โค้ดตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ



รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

ผู้ประสานงาน คุณภาพิณล สายสออด
โทรศัพท์ : 0 2537 6136 ตำแหน่ง : PS1/P, PS1/O, PS1/S, PTN/A

Subson G.

หมายเลข / Registration No. 010503000016

เอกสารแนบ 8 หนังสือขอเชิญผู้อำนวยการโรงพยาบาลกรุงเทพ พิษณุโลก เข้าร่วมประชุมและฝึกซ้อมแผนอพยพและป้องกันระดับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-36
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร เขตจตุจักร
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ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566
เรียน ผู้อำนวยการท่าอากาศยานพิษณุโลก

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ


ด้วย บริษัท ปตท.สผ. สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันในสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกถังใส่รถไฟบรรทุกน้ำมันดิบผ่านประจวบสถับราง กลไกได้เกิดชำรุด เป็นเหตุให้ตู้รถไฟบรรทุกน้ำมันดิบตกราง 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ฝ่ายปฏิบัติการ เข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ ในวันพุธที่ 25 ตุลาคม 2566 โดยมีรายละเอียดกำหนดการดังต่อไปนี้

- เวลา 08:30-10:30 น. ประชุมชี้แจงรายละเอียดขั้นตอนและฝึกซ้อมแผนฯ ตามเหตุการณ์สมมติบึงพระ ณ ห้องประชุมคลังน้ำมันดิบบึงพระ
- เวลา 11:00-12:00 น. ฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ณ คลังน้ำมันดิบบึงพระ เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอกรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ดังถึง คุณภาพิณล สายสออด อีเมล PapimonS@pttep.com หรือสแกนคิวอาร์โค้ดตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ



รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

ผู้ประสานงาน คุณภาพิณล สายสออด
โทรศัพท์ : 0 2537 6136 ตำแหน่ง : PS1/P, PS1/O, PS1/S, PTN/A

Subson G.

หมายเลข / Registration No. 010503000016

เอกสารแนบ 9 หนังสือขอเชิญผู้อำนวยการท่าอากาศยานพิษณุโลก เข้าร่วมประชุมและฝึกซ้อมแผนอพยพและป้องกันระดับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-36 Energy Complex Building A, Floors 19-36
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร เขตจตุจักร กรุงเทพฯ 10900 555/1 Vibhavadi Rangsit Road, Chatchanak Bangkok 10900, THAILAND Tel : +66(0) 2537 4000 Fax : +66(0) 2537 4444 www.pttep.com

ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566

เรียน ผู้กำกับสถานีตำรวจภูธรวังนาคู

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ. สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกส่งน้ำมันดิบบรรทุกไฟรั่วทุกน้ำมันดิบผ่านประแจสับราง กลไกได้เกิดชำรุด เป็นเหตุให้รถบรรทุกน้ำมันดิบบรรทุก 2 คัน และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน


ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ฝ่ายปฏิบัติการ เข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ ในวันพุธที่ 25 ตุลาคม 2566 โดยมีรายละเอียดกำหนดการดังต่อไปนี้

- เวลา 08:30-10:30 น. ประชุมชี้แจงรายละเอียดขั้นตอนและฝึกซ้อมแผนฯ ตามเหตุการณ์สมมติบนโต๊ะ ณ ห้องประชุมคลังน้ำมันดิบบึงพระ
- เวลา 11:00-12:00 น. ฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ณ คลังน้ำมันดิบบึงพระ

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ลงถึง คุณภาวิมล สายสอด อีเมล PaipamonS@pttep.com หรือแนบตัวอาร์โค้ดตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ



รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเขต 1

ผู้ประสานงาน คุณภาวิมล สายสอด
โทรศัพท์ : 0 2537 6136 สำเนาเรียน : PS1/P, PS1/O, PS1/S, PTN/A
Suban G.

รณีนันท์ / Registration No. 012503000016

เอกสารแนบ 10 หนังสือขอเชิญผู้กำกับสถานีตำรวจภูธรวังนาคู เข้าร่วมประชุมและฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-36 Energy Complex Building A, Floors 19-36
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร เขตจตุจักร กรุงเทพฯ 10900 555/1 Vibhavadi Rangsit Road, Chatchanak Bangkok 10900, THAILAND Tel : +66(0) 2537 4000 Fax : +66(0) 2537 4444 www.pttep.com

ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566

เรียน สวัสดิการและคุ้มครองแรงงานจังหวัดพิษณุโลก

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ


ด้วย บริษัท ปตท.สผ. สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกส่งน้ำมันดิบบรรทุกไฟรั่วทุกน้ำมันดิบผ่านประแจสับราง กลไกได้เกิดชำรุด เป็นเหตุให้รถบรรทุกน้ำมันดิบบรรทุก 2 คัน และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันพุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันดิบบึงพระ จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ลงถึง คุณภาวิมล สายสอด อีเมล PaipamonS@pttep.com หรือแนบตัวอาร์โค้ดตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ



รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเขต 1

ผู้ประสานงาน คุณภาวิมล สายสอด
โทรศัพท์ : 0 2537 6136
สำเนาเรียน : PS1/P, PS1/O, PS1/S, PTN/A
Suban G.

รณีนันท์ / Registration No. 012503000016

เอกสารแนบ 11 หนังสือขอเชิญสวัสดิการและคุ้มครองแรงงานจังหวัดพิษณุโลก เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.ส.ม. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-36
555/1 ถนนพหลโยธิน แขวงจตุจักร เขตจตุจักร
กรุงเทพฯ 10000

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ที่ ปตท.ส.ม.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566

เรียน นายกสมาคมอนุรักษ์สภาพแวดล้อมของกลุ่มอุตสาหกรรมน้ำมัน (IESG)

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.ส.ม. สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดับเพลิง เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดับเพลิงพระตำบับึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์ขโมยถังบรรจุผู้รั่วไฟบรรทุกน้ำมันดิบผ่านประแจดับแรง กดโกได้เกิดชำรุด เป็นเหตุให้ผู้รั่วไฟบรรทุกน้ำมันดิบตกวาง 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันพุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันดับเพลิง จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ลงถึง คุณภาพินต สายสออด อีเมล PaipimonS@pttep.com หรือแนบตัวอาร์โค้ด ตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ

รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โรงการเอส 1

ผู้ประสานงาน คุณภาพินต สายสออด
โทรศัพท์ : 0 2537 6136
ตำแหน่ง : PS1/P, PS1/O, PS1/S, PTN/A

ณ วันที่ 10/10/2023 / Registration No. 010502000016

เอกสารแนบ 12 หนังสือขอเชิญนายกสมาคมอนุรักษ์สภาพแวดล้อมของกลุ่มอุตสาหกรรมน้ำมัน (IESG) เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.ส.ม. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-36
555/1 ถนนพหลโยธิน แขวงจตุจักร เขตจตุจักร
กรุงเทพฯ 10000

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ที่ ปตท.ส.ม.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566

เรียน ผู้แทน PTT Group Transportation Safety Taskforce

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.ส.ม. สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดับเพลิง เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดับเพลิงพระตำบับึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์ขโมยถังบรรจุผู้รั่วไฟบรรทุกน้ำมันดิบผ่านประแจดับแรง กดโกได้เกิดชำรุด เป็นเหตุให้ผู้รั่วไฟบรรทุกน้ำมันดิบตกวาง 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันพุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันดับเพลิง จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ลงถึง คุณภาพินต สายสออด อีเมล PaipimonS@pttep.com หรือแนบตัวอาร์โค้ด ตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ

รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โรงการเอส 1

ผู้ประสานงาน คุณภาพินต สายสออด
โทรศัพท์ : 0 2537 6136
ตำแหน่ง : PS1/P, PS1/O, PS1/S, PTN/A

ณ วันที่ 10/10/2023 / Registration No. 010502000016

เอกสารแนบ 13 หนังสือขอเชิญผู้แทน PTT Group Transportation Safety Taskforce เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและปฏิบัติการ อาคาร A ชั้น 19-36
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร กรุงเทพฯ 10900

Energy Complex Building A, Floors 19-36
555/1 Vibhavadi Rangsit Road, Chatsuchak
Bangkok 10900, THAILAND

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ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566

เรียน ท่านผู้บังคับบัญชา

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ.สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกนำน้ำมันดิบมาผ่านประแจสลักราง กลไกได้เกิดชำรุด เป็นเหตุให้รถบรรทุกนำน้ำมันดิบบรรทุก 2 คัน และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันพุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันดิบบึงพระ จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอกรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ดังถึง คุณภาพิฒล สายสอด อีเมล Paapimons@pttep.com หรือสแกนคิวอาร์โค้ด ตามเอกสารแนบ ภายใต้วันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ

[Redacted Signature]

รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

ผู้ประสานงาน คุณภาพิฒล สายสอด
โทรศัพท์ : 0 2537 6136
สำเนาเรียน : PS1/P, PS1/O, PS1/S, PTN/A
Bumun G.

การขึ้นทะเบียน / Registration No. 0105023005018

เอกสารแนบ 14 หนังสือขอเชิญท่านผู้บังคับบัญชา เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและปฏิบัติการ อาคาร A ชั้น 19-36
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร กรุงเทพฯ 10900

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ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566

เรียน หัวหน้าคลังน้ำมัน ปตท.พิษณุโลก

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ.สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกนำน้ำมันดิบมาผ่านประแจสลักราง กลไกได้เกิดชำรุด เป็นเหตุให้รถบรรทุกนำน้ำมันดิบบรรทุก 2 คัน และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันพุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันดิบบึงพระ จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอกรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ดังถึง คุณภาพิฒล สายสอด อีเมล Paapimons@pttep.com หรือสแกนคิวอาร์โค้ด ตามเอกสารแนบ ภายใต้วันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ

[Redacted Signature]

รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

ผู้ประสานงาน คุณภาพิฒล สายสอด
โทรศัพท์ : 0 2537 6136
สำเนาเรียน : PS1/P, PS1/O, PS1/S, PTN/A
Bumun G.

การขึ้นทะเบียน / Registration No. 0105023005018

เอกสารแนบ 15 หนังสือขอเชิญหัวหน้าคลังน้ำมัน ปตท. พิษณุโลก เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและปฏิบัติการ อากาศ A ชั้น 19-38 Energy Complex Building A, Floors 19-38 Tel : +66(0) 2537 4000
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร เขตจตุจักร Bangkok 10900, THAILAND Fax : +66(0) 2537 4444
กรุงเทพฯ 10900 www.pttep.com

ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566
เรียน หัวหน้าคลังน้ำมัน พีทีจี พิษณุโลก

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ. สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถลากจูงตู้รถไฟบรรทุกน้ำมันดิบผ่านประแจสลักราง กลไกได้เกิดชำรุด เป็นเหตุให้ตู้รถไฟบรรทุกน้ำมันดิบตกราง 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันพุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันดิบบึงพระ จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ดังถึง คุณภาพิมล สายสอด อีเมล Paipimons@pttep.com หรือส่งแกนคิวอาร์โค้ด ตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ

รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

ผู้ประสานงาน คุณภาพิมล สายสอด
โทรศัพท์ : 0 2537 6136
ตำแหน่ง : PS1/P, PS1/O, PS1/S, PTN/A
Subson D.

กรณีเอกสาร / Registration No. 0105022000018

เอกสารแนบ 16 หนังสือขอเชิญหัวหน้าคลังน้ำมัน พีทีจี พิษณุโลก เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและปฏิบัติการ อากาศ A ชั้น 19-38 Energy Complex Building A, Floors 19-38 Tel : +66(0) 2537 4000
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร เขตจตุจักร Bangkok 10900, THAILAND Fax : +66(0) 2537 4444
กรุงเทพฯ 10900 www.pttep.com

ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566
เรียน ผู้ใหญ่บ้านหมู่ที่ 2 ตำบลบึงพระ

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ. สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถลากจูงตู้รถไฟบรรทุกน้ำมันดิบผ่านประแจสลักราง กลไกได้เกิดชำรุด เป็นเหตุให้ตู้รถไฟบรรทุกน้ำมันดิบตกราง 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันพุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันดิบบึงพระ จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ดังถึง คุณภาพิมล สายสอด อีเมล Paipimons@pttep.com หรือส่งแกนคิวอาร์โค้ด ตามเอกสารดังแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ

รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

ผู้ประสานงาน คุณภาพิมล สายสอด
โทรศัพท์ : 0 2537 6136
ตำแหน่ง : PS1/P, PS1/O, PS1/S, PTN/A
Subson D.

กรณีเอกสาร / Registration No. 0105022000018

เอกสารแนบ 17 หนังสือขอเชิญผู้ใหญ่บ้านหมู่ที่ 2 ตำบลบึงพระ เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

PTTEP บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-36 Energy Complex Building A, Floors 19-36 Tel : +66(0) 2537 4000
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร เขตจตุจักร 10900 Bangkok 10900, THAILAND Fax : +66(0) 2537 4444
www.pttep.com

ที่ ปตท.สผ.สยาม 13247/00-11246/2023
5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566
เรียน ผู้นำชุมชน หมู่บ้านวังทองธานี

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ.สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และอุทัยธานี ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่อู่ต้นน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกผู้รั่วไหลบรรทุกน้ำมันดิบผ่านประแจสลักราง กลไกเกิดชำรุด เป็นเหตุให้ผู้รั่วไหลบรรทุกน้ำมันดิบตกจาก 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันพุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันดิบบึงพระ จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ส่งถึง คุณภาพิณต สายสออด อีเมล Papimon.S@pttep.com หรือแทนคิวอาร์โค้ด ตามเอกสารแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ

รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเขต 1

ผู้ประสานงาน คุณภาพิณต สายสออด
โทรศัพท์ : 0 2537 6136
สำเนาเรียน : PS1/P, PS1/O, PS1/S, PTN/A
Subson G.

พ.ร.บ.ข้อมูลข่าวสาร พ.ศ. 2540 / Registration No. 0105533002016

เอกสารแนบ 18 หนังสือขอเชิญผู้นำชุมชนหมู่บ้านวังทองธานี เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

PTTEP บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-36 Energy Complex Building A, Floors 19-36 Tel : +66(0) 2537 4000
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร เขตจตุจักร 10900 Bangkok 10900, THAILAND Fax : +66(0) 2537 4444
www.pttep.com

ที่ ปตท.สผ.สยาม 13247/00-11246/2023
5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566
เรียน พนักงานจังหวัดพิษณุโลก

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ.สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และอุทัยธานี ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่อู่ต้นน้ำมันดิบบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกผู้รั่วไหลบรรทุกน้ำมันดิบผ่านประแจสลักราง กลไกเกิดชำรุด เป็นเหตุให้ผู้รั่วไหลบรรทุกน้ำมันดิบตกจาก 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันพุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันดิบบึงพระ จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ส่งถึง คุณภาพิณต สายสออด อีเมล Papimon.S@pttep.com หรือแทนคิวอาร์โค้ด ตามเอกสารแนบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ

รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเขต 1

ผู้ประสานงาน คุณภาพิณต สายสออด
โทรศัพท์ : 0 2537 6136
สำเนาเรียน : PS1/P, PS1/O, PS1/S, PTN/A
Subson G.

พ.ร.บ.ข้อมูลข่าวสาร พ.ศ. 2540 / Registration No. 0105533002016

เอกสารแนบ 19 หนังสือขอเชิญพนักงานจังหวัดพิษณุโลก เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

ภาคผนวก 3 กรอบประเมินเชิงประจักษ์

บริษัท ปตท.สผ. สยาม จำกัด
PTTEP Siam Limited
A Company of PTTEP Group

ศูนย์ควบคุมและป้องกันภัย อาคาร A ชั้น 19-38
555/1 ถนนวิภาวดีรังสิต แขวงจตุจักร เขตจตุจักร
กรุงเทพฯ 10900

Energy Complex Building A, Floors 19-38
555/1 Vibhavadi Rangsit Road, Chatchuk
Bangkok 10900, THAILAND

Tel : +66(0) 2537 4000
Fax : +66(0) 2537 4444
www.pttep.com

ที่ ปตท.สผ.สยาม 13247/00-11246/2023

5 ตุลาคม 2566

เรื่อง ขอเชิญร่วมสังเกตการณ์การฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566
เรียน หัวหน้าสถานีรถไฟบึงพระ

สิ่งที่ส่งมาด้วย 1. กำหนดการและสถานการณ์จำลองการฝึกซ้อมดับเพลิงและอพยพหนีไฟ
2. แบบตอบรับเข้าร่วมประชุมและฝึกซ้อมดับเพลิงและอพยพหนีไฟ

ด้วย บริษัท ปตท.สผ. สยาม จำกัด บริษัท ในกลุ่ม บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน) ผู้ดำเนินการสำรวจ ผลิตและพัฒนาปิโตรเลียมจากแหล่งน้ำมันสิริกิติ์ ครอบคลุมพื้นที่จังหวัดพิษณุโลก กำแพงเพชร และสุโขทัย ซึ่งครอบคลุมงานปฏิบัติการขนส่งน้ำมันดิบจากสถานีผลิตลานกระบือสู่คลังน้ำมันบึงพระ เพื่อขนส่งทางรถไฟไปยังโรงกลั่นน้ำมันบางจาก และโรงกลั่นน้ำมันไทยออยล์ มีแผนดำเนินการฝึกซ้อมดับเพลิงและอพยพหนีไฟจังหวัดพิษณุโลก ประจำปี 2566 ณ คลังน้ำมันบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก โดยสมมติสถานการณ์รถบรรทุกส่งน้ำมันดิบมาขึ้นที่ลานประแจสลับราง ใกล้เคียงเกิดชำรุด เป็นเหตุให้รถบรรทุกน้ำมันดิบตกจาก 2 ตู้ และเกิดเพลิงลุกไหม้ มีผู้ได้รับบาดเจ็บ 1 ท่าน

ในการนี้ บริษัทฯ ขอเชิญท่านและเจ้าหน้าที่ จำนวน 1-2 ท่าน เข้าร่วมสังเกตการณ์การฝึกซ้อมตามเหตุการณ์สมมติภาคสนาม ในวันที่พุธที่ 25 ตุลาคม 2566 เวลา 11:00-12:00 น. ณ คลังน้ำมันบึงพระ จ.พิษณุโลก

เพื่อจัดเตรียมความพร้อมในการฝึกซ้อมแผนฯ ขอความกรุณากรอรายละเอียดในแบบตอบรับยืนยันการเข้าร่วม ดังถึง คุณภาพิณต สายสออด อีเมล Paiporn.S@pttep.com หรือสแกนคิวอาร์โค้ด ตามเอกสารแนบแบบ ภายในวันศุกร์ที่ 20 ตุลาคม 2566

จึงเรียนมาเพื่อโปรดพิจารณาสนับสนุนและขอขอบคุณมา ณ โอกาสนี้

ขอแสดงความนับถือ

รักษาการ ผู้จัดการอาวุโส ฝ่ายปฏิบัติการผลิต โครงการเอส 1

ผู้ประสานงาน คุณภาพิณต สายสออด
โทรศัพท์ : 0 2537 6136
สำเนาเรียน : PS1/P, PS1/O, PS1/S, PTN/A

การันตีด้วย / Registration No: 0105003000018

เอกสารแนบ 20 หนังสือขอเชิญหัวหน้าสถานีรถไฟบึงพระ เข้าร่วมสังเกตการณ์การฝึกซ้อมแผนอพยพและป้องกันระงับอัคคีภัยในพื้นที่จังหวัดพิษณุโลก ประจำปี 2566

กรอบการประเมินผลเชิงประจักษ์ 7 ด้าน

การฝึกซ้อมแผนอพยพและแผนป้องกันระงับอัคคีภัยประจำปี 2566

บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน)
ณ. คลังน้ำมันบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก

1. ด้านการรักษาพยาบาล

ประเด็นประเมิน	ผลการประเมิน	ข้อเสนอแนะเพิ่มเติม
1.1 การสื่อสารและการรับแจ้งเหตุ (รวดเร็ว/ครบถ้วน/ข้อมูลถูกต้อง/น่าเชื่อถือ)	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
1.2 การคัดกรอง/คัดแยก ผู้ประสบภัยตามระดับความรุนแรง ณ จุดเกิดเหตุ (เสียชีวิต/บาดเจ็บเล็กน้อย/บาดเจ็บปานกลาง/บาดเจ็บรุนแรง)	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	
1.3 การจัดเตรียมความพร้อมในการรักษาพยาบาลเบื้องต้น (สถานที่/ทรัพยากร/ยานพาหนะ/ทีม/เครื่องมือ/อุปกรณ์)	<input checked="" type="radio"/> เกือบพอ <input type="radio"/> ไม่เพียงพอ	
1.4 การปฏิบัติการในการรักษาพยาบาลเบื้องต้นของทีมฉุกเฉิน	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
1.5 การประสานงานการปฏิบัติงานระหว่างเจ้าหน้าที่	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
1.6 จุดจอดรถพยาบาล จุดนำส่ง/รับรถ เสิ่นทางเดินรถพยาบาล	<input checked="" type="radio"/> สะดวก <input type="radio"/> ไม่เหมาะสม	
1.7 ระบบลำเลียง ขนย้าย และการนำส่งผู้ประสบภัย (ถูกต้อง/เหมาะสม/วิธีการ/การนำส่ง/ส่งสถานพยาบาล/การดูแลระหว่างนำส่ง)	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่สะดวก	
1.8 การดูแลผู้บาดเจ็บของทีมงานพยาบาล ทีมอาสาสมัคร (การปฐมพยาบาล/การช่วยฟื้นคืนชีพ/การดูแลและการเคลื่อนย้ายผู้บาดเจ็บ/การช่วยเหลือ/การตามรถฉุกเฉิน/รถไฟไหม้)	<input checked="" type="radio"/> ถูกต้อง <input type="radio"/> ไม่ถูกต้อง	
19. อื่นๆ		

* ทีมรถพยาบาลจาก คลังน้ำมัน 11.09 น. ช่วงเปลี่ยนรถคันแรก
* ทีมรถพยาบาลจาก รพ. กรุงเทพ 11.15 น. รถมาช้า วนรอบ 11.22 น. 3 มุ่งมาที่จุดเกิดเหตุ
โรงพยาบาล

เอกสารแนบ 21 ด้านการรักษาพยาบาล

กรอบการประเมินผลเชิงประจักษ์ 7 ด้าน

การฝึกซ้อมแผนอพยพและแผนป้องกันระดับอภิศักดิ์ประจำปี 2566

บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน)

ณ. คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก

1.ด้านการรักษาพยาบาล

แผน (ปี 2566) 2.

ประเด็นประเมิน	ผลการประเมิน	ข้อเสนอแนะเพิ่มเติม
1.1 การสื่อสารและการรับแจ้งเหตุ (รวดเร็วชัดเจน)	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
1.2 การคัดกรองคัดแยก ผู้ประสบภัยตามระดับความรุนแรง ณ จุดเกิดเหตุ (เสียชีวิตบาดเจ็บเล็กน้อยบาดเจ็บปานกลาง/บาดเจ็บรุนแรง)	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	มีความเหมาะสม 03/10/2566
1.3 การจัดเตรียมความพร้อมในการรักษาพยาบาลเบื้องต้น (สถานที่แพทย์ พยาบาลเจ้าหน้าที่ที่เครื่องมืออุปกรณ์)	<input checked="" type="radio"/> เพียงพอ <input type="radio"/> ไม่เพียงพอ	จัดเตรียมความพร้อมในการรักษาพยาบาลเบื้องต้น ณ สถานี ปตท. คลังน้ำมันดิบบึงพระ 03/10/2566 (ณ สถานีน้ำมันดิบบึงพระ จังหวัดพิษณุโลก)
1.4 การปฏิบัติการในการรักษาพยาบาลเบื้องต้นของทีมฉุกเฉิน	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
1.5 การประสานงานการปฏิบัติงานระหว่างเจ้าหน้าที่	<input type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
1.6 จุดจอดรถพยาบาล จุดนำส่งขึ้นรถ เส้นทางเดินรถพยาบาล	<input type="radio"/> สะดวก <input type="radio"/> ไม่เหมาะสม	
1.7 ระบบสื่อสาร วิทยุ และการนำส่งผู้ประสบภัย (ถูกต้องตามวิธีการการนำส่งถึงสถานพยาบาล/การดูแลระหว่างนำส่ง)	<input type="radio"/> เหมาะสม <input type="radio"/> ไม่สะดวก	
1.8 การดูแลบาดเจ็บของทีมงานแพทย์ พยาบาล ทีมอาสาสมัคร (การปฐมพยาบาล/การช่วยฟื้นคืนชีพ/การออกและการเคลื่อนย้ายผู้บาดเจ็บ/การห้ามเลือด/การตามกระดูก/แผลไหม้/อื่น ๆ)	<input type="radio"/> ถูกต้อง <input type="radio"/> ไม่ถูกต้อง	
19. อื่นๆ		

ณ. คลังน้ำมันดิบบึงพระ, BPR → first Aid 11:04 → Hospital 11:29

เอกสารแนบ 22 ด้านการรักษาพยาบาล

กรอบการประเมินผลเชิงประจักษ์ 7 ด้าน

การฝึกซ้อมแผนอพยพและแผนป้องกันระดับอภิศักดิ์ประจำปี 2566

บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน)

ณ. คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก

2.ด้านการเผชิญเหตุ

ประเด็นประเมิน	ผลการประเมิน	ข้อเสนอแนะเพิ่มเติม
2.1 การรับแจ้งเหตุ การประสาน การร้องขอคำสั่งสนับสนุน (รวดเร็วชัดเจน)	<input type="radio"/> รวดเร็วชัดเจน <input checked="" type="radio"/> ลำช้า/ไม่ชัดเจน	การร้องขอคำสั่งสนับสนุนจากผู้เกี่ยวข้อง ไม่ชัดเจน OSC จากสถานีรถดับเพลิง
2.2 ระบบการบัญชาการเหตุการณ์ (การบัญชาการเหตุการณ์ในแต่ละระดับชั้น)	<input checked="" type="radio"/> ถูกต้อง <input type="radio"/> ไม่ถูกต้อง	
2.3 ปัญหาการเหตุการณ์มีสัญญาณบ่งบอกที่ชัดเจน	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	
2.4 การรายงานตัวต่อผู้บัญชาการเหตุการณ์เพื่อรองรับการสั่งการ	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	
2.5 การประเมินสถานการณ์ ณ จุดเกิดเหตุ (ความปลอดภัย/ตั้งจำเป็นในการกู้ภัย-อุปกรณ์ผู้ถือ การวางตำแหน่งพหุและอุปกรณ์ กำลังคน/การประเมินความเสี่ยงแวดล้อม)	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	จาก: ช่วงแจ้งสถานการณ์ ณ จุดเกิดเหตุ ลำช้า สะท้อนการตั้งทีมวางแนวตั้งพื้นที่เสี่ยง อาจใช้ทีมอื่นจากหน่วยอื่น
2.6 การกำหนดพื้นที่	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	กับชุมชนรอบข้าง
2.7 ความรวดเร็วในการเคลื่อนย้ายผู้ประสบภัย	<input checked="" type="radio"/> รวดเร็ว <input type="radio"/> ลำช้า	
2.8 วิธีปฏิบัติการช่วยเหลือผู้ประสบภัยโดยใช้เครื่องมือ อุปกรณ์ รวมทั้งกำลังพล ทีมแพทย์ พยาบาล ทีมกู้ชีพ กู้ภัย ฯลฯ	<input checked="" type="radio"/> ถูกต้อง <input type="radio"/> ไม่ถูกต้อง	
2.9 และอื่นๆ		จาก: ทรัพยากรปฏิบัติงานในสถานการณ์จริง ปตท. ภาณุ จังหวัดพิษณุโลก


เอกสารแนบ 23 ด้านการเผชิญเหตุ

กรอบการประเมินผลเชิงประจักษ์ 7 ด้าน

การฝึกซ้อมแผนอพยพและแผนป้องกันรับอัคคีภัยประจำปี 2566

บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน)

ณ. คลังน้ำมันดิบปิโตรเว ตำบลบึงพระ อำเภอเมือง จังหวัดพินูโลก




2.ด้านการเผชิญเหตุ

ประเด็นประเมิน	ผลการประเมิน	ข้อเสนอแนะเพิ่มเติม
2.1 การรับแจ้งเหตุ การประสาน การร้องขอกำลังสนับสนุน (รวดเร็วชัดเจน)	<input checked="" type="checkbox"/> รวดเร็วชัดเจน <input type="checkbox"/> ช้า/ไม่ชัดเจน	
2.2 ระบบบัญชาการเหตุการณ์ (การบัญชาการเหตุการณ์ในแต่ละระดับชั้น)	<input checked="" type="checkbox"/> ถูกต้อง <input type="checkbox"/> ไม่ถูกต้อง	
2.3 บัญชีรายการเหตุการณ์มีสัญลักษณ์บ่งบอกที่ชัดเจน	<input checked="" type="checkbox"/> มี <input type="checkbox"/> ไม่มี	
2.4 การรายงานตัวต่อผู้บัญชาการเหตุการณ์เพื่อขอรับการสั่งการ	<input checked="" type="checkbox"/> มี <input type="checkbox"/> ไม่มี	
2.5 การประเมินสถานการณ์ ณ จุดเกิดเหตุ (ความปลอดภัย / สิ่งจำเป็นในการกู้ภัย-อุปกรณ์กู้ภัย การวางตำแหน่งพาหนะ อุปกรณ์ กำลังคนการประเมินด้านสิ่งแวดล้อม)	<input checked="" type="checkbox"/> มี <input type="checkbox"/> ไม่มี	
2.6 การกำหนดพื้นที่	<input checked="" type="checkbox"/> เหมาะสม <input type="checkbox"/> ไม่เหมาะสม	
2.7 ความรวดเร็วในการเคลื่อนย้ายผู้ประสบภัย	<input checked="" type="checkbox"/> รวดเร็ว <input type="checkbox"/> ช้า	
2.8 วิธีปฏิบัติการช่วยเหลือผู้ประสบภัยโดยใช้เครื่องมือ อุปกรณ์ รวมถึงกำลังพล ทีมแพทย์ พยาบาล ทีมกู้ชีพ กู้ภัย ฯลฯ	<input checked="" type="checkbox"/> ถูกต้อง <input type="checkbox"/> ไม่ถูกต้อง	
2.9 และอื่นๆ		

การประเมินเรื่อง สิ่งตกค้าง
 - ตรวจแจ้ง ว่า มีถังแก๊ส ที่ชำรุด / หมด
 15 ลูกกลิ้ง 2 ลูกกลิ้ง 1 ลูกกลิ้ง 1 ลูกกลิ้ง
 1 ลูกกลิ้ง 1 ลูกกลิ้ง 1 ลูกกลิ้ง 1 ลูกกลิ้ง
 1 ลูกกลิ้ง 1 ลูกกลิ้ง 1 ลูกกลิ้ง 1 ลูกกลิ้ง
 1 ลูกกลิ้ง 1 ลูกกลิ้ง 1 ลูกกลิ้ง 1 ลูกกลิ้ง

เอกสารแนบ 25 ด้านการเผชิญเหตุ




กรอบการประเมินผลเชิงประจักษ์ 7 ด้าน
 การฝึกซ้อมแผนอพยพและแผนป้องกันระดับพื้นที่ประจำปี 2566
 บริษัทปตท.สำรวจและผลิตปิโตรเลียมจำกัด (มหาชน)
 ณ. คลังน้ำมันดิบปิระ ต่าบปึงพระ อำเภอเมือง จังหวัดพิษณุโลก

4.ด้านการสื่อสาร

ประเด็นประเมิน	ผลการประเมิน	ข้อเสนอแนะเพิ่มเติม
4.1 ระบบการติดต่อสื่อสาร		
- รูปแบบการติดต่อสื่อสาร	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	โดยใช้ <u>วิทยุสื่อสาร / โทรศัพท์</u> เพราะ
- อุปกรณ์ที่ใช้ในการสื่อสาร	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	โดยใช้ <u>วิทยุสื่อสาร</u> เพราะ
- เครือข่ายหลักและเครือข่ายสำรอง	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	
- ความสามารถในการจัดช่องทางสื่อสารที่สำคัญต่อการสนับสนุนการปฏิบัติงานตอนใต้ทะเลจากจีน	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
4.2 การรับส่งข่าวสารข้อมูลในการกิจต่างกับศูนย์บัญชาการ	<input checked="" type="radio"/> จัดเจน/ถูกต้อง <input type="radio"/> ไม่ชัดเจน / ไม่ถูกต้อง	
4.3 การประสานการปฏิบัติในการส่งข้อมูลข่าวสารแก่หน่วยงาน และเครือข่ายต่างๆ	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	
4.4 และอื่นๆ		

เอกสารแนบ 26 ด้านการสื่อสาร



กรอบการประเมินผลเชิงประจักษ์ 7 ด้าน
 การฝึกซ้อมแผนอพยพและแผนป้องกันระดับพื้นที่ประจำปี 2566
 บริษัทปตท.สำรวจและผลิตปิโตรเลียมจำกัด (มหาชน)
 ณ. คลังน้ำมันดิบปิระ ต่าบปึงพระ อำเภอเมือง จังหวัดพิษณุโลก

4.ด้านการสื่อสาร

ประเด็นประเมิน	ผลการประเมิน	ข้อเสนอแนะเพิ่มเติม
4.1 ระบบการติดต่อสื่อสาร		
- รูปแบบการติดต่อสื่อสาร	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	โดยใช้
- อุปกรณ์ที่ใช้ในการสื่อสาร	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	โดยใช้
- เครือข่ายหลักและเครือข่ายสำรอง	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	
- ความสามารถในการจัดช่องทางสื่อสารที่สำคัญต่อการสนับสนุนการปฏิบัติงานตอนใต้ทะเลจากจีน	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
4.2 การรับส่งข่าวสารข้อมูลในการกิจต่างกับศูนย์บัญชาการ	<input checked="" type="radio"/> จัดเจน/ถูกต้อง <input type="radio"/> ไม่ชัดเจน / ไม่ถูกต้อง	
4.3 การประสานการปฏิบัติในการส่งข้อมูลข่าวสารแก่หน่วยงาน และเครือข่ายต่างๆ	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	
4.4 และอื่นๆ		

เอกสารแนบ 27 ด้านการสื่อสาร

๗. คลังน้ำมันดิบปึงพระ ตำบลปึงพระ อำเภอเมือง จังหวัดพิษณุโลก

ประเด็นประเมิน	ผลการประเมิน	ข้อเสนอแนะเพิ่มเติม
5.1 การแจ้งเตือนภัย	<input checked="" type="radio"/> วาดเร็วชัดเจน <input type="radio"/> ลำช้า ไม่ชัดเจน	
5.2 มีการวางแผนการอพยพผู้ประสบภัยออกจากพื้นที่ประสบภัย	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	
- การกำหนดเส้นทางอพยพ	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
- มีการจัดกำลังพลและผู้นำการอพยพ	<input checked="" type="radio"/> มี <input type="radio"/> ไม่มี	
- เครื่องมือ อุปกรณ์ ยานพาหนะที่ใช้ในการอพยพ	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
- สถานที่รองรับรับการอพยพ	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
5.3 กระบวนการลงทะเบียนผู้อพยพ	<input checked="" type="radio"/> เหมาะสม <input type="radio"/> ไม่เหมาะสม	
5.4 และอื่นๆ		

၇) ဓာတ်ငွေ့ကွဲပြားမှု

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การฝึกซ้อมแผนอพยพและแผนป้องกันระงับอัคคีภัยประจำปี 2566
บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน)
ณ. คลังน้ำมันดิบบึงพระ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก

ประเด็นประเมิน	ผลการประเมิน	ข้อเสนอแนะเพิ่มเติม
6.1 การจัดการการจราจร	<input type="radio"/> เหมาะสม รวดเร็ว <input checked="" type="radio"/> ไม่เหมาะสม	การปรับปรุง
6.2 การควบคุมสิ่งขุ่น การเก็บกักอุปติเหตุซ้ำซ้อน	<input checked="" type="radio"/> มีเหมาะสม <input type="radio"/> ไม่มี	11 สิ่งไม่ถูกต้อง
6.3 การดูแลความปลอดภัยในชีวิต และทรัพย์สินบริเวณพื้นที่เกิดภัย	<input checked="" type="radio"/> มีเหมาะสม <input type="radio"/> ไม่มี	พบภัยบริเวณถนน
6.4 และอื่นๆ		

เอกสารแนบ 30 ด้านการรักษาสภาพสงบเรียบร้อยและจรรยาบรรณ

การฝึกซ้อมแผนอพยพและแผนป้องกันระงับอัคคีภัยประจำปี 2566
บริษัท ปตท.สำรวจและผลิตปิโตรเลียม จำกัด (มหาชน)
ณ. คลังน้ำมันดิบปิระหวะ ตำบลบึงพระ อำเภอเมือง จังหวัดพิษณุโลก

ประเด็นประเมิน	ผลการประเมิน	ข้อเสนอแนะเพิ่มเติม
6.1 การจัดระบบการวางผัง	<input checked="" type="radio"/> เหมาะสม รวดเร็ว <input type="radio"/> ไม่เหมาะสม	
6.2 การควบคุมผังเมือง การป้องกันภูมิทัศน์ให้ชัดเจน	<input checked="" type="radio"/> มีเหมาะสม <input type="radio"/> ไม่มี	
6.3 การดูแลความปลอดภัยในชีวิต และทรัพย์สินบริเวณที่ก่อสร้าง	<input checked="" type="radio"/> มีเหมาะสม <input type="radio"/> ไม่มี	
6.4 ภาระอื่นๆ		

၂၀၁၆ ခုနှစ် ဇန်နဝါရီလ ၁ ရက်နေ့
 မြန်မာနိုင်ငံတော် အစိုးရတော်
 ဝန်ကြီးရုံး၊ ဝန်ကြီးရုံးအတွင်း
 ဝန်ကြီးရုံးအတွင်း

เอกสารแนบ 30 ด้านการรักษาสภาพสงบเรียบร้อยและจรรยาบรรณ

องค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

ให้ใส่เครื่องหมาย / ลงในช่องระดับความเหมาะสม/สอดคล้อง ตามความเห็นของท่าน

ขั้นตอน	ระดับความเหมาะสม/สอดคล้อง				ข้อคิดเห็นเพิ่มเติม
	ดี มาก 4	ดี 3	พอใช้ 2	ควร ปรับปรุง 1	
การฝึกภาคปฏิบัติภาคสนาม (FTX)					
1. การควบคุม สั่งการ ของผู้บัญชาการเหตุการณ์แต่ละระดับ		✓			
2. การจัดสถานการณ์จำลอง พื้นที่ภัยพิบัติภัย ภัยธรรมชาติ และผู้ประสบภัย	✓				
3. ความเข้าใจของเจ้าหน้าที่แต่ละหน่วยในการปฏิบัติงาน		✓			
4. อุปกรณ์เครื่องมือเครื่องใช้ที่นำมาใช้ในการฝึกซ้อมฯ	✓				
5. ระบบการติดต่อสื่อสารและความถูกต้องของข้อมูลข่าวสาร		✓			
6. ความคล่องตัวและรวดเร็วในการปฏิบัติงานของชุดปฏิบัติการต่างๆ		✓			
7. การให้ความร่วมมือของทุกภาคส่วนที่ร่วมฝึกซ้อมแผนฯ	✓				
8. การจัดระบบจราจรในที่เกิดเหตุ	✓				
9. การบรรลุวัตถุประสงค์ของการฝึกซ้อมแผนฯ	✓				

ที่มา: จากหนังสือคู่มือการปฏิบัติงานตามกระบวนการฝึกซ้อมแผนฯ สำนักนโยบายป้องกันและบรรเทาสาธารณภัย กรมป้องกันและบรรเทาสาธารณภัย กระทรวงมหาดไทย สิงหาคม 2553

เอกสารแนบ 31 แบบประเมินองค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

องค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

ให้ใส่เครื่องหมาย / ลงในช่องระดับความเหมาะสม/สอดคล้อง ตามความเห็นของท่าน

ขั้นตอน	ระดับความเหมาะสม/สอดคล้อง				ข้อคิดเห็นเพิ่มเติม
	ดี มาก 4	ดี 3	พอใช้ 2	ควร ปรับปรุง 1	
การฝึกภาคปฏิบัติภาคสนาม (FTX)					
1. การควบคุม สั่งการ ของผู้บัญชาการเหตุการณ์แต่ละระดับ					
2. การจัดสถานการณ์จำลอง พื้นที่ภัยพิบัติภัย ภัยธรรมชาติ และผู้ประสบภัย		✓			
3. ความเข้าใจของเจ้าหน้าที่แต่ละหน่วยในการปฏิบัติงาน		✓			
4. อุปกรณ์เครื่องมือเครื่องใช้ที่นำมาใช้ในการฝึกซ้อมฯ	✓				
5. ระบบการติดต่อสื่อสารและความถูกต้องของข้อมูลข่าวสาร		✓			
6. ความคล่องตัวและรวดเร็วในการปฏิบัติงานของชุดปฏิบัติการต่างๆ	✓				
7. การให้ความร่วมมือของทุกภาคส่วนที่ร่วมฝึกซ้อมแผนฯ	✓				
8. การจัดระบบจราจรในที่เกิดเหตุ		✓			
9. การบรรลุวัตถุประสงค์ของการฝึกซ้อมแผนฯ		✓			

ที่มา: จากหนังสือคู่มือการปฏิบัติงานตามกระบวนการฝึกซ้อมแผนฯ สำนักนโยบายป้องกันและบรรเทาสาธารณภัย กรมป้องกันและบรรเทาสาธารณภัย กระทรวงมหาดไทย สิงหาคม 2553

เอกสารแนบ 32 แบบประเมินองค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

องค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

ให้ใส่เครื่องหมาย / ลงในช่องระดับความเหมาะสม/สอดคล้อง ตามความเห็นของท่าน

ขั้นตอน	ระดับความเหมาะสม/สอดคล้อง				ข้อคิดเห็นเพิ่มเติม
	ดี มาก 4	ดี 3	พอใช้ 2	ควร ปรับปรุง 1	
การฝึกภาคปฏิบัติภาคสนาม (FTX)					
1. การควบคุม สั่งการ ของผู้บัญชาการเหตุการณ์แต่ละระดับ		✓			
2. การจัดสถานการณ์จำลอง พื้นที่เกิดภัย ที่ตั้งศูนย์บัญชาการเหตุการณ์ และผู้ประสบภัย		✓			
3. ความเข้าใจของเจ้าหน้าที่แต่ละหน่วยในการปฏิบัติงาน		✓			
4. อุปกรณ์เครื่องมือเครื่องใช้ที่นำมาใช้ในการฝึกซ้อมฯ		✓			
5. ระบบการติดต่อสื่อสารและความถูกต้องของข้อมูลข่าวสาร		✓			
6. ความคล่องตัวและรวดเร็วในการปฏิบัติงานของชุดปฏิบัติการต่างๆ		✓			- สัทธิพร จาภา ปตท. ก่อนเข้าร่วม
7. การให้ความร่วมมือของทุกภาคส่วนที่ร่วมฝึกซ้อมแผนฯ	✓				
8. การจัดระบบจราจรในที่เกิดเหตุ	✓				
9. การบรรจรถฉุกเฉินส่งต่อการฝึกซ้อมแผนฯ		✓			

ที่มา: จากหนังสือคู่มือการปฏิบัติงานตามกระบวนการฝึกซ้อมแผนฯ สำนักนโยบายป้องกันและบรรเทาสาธารณภัย กรมป้องกันและบรรเทาสาธารณภัย กระทรวงมหาดไทย สิงหาคม 2553

เอกสารแนบ 33 แบบประเมินองค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

องค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

ให้ใส่เครื่องหมาย / ลงในช่องระดับความเหมาะสม/สอดคล้อง ตามความเห็นของท่าน

ขั้นตอน	ระดับความเหมาะสม/สอดคล้อง				ข้อคิดเห็นเพิ่มเติม
	ดี มาก 4	ดี 3	พอใช้ 2	ควร ปรับปรุง 1	
การฝึกภาคปฏิบัติภาคสนาม (FTX)					
1. การควบคุม สั่งการ ของผู้บัญชาการเหตุการณ์แต่ละระดับ		/			
2. การจัดสถานการณ์จำลอง พื้นที่เกิดภัย ที่ตั้งศูนย์บัญชาการเหตุการณ์ และผู้ประสบภัย			/		
3. ความเข้าใจของเจ้าหน้าที่แต่ละหน่วยในการปฏิบัติงาน		/			
4. อุปกรณ์เครื่องมือเครื่องใช้ที่นำมาใช้ในการฝึกซ้อมฯ		/			
5. ระบบการติดต่อสื่อสารและความถูกต้องของข้อมูลข่าวสาร		/			
6. ความคล่องตัวและรวดเร็วในการปฏิบัติงานของชุดปฏิบัติการต่างๆ		/			
7. การให้ความร่วมมือของทุกภาคส่วนที่ร่วมฝึกซ้อมแผนฯ		/			
8. การจัดระบบจราจรในที่เกิดเหตุ		/			
9. การบรรจรถฉุกเฉินส่งต่อการฝึกซ้อมแผนฯ		/			

ที่มา: จากหนังสือคู่มือการปฏิบัติงานตามกระบวนการฝึกซ้อมแผนฯ สำนักนโยบายป้องกันและบรรเทาสาธารณภัย กรมป้องกันและบรรเทาสาธารณภัย กระทรวงมหาดไทย สิงหาคม 2553

เอกสารแนบ 34 แบบประเมินองค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

องค์ประกอบ โดยรวมของการฝึกซ้อมแผนฯ

ให้ใส่เครื่องหมาย / ลงในช่องระดับความเหมาะสม/สอดคล้อง ตามความเห็นของท่าน

ขั้นตอน	ระดับความเหมาะสม/สอดคล้อง				ข้อคิดเห็นเพิ่มเติม
	ดี มาก 4	ดี 3	พอใช้ 2	ควร ปรับปรุง 1	
การฝึกภาคปฏิบัติภาคสนาม (FTX)					
1. การควบคุม สั่งการ ของผู้บัญชาการเหตุการณ์แต่ละระดับ		✓			
2. การจัดตั้งแผนการนิรโทษ พ้นที่เกิดภัย ที่ตั้งศูนย์บัญชาการเหตุการณ์ และผู้ประสานภัย		✓			
3. ความเข้าใจของเจ้าหน้าที่แต่ละหน่วยในการปฏิบัติงาน	✓				
4. อุปกรณ์เครื่องมือเครื่องใช้ที่นำมาใช้ในการฝึกซ้อมฯ	✓				
5. ระบบการติดต่อสื่อสารและความถูกต้องของข้อมูลข่าวสาร	✓				
6. ความคล่องตัวและรวดเร็วในการปฏิบัติงานของชุดปฏิบัติการต่างๆ		✓			
7. การให้ความร่วมมือของทุกภาคส่วนที่ร่วมฝึกซ้อมแผนฯ	✓				
8. การจัดระบบจราจรในที่เกิดเหตุ		✓			
9. การบรรลุวัตถุประสงค์ของการฝึกซ้อมแผนฯ	✓				

ที่มา: จากหนังสือคู่มือการปฏิบัติงานตามกระบวนการฝึกซ้อมแผนฯ สำนักนโยบายป้องกันและบรรเทาสาธารณภัย กรมป้องกันและบรรเทาสาธารณภัย กระทรวงมหาดไทย สิงหาคม 2553

เอกสารแนบ 35 แบบประเมินองค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

องค์ประกอบ โดยรวมของการฝึกซ้อมแผนฯ

ให้ใส่เครื่องหมาย / ลงในช่องระดับความเหมาะสม/สอดคล้อง ตามความเห็นของท่าน

ขั้นตอน	ระดับความเหมาะสม/สอดคล้อง				ข้อคิดเห็นเพิ่มเติม
	ดี มาก 4	ดี 3	พอใช้ 2	ควร ปรับปรุง 1	
การฝึกภาคปฏิบัติภาคสนาม (FTX)					
1. การควบคุม สั่งการ ของผู้บัญชาการเหตุการณ์แต่ละระดับ		✓			
2. การจัดตั้งแผนการนิรโทษ พ้นที่เกิดภัย ที่ตั้งศูนย์บัญชาการเหตุการณ์ และผู้ประสานภัย	✓				
3. ความเข้าใจของเจ้าหน้าที่แต่ละหน่วยในการปฏิบัติงาน		✓			
4. อุปกรณ์เครื่องมือเครื่องใช้ที่นำมาใช้ในการฝึกซ้อมฯ		✓			
5. ระบบการติดต่อสื่อสารและความถูกต้องของข้อมูลข่าวสาร		✓			
6. ความคล่องตัวและรวดเร็วในการปฏิบัติงานของชุดปฏิบัติการต่างๆ		✓			
7. การให้ความร่วมมือของทุกภาคส่วนที่ร่วมฝึกซ้อมแผนฯ	✓				
8. การจัดระบบจราจรในที่เกิดเหตุ	✓				
9. การบรรลุวัตถุประสงค์ของการฝึกซ้อมแผนฯ	✓				

ที่มา: จากหนังสือคู่มือการปฏิบัติงานตามกระบวนการฝึกซ้อมแผนฯ สำนักนโยบายป้องกันและบรรเทาสาธารณภัย กรมป้องกันและบรรเทาสาธารณภัย กระทรวงมหาดไทย สิงหาคม 2553

เอกสารแนบ 36 แบบประเมินองค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

องค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

ให้ใส่เครื่องหมาย / ลงในช่องระดับความเหมาะสม/สอดคล้อง ตามความเห็นของท่าน

ขั้นตอน	ระดับความเหมาะสม/สอดคล้อง				ข้อคิดเห็นเพิ่มเติม
	ดี มาก	ดี	พอใช้	ควร ปรับปรุง	
	4	3	2	1	
การฝึกภาคปฏิบัติภาคสนาม (FTX)					
1. การควบคุม สั่งการ ของผู้บัญชาการเหตุการณ์แต่ละระดับ		/			
2. การจัดสถานการณ์จำลอง พื้นที่เกิดภัย ที่ตั้งศูนย์บัญชาการเหตุการณ์ และผู้ประกอบภัย		/			
3. ความเข้าใจของเจ้าหน้าที่แต่ละหน่วยในการปฏิบัติงาน		/			
4. อุปกรณ์เครื่องมือเครื่องใช้ที่นำมาใช้ในการฝึกซ้อมฯ		/			
5. ระบบการติดต่อสื่อสารและความถูกต้องของข้อมูลข่าวสาร		/			
6. ความคล่องตัวและรวดเร็วในการปฏิบัติงานของชุดปฏิบัติการต่างๆ		/			
7. การให้ความร่วมมือของทุกภาคส่วนที่ร่วมฝึกซ้อมแผนฯ	/				
8. การจัดระบบจราจรในที่เกิดเหตุ		/			
9. การบรรจุวัตถุประสงคของการฝึกซ้อมแผนฯ		/			

ที่มา: จากหนังสือคู่มือการปฏิบัติงานตามกระบวนการฝึกซ้อมแผนฯ สำนักนโยบายป้องกันและบรรเทาสาธารณภัย กรมป้องกันและบรรเทาสาธารณภัย กระทรวงมหาดไทย สิงหาคม 2553

เอกสารแนบ 37 แบบประเมินองค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ


องค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ

ให้ใส่เครื่องหมาย / ลงในช่องระดับความเหมาะสม/สอดคล้อง ตามความเห็นของท่าน

ขั้นตอน	ระดับความเหมาะสม/สอดคล้อง				ข้อคิดเห็นเพิ่มเติม
	ดี มาก	ดี	พอใช้	ควร ปรับปรุง	
	4	3	2	1	
การฝึกภาคปฏิบัติภาคสนาม (FTX)					
1. การควบคุม สั่งการ ของผู้บัญชาการเหตุการณ์แต่ละระดับ	/				
2. การจัดสถานการณ์จำลอง พื้นที่เกิดภัย ที่ตั้งศูนย์บัญชาการเหตุการณ์ และผู้ประกอบภัย	/				
3. ความเข้าใจของเจ้าหน้าที่แต่ละหน่วยในการปฏิบัติงาน	/				
4. อุปกรณ์เครื่องมือเครื่องใช้ที่นำมาใช้ในการฝึกซ้อมฯ	/				
5. ระบบการติดต่อสื่อสารและความถูกต้องของข้อมูลข่าวสาร	/				
6. ความคล่องตัวและรวดเร็วในการปฏิบัติงานของชุดปฏิบัติการต่างๆ	/				
7. การให้ความร่วมมือของทุกภาคส่วนที่ร่วมฝึกซ้อมแผนฯ	/				
8. การจัดระบบจราจรในที่เกิดเหตุ	/				
9. การบรรจุวัตถุประสงคของการฝึกซ้อมแผนฯ	/				

ที่มา: จากหนังสือคู่มือการปฏิบัติงานตามกระบวนการฝึกซ้อมแผนฯ สำนักนโยบายป้องกันและบรรเทาสาธารณภัย กรมป้องกันและบรรเทาสาธารณภัย กระทรวงมหาดไทย สิงหาคม 2553

เอกสารแนบ 38 แบบประเมินองค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ



องค์กรประกอบโดยรวมของการฝึกซ้อมแผนฯ

ให้ใส่เครื่องหมาย / ลงในช่องระดับความเหมาะสม/สอดคล้อง ตามความเห็นของท่าน

ขั้นตอน	ระดับความเหมาะสม/สอดคล้อง				ข้อคิดเห็นเพิ่มเติม
	ดี มาก 4	ดี 3	พอใช้ 2	ควร ปรับปรุง 1	
การฝึกภาคปฏิบัติภาคสนาม (FTX)					
1. การควบคุม สั่งการ ของผู้บัญชาการเหตุการณ์แต่ละระดับ		✓			
2. การจัดสถานการณ์จำลอง พื้นที่ภัยพิบัติ ที่ตั้งศูนย์บัญชาการเหตุการณ์ และผู้ประกอบภัย		✓			
3. ความเข้าใจของเจ้าหน้าที่แต่ละหน่วยในการปฏิบัติงาน	✓				
4. อุปกรณ์เครื่องมือเครื่องใช้ที่นำมาใช้ในการฝึกซ้อมฯ	✓				
5. ระบบการติดต่อสื่อสารและความถูกต้องของข้อมูลข่าวสาร	✓				
6. ความคล่องตัวและรวดเร็วในการปฏิบัติงานของชุดปฏิบัติการต่างๆ		✓			
7. การให้ความร่วมมือของทุกภาคส่วนที่ร่วมฝึกซ้อมแผนฯ	✓				
8. การจัดระบบจราจรในที่เกิดเหตุ	✓				
9. การบรรลุวัตถุประสงค์ของการฝึกซ้อมแผนฯ	✓				

ที่มา: จากหนังสือคู่มือการปฏิบัติงานตามกระบวนการจัดการฝึกซ้อมแผนฯ สำนักนโยบายป้องกันและบรรเทาสาธารณภัย กรมป้องกันและบรรเทาสาธารณภัย กระทรวงมหาดไทย สิงหาคม 2553

เอกสารแนบ 39 แบบประเมินองค์ประกอบโดยรวมของการฝึกซ้อมแผนฯ



บริษัท ปตท.สผ. สยาม จำกัด

รายงานผลการปฏิบัติตามมาตรการป้องกันและแก้ไขผลกระทบสิ่งแวดล้อม และมาตรการติดตามตรวจสอบผลกระทบสิ่งแวดล้อม
โครงการในพื้นที่จังหวัดกำแพงเพชร
ฉบับเดือนมกราคม - ธันวาคม พ.ศ. 2566

ภาคผนวกที่ 34

เอกสารการฝึกอบรมการดับเพลิงเบื้องต้น

Basic Firefighting (Further Onshore Safety Training)



Basic First Aid (Further Onshore Safety Training)



รอบการอบรม

- Further Onshore Safety Training (FOnST)

รอบ	วันที่
1	19-Jan-23
3	20-Jun-23
2	30-Oct-23

- Basic Fire Fighting

รอบ	วันที่
1	27-Mar-23



บริษัท ปตท.สผ. สยาม จำกัด

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ภาคผนวกที่ 35

Blow Out Contingency Plan



PTT Exploration and Production Public Company Limited

Blow Out Contingency Plan Manual

Document Code: 10009-WMS-MNL-2002

Revision: 00

February 2016



Blow Out Contingency Plan Manual

10009-WMS-MNL-2002

Approval Register	
Document Title:	Blow Out Contingency Plan Manual
Document Code:	WMS-10009-MNL-2002

Function	Title	Name	Signature	Date
Prepared By:	OWE/S			15/2/16
Technical Review:	OWO/P			15/3/16
	OTF			15 Feb 16
	OTF/D			16/2/16
	OTN			16/2/16
	OTN/D			17/2/16
	OWE/D			15/2/16
Document Custodian:	OWE			10/3/16
	OWO			10/3/16
	OPS			16/3/16

Document Revision History			
Rev.	Description of Revision	Revised by	Date
00	Update old format and review contents		
This document will be reviewed 3 years from date of approval or revised earlier if necessary.			



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1.0 PURPOSE

This PTTEP document has been written to detail the minimum requirements of projects and assets to comply with the PTTEP Corporate Policy on Blow Out Contingency Planning within the Well Engineering discipline.

This corporate level document provides the framework for the management and assurance of Well Engineering within all PTTEP assets and has the following objectives:

- To specify a mechanism to ensure that PTTEP assets remain fit for service and deliver the required safety, environmental and commercial performance throughout the asset life cycle.
- To provide a basis for the management of equipment reliability and integrity through the assets, business processes and organization.
- To ensure that effort is focused on the equipment most critical to safety, environmental and business performance.
- To ensure that the risk of Major Accident Events (MAE's) are reduced to 'As Low As Reasonably Practicable' (ALARP).
- To be flexible to and reflect operational experience and accommodate change.

PTTEP Assets shall adhere to this document and take account of other guidelines and procedures which shall be applied throughout the well/asset life cycle.

2.0 SCOPE

This document applies to the following project life cycle phases:				
Identify / Assess	Select	Define	Execute	Operate
X	X	X	X	X

This document defines the processes that shall be implemented by all PTTEP onshore & offshore oil and gas production and related assets. The processes shall be applied at project development phase through to abandonment.

Where National Regulatory requirements are more stringent, they shall take precedence over this document. In such cases, the document owner shall be notified to determine whether document revision is required.

2.1 LANGUAGE

In this document, the words may, should, and shall have the following meanings:

May	Indicates a possible course of action
Should	Indicates a preferred course of action
Shall	Indicates a course of action with a mandatory status

3.0 REFERENCES

3.1 PTTEP INTERNAL REFERENCES

Internal documents applicable to this document are indicated in the table below.

Document Number	Document Title
Various	WMS Controlling Documents
Various	SSHE Controlling Documents
Various	CMS Controlling Documents

3.2 INTERNATIONAL REFERENCES

International Standards applicable to this document are indicated in the table below.

Document Number	Document Title
Various	API/ISO Controlling Documents
Various	Norsok Controlling Documents

3.3 REGIONAL REFERENCES

Regional Standards applicable to this document are indicated in the table below.

Document Number	Document Title

4.0 DEFINITIONS

4.1 WELL BARRIER DEFINITIONS

Terminology	Description
Well Barriers	Well barriers are envelopes of one or several dependent Well Barrier elements located on a potential leak path able to stop any fluid flow. Each barrier element shall be designed with regard to fluid characteristics and maximum pressure constraints expected at the considered barrier depth.
Well Integrity Envelope	A well integrity envelope is that which can be a combination of barriers and shall be designed to meet all potential load and environment conditions for the required design life of the well. It is also a means to prevent fluid flow and pressure transmission from one zone to another or to the surface and allow safe well killing operations.
Well Barrier Schematic	Is the drawing that will show the well barrier elements, the envelopes at each stage of the wells lifecycle, from "cradle to grave".
Primary Barrier	A system which provides first line fluid containment.
Secondary Barrier	A system which provides backup to the primary system.
Tertiary Well Barrier	Third (and generally optional) well barrier that prevents flow from a source and can act as backup to Secondary or Primary Well Barriers.
Independent Barrier	A barrier system which does not rely on another barrier to ensure pressure integrity, e.g. two similar plugs, can be considered as independent, providing that each plug can be regarded as reliable in its own right.
Verified Well Barrier	Whereby appropriate measures have been taken to confirm the Well Barrier will provide the required isolations. In this document, the term "Well Barrier" means a verified Well Barrier.
A barrier is also defined as either permanent or temporary as follows:	
Temporary Barrier	Non-permanent on or in the well; i.e. BOPs, retrievable plugs. Under specific circumstances the drilling fluid or wellbore fluid, or reservoir fluid may be considered a temporary barrier.
Permanent	Those barriers remaining on or in the well to provide permanent isolation.
Well Classification for Barriers:	
Non-Flowing	A well shall be considered as non-flowing if once the injection / activation system is de-activated, once the injecting/producing bore had been bled-off to atmospheric pressure and once well mean temperature is stabilized, no sustained flow can be observed at surface. This test shall be repeated at least once a year or more often if reservoir conditions can vary.
Eruptive	Any well, which does not fulfil the "non-flowing" well criteria, is named Eruptive.

4.2 GENERAL DEFINITIONS

Terminology	Description
Asset	Any physical facilities onshore or offshore used in the exploration, production, processing or transportation of oil and gas, and any supporting facilities or equipment.
Asset Integrity (AI)	Asset integrity is related to the prevention of major accidents. It is the outcome of good design, construction and operating practices. It is achieved when facilities are structurally and mechanically sound and perform the processes and produce the products for which they were designed
Audit	A structured independent assessment of the efficiency, effectiveness and reliability of the process or system.
As Low As Reasonably Practical (ALARP)	A term used to define tolerable risk acceptance only where risk reduction is impractical or cost benefit analysis is carried out and a judgment is made that the cost of further risk reduction is grossly disproportionate when compared to the actual risk reduction that would be achieved.
Hazard	A hazard is an intrinsic property of anything with the potential to cause harm. Harm includes ill-health, and injury, damage to property, plant, products or the environment, production losses, or increased liabilities.
Hazardous activity	Activity or task that exposes the person(s) carrying out the task to a hazard (e.g. welding, falls, etc.).
Hazard Register	The Hazard Register is an assessment record and communication document that demonstrates that all hazards associated with the Facility or Activity have been identified, and their associated risks assessed, such that appropriate risk controls can be implemented.
Major Accident Event (MAE)	Any incident that results in multiple fatalities or equivalent damage, production loss, environmental impact as per the risk matrix.
Mitigation	Limitation of the undesirable effects of a particular event.
Management Review	A systematic and timely study of a facility's equipment and management systems to help ensure safe operation.
Management System	A structured set of interdependent doctrines, processes, documents and principles that are intended to ensure that the activities of an organization are directed, planned, conducted and controlled in such a way to provide reasonable assurance that the objectives of the organization at met.
Quantitative Risk Assessment (QRA)	QRA is the evaluation of the extent of risk arising, with incorporation of Calculations based upon the frequency and magnitude of hazardous events.
Risk	Risk is a combination of the probability of occurrence of a consequence and the severity of that consequence.
Risk Assessment	An overall process of risk analysis and risk evaluation.
Safety Case	A formal demonstration that Health safety and environmental risks associated with the facility have been assessed and are being effectively managed.
Technical Authority (TA)	PTTEP personnel responsible for technical standards, and for providing advice on issues relating to their discipline, including advice on whether proposals to change or to deviate from a standard or from the reliability and integrity envelope should be approved.

4.3 ORGANISATION AND DEPARTMENTS

In this document, the terms Corporate, Division and Asset have the following meanings:

Corporate	Refers to the PTTEP Business Groups hierarchically above Asset level, and located in the PTTEP headquarters, Bangkok.
Group	Refers to a corporate level Business Group. These may have associated Divisions, Departments, or operational Assets within their hierarchy.
Division	A Business Group may have one or more distinct groups within its hierarchy.
Asset	Refers to an operational Asset, site, or location within a respective Business Group.
Department	A subgroup within a Business Group, Division or Asset.
Subsidiaries	Juristic persons which PTTEP is a shareholder of more than 50%.

4.4 LANGUAGE

In this document, the words may, should, and shall have the following meanings:

May	Indicates a possible course of action
Should	Indicates a preferred course of action
Shall	Indicates a course of action with a mandatory status

4.5 COMMON ACRONYMS

/E	Engineering
/O	Operations
ACV	All-Purpose Capping Vehicle
ALARP	As Low As Reasonably Practicable
AMSL	Average Mean Sea Level
API	American Petroleum Institute
B&C/IWC	Boots & Coots IWC
BCP	The Blowout Contingency Plan
BCTF	Blowout Contingency Task Force
BHA	Bottom Hole Assembly
BOP	Blow Out Preventer
BOPE	Blow Out Prevention Equipment
BOPs	Blow Out Preventers
BPV	Back Pressure Valve
CMP	Crisis Management Plan
CMS	CMS Controlling Documents
CMT	Crisis Management Team
CO ₂	Carbon Dioxide
CP	Command Post
CSE	Safety, Security, Health and Environment Division
CWCI	Cudd Well Control
DC	Drill Collars
DMF	Department of Mineral Fuels
DP	Drill Pipe
DSV	Drill Supervisor
E.C.R.	Emergency Control Room
E.V.P / EVP	Executive Vice President
EMP	Emergency Management Plan
EMS	Electro Magnetic Survey
EMT	Emergency Management Team
EPA	Environmental Protection Agency
EPC	Procurement
EPS	EVP, Eng., Operations & SC
ERP	Emergency Response Plan
ERT	Emergency Response Team
ESD	Emergency Shut Down
ETA	Estimated Time of Arrival
EU	European Union
EZ	Exclusion Zone
FAC	Accounting Division
FNA	Finance & Accounting Group
GSX	Geoscience & Exploration Group

H ₂ S	Hydrogen Sulfide
HDY	Hat Yai Airport designation - IATA
HHP	Hydraulic Horse Power
HHR	Personnel Administration
HIT	Information Technology & Information Management Dept.
HRS	Human Recourses & Business Services Group
HSE	Health, Safety, and the Environment
HTHP	High Temperature High Pressure
IATA	International Air Transit Association
ICAO	International Civil Aviation Organization
ICS	Incident Command Structure
IESG	Oil industry Environment Safety Group Association of Thailand
ISO	International Organization for Standardization
KOP	Kick Off Point
LEL	Lower Explosive Limit
MAE	Major Accident Event
MASP	Maximum Anticipated Surface Pressure
MNL	Manual
MODU	Mobile Offshore Drilling Units
MSV	Primary Support Vessel
MWD	Measurement While Drilling
N ₂	Nitrogen
OIC	On-Scene Incident Commander
OIM	Offshore Instillation Manager
OLG	Logistics/Marine Support
OLG/O	Marine Engineering Operations Section
OP	Operations
OSC	On Scene Commander
OSHA	Occupational Safety and Health Administration
OTF	Thai Offshore Well Operations Department
OTF/D	Drilling Operations Section
OTF/E	Drilling Engineering Section
OTF/O	Thai Offshore Well Operations Department
PDT	Product Asset Group
PIC	Person in Charge
PIN	International Asset
POB	Persons On Board
PSB	Petroleum Development Support
QRA	Quantitative Risk Assessment
RTN	Royal Thai Navy
S.V.P. / SVP	Senior Vice President
SAR	Search And Rescue
SBD	Strategy & Business Development Group

SCBA	Self-contained breathing apparatus
SDSV	Senior Drilling Supervisor
SF	Safety Factor
SO ₃	Sulphur Dioxide
SOP	Standard Operating Procedure
SSHE	Safety, Security, Health and Environment
SSSV	Sub Surface Safety Valve
TA	Technical Authority
TSD	Technology & Sustainability Development Group
TSH	Safety, Security, Health & Environment Division
UTM	Universal Transverse Mercator (coordinate system)
VTSS	Hat Yai Airport designation - ICAO
WMS	Well Management System
WWCI	Wild Well Control Inc.

5.0 RESPONSIBILITIES

5.1 DOCUMENT OWNER

The owner shall be the Well Operations Division SVP and is responsible for:

- Issuing the approval of this document and its revisions.
- Leading and demonstrating commitment by endorsing the implementation of this document.
- Giving clear direction on how the document is to be implemented and maintained.

5.2 DOCUMENT CUSTODIAN

The custodian shall be the OWE VP and is responsible for:

- Identifying deficiencies or potential improvements.
- Initiating periodic revisions.
- Maintaining revision history and document status register.
- Advising the document controller of any document changes, including register status.

6.0 INTRODUCTION

In compliance with legislation and moral obligations to protect the safety of personnel and the environment, the corporate team at PTTEP has developed this document to use in support of a rapid and effective response to a well control emergency. This plan outlines the onshore response to an offshore well control incident from a minor situation to extreme case (e.g. blowout). This corporate document can be used as an example for assets to use as a basis for their country or worksite specific plans.

The Blowout Contingency Plan (BCP) is not intended to replace sound judgment and offers only **guidelines** to be followed in the context of the emergency. For illustration this document is written in the context of PTTEP's domestic operations in the Gulf of Thailand however it is intended to be used as a guide for other assets to define/develop a country or location specific BCP.

6.1 OBJECTIVE OF THE PLAN

The aim of any BCP is to enable the swift and effective mobilization internal and external resources to combat and minimize the effects of a blowout. Due to the nature of this type emergency *initial actions* can considerably affect the latter stages of control. Delays of critical actions can cause knock-on effects which would hamper later efforts to control the situation. For example, a minor leak can be easily controlled, but given time it may escalate into a major fire and explosion. Therefore, it may be important to act quickly in the initial stages of the event. The Contingency Plan provides, or indicates, the source of information to enable all those involved in combating the emergency to take the initial, crucial actions required.

The BCP is not a replacement for other manuals/plans such as the PTTEP "Emergency and Crisis Management Standard" or for example in Thailand the "Bongkot Field Emergency Procedure Manual". The BCP is to be used in conjunction with these manuals/plans and bring specific information to handling a blowout.

The BCP does not discuss procedures intended to prevent a loss of well control. The BCP presents only the reactions expected for well control incidents.

6.2 SCOPE OF THE PLAN

The plan also includes the **long-term-activities** required, as a guide to eventual control of the well such as capping operations and/or relief wells.

These procedures begin assumes that immediate actions have already been undertaken to reduce the exposure of personnel to the consequences of the loss of well control (e.g. down manning of non-essential personnel and they have been moved to a safe location, medical attention given where needed, etc.)

The well control event may be the cause or be related to other types of emergencies, such as oil spills. Therefore this BCP plan refers directly to relevant corporate Emergency Procedures and Contingency Plans, rather than including them in this procedure. Users of this plan should ensure that they are familiar with these related documents and corporate policies.

This plan has been kept reasonably concise for ease of use.

6.3 BCP PLAN SUMMARY

Although this BCP covers one operational area as an example (drilling utilizing a jack-up rig and tender assist barge in the Gulf of Thailand), all well control situations require unique equipment, services and procedures to ensure safety, to minimize loss and deal with the problem in an efficient and effective manner. This BCP presents a template and highlights to all assets the need for an operation plan complete with evaluation of the situation and a mobilization scheme.

The most important consideration in the early stages of a blowout, second only to personnel safety, is the mitigation of damage. The BCP includes damage control measures that may be implemented before Blowout Contingency Task Force (BCTF) takes command and a well control team arrives. At times these procedures may conflict with personnel safety which must remain the paramount consideration. These situations require common sense and professional judgment on the part of the person(s) who are directing any mitigation efforts and are in charge of operations.

NOTE: No operation should be undertaken if it involves risk to personnel.

6.4 CONTROL OF A DRILLING EMERGENCY

In most cases, a blowout occurring during operations is the outcome of a period during which difficulties have been experienced in controlling the well. Shallow gas blowouts are exceptions. However, these do not generally require capping or relief wells. Therefore, the only action after a shallow gas blowout has started is abandonment and personnel protection. The figure 1.1 show 3 levels of incident classified.

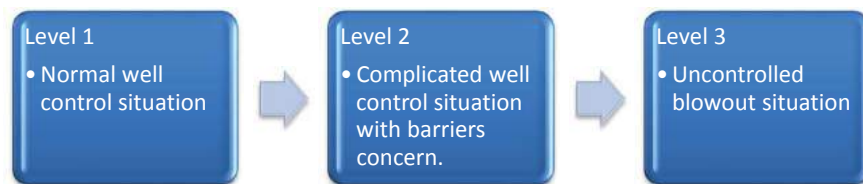


Figure 1 Level of Incident

The escalation period, between "well fully under control", and "well control lost" (e.g. Level 2 incident per definition of Section 1.4 above) during which well control operations are carried out, deserves a special status as regards to onshore management of operations. The escalation often lasts 10 hours, sometimes more, and the decisions taken during this time are often more critical than after the blowout has begun. The reason for this is that up to and until control is lost, one may avoid a potential disaster altogether, whereas after the disaster has already taken place, one can only mitigate the consequences, and often only ineffectively, until major logistics are in place.

In the control operation (example: for the control of a kick) the field team efforts should not be hampered in any way from the primary objective of regaining control of the well.

The decision to move to a Level 2 and thereby assemble the Blowout Control Task Force should be taken before losing control or when loss of control becomes a distinct possibility. Even then, care should be taken not to disrupt the on-going efforts made by the field crews to regain full control of the well.

6.5 MULTIPLE EMERGENCY POTENTIAL

The repercussions of a blowout are likely to be more extensive than any other single event, with possible fire, explosion and associated damage risks. With the potential need for evacuation and oil spillage procedures, the emergency may require the deployment of large numbers of personnel in various teams to deal with specific aspects of the situation. One of the primary actions required in this event would therefore be the allocation of additional space and support in the field for emergency teams, in addition to the Emergency Response Room.

6.6 COORDINATION OF EFFORTS

It should be emphasized that in the case of a blowout occurring on the field, the utmost coordination and cooperation must be established between Drilling Contractors and the Vice President of Drilling Department so as to avoid the redundancy of efforts and to optimize the mutual assistance.

To this end a dedicated telephone line shall be established between the drilling contractors and the Emergency Control Room (E.C.R). It must be emphasized that this line will be used for this purpose only.

6.7 NOTIFICATION

The first responder will typically be the Senior Drilling Supervisor (SDSV). The SDSV after collecting data will notify the **Drilling Superintendent** and the **Drilling Manager** of the Incident. Once the Level of Incident is known, the Drilling Superintendent will assist the SDSV and proceed to respond accordingly. It is common to have kicks or influxes of hydrocarbons and sometimes water during a drilling operation, and these are typically handled by using standard well control procedures. PTTEP has established well control standard procedures for the use of these common well control incidents. There may be cases where small well control incidents escalate into more severe ones. These incidents are known as Level 2 incidents and some examples of these are listed below. If this occurs it may be necessary to consult a well control specialist to assist in normalizing and controlling the well.

6.8 ICS PRINCIPAL

Emergency Response Organization

This plan employs the Incident Command Structure (ICS) system for response to a blowout. ICS is a system of definitions, procedures, job descriptions and instructions for actions to be taken in the event of an emergency. The Incident Command System (ICS) consists of three (3) organizations or teams, and these teams are designed to handle the planning and the response to all well control and blowout incidents specific to PTTEP. The teams are defined as the Emergency Response Team (ERT), the Emergency Management Team (EMT) and the Crisis Management Team (CMT). The Spill Contingency Plan will be launched by SSHE duty in EMT if required.

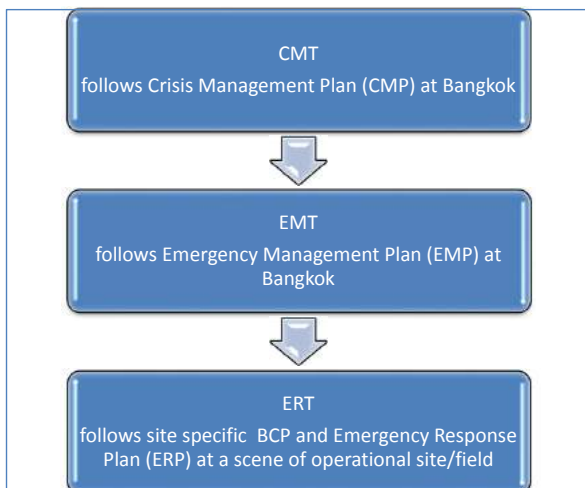


Figure 2: Emergency of PTTEP and crisis management

Emergency Response Team (ERT) on-scene initially and then onshore support teams. Onsite ERT member, comprise the site/field VP/Manager or top authorized person as an on-scene commander as show in Figure 3.

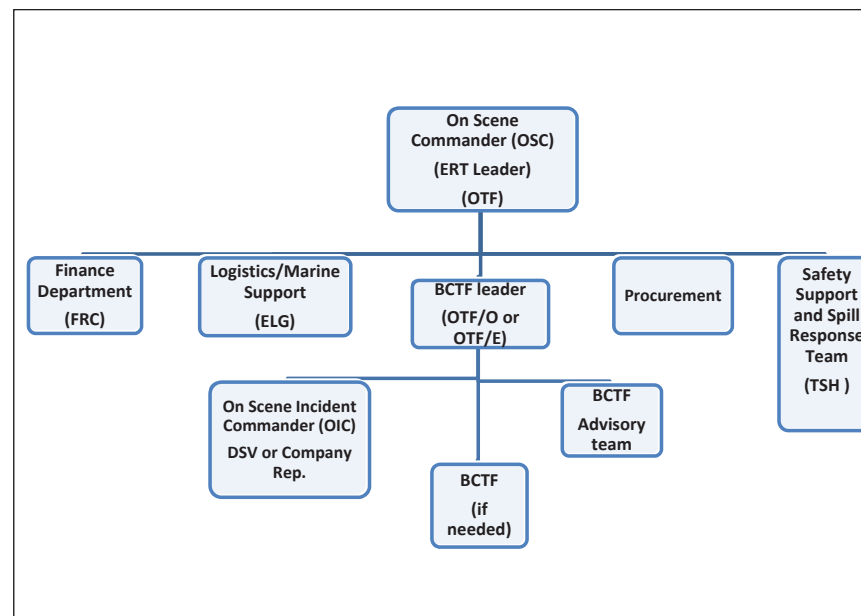


Figure 3: Organization of the ERT

Emergency Management Team (EMT) is involved with an emergency with greater magnitude and major severity in nature or has the potential to escalate and continue for significant period of time until the public may raise concern. EMT member, comprise the top management/authorities in the impact area i.e. the Oil industry Environment Safety Group Association of Thailand (IESG), Royal Thai Navy (RTN), etc., as show in Figure 4.

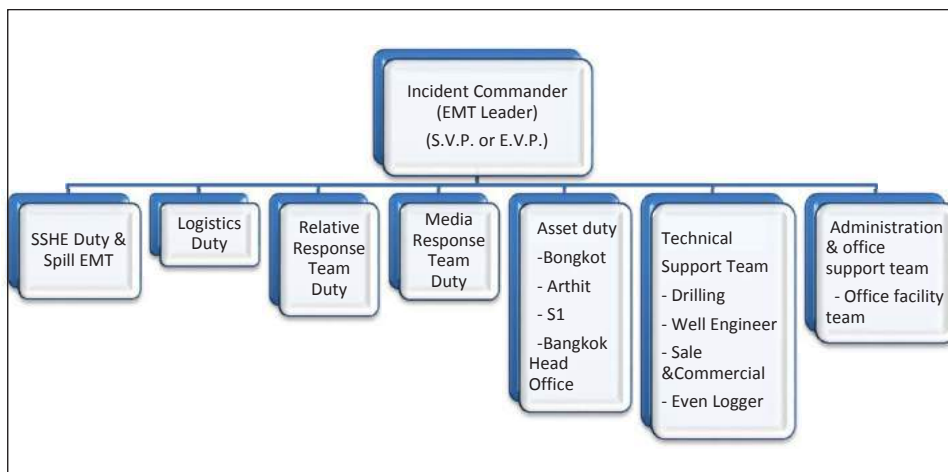


Figure 4: Organization of the EMT

Crisis Management Team (CMT) which is management's role in a complex event (in this plan PTTEP nomenclature will be the Crisis Cell). Corporate CMT member, consists of the top management at the corporate level and other supporting functions as show in Figure 5, their responsibilities and procedure, is defined in the corporate Crisis Management Plan (CMT).

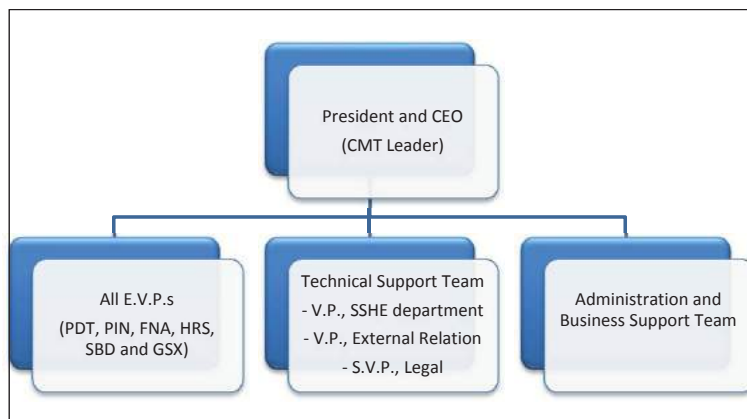


Figure 5: Organization of the CMT

ICS

ICS is a highly structured organizational system developed specifically to manage emergency incidents. It uses a 'command & control' incident management approach to reduce responder risk and to optimize the outcome. It is adaptable, as it allows effective, predefined organizations to function in stressful, high-risk environments. ICS is modular from the top down, which allows it to expand or contract to meet the needs of the task at hand. It has proven to be effective over the past 20 years and has been adopted by many response organizations worldwide. In the USA it is a Federal Law that ICS be employed in emergency response situations (OSHA and EPA).

Response Goals

The goals of the response team are to respond quickly and effectively with a bias toward a structured and unified organizational system. All levels of the overall response teams will follow the decision process described by Figure 6 below:

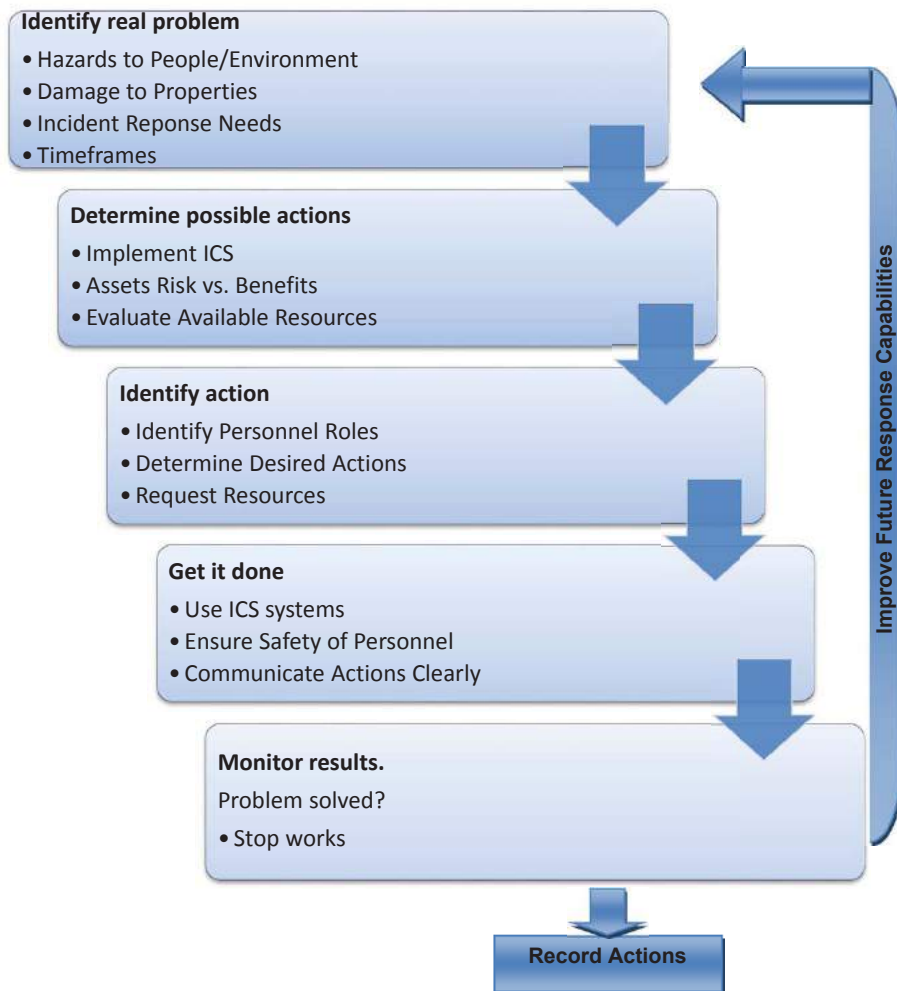


Figure 6: Response Decision Process

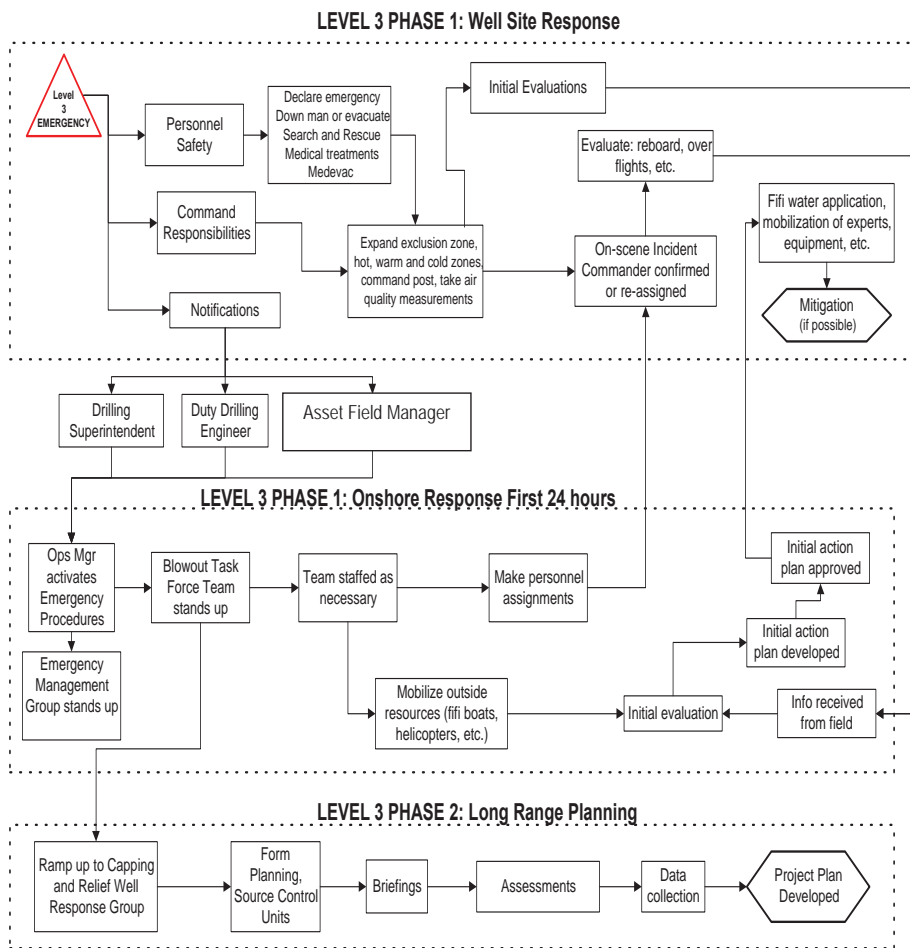
ICS Components

The ICS system depends on ten components to provide the glue that keeps the organization together and functioning properly:

- Common terminology
- Modular organization
- Manageable span of control
- Comprehensive resource management
- Pre-designated incident facilities
- Unified Command structure
- Integrated communications
- Incident action plans
- Common responsibilities for all ICS personnel
- Common Reporting system

ICS Modification for Blowouts

ICS is designed for field activities that are not supported or for blowouts driven by project rules and systems. The first actions to be taken when a blowout occurs must be immediate, which fits the ICS very well. The proactive part of the response will be the control efforts that are best modelled and run as a project, similar to drilling an exploration well or constructing a refinery. Elements of the ICS will however work well for implementation of the project control plan. Therefore, the organizational structures offered in this guideline are modifications of the ICS system and project engineering and design control; e.g., the best of both systems have been utilized.



LWA May-98

Figure 7 Milestone Diagram for Onshore and Offshore Initial Response Action

More detail of this diagram can be found in Section 8.

7.0 NOTIFICATIONS AND INCIDENT LEVELS

This section outlines notifications that are to be made should a well control incident occur. The section described three (3) levels of response, which range from the minor to the very serious. In line with the increasing levels of response, there will be a ramp up of personnel involved. This ramp up of involvement by key personnel is described in the matrix charts shown below:

Affected Personnel Incident Level Drilling	Drilling Supervisor	Drilling Superintendent	Manager, Drilling Operation	VP, Drilling Department	Asset Field Manager	SVP, Operation Support	Duty Officer	VP, Logistics Department	Songkhla Base manager	Executive Vice President	SVP, SSHE Manager	VP, Personnel & Admin. Manager	VP, Reservoir & Exploration Dept.	Blowout Control Task Force (BCTF)
Level 1	X	X	X	N	N									
Level 2	X	X	X	X	X	N	N	N	N	N	N	N		
Level3		X	X	X	X	X	X	X	X	X	X	X	X	X

Figure 8: Drilling Rig Operations Notification Diagram

N = inform only
X = Action

7.1 INCIDENT RESPONSE LEVELS

A three (3) level response based on the severity of the incident is to be implemented. The operational circumstances, the potential for escalation and the potential risk/consequence impact on HSE and Company operations shall be considered in the declaration of the emergency and its level. This approach is outlined in Figure 9.

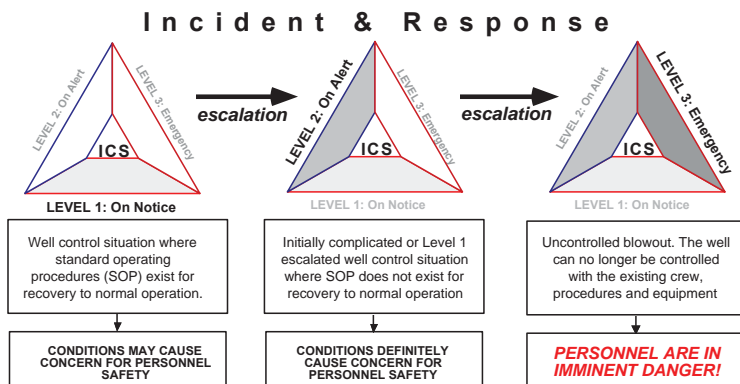


Figure 9: Well Control Incident and Response Levels

The primary components of the response levels are summarized in the following paragraphs:

Level 1 Response (On Notice)

This response is for incidents that on-site operations staff should be capable of handling with standard operating procedures. The incident is of sufficient severity that there is concern for personnel safety and/or potential damage to the well or structure. Level 1 incident classification will be subjective and may be misinterpreted by the on-site staff as routine while it has the potential to escalate to a higher severity level. Notifications are made to immediate supervisors who will approve the classification and proposed control procedures. All level 1 incidents should be appropriately documented and made available for review by other operations staff.

Level 2 Response (On Alert)

This response is for well control or related incidents where there is not a Standard Operating Procedure (SOP) for recovery to normal operations. Control may require resources in addition to the on-site operations staff and/or the use of unfamiliar, more difficult, well control procedures. The incident is of sufficient severity that there is **DEFINITE** concern for personnel safety and/or potential damage to the well or structure. Well control, however, has not been lost. The Level 2 incident classification will be subjective. The Drilling Manager and Area Operation Manager will make the final decision as when Level 1 becomes Level 2. This decision will be based on the risk/consequence for further escalation during non-routine, potentially higher risk, control procedures.

Level 3 Response (Emergency)

This response is for well control incidents where control of the well has been lost. The personnel and structure are potentially in **IMMINENT DANGER**. This would include underground, surface or subsea blowouts. A Level 3 response would initiate a ramp-up to an incident response organization. Resources will potentially be required from outside Thailand. Level 3 incidents have the potential to escalate further during control procedures. Further escalation may include massive pollution, loss of life, serious structural damage or total loss of the MODU or platform and wellhead due to explosion, fire or seabed cratering. Adjacent wells may also be damaged at the surface and seabed, due to fire or flow erosion damage caused by the initial blowout, creating multiple, simultaneous blowouts. Production from other parts of the field may be suspended if the blowout is on a platform that acts as a gathering station for multiple pipelines.

An appropriate response will depend on an accurate assessment of the situation. Therefore, information is essential both in the initial phases and throughout the intervention project. Suggestions are included in each section for information that should be gathered both at the wellsite and from well records.

All situations will require the availability of immediate medical assistance. Additional safety measures and equipment will be required to deal with toxic gas if it is present.

The equipment best suited for intervention varies with each operational setting (i.e., jack-up, platform, floater, etc.). A "standard" firefighting and well control package are specified for the PTTEP Operations setting based on previous experience with such situations. Other equipment and services are specified for support of the intervention project.

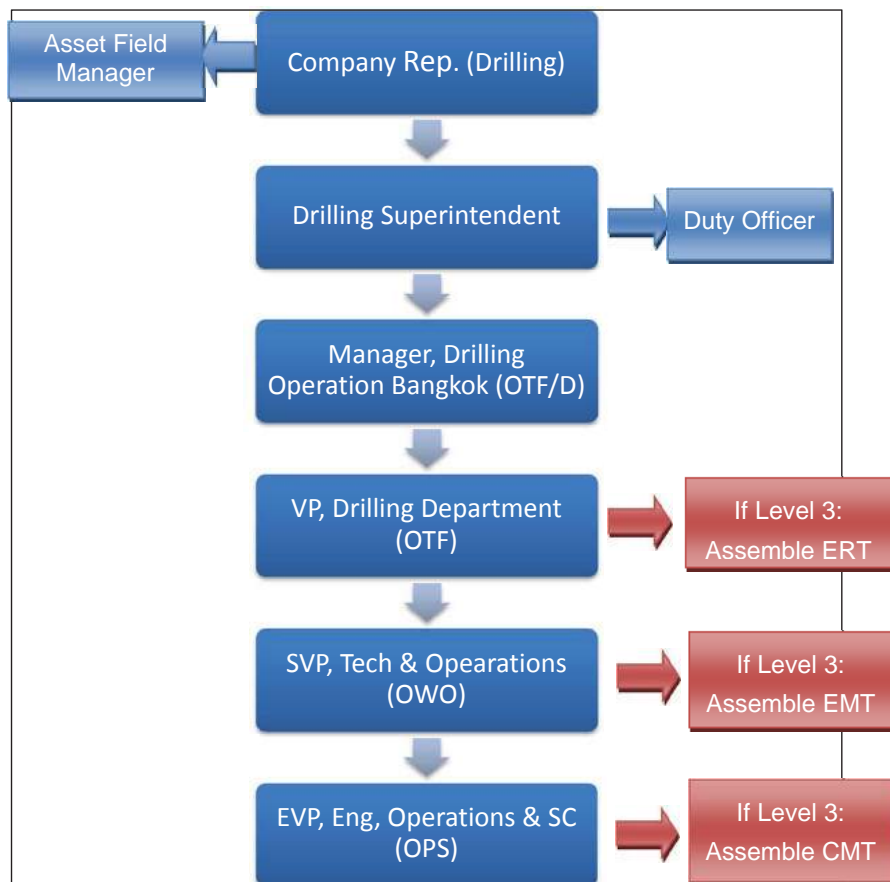
7.2 EMERGENCY RESPONSE TEAM (ERT)

The Emergency Response Team (ERT) will be mobilized by the Vice President (VP) or acting VP. It will be assembled in the Emergency Response Room (room 2948) at the Energy Complex Building A 29th floor. The primary duties of the ERT are to:

- Follow the rules as detailed in the PTTEP Emergency and Crisis Management Standard.
- Take control of the logistics situation.

7.3 NOTIFICATION, ACTIVATION AND ASSEMBLY

The notification charts for personnel involved in the activation of the various response teams are given in diagram below:

a) **Alert Diagram (including out of working hour)**


8.0 INITIAL FIELD RESPONSE ACTION

The response to a well control incident will be according to the appropriate level of the incident (e.g. Level 1, 2 or 3) as defined in Section 2.0. Additionally, the response will be divided into "reaction" and "proactive" actions. The reaction will take place in the first 48-hours +/- of the event. The proactive actions follow the reaction and are designed to bring the situation back to normal operations.

8.1 ON SCENE INCIDENT COMMANDER AND PERSON IN CHARGE

In the situation where a Level 3 emergency has begun certain priorities and actions are required. The most important will be the safety of all personnel, second the facility and support vessels, rig and equipment. The operation will then focus on a solution once initial damage control steps have been taken.

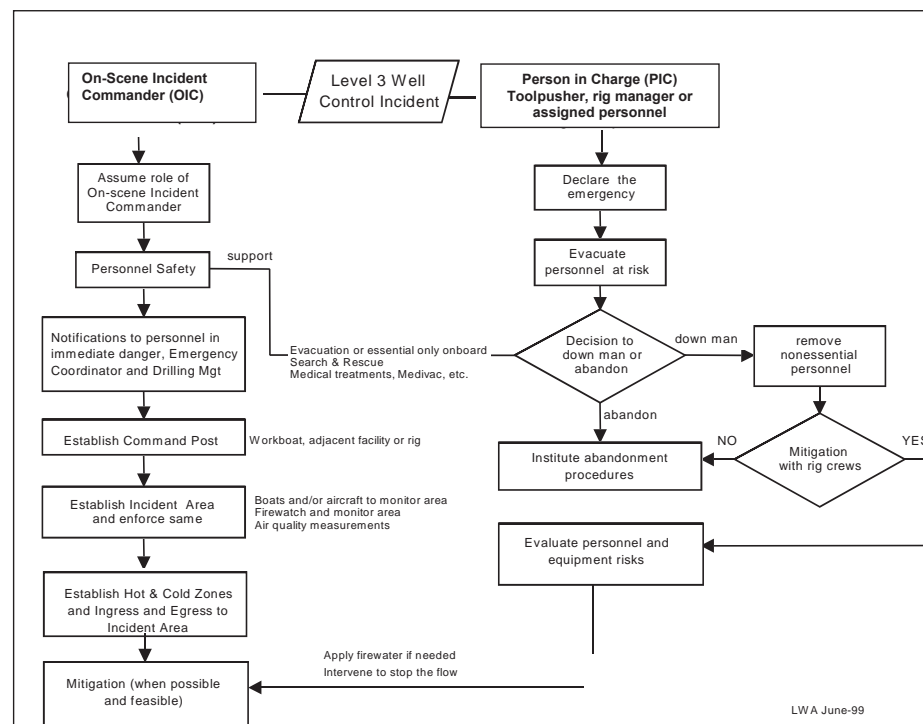


Figure 10 On-Scene Incident Commander and Person In Charge Tasks Flowchart

8.2 PERSONNEL RESPONSIBILITIES AND DESCRIPTION

Responsibilities of Key Off-shore Personnel	Listed below are brief descriptions of the responsibilities of key off-shore personnel who are expected to respond to a well control incident. This plan defines three levels of incident escalation: Level 1 - Notice, Level 2 - Alert and level 3 - Emergency. Level 1, normal and routine well control incidents, are covered by PTTEP's standard operational procedures, and are not addressed here. Responsibilities for Level 2 and Level 3 are outlined below.
Drilling Supervisor On-site Incident Commander (OIC)	Drilling Supervisor is responsible for ensuring that the Drilling Program, Procedures and Policies are carried out by the Drilling Contractor and Third-party Service Companies. The OIC is designated as being in charge of all emergency situations on the drilling rig. He may be advised by the barge captain and rig superintendent (PIC), but the ultimate authority is his and his decision will be final.
LEVEL 2 Alert	The Drilling Supervisor will be responsible for: <ul style="list-style-type: none"> <input type="checkbox"/> determining that Level 2 should be declared, in consultation with the PIC. <input type="checkbox"/> notifying management of a Level 2 well control incident <input type="checkbox"/> activating the appropriate response level on the rig <input type="checkbox"/> maintaining liaison between the PIC and management
LEVEL 3 Emergency	The Drilling Supervisor will continue the appropriate duties above and: <ul style="list-style-type: none"> <input type="checkbox"/> declare the emergency. <input type="checkbox"/> take on the role of OIC (On-scene Incident Commander) until relieved by the Drilling Superintendent or a designee nominated by OTF. <input type="checkbox"/> notify management of a Level 3 well control incident per the notification guidelines <input type="checkbox"/> provide the communications focal point for PTTEP's shore-based management <input type="checkbox"/> coordinate with the Marine Superintendent for standby/supply vessels, fiifi vessels, helicopters, search and rescue support, shore-based support, support from other rigs in the field, medivac, etc. <input type="checkbox"/> assist in the abandonment, medivac and search & rescue as needed <input type="checkbox"/> monitor the situation and communicate developments to Drilling as they occur <input type="checkbox"/> declare an exclusion zone (see guidelines in Section 4.0) <input type="checkbox"/> assist in asset protection procedures (application of firewater, etc.)

Person in Charge (Contractor Rig Superintendent)	The PIC has responsibility for safety of the drilling rig and the safety, health and welfare of all personnel on board or working in the near vicinity of the drilling rig, including the Drilling Contractor's personnel, PTTEP personnel and Third-party Contractors' personnel.
LEVEL 2 Alert	The PIC will be responsible for: <ul style="list-style-type: none"> <input type="checkbox"/> safety of personnel at all times <input type="checkbox"/> declaring a Level 2 alert <input type="checkbox"/> making notifications to contractor management. <input type="checkbox"/> down-manning of personnel if necessary <input type="checkbox"/> directing the Drilling and Rig crew in performance of their specific response duties while assisting a Drilling Supervisor to control the well <input type="checkbox"/> liaison with the Drilling Supervisor in performance of his duties <input type="checkbox"/> notifying the Drilling Supervisor of emergencies <input type="checkbox"/> suspension of hot work <input type="checkbox"/> securing rig for abandonment if this becomes necessary <input type="checkbox"/> advising Drilling Supervisor when the emergency is over and the return to normal operating status • In case the OIC is incapacitated, he shall assume this role until relieved by PTTEP.
LEVEL 3 Emergency	The PIC will continue the duties above as well as: <ul style="list-style-type: none"> <input type="checkbox"/> declare the emergency after consulting with Drilling Supervisor. <input type="checkbox"/> along with Drilling Supervisor determine a decision of abandonment <input type="checkbox"/> along with Drilling Supervisor determine method of abandonment. <input type="checkbox"/> along with Drilling Supervisor order evacuation of personnel. <input type="checkbox"/> initiate emergency SOP's for abandonment (emergency disconnect). <input type="checkbox"/> call an immediate muster of all persons on board when necessary. <input type="checkbox"/> ensure crew has responded to the alarm. <input type="checkbox"/> Direct and control support vessel and helicopter operations in the vicinity of the rig. • In case the OIC is incapacitated, he shall assume this role until relieved by PTTEP.
Vessel Master (if On-site)	One or more vessels may be tied up to or be in the vicinity of the drilling rig during an emergency or may be dispatched to the site by the marine superintendent. Any vessel in the immediate vicinity or participating in the emergency shall be responsible for the following:
LEVEL 2 Alert and LEVEL 3 Emergency	The VESSEL MASTER has ultimate responsibility and authority for the safety of his vessel and crew. The primary objective of the Vessel Master, in the event of an emergency, shall be to SAVE LIVES by assisting in rescue efforts and/or the application of firewater. If he is notified of an emergency on a drilling rig, he will immediately suspend current operations and offer assistance as requested or as he deems appropriate. He will be responsible to the PIC on the drilling rig, but he may also be directed by the Marine Superintendent or Drilling Supervisor. A partial list of responsibilities are to: <ul style="list-style-type: none"> <input type="checkbox"/> accommodate all drilling rig personnel on a short term basis. <input type="checkbox"/> provide first aid to rescued people as necessary.

	<ul style="list-style-type: none"> <input type="checkbox"/> act as a reserve/relay radio station between base and installation. <input type="checkbox"/> standby close to the drilling rig for helicopter landings and take offs.
	<ul style="list-style-type: none"> <input type="checkbox"/> oversee personnel working over the side; personnel working in/near water <input type="checkbox"/> keep continuous look-out for other vessels that might come near the drilling rig <input type="checkbox"/> assume responsibility for communication with other vessels as the situation demand OTF/O <input type="checkbox"/> transmit messages to air and surface craft <input type="checkbox"/> act as an On-scene Incident Commander until relieved, as directed by management <input type="checkbox"/> maintain communication with the drilling rig, using all visual and audible means available for as long as possible <input type="checkbox"/> monitor the situation and report development to management and the On-scene Incident Commander
Safety Officer/ Technician	Support PIC and OIC as follows: <ul style="list-style-type: none"> • Oversee the practices being used for emergency response. • Participate in decision making process. • Provide advice to Drilling Supervisor and O.I.M.. • Ensure safety equipment is available and working properly. • Make preparations for evacuation, if necessary.
Driller	Support PIC and OIC as follows: <ul style="list-style-type: none"> • Secure well as instructed or based on experience. • Assist Offshore Installation Manager (O.I.M.) and Drilling Supervisor. • Carry out assigned emergency actions.
Barge Engineer, Crane Operator, Electrician, Mechanic, Mud Engr., Radio Operator, Derrickman, Floorman, and Roustabouts	<ul style="list-style-type: none"> • Assist O.I.M. and Drilling Supervisor. • Carry out assigned emergency actions as per SOP. As shown in Transocean Emergency Response Plan.

8.3 GUIDELINES FOR INITIAL RESPONSE

8.3.1 Personnel Safety

In blowout situation the most important consideration is personnel safety. PTTEP operations have developed this document and plan which refer with Emergency Management Plan (EMP). Once the well blowout, all personnel on board need to be checked and accounted. Emergency team such as rescue team needs to be activated. Medivac will be organized if needed. Then activate evacuation plan.

8.3.2 Activate Exclusion Zone

After the rig/platform has been abandoned, the On-scene Incident Commander will be responsible for activating an Exclusion Zone (EZ) for: third party general marine and aviation traffic and any fixed structures and MODUs within the zone. The initial EZ should be a fixed radius around the blowout exit point(s) (some broached blowouts have surfaced several kilometres from the wellhead). The fixed radius should be based on gas dispersion and oil slick modelling for a worst case blowout. Consider:

- Maximum blowout oil flow rates and slick movement on dead calm water
- Lower Explosive Limit (LEL) distances for very stable atmospheric conditions and light wind (< 2 mph).

If modelling parameters are uncertain assume 1 km as a minimum initial radius. Air quality measurement will be used to alter the generalized no-go zones.

8.3.3 Establish On-Scene Command Post

A command post (CP) needs to be established by the On- scene Incident Commander as soon as practical to facilitate coordination of further response activities. If the rig has been partially evacuated, the CP would be the drilling rig, with an observing standby boat acting as a backup in case rapid escalation prevented On-scene Incident Commander communication with support resources. If the rig has been abandoned the CP might be established on a supply vessel, another rig or offshore structure outside the exclusion zone. Good communication equipment is essential between the On-scene Incident Commander, the field support resources and the shore base. The location of the CP may be moved as appropriate at the discretion of the On-scene Incident Commander.

8.3.4 Site Safety

After evacuations and the other initial command structure steps are **taken** by the On-scene Incident Commander, the next issue to be addressed is site safety. Site safety for third parties and responders will be addressed by these steps:

Activate the Initial. Exclusion Zone

This is a pre-determined no-go and evacuation zone designed around a worst case blowout release using gas dispersion modelling tools. Under certain stable atmospheric and wind conditions dangerous concentrations of H₂S gas can travel long distances. For this reason the size of the initial Exclusion Zone should be conservative.

The activation of this zone is a safety measure designed to protect third parties and non-essential personnel from potential exposure while measurements are taken to define a more accurate Exclusion Zone. The activation of the zone will be made by notification to all vessels, aircraft and structures inside the zone. Securing the zone after activation will require several of vessels and/or aircraft.

Define Hot, Warm and Cold Zones

These are safety zones designed to establish levels of increasing potential risk to responders as they move from Cold to Hot. Each zone will have increasing levels of safety requirements before responders are allowed to enter. The combined Hot, Warm and Cold zones will establish the working Exclusion Zone for third parties and non-essential personnel. These zones will be established systematically and should consider the longest reaching hazards first, for example:

- H₂S and/or SO₂ exposure (if applicable)
- gas ignition and explosion with flying debris
- gas ignition and fire
- pool fires
- secondary explosions after primary ignition
- oxygen deficiency
- gas plume hazards on sea surface
- rig instability and/or deterioration
- shifting wind directions and velocities
- blowout intensity escalating
- oil slick movement.

These zones will initially be established by the On-scene Incident Commander in consultation with the Safety Officer (if possible) evaluating each of the potential hazards individually and again as a system. A site specific safety plan must be developed for the team designated to access the zone boundaries, to include support and escape plans. Weather and blowout conditions can change on short notice, therefore these boundaries can also change and must be re-evaluated constantly. If there is uncertainty concerning the potential hazards involved then the On-scene Incident Commander should maintain the Initial Exclusion Zone until relieved trained response person. See also Guidelines, Flowcharts and Checklists section at the end of this chapter.

Define Access and Egress Routes

OIC is responsible for setting the boundaries for the Hot, Warm and Cold Zones. Routes into and out-of the zones must be established for response personnel for re-entry and emergency escape. Generally the access and egress routes are best made in the upwind hemisphere. If approach is made in a vessel current and waves should also be considered if an oil slick is to be avoided or if power failure of the vessel might cause it to drift down wind into the danger zone. The preferred course of access may be to approach at 90° angles to the wind/current direction. All hazards must be considered, however, before finalizing the routes note that the egress route may change during the course of a work period, due to changes in conditions and should be monitored continuously.

Exclusion Zone Safety Procedures

Site specific exclusion zone safety procedures must be established for all personnel entering each of the three zones. The On-scene Incident Commander in consultation with the Safety Officer and Toolpusher (as applicable) and shore base supervisor would define these procedures. If re-entry is to be considered after an abandonment, the OIC must consider the following:

- The need for entry
- Evaluate risks for entry team
- Develop tasks for entry team
- Develop contingency plans and escape means for various scenarios, e.g.:

- Operational "Site Safety" meeting with all concerned
- discuss personnel safety
- - emphasis on buddy system
- set objectives of re-entry- emphasis on escape and contingencies,
- equipment checks for hot and warm zone participants
- Issue Personnel Protection Equipment For Staff In Each Zone (if needed)
 - SCBA (if appropriate)-
 - heat fire resistance clothing-
 - hearing and eye-protection (with heat shielding)-
 - hand held communications-
 - air quality monitoring devices-
 - head, hand and foot protection
- General Site Security and areas to avoid:
 - closed areas- highly contaminated areas (gas, oil, etc.) g
 - as concentration (high LEL, H₂S, etc.)
 - onsite toxicants and chemical exposure (caustic, acids, etc.)
 - site procedures for access control and personnel monitoring
- Site safety will be a particularly important issue if the decision is made to allow essential personnel to remain on the facility to execute mitigation procedures (pumping, firefighting, etc.) or if firefighting vessels are to be deployed in the warm zone to spray water after the rig has been abandoned. If the facility is destroyed or the perceived danger is high, the site safety issue should be left to the Level 3 Source Control Team

8.3.5 Asset Protection & Damage Control

After the site safety issues are addressed, asset protection and damage control may be addressed by the On-scene Incident Commander. Listed below are a few procedures that may be considered:

- ESD initiation (if appropriate)
- Blowdown of site hydrocarbon inventory
- Shut-in of wells and pipelines feeding facility
- Secure adjacent wells in well bay (if possible)
- Firewater Application, deluge systems (if appropriate), fifi water application from marine vessel(s) to minimize ignition hazard or to cool structure and/or adjacent wells

Some of the steps listed above may be part of the facility operations standing procedures in a Level 2 emergency (example: simultaneous operations on a joint drilling and production operation). They are mentioned here to alert the reader to the situation where they are not standing procedures and may be considered in the overall action plan taken by the on On-scene Incident Commander. It is important to maintain control over any firefighting vessel that might be deployed to spray water on the rig. The captain and crew of the vessel must be debriefed and fully understand the potential dangers of escalation and safety procedures that must be followed before they are deployed into a potentially dangerous situation. Non-essential crew should be removed before entry into the Hot or Warm Zone.

All safety equipment and breathing systems must be checked before entry.

8.3.6 Rig or Structure Re-entry by Initial Response Team

Re-entry of the rig or structure where a surface blowout is underway should not be attempted by the Initial Response Team without approval from PTTEP management. The case of search and rescue (SAR) may be accepted, but only then after a detailed safety/rescue plan is in place for the responders. For all other purposes (e.g., assessment or mitigation) the Initial Response Team should wait for the Level 3 professional response team to arrive and develop a detailed proactive plan of action.

8.3.7 Blowout Control Response Actions

Blowout control response actions should not be attempted by the field personnel unless approved by PTTEP management and only then after a credible operation plan has been devised along with a site safety and escape plan. In cases where the blowout occurred rapidly with no chance for off-site support, the rig/structure should be secured and abandoned. Blowout control response would wait for the Level 3 ramp-up and a proactive plan to be developed by the Source Control Team. Circumstances where the ECT might attempt blowout control actions would be where an escalation has occurred gradually from a Level-2, Incident, the rig has been down manned, and the shore based support team has already been activated. In this case, if the ECT and the support team both feel an immediate control attempt has a high probability of success, the safety risk is low, further rapid escalation risk is low and a site safety plan has been developed then control attempts may be initiated. An underground blowout that has a low probability of broaching would be an example.

*** WARNING ***

- In no case shall the response team be subjected to unreasonable risk. At all times during this initial phase 1 period, safety of personnel will be the number 1 priority. The rig crews should not be expected or asked to perform potentially dangerous tasks that they have not been trained to perform.

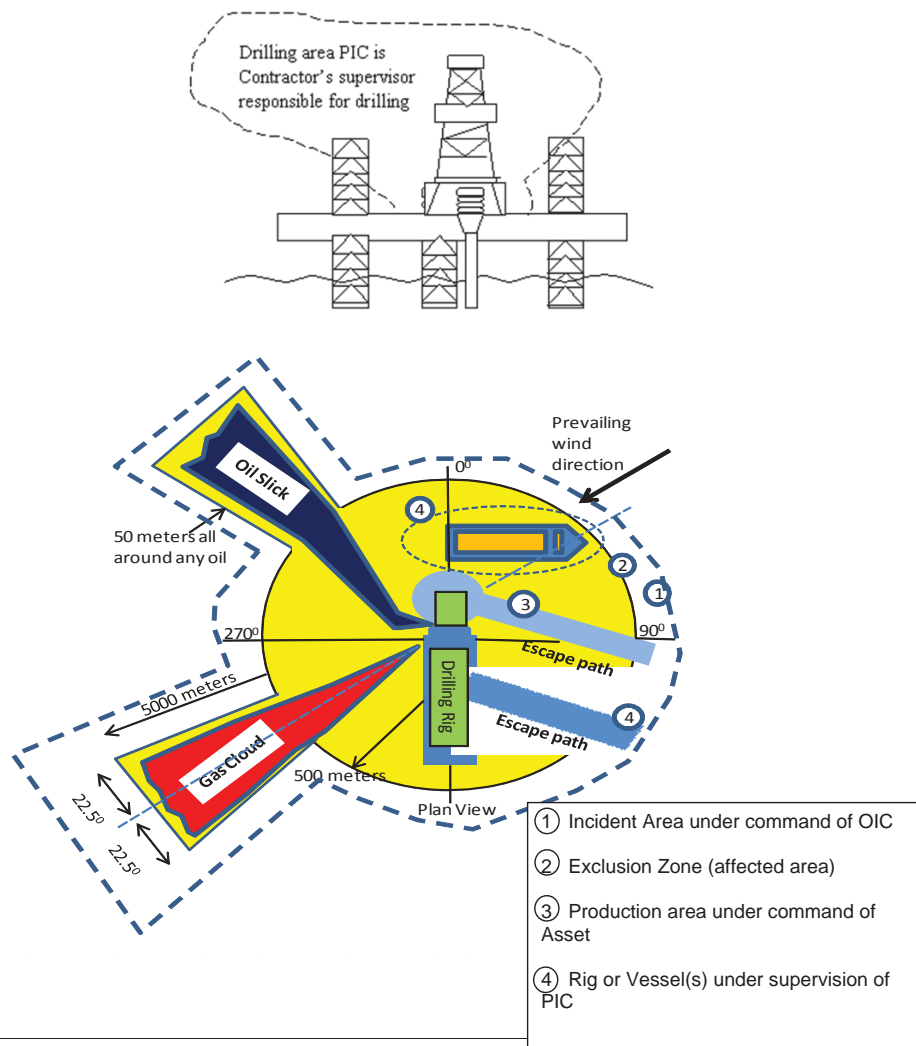
Level 3 - Phase 1 on-site blowout control response actions will be specific to company approved policy and: (1) the type of rig or structure (e.g., rig or platform rig); (2) the circumstances of the blowout (e.g., surface, on fire, underground, potential risk for escalation); (3) the operation at the time of the incident (e.g., drilling related, workover related, testing related or production related); (4) potential for sabotaging future proactive control plans if an immediate attempt fails, and (5) the local environment at the time of the incident (e.g., night/day, weather, fire, pollution, available resources, willingness, training level and skill of crew.

8.4 ON-SCENE INCIDENT COMMANDER & PERSON IN CHARGE TASK LISTS

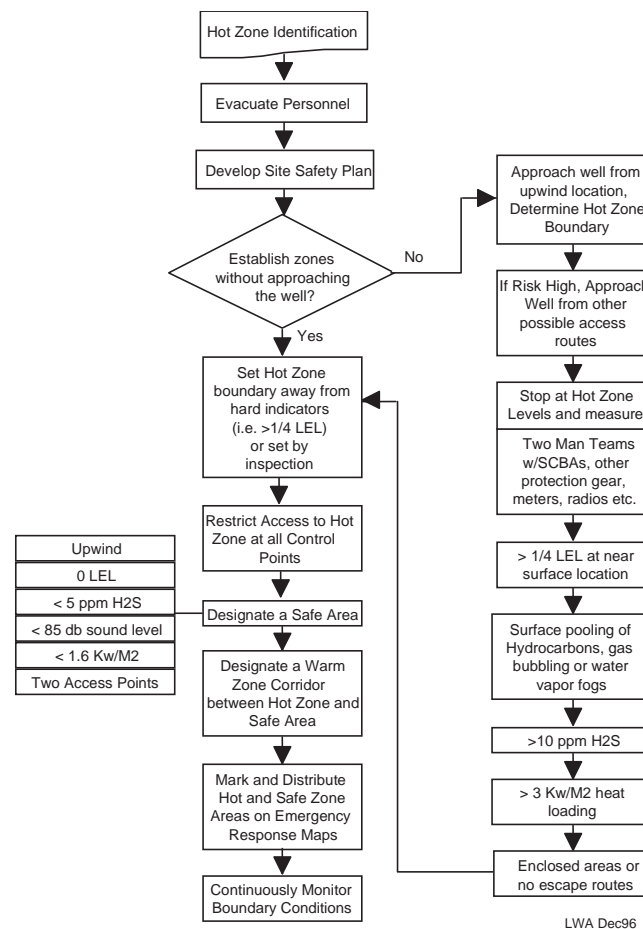
Command Organization and Responsibilities	
Level 3 - Phase 1	
Initial On-scene Incident Commander and essential crew only	
Item	Action or Consideration
1	When the decision is made to abandon the rig or platform, the PIC will maintain command of the evacuation operation until his charges have been rescued and is relieved of his duties. During this time, close liaison will be maintained with the PTTEP Representative, whose duties will be to assist the PIC as directed and to coordinate off site notifications and support. After the rig or platform has been abandoned the PTTEP OIC will assume command of further response operations. There can be only one man in charge, if the pre-designed On-scene Incident Commander cannot assume his command one must be appointed.
2	Make notifications as per the notification diagram in section 2.
3	Appoint deputy On-scene Incident Commander and team leaders (ex: toolpusher is deputy, barge engineer becomes team leader, etc.).
4	Establish essential personnel roster. Appoint support staff and outline responsibilities (drillers, electrician, mechanic, medic, etc.).
5	Set up command post (standby boat, control room, radio room, etc.) Man communication equipment, keep channels of communication open for important relays (e.g. essential communications only).
6	Establish Incident Area, activate Exclusion Zones for general aviation and marine traffic enforce the same.
7	Establish preliminary Hot Zone boundary.
8	Hold initial briefing meeting with team members - address personnel safety and medical issues - search & rescue necessary? - mitigation and or damage control objectives - re-board for evaluation - refer to BCP plans and checklists
9	Assign monitoring responsibilities - begin fire watch, organize fly-by and or marine observation.
10	Begin reporting sequences
11	Mitigation when possible (firefighting, etc.) and ONLY with approval of management.

8.5 HOT ZONE IDENTIFICATION

If a level 3 event occurs (like a blowout) certain key personnel are expected to take charge of their respective areas. In the drilling scenario the Companyman becomes the On-scene Incident Commander (OIC) in charge of the overall incident area. The rig or, any vessel, will be commanded by a Person In Charge (PIC) who has ultimate responsibility for his respective area. The diagram below shows the various areas of responsibility:



8.5.1 Hot Zone Identification Flow Chart



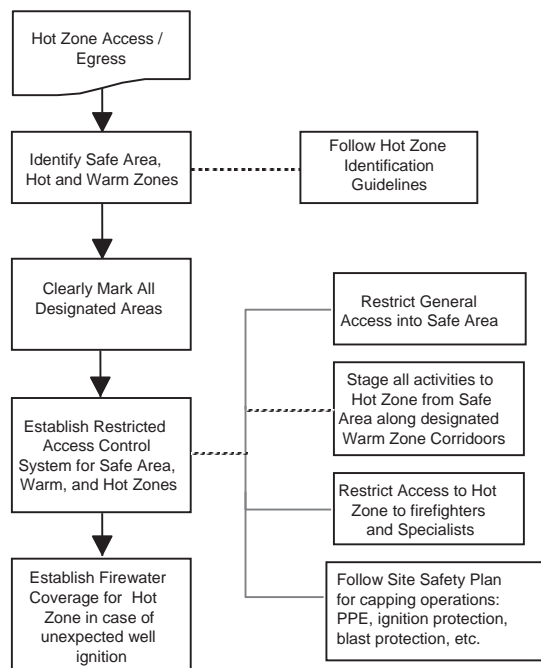
8.5.2 Hot Zone Identification Checklist

HOT ZONE IDENTIFICATION	
Level 3 - Phase 1	
Initial On-scene Commander and essential crew only	
Item	Action or Consideration
1	A "SITE SAFETY PLAN" is required before wellsite work can start. This plan is developed and implemented by the On-scene Incident Commander after initial evacuation of personnel.
2	The "Hot Zone" boundary must be realistically based on presence or the anticipated presence of an explosive mixture (LEL levels), rain of hydrocarbons or H ₂ S and is principally controlled by wind direction but is influenced by the leak rate and location as well as the direction of the flow.
3	On burning blowouts the "Hot Zone" will likely be set on radiant heat limits and smoke avoidance. Wind direction also has considerable impact in Hot Zone boundaries. Some fires do not burn clean and product can exist in the presence of a fire, therefore item 2) and 3) must be considered together.
4	Generally the hot zone will be set by inspection and not from a quantitative analysis. This will be revised as time goes on and will be monitored carefully throughout the project.
5	If the "Hot Zone" boundary is set by actual measurements, it will be done by two men with SCBAs. They should approach blowout using LEL meter, H ₂ S meter, dB meter and Radiant Heat Meter (if available) and check levels down wind of the well area. Initial approach should be from an upwind direction.
6	The boundary of the HOT zone is defined as when first indication is seen of either: <ul style="list-style-type: none"> • >1/4 LEL level (1% concentration of hydrocarbons in air) at any near surface elevation (ground level or standing on top of a truck). • surface pooling or streaming of liquid hydrocarbons, surface gas bubbling or hydrocarbon and water vapor fogs (restricted visibility and explosive vapor) • >10 ppm H₂S • >90 dB noise level • Over 3 Kw/m² heat loading or practically the point where exposed skin cannot sustain exposure without protection for more than a few minutes. CONTINUED....
7	When measuring parameters, approach problem well from any possible access route (including those located downwind) and repeat this process.
8	Where possible, set Hot Zone boundaries away from these hard indicators (ex: 1/4 LEL) at good control points. CONTINUED....
9	"Hot Zone" shall be restricted to well control experts or designee of the On-scene Incident Commander and shall be allowed in the zone on a permit only basis and only for a prescribed and defined task. Buddy system will be maintained at all times and cover of water provided for each when appropriate.
10	Manpower with radios from drilling rig crew, safety and production can be used at these defined "Hot Zone" control points to restrict access into the "Hot Zone". Downwind "Hot Zone" boundary must be tightly controlled and continuously monitored as variable winds can quickly change the boundary. Some access routes should be blocked to prevent accidental entry.
11	The "Safe Area" or "Cold Zone" location is based on the "measurable" Hot Zone boundaries, available work areas and access and wind direction.

12	The safe distance seen in the downwind approach of the "Hot Zone" boundary is then used as one guideline for setting the "Safe Area". Additionally dispersion modeling can be used with the measurements taken to help predict downwind conditions if wind is blowing across blowout out to sea.
13	The "Safe Area" is not a contour like the "Hot Zone" but is a dedicated staging area for control efforts for blowout. Access to areas inside the "Hot Zone" must be from "Safe Area". Other alternate paths into "Hot Zone" are blocked.
14	"Safe Area" should be accessible from two directions.
15	"Safe Area" restricted to essential personnel with proper protective equipment.
16	"Safe Area" should be in area with 0 LEL, <5 ppm H ₂ S, <85 dB sound level and <1.6 Kw/m ² heat loading.
17	Mark the designated "Hot Zone" and "Safe Area" on the available Emergency Response Maps for distribution and all procedures.
18	As the well and wind conditions change, the "Hot Zone" boundaries will shift. The "Safe Area" could also be moved. An example would be shifting boundaries after well ignition.
19	The "Warm Zone" is the route between the "Safe Area" and the "Hot Zone". Control indicators (LEL levels, H ₂ S, radiant heat etc.) are continuously monitored within the "Warm Zone" at the entrance to the "Hot Zone".
20	The "Warm Zone" is restricted to essential support personnel only.

8.6 HOT ZONE ACCESS & EGRESS

8.6.1 Hot Zone Access and Egress Flow Chart

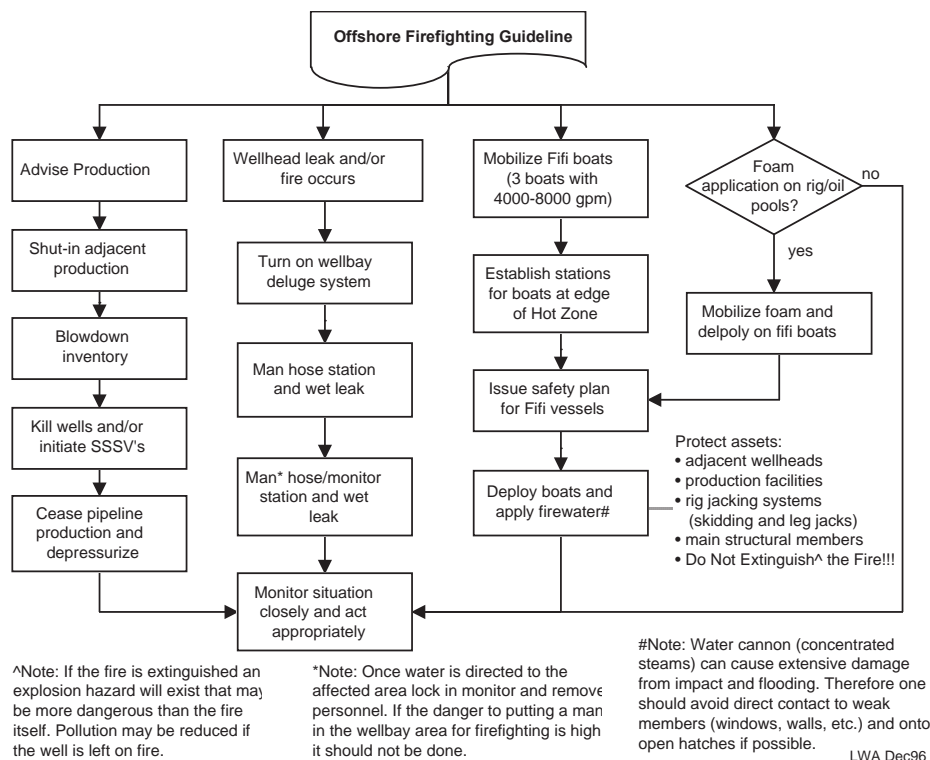


8.6.2 Hot Zone Access and Egress Checklist

HOT ZONE ACCESS and EGRESS ROUTES	
Level 3 - Phase 1	
Initial On-scene Incident Commander and key personnel from the site crew	
Item	Action or Consideration
1	On-scene Incident Commander to define "Hot Zone" boundaries and "Safe Area". This defines "Warm Zone" along access route between the "Hot Zone" and "Safe Area".
2	Stage all activities to the "Hot Zone" out of the "Safe Area" along the designated and continuously monitored "Warm Zone".
3	On-scene Incident Commander to establish access system at "Safe Area"
4	On-scene Incident Commander to maintain control points at all possible access routes and/or block the access
5	On-scene Incident Commander to allow access to "Hot Zone" only along the Warm Zone" route by strict control.
6	Only experienced firefighters and blowout specialists are allowed within the "Hot Zone" under strict access coordination with Safety and the OIC.
7	Offshore rigs may have significant blast hazard inherent in design. Enclosed spaces filled with explosive vapor may explode if well ignition occurs.
8	"Hot Zone" approach lanes must be set up with fire water coverage to protect men from fire or unexpected well ignition. Shield safe havens may be needed.
9	Approach lanes to and within "Hot Zone" must be upwind and clearly marked
10	"Hot Zone" approach lanes must be aligned straight away from rig structure corner to limit potential blast exposure from unexpected ignition. Make use of available blast cover.
11	Personnel working in "Hot Zone" may will require Decontamination areas at edge of "Hot Zone" with communications.
12	Personnel must check in and out of Warm areas
13	Access must be tightly controlled if well is not burning. A minimum of exposed personnel must be maintained as explosive vapor cloud ignition can occur naturally at any time.
14	Vapor clouds have the capability to throw debris great distances if ignition occurs. Debris away from the ignition source can be thrown great distances and therefore present a grave danger to personnel.

8.7 FIREFIGHTING AND ASSET PROTECTION

8.7.1 Firefighting and Asset Protection Flow Chart

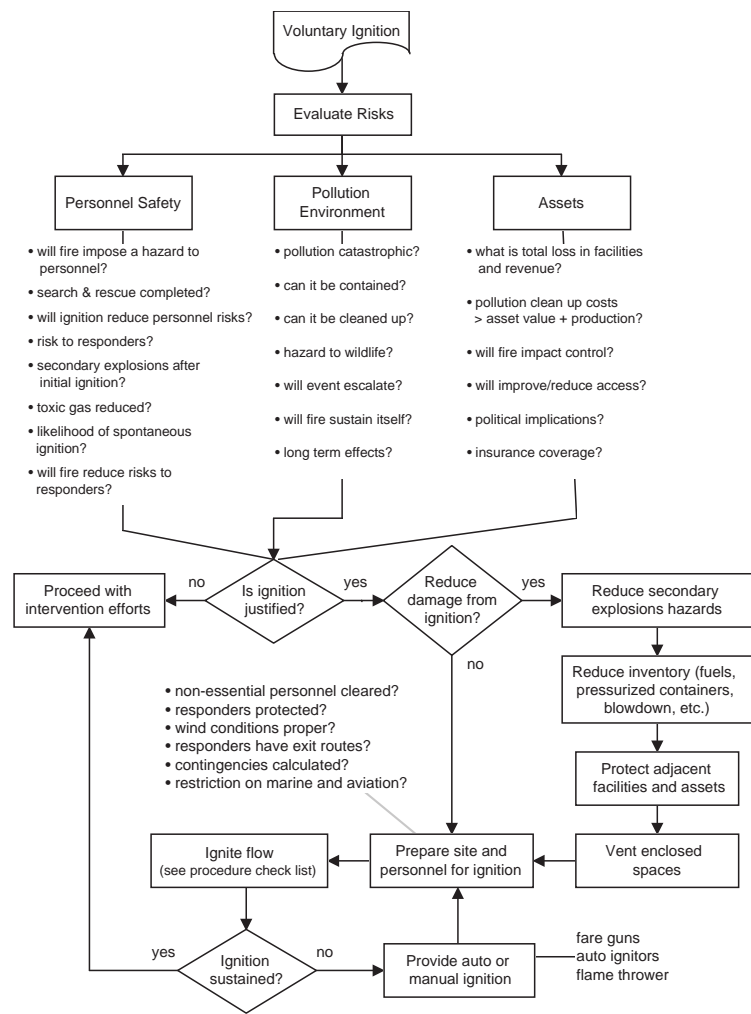


8.7.2 Firefighting and Asset Protection Checklist

FIREFIGHTING & ASSET PROTECTION	
Level 3 - Phase 1	
On-scene Incident Commander & Company Representative	
Item	Action or Consideration
1	Initial firefighting and asset protection should start at the rig and expand to the locally available Firefighting Units. This list assumes that there is a pressure fed well fire.
2	Turn on rig sprinkler system and use fire hoses to keep fire away from personnel if necessary during evacuation (if rig is equipped and feasible).
3	Establish "Hot Zone" & "Safe Area"
4	Establish Hot Zone Access & Egress Control
5	Mobilize locally available mobile fighting equipment, field boats with firewater capability (three boats with 4000 to 8000gpm each are needed)
6	Local firewater capability must not wait for blowout specialists to arrive as fire damage to the structure, surrounding wells and process equipment must be quickly limited.
7	All of the required firefighting equipment (outside of vessel fifi) is currently located in Europe or the USA and must be mobilized to the site.
8	Crew should hook up to rig deluge system if possible & activate if rig is on fire.
9	<p>Spray water to protect adjacent wellhead areas and production equipment.</p> <p>Spray water to protect rig equipment and jacking hydraulics to assist in skidding drilling package.</p> <p>Blow down all production lines and displace with nitrogen or water if possible.</p> <p>Confirm that all adjacent wells are shut-in on subsurface safety valve and surface valves. If possible kill offset wells.</p> <p>If possible, dump or pump out all stored combustible fluids on rig or nearby production facilities (diesel, methanol, glycol). Displace storage vessels with water or nitrogen.</p> <p>Remove any stored chemicals or pressurized containers. Even fire extinguishers can blow up if they get too hot.</p> <p>Spray water only on those areas that are too hot. Do not extinguish fire.</p>

8.8 VOLUNTARY IGNITION PROCEDURE

8.8.1 Voluntary Ignition Flow Chart



See ignition guidelines below

8.8.2 Voluntary Ignition Guideline and Procedure Ignition Criteria

Voluntary Ignition Guidelines and Procedures Ignition Criteria

The following sections discuss purposeful ignition of a blowout. If significant concentrations of oil, toxic gas (H₂S, SO₂, etc.) or pollution are resulting from the blowout, consideration should be given to ignition of the well. The following is suggested criteria, equipment and procedures for ignition. Under certain conditions it may be necessary to ignite well flows which do not contain H₂S. This is typically a difficult decision based on safety and environmental factors such as pollution and the perception that ignition will reduce risks and pollution. This decision can involve legal and insurance related issues. If significant concentrations of H₂S are resulting from the blowout, consideration may have to be given to ignition of the flow. This is especially important if the well is situated in or near navigable waterways (inland waters), near populated areas or in extremely sensitive environmental areas.

NOTE! Unless ignition of the well flow will obviously reduce the immediate danger to the public or personnel, the OIC in charge should consult with ERT before making the decision to ignite the well.

Ignition can be a very dangerous operation, especially if oil slicks surround the structure or appreciable oil accumulates on and in the rig. The ignition of any blowout by untrained or under-equipped personnel should only be attempted if no other means exists to protect the safety of personnel in the vicinity. Further, proper equipment to do so safely must be available. If it is apparent that the hydrogen sulfide gas being released may endanger the health and safety of the public or wellsite personnel or may cause serious environmental contamination, the OIC in charge (or personnel designated by the OIC in charge) will ignite the gas cloud.

In some instances it may be prudent to ignite well flows which do not contain toxic concentrations of hydrogen sulfide. This is typically a difficult decision based on safety and environmental factors and often involves legal and insurance related issues. Unless ignition of the well flow will obviously reduce the immediate danger to the public or wellsite personnel, the OIC in charge, or designated representative, should consult with Regional Management before making the decision.

The decision to voluntarily ignite a blowout carries with it major implications. The worst being that the situation becomes worse rather than better. The greatest concern is that ignition will cause severe structural damage or, in the worst case, will damage adjacent wellheads causing additional blowouts and fires (multiple wells in an inland water situation). Further, this may cause the well control effort to be orders of magnitude greater than if a single well was blowing out but not on fire. The decision to purposefully ignite a blowout can only be done if it is thought that human life can be saved as a result or major pollution avoided. There will be other considerations that enter into the decision and are outlined below.

When H₂S is emitted from a blowout the decision becomes somewhat less complex due to the eminent danger to life. What must be considered in the ignition of an H₂S flow is the by-product of the reaction, SO₂. Sulfur dioxide is also a toxic gas that causes irritation of the upper respiratory tract, inflammation of mucous membranes, dry throat, cough and burning of the eyes with concentrations of 5 ppm to 100 ppm. High SO₂ levels or extended exposure can lead to death by asphyxia, chronic pneumonia or bronchitis, increased sensitivity to SO₂ and possibly cancer. The outcome is that fire does not remove the danger but it alters the characteristics. The downwind side of the fire still poses a danger in the form of SO₂ and should be isolated from access by personnel and vessels. In certain situations, where H₂S levels in the flow are not extreme, the SO₂ released due to burning may be manageable. Ignition in these cases may be the best alternative where extreme risk to the lives of personnel is at stake. Under most conditions, it is not advisable to automatically ignite an H₂S flow unless lives are in danger.

Once the decision to ignite is made, the decision then turns to the method. Although a remotely operated ignition system similar to that used to ignite a flare is an alternative, the risk of an unintentional or premature actuation due to panic makes this method undesirable. In most

situations the best alternative may be the use of a flare gun or other similar device to ignite the flow from the upwind side. This may be risky due to the limited access caused by the H₂S.

To assure proper consideration is given, the matters listed below should be examined:

- evacuation of all personnel from the area or facility.
- assure that no one or no equipment is working within a minimum of a two (2) kilometer or 1.2 miles downwind radius of the site.
- close valves or other devices which may provide a possible fuel source or migration path for a fire or flow.
- evaluate wind and weather conditions to ascertain whether the situation can change to endanger personnel either on the wellsite or at an adjacent installation.
- the nature of the flow, cause, probability of increased severity and assessment of methods to stop the flow through short term efforts
- will conditions permit a safe assessment without putting the evaluation team in undue risk
- whether ignition using a flare gun is possible from a safe distance, i.e., strong prevailing winds away from the firing position, H₂S free atmosphere from which to work, available cover from a flashback and clear access for escape.
- the range of the flare gun and whether access to the wellsite within this range is safe and possible in view of the presence of H₂S and heat radiation from the fire after ignition. Proceed if these conditions can be met.
- can one clear all personnel, aircraft, vehicles and equipment from within a 2 kilometer (1.2 mile) radius except for the vehicle required for a firing base.
- is an approach to the site from upwind side while monitoring H₂S levels available.
- once ignition has taken place no attempt to approach the site should be made until the situation stabilizes and conditions permit access with reasonable safety and under strict supervision of experts.

A basic decision tree is presented in the flowchart shown in section 3 8.8.1 to aid in the decision making process that must take place before igniting an H₂S flow. An alternate method using a helicopter may be considered. In this case a flare gun is the recommended method to ignite the flow.

Ignition Equipment

The following equipment will be available and on-site for use by the ignition team personnel:

- 2 - Flare gun with two dozen flares (one for ignition and one for spare).
- 2 - 500 ft. fire resistant retrieval rope.
- 1 - Portable Combustible Gas Detector.
- 1 - Portable H₂S meter and/or personnel monitors.
- 3 - Adequate number of SCBA's for ignition team members (min. of 3).
- 1 - Marine vessel with communication equipment (two-way radio, etc.).

Specific Ignition Procedures

The OIC in charge or alternate will ensure that wellsite personnel are evacuated to a safe location upwind of the well. The OIC in charge will then proceed with the following ignition procedures:

- The OIC and a designated assistant (either drilling supervisor or safety consultant), backed up by one or two designated wellsite personnel, will comprise the ignition team.
- The backup member(s) will be positioned by a radio equipped vehicle at a safe distance from the gas/oil release. They will standby to rescue the primary ignition team with the retrieval ropes, if necessary.
- The assistant of the team will carry an explosimeter and will continuously monitor the area for explosive gases.
- The OIC in charge will carry the flare gun. (Flare shells are to be carried in a separate container - not in your pocket).
- All personnel not required to operate the vessel used to make the approach should have been removed. Once within a safe range a single man should stand behind a protective barrier (vehicle, etc.). Escape from the area should be made with haste due to the possibility of secondary explosions and falling debris.
- The ignition team will determine the hazardous area (10% of lower flammable limits) and establish safe perimeters. Once this is determined, the ignition team should move to the upwind area of the leak perimeter and fire a flare into the area. If the leak is not ignited on the first attempt, move in 20 to 30 meters parallel to the well and fire again. If trouble is incurred in igniting the gas, attempt to fire a flare at 40 to 90 degrees to each side of the area where you have been firing. If adequate equipment is not available or ignition is not possible, the toxic leak perimeter must be established and continued until the emergency is secured.
- Escape from the area should be made with haste due to the possibility of secondary explosions and falling debris.

**8.9 PERSONNEL SAFETY & VICTIM MANAGEMENT CHECK LIST**

Date : _____ Time : _____ Filed by : _____ Title : _____

IMMEDIATE VICTIMS	YES	NO	REMARK
• All personnel/contractors accounted for?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Triage/treatment/transport functions established?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Medical facilities identified/notified?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Transportation to specialty hospitals?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Police notifications?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Victims identified?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Victim list complete/verified?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Victims' families notified?	<input type="checkbox"/>	<input type="checkbox"/>	_____
SEARCH AND RESCUE			
• PTTEP personnel rescue?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Public agency rescue?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Full protection for rescue/back-up personnel?	<input type="checkbox"/>	<input type="checkbox"/>	_____
PUBLIC			
• Evacuation of public required?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Medical assistance required?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Local agencies notified to assist?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Weather or other factors to potential affect the isolation area?	<input type="checkbox"/>	<input type="checkbox"/>	_____
CONTROL (MINIMIZE IMPACT)			
• Special diagnostic and care facilities identified?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Employee and family assist/counselling identified?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Human resources support identified?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Personnel Center activated?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Liaison with Authorities underway?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• All communication between sites OK?	<input type="checkbox"/>	<input type="checkbox"/>	_____



RESPONSE	YES	NO	REMARK
SPILL MANAGEMENT			
• ECG/EOC activated?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Source identified?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Leak/release stopped?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Release continuing?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Downwind evacuation?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Ignition sources eliminated?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Released ignited/burning?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Perimeter/exclusion zone established?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Exposures?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Command Post established?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Unified command with responding agencies?	<input type="checkbox"/>	<input type="checkbox"/>	_____
CONTROL & SUPPRESSION			
• Incident Action Plan developed?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Control method identified?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Control method risk v. gain agreement?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Foam applied to suppress flammable vapors?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Foam applied to burning pool fires?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Foam applied to burning pool fires?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Fire allowed to burn out?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Water fog applied to exposed wellheads and equipment?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Fuel control accessible?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Suppression strategy developed?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Suppression strategy acceptable for safety?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Expected release duration: _____ days/hrs.			
STATUS			
• Extinguished?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Still burning/size?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Contained?	<input type="checkbox"/>	<input type="checkbox"/>	_____
• Exposures?	<input type="checkbox"/>	<input type="checkbox"/>	_____



RESPONSE	YES	NO	REMARK
SAFETY			
• Site Safety Plan completed?	<input type="checkbox"/>	<input type="checkbox"/>	
• Hazard monitoring completed?	<input type="checkbox"/>	<input type="checkbox"/>	
• PPE requirements defined?	<input type="checkbox"/>	<input type="checkbox"/>	
• Decon area(s) established?	<input type="checkbox"/>	<input type="checkbox"/>	
• Site Security plan completed?	<input type="checkbox"/>	<input type="checkbox"/>	
• Site Security enforced?	<input type="checkbox"/>	<input type="checkbox"/>	
• Air quality monitoring underway?	<input type="checkbox"/>	<input type="checkbox"/>	
HAZARDOUS MATERIALS			
• Affected facilities notified?	<input type="checkbox"/>	<input type="checkbox"/>	
• Gas characteristics known?	<input type="checkbox"/>	<input type="checkbox"/>	
• Toxic or hazardous?	<input type="checkbox"/>	<input type="checkbox"/>	
• Plume model run?	<input type="checkbox"/>	<input type="checkbox"/>	
• Exposure areas identified?	<input type="checkbox"/>	<input type="checkbox"/>	
• Site control in effect to protect response workers?	<input type="checkbox"/>	<input type="checkbox"/>	
• Evacuation or affected-area-control initiated?	<input type="checkbox"/>	<input type="checkbox"/>	
WELL CONTROL			
• Well control be established field/rig?	<input type="checkbox"/>	<input type="checkbox"/>	
• Capping and or firefighting required?	<input type="checkbox"/>	<input type="checkbox"/>	
• Technical well-control ex-perts on-scene at command post or tele-linked?	<input type="checkbox"/>	<input type="checkbox"/>	
• Relief well required?	<input type="checkbox"/>	<input type="checkbox"/>	



9.0 BLOW OUT RESPONSE PLAN INTRODUCTION

The Blowout Response Plan is cover to the long-term action once the immediate emergency is blow out in Level 3 accident. The Blowout Response Plan will be under Blowout Control Task Force (BCTF) member.

The Blowout Control Task Force is a team within the ERT. Decision to mobilize the Blowout Task Force is taken by the ERT Leader and the BCTF leader will report to the Incident Commander.

The BCTF will be independent of normal activities to minimize the impact on routine operations. There will always be single point leadership of the various components of the Task force to ensure that they are working in a coordinated manner.

The Task force will generally consist of two or more teams:

- Well capping team
- Relief well team.

9.1 EMERGENCY RESPONSE TEAM -ERT

The Emergency Response Team (ERT) will be activated and mobilized by the Vice President or acting VP and assembled in the Emergency Response Room (room 2948) at the Energy Complex Building A, 29th floor. The ERT **shall follow the guidelines and procedures** as detailed in the PTTEP Duty Officer and Emergency Management Plan. The ERT is charged with the full responsibility for the control operation and shall take control of all aspects of the logistics situation.

Notification of the Emergency leading to the ERT mobilization will be done as per section 2.3, Notifications.

9.1.1 Authorities and Responsibilities (1st Priorities Assigned to ERT)

A summary of action and liaison responsibilities for the ERT during a Blowout Emergency is given here below. This just highlights the main duties. For the additional tasks the reference manual is the Duty Officer and Emergency Response Group manual. ERT organization chart as per Figure 1.

ERT Member	Action	External Liaison Responsabilités
On-Scene Commander (OSC) ERT Leader (EDL)	<ol style="list-style-type: none"> Ensure that all appropriate ERT disciplines have been contacted and have a representative. Maintain permanent contact with site. Mobilize additional resources if needed. Assess the number, type and identity of casualties, extent of damage to facilities. Nominate a Blowout Control Task Force leader. Liaise with EMT leader. 	Site of Emergency. Specialized Contractors in Blowout Control.
Manager, Drilling Operation (EDL/O)	<ol style="list-style-type: none"> Receive Control of BCTF from Emergency Controller. Coordinate and Organize the Blow Out Control Task Forces. Notify the Blow Out to the rig owners and all sub contractors. Contact Blowout Advisor. Start to organize the BCTF. 	Rig owners, Capping Co., Blowout Advisors.
Logistic/Marine Support (OLG)	<ol style="list-style-type: none"> Liaise with the Logistic Base Superintendent in Songkhla (OLG/O) and establish the position of the marine vessels and helicopters that can be made available. Ensure readiness of logistics in nearby PARTNERS subsidiaries in the event they have the necessary equipment and personnel Obtain Weather Forecast. Contact and liaise with the shipping contractor, marine contractor and helicopter contractor. Arrange general transport. Arrange transportation for specialists. 	Marine Weather Services Service Vessels Owners Lloyd Helicopter GCNK Logistics Singapore Equipment Suppliers Transport
Safety, Security, Health, & Environment Division (TSH)	<ol style="list-style-type: none"> Obtain POB information for the site concerned and dispatch to all ERT members. Advise the Emergency controller on health, safety and 	<ul style="list-style-type: none"> Police, Thai Navy, DMF. Fire fighting resources, Contractors

	<ol style="list-style-type: none"> environmental matters. Establish fire-fighting resources that can be made available for support. If relevant implement the Spill Contingency Plan. Obtain immediate assistance from other companies as required. Establish liaison with DMF. 	
Personnel Administration (HHR)	<ol style="list-style-type: none"> Organize the administrative support required by the BCTF. Supply housing to outside experts joining the BCTF. Takes care of visa / work permit problems (if any) Supply additional medical support. Support Relatives Response Team 	
Asset Finance Department (FAC)	<ol style="list-style-type: none"> Organize the finance officer on duty support required by the BCTF. Support Risk Management Information 	
Procurement (POC)	<ol style="list-style-type: none"> Organize the procurement officer on duty support required by the BCTF. Support Procurement Information and Process 	

9.2 BLOWOUT CONTROL TASK FORCE- BCTF

The BCTF is a team composed of PTTEP, Partners and external personnel dedicated to the well killing operations.

The different leaders in the BCTF will be nominated by the Operation Support.

9.2.1 Notification, Activation and Assembly

The BCTF is the operational entity that is exclusively dedicated to the blowout control operation.

Some main principles must be kept in mind in organizing the BCTF:

- Personnel assigned to the BCTF from within PTTEP must be relieved from all other duties.
- Personnel who might have been deeply affected by the trauma caused by the blowout should not be assigned to the BCTF in any case, and should be replaced by other personnel.
- The best experts must be chosen to perform the job within or outside of PTTEP, such as partners. There should be no hesitation in obtaining assistance from whatever source necessary.
- It is the responsibility of both the Operations Manager, Chief Engineering Operation, and the DSV to gather the best team possible, as quickly as possible, to deal with the situation.
- The BCTF leader will first organize the BCTF with the Operations Unit people and complete it thereafter with external assistance such as PARTNERS personnel.
- A secretarial assistance should be organized for the BCTF in order to keep an accurate and detailed log of events. The ERT will organize this.
- A specific cost controller (from Finance Department) must be assigned to the BCTF to follow up the costs related to the capping and relief well operations.

**THE BCTF MUST BE GIVEN ALL AVAILABLE MEANS TO
FULFILL 100% OF ITS OBJECTIVE:**

RECOVERING THE CONTROL OF THE WELL

The Manager, Drilling Operation is nominated by the Technology and Operations Division as the Task Force Leader.

In case he is not available the Technology and Operation Division will then designate another Task Force Leader.

The basic philosophy adopted by PTTEP Operations and adhered to, will be to create two separate teams inside the BCTF:

- The Capping Operations Team.
- The Relief Well Operations Team.

The main objective of the BCTF Leader (OTE/O) will be to simultaneously start preparation of both activities, so as each one may start independently of the other one and in the shortest possible time scale.

The BCTF leader will then appoint the leaders for the Capping and Relief Well teams. He will submit the names of the above persons to the Operation Support for his approval.

In addition and in parallel to the BCTF a Crisis Advisory is set up. The Crisis Cell will be led by the BCTF leader. A composition of the Crisis Cell is shown in the Fig below.

9.2.2 General Organization of the BCTF

The basic philosophy adopted by PTTEP Operations and adhered to is to create two (2) separate teams inside the BCTF.

They are

- The Capping Operation Team
- The Relief Well Operation Team



Note : The Blowout Advisor will be mobilized by the BCTF leader.

The Insurance Advisor will be mobilized through PTTEP

9.3 BCTF MEMBERS JOB DESCRIPTION

The following pages outline the "Job Specifications" for various critical members of the BCTF. They intend to fulfil two purposes:

- To outline the requirements for various members of the BCTF so that a fast and effective search can be made within or outside PTTEP for the best personnel to assist in dealing with the emergency.
- To assist in briefing the personnel as they arrive at their desired location, enabling a speedy assimilation into the organization.
- Any personnel assigned to the BCTF will be relieved of all other duties for the duration of the emergency.
- The selection of the people to be assigned to the BCTF should be as follow:

- Operational Staff having the required level of knowledge and competency shall be assigned to the blowout task force as much as possible. This is motivated by their good knowledge of the specific field problems.
- However, as per EMP, OTF/O judgment any PTTEP personnel deeply affected by the trauma caused by the blowout shall be replaced by other available engineers, PARTNERS for instance.
- Specific tasks must be assigned to people having already gained practical field experience. Therefore the BCTF leader shall not hesitate to call for PARTNERS specialists, if none are available in PTTEP staff.

9.3.1 The Crisis Advisory

Crisis Cell Member	Origin	Responsibilities
BCTF Leader	Shall be Chief, Drilling Operation (OTF/O).	<ul style="list-style-type: none"> Coordinates the various operations and takes the experts advice. He is responsible for the operations carried out. He shall report to the Incident Commander and obtain his approval for major decisions.
Partners and/or Management Representative	A Expert with good leadership and technical background. He must have a good knowledge of blowout control operations.	<ul style="list-style-type: none"> Strictly an advisory function: as PARTNERS representative he shall provide the best advice possible so as to assist the local team in decision making. He is not entitled to take any technical leadership during the operations nor to give any orders or instructions
Blowout Advisor	<ul style="list-style-type: none"> Boots & Coots IWC or Any reputable Consultant. 	<ul style="list-style-type: none"> Advisory role only. Due to his high competence in blowout engineering he will advise on the best well control strategy. He shall assist the BCTF leader in making the decision on relief wells matters. He shall only give advises to PTTEP management. His assistance will be of particular importance in the liaison with the insurance representative to their full cooperation and assistance.
Insurance Surveyor	Insurance Company Representative	<ul style="list-style-type: none"> Consultation Information only.

9.3.2 Blowout Task Force Teams

Capping Operations

Capping Team Member	Origin	Responsibilities
Capping Operation Leader Drilling Superintendent	PTTEP staff must have : - Good knowledge of the overall structure and systems on the particular installation (Rig, Platform). - A perfect knowledge of the well status - A perfect knowledge of local suppliers and of the general logistics organization. This providing he has not been deeply affected by the shock of the blowout. - He shall be relieved from any other duty if deemed necessary.	<ul style="list-style-type: none"> - Planning and Supervision of Capping operations. - Submit to the BCTF leader all the plan of actions he has approved. - He is the only person entitled to give orders/instructions to the Capping Consultant - Define materials and equipment - Preparation of the Capping Operations and decision tree. - Liaison with the Blowout Advisor and Capping Consultant to find out the quickest and the safest way to kill the well. - He shall supply the above specialist with all data in relation to the concerned installation. - He shall give assistance to the Capping Team. - He is responsible for carrying out the technical investigation with the local suppliers so as selecting the specific equipment required. He then passes the investigation results to Logistic for actions.
Drilling Engineer	Supply the Blowout Advisor with field data as well as the Capping Consultant.	<ul style="list-style-type: none"> - Preparation of the capping program and in relation with Drilling Superintendent and Capping Consultant. - Liaison with capping specialist as Operations safety representative to Organ; efficient well site safety and secur coverage.
		<ul style="list-style-type: none"> - Responsible for supplying pertinent well at field data.
Mud Superintendent	Staff with a perfect knowledge of local supplying capacities for swift assistance to the capping team.	<ul style="list-style-type: none"> - Assistance to the capping team to find all required killing equipment such as pumps, killing fluid, piping.

Capping Team Member	Origin	Responsibilities
Capping Consultant	Recommended companies are: 1. Wild Well Control Inc. (WWCI) 2. Boots & Coots IWC (B&C/IWC) 3. Alert Disaster Control Singapore 4. Cudd Well Control (CWC)	<ul style="list-style-type: none"> - Organization and safety for capping personnel and operation. - They shall advise the BCTF Leader and the Capping Operation Leader and report to them. - They receive orders only from the capping Operation leader. - They may require the assistance of the Drilling Superintendent and Logistic support for the supply of any required item. - They will require data from the Drilling Engineer. - Once their plan of action is completed they must get the approval of the Capping Operation Leader before implementation.
Logistic Support	A minimum of two (2) persons must be assigned to the Capping Team. One will be in charge of the Procurement and the other one of the Transport.	<ul style="list-style-type: none"> - Urgent contact with the local Assistance Organization (if any), in liaison with the safety team, in order to bring the additional facilities to the field, to fight the fire, to provide lifting and power facilities. - Assignment of supply boats in liaison with the Marine Superintendent and of the Helicopters to the exclusive use of the capping operations. - Mobilization of emergency accommodation for the various specialized personnel and additional hands required to carry out construction, firefighting, debris cleaning. - Coordination of all engineering tasks to be implemented on the blowout site (works for supply, spraying, placing protection shield, illumination for night works...). - Organization of an efficient and rapid transportation of all specific equipment (from USA or EU). - Quick settlement of all purchasing and rental paperwork, for earliest delivery. - Rapid contact with all possible suppliers. - Massive and rapid purchase of cement and barite that might be required for killing operations.

Relief Well Operations

Relief Well Team Member	Origin	Responsibilities
Relief Well Leader	<ul style="list-style-type: none"> -Should normally be Senior Drilling Engineers -Shall have a good leadership capability and a good knowledge of PTTEP field's specific problems. -He also needs experience in directional drilling in the Gulf of Thailand. 	<ul style="list-style-type: none"> - Planning and supervision of relief well drilling, completion and subsequent kill . - Shall submit to the BCTF Leader all the programs of action for approval, review or comments.
Drilling Engineer	<ul style="list-style-type: none"> - Engineer with a good knowledge of BHA behaviour. - He must be experienced drilling engineer to be able to rapidly starts to organize a possible relief well. - He shall be relieved from any other duties. 	<ul style="list-style-type: none"> - Preparation and day to day follow up of the program with the directional coordinator. - Preparation of the relief well decisions tree. - He is responsible for finding all directional equipment and proximity tools. - He shall provide full assistance to the directional coordinator, as well as all the data required by him. - He is responsible for the relief well casing design and geometry according to the selected kill strategy and program. - Liaise will kill coordinator and reservoir engineer
		<ul style="list-style-type: none"> - Carry out all necessary calculations related to the relief well options. - Work out the necessary pumping pressure and power required to stop the blowout. - To advise the killing coordinator.
Reservoir Engineer	PTTEP or PARTNERS shall be integrated in the BCTF He must be an expert in mono or biphasic flow calculations	<ul style="list-style-type: none"> - To liaise with the blowout advisor to supply him data required for the killing calculations. - To liaise with the killing coordinator and perform the necessary computer runs to assess the BHFP, the required kill pumping rate and the related killing procedure. - Evaluate the possible depletion that may affect the formations drilled by the relief well.
Mud Engineer	If both capping and relief well activities are ran in paralleled the local Mud Engineer will need external support.	
Drilling Superintendent	PTTEP staff or PARTNERS if needed	<ul style="list-style-type: none"> - Follow up of day to day drilling operations. - Shall be involved in the selection of the relief well drilling rigs and shall closely supervise the BOP inspection and refurbishing. - Shall liaise with the Kill coordinator to select the proper kill string.
Directional Coordinator	Contracted. Must be an expert in directional drilling	<ul style="list-style-type: none"> - Lead the relief well location. - Deciding in cooperation with the

Relief Well Team Member	Origin	Responsibilities
	and proximity tools.	<ul style="list-style-type: none"> Drilling Engineer the directional drilling and survey policy of the relief well. - To submit the program to the Relief Well leader for approval. - Fully in charge of field leadership. - Shall be the only person to give orders or instructions to the offshore directional team and to the proximity tool operator.
Kill Coordinator	<p>Contracted</p> <p>Must be a specialist having already managed similar operations and / or having a good knowledge of HP pumps technology.</p> <p>He shall be nominated as soon as the blowout has initiated to immediately start to investigate on pumping equipment needed.</p>	<ul style="list-style-type: none"> - Immediately investigate for pumping equipment available in the South East Asia, Europe and United States. - Calling out for a competent pump expert from Halliburton or Dowell or BJ and put at PTTEP sole disposal. - Design the equipment layout with the pump expert. - Organize the kill program as per the selected killing procedure. - Liaise with Reservoir and Petroleum engineers and workout the pumping program in order to avoid any formation breakdown. - Investigate according to the situation the need of a second kill line system is necessary and settle the matter with the suppliers, in liaison with the Drilling Superintendent regarding all matters in relation with BOP risers modifications. - Liaise with the Drilling Superintendent to design the kill string, to check the rig deck space, pit capacity, BOP design, riser modifications, quality control..... - Request Mud Engineer to build the kill mud for the relief well. Assign specific transportation means to the relief well rig.
Pump Expert	Contracted from one company like Halliburton, Dowell or BJ. He must be competent in massive pumping operations and if possible some experience in this kind of operation.	<ul style="list-style-type: none"> - Organize the localization and the availability of all necessary pumping units in South East Asia, United States or Europe. - Perform the pre-assembly, test and modifications if needed onshore. - Organize the future offshore pattern. - Planning for offshore transportation, spare parts, offshore hook-up, water and mud supply, monitoring, communications, etc. - Selection of the proper surface piping and manifolding in order to minimize the pressure drops.
Drilling Supervisor	As a 24 hours continuous supervision is mandatory two (2) supervisors will be needed. They must have a consistent experience in regards with the type of rig selected for the relief well operation.	<ul style="list-style-type: none"> - Supervision of the relief well operations and drilling on site. - Permanent communication with the Drilling Superintendent. - Give to the onshore team all the information needed to make the best decision.

Relief Well Team Member	Origin	Responsibilities
Rig Engineer	Only if deemed necessary by the BCTF leader. Must have experience in directional and well engineering.	- Adaptation and follow up of the relief well engineering on a day-to-day basis.
Mud Supervisor	One must be assigned in each supervision team.	- In charge on site of the follow up of the mud program.
Logistic Support	A minimum of two (2) persons must be assigned to the Relief Well Team. One will be in charge of the procurement. One will be in charge of the Transports	Release the casing required. Arrange for urgent delivery if not available. - Investigate with other operators stocks. - Arrange reception/storage for extra equipment in pre-designated area. - Assistance to the transfer of the relief well rig to the required location.

9.4 BLOW OUT RESPONSE PLAN IN 1ST 24 HOURS

PTTEP Emergency Response Team (ERT) will be activated after received notice of emergency from offshore. The initiate action need to be done in first 24 hrs as follow.

- Initial evaluation
- Make personnel assignments
- Develop Initial Action Plan and Approve
- Issue Initial Action Plan detail to field
- Mobilize outside experts
- Make notices to Government and Partners
- Mobilize fifi boats and oil booms
- Activate BCTF

PTTEP Emergency Response Team (ERT) Mobilization

The procedure shall be as per PTTEP EMP Manual and the alert diagram shown in the Notifications section 2.3 of this plan.

Action Required	Action By
Notification of the Blowout to TSD, OTF, or Duty Officer and Field Manager	Drilling Supervisor or Duty Drilling Superintendent
Notification of the blowout to EVP, VP or acting VP. and TSD.	TSD, OTF or Drilling Superintendent or Duty Officer
Assembly of the ERG in PTTEP Emergency Response Room in ENCO office building A 29th floor, room 2948	TSD (Authorization by EVP, actual callouts by Duty Officer/telephone operator)

9.4.1 First Priorities assigned to the ERT (first hours after the blowout)

Once all personnel has been safely evacuated, the main objective is to initiate simultaneously the Capping operation and the Relief Well preparation, whilst safeguarding the installation. (refer to PTTEP Emergency Management Plan)

Always remember that, it is as important thinking about the vital need to slow down the fire destruction effect as initiating capping and relief well activities. The Logistics efforts will thus be of prime importance to ensure that all available firefighting means are on the site before the arrival of the capping team, so as:

- to avoid a total havoc and destruction from the fire.
- to facilitate the capping team job.
- However, obtain first of all a correct assessment of the situation:
- discuss with the PIC at the rig or location if still feasible
- obtain reports from witnesses still on the scene (supply boats, helicopters).
- organize (if needed/if possible) helicopter flights to visualize the disaster.

The objectives are:

- To give assistance to the casualties.
- To assess the **magnitude** and the type of problem.
- To determine the type of flow and source of flow.
- To identify the number of blowing/burning well.
- To evaluate the need for firefighting.
- To assess the extent of the structural damages.
- To find out whether the main power of the platform has been totally/partially lost.

Once this has been done it is important to avoid dissipation of energies and repetition of major phone calls, to define each person objectives, and to ensure the effective mobilization of the BCTF

At that time give the first major phone calls.

Action Required	Action By
Contact government and local authorities, and request support (Hospital, Police, Thai Navy, etc.)	TSD
Organization of the BCTF (see table 1 and 2 in section 2)	TSD/O
Contact with Partners to notify the blowout. Request Partners Rep. to come to Bangkok PTTEP Office. Request extra personnel assistance to: Take over routine activities (if any). Take part in the BCTF organization. (if required)	TSD
Notify the blowout to the rig owner and all subcontractors.	TSD/O
Contact the Blowout Advisor	TSD/O
Contact Insurance Co. and request the Insurance surveyor to come to Bangkok.	FAC
Contact Capping consultant.	TSD/O
Contact with "Operator Assistance club", if any, to call for MSV, crane barge, cranes, firefighting support....	OLG
Assignment of workboats and helicopter exclusively to the blowout.	OLG

9.4.2 Second Priorities (First 24 Hours after the blowout)

The objectives are

- To finalize the BCTF organization.
- To start investigating about the major required equipment (Capping, Relief Wells).
- To initiate massive purchasing (barite, cement).
- To gather the fundamental data required by the "Crisis Cell" and the Consultants.

Action Required	Action By
Select all required Partners assistance team.	EDL/O (BCTF leader)
Instruct Drilling Engineer to start gathering data on the blowing well.	Capping Operation Leader
Contact Rental Suppliers to specify equipment required by Capping Consultant.	Drilling Superintendent (Capping Ops.)
Notify DOWELL/HALLIBURTON /BJ to initiate search for pumps required by Capping Consultant.	Drilling Superintendent (Capping Ops.)
Organize heavy logistics to bring specific equipment (Capping) from Singapore, USA or Europe if needed	Logistic Coordinator (Capping)
Arrange for urgent transfer of extra firefighting support units to the site.	Logistic Coordinator (Capping)
Investigation about available drilling rigs for the Relief Wells.	Relief Well Leader
Notify to Directional Drilling Co. to put tools on standby and to mobilize experienced directional team.	Drilling Engineer (Relief Well)
Notify to Proximity Tools Co. to investigate on tools and delivery conditions.	Drilling Engineer (Relief Well)
Mobilize the means to fight or contain pollution if needed.	SSHE Manager

9.4.3 Convening the "Crisis Advisory" (within 48 hours after the blowout)

Once the "Crisis Advisory" members have been gathered in Bangkok (Special conference room, different from the ERT) all gathered data are supplied so as to assist them in decisions making.

Information about the "Crisis Advisory" suggestion / recommendations are given to the TSD by the BCTF leader.

The objectives of that phase is to define the delicate first steps of action. The experience / judgment of the PTTEP Manager and Partners Representative and blowout Advisor will be of particular importance, to assess the feasibility of a direct cap and kill which would not worsen the situation and/or put the whole structure in jeopardy

9.5 BLOW OUT RESPONSE PLAN IN CYCLE 2-5 DAYS

Once the BCTF is properly organized, and once the major options have been taken by the "Crisis Cell", the next step involves the practical implementation of the said options by the two BCTF teams.

This is a non-exhaustive list of the main actions which shall be taken so as to start capping and relief well activities under shortest term:

Relief Well Team

Action Required	Action By
Convening a Kill Strategy meeting to: <ul style="list-style-type: none"> Set up the type of killing procedure Decide on the number of killing wells. Define exact calculations and reservoir simulation requirements. Assess the possible type of pumping support. 	Relief Well Leader Kill Coordinator Reservoir Engineer Petroleum Engineer
Convening a Directional Strategy meeting to: <ul style="list-style-type: none"> Decide on general relief well(s) profile / program. Analyse all potential problems (Surface formation pressure charging.) Decide the surface location of the relief wells. Select the directional equipment. 	Relief Well Leader Drilling Engineer (Relief Well Team) Directional Coordinator Reservoir Engineer Drilling Superintendent (Relief Well Team)
Notification to SCHLUMBERGER / HALLIBURTON / BJ to initiate search for pumping support (skid unit or frac vessel) needed for the killing through the relief well.	Kill Coordinator
Inspection of the drilling rig(s) (if needed) to be used for the relief well.	Drilling Superintendent (Relief well team)
Preparation of the relief well programs and decision trees.	Directional Coordinator Drilling Engineer (Relief Well Team)
Release of casing for relief wells. Prepare to receive / store extra equipment / material in pre-designated area.	Logistic Support (Relief Well Team)
Transfer of selected rig to the relief well location. Transportation of all equipment to rig.	Logistic Support (Relief Well Team) Marine Superintendent
Installation of communication Network on the rig (if needed)	HIT
Analysis / Finalisation of Relief Well program and decision trees.	BCTF Leader Relief Well Leader

Capping Team

Action Requested	Action By
Convening a Capping Strategy Meeting to: <ul style="list-style-type: none"> Set up the field action/coordination Set up the exact requirements for equipment. Set up the logistic support / assistance. 	Capping Operation Leader Capping Consultant Drilling Superintendent (Capping Team) Drilling Engineer (Capping Team) Logistic Coordinator (Capping Team)
Preparation of Capping program and decision tree.	Drilling Engineer (Capping Team) Drilling Superintendent (Capping Team) Capping Consultant
Analysis / finalisation of the Capping program and decision tree.	BCTF Leader Capping Operation Leader
Transfer of specific equipment required for the capping to the site. Follow up of firefighting conditions, supply of back-up means if needed.	Logistic Coordinator (Capping Team)

Remark: Blowout Capping, Relief Well Drilling and Kill Strategy meetings shall be run simultaneously:

Blowout Capping is to be treated as urgent and with priority.

Kill Strategy will have a tremendous impact on relief well design (diameters) and profile (depth of kill, proximity required), on rig equipment, pumping equipment, kill fluid types, pump rates and pressures, etc.

Relief Well Drilling requires an extensive equipment mobilisation.

Before starting the operations do remember an important factor which will be very important for proper implementation of decisions and for logging of events:

Set all leaders' watches to ZERO, make sure they all show the same time.

9.6 ROUTINE OPERATIONS

According to the PTTEP philosophy three different situations have to be taken into account, which are:

- A blowout on the Exploration/Delineation rig operation.
- A blowout on the Development rig operation.
- A blowout on the Production Facility (production operations, wireline, coiled tubing, etc.

9.7 GEOLOGICAL ASSISTANCE

A geologist will be entirely dedicated to the relief well operations.

The mud logging company selection for the relief well shall be left in the hands of the Relief Well Operation leader.

9.8 SAFETY MEASUREMENTS AND ASSISTANCE

The ERT should be aware, following a blowout, of the potential of further incidents resulting from a lack of preventive measures.

Although many aspects of these safety measures will be met and attended to in the normal course of communication with various authorities and specialist groups, care should be taken in the following area:

- The setup of safety zone around the site of the blowout. All shipping in the vicinity, and for the duration of the emergency, should be made aware of the hazard.
- The Thai Navy should be continually kept informed on the area affected by the blowout.
- Adjacent facilities and any marine activities should be notified of the situation as soon as possible by whatever means necessary.
- All assessments of the situation should be notified to any craft proceeding toward the area to help in dealing with the emergency. This should enable the timely provision of the necessary safety facilities to protect personnel and equipment on board.

ALL THESE ACTIVITIES HAVE TO BE PERFORMED IN CO-ORDINATION WITH THE NAVY VIA THE PTTEP HSE MANAGER.

It is suggested to request the assistance of CSH and/or partners and ask for the most experienced and competent safety personnel especially in the case of pollution.

It is suggested also to call for people field experienced with blowout events.

The safety team shall focus on:

- Mobilizing rescue facilities and protective clothing.
- Providing full medical and evacuation support close to the blowout site.
- Evaluating the fire-fighting needs. Remember that the well capping success highly depends on the quick response to the fire destructive effect (*)
- Carrying out gas monitoring and erecting warning signs.
- Evaluating the needs to fight against the pollution.
- Identifying hazardous areas and finding out whether it is necessary (in cooperation with the blowout advisor) to ignite the blowout to secure the safety of the people.
- (*)Note that the "Blowout Concept" shall be taken into account when designing the fire-fighting equipment of offshore development drilling platforms.
- The main objective is to be able to cool the structures and avoid its collapse.
- Advise the capping consultant on safety matters in order to have a safe capping operation.
- Call for external fire-fighting means and to have these supports on the site in the shortest time.

10.0 APPENDICES

10.1 LOGISTICAL CONSIDERATIONS FOR OFFSHORE AND MAJOR RESPONSE

IMPORTANT: Prior knowledge of what will be required and how it can be obtained will be extremely important. This is precisely what this section will outline and discuss. One of the very first assignments of the Incident Manager should be to designate the Logistics Coordinator to locate and define the availability of equipment and services required to respond to a major blowout.

In the event of a major blowout, efficient mobilization of the necessary equipment will depend on knowledge of what equipment is needed. This section provides guidance on such logistical considerations.

A listing of the equipment typically requires for a large surface blowout is outlined below. In Thailand, much of this type of equipment is available and can be procured in country. If this equipment is unavailable, specialized firefighting equipment has to mobilize from Houston and Singapore.

10.1.1 Logistics

PTTEP's logistic base, Petroleum Development Support Base (PSB), is located in the Singhanakorn District at 07° 14' N 100° 34' E close to the entrance of Songkhla Lake. The Base is about 50 km from Hat Yai Airport and 30 km from Hat Yai railway station. Access to the Base by road is either via Highway 407 from Hat Yai or by coastal Highway 408 from Nakorn Srithammarat. The base is about 900 km North of Singapore by road.

PSB will be used as the logistic base to support the three fields covered by this plan, namely, Bongkot, Arthit and Nang Nuan, which are at a distance of about 110, 132 and 195 nautical miles from the base, respectively. PSB is the subsidiary of PTTEP International. It is the only dedicated supply base supporting oil and gas industry in the Gulf of Thailand. It operates year round, 24 hours a day. Base facilities include a six-berth Jetty, warehouses, open storage yards, bulk storage tanks and silos, cold storage, workshops, and a marshalling yard. The facilities are fully protected by security services. All marine activities are controlled from the Operations Centre in the Base Administrative Building. PSB is located close to Songkhla Deep Sea Port, and within easy reach of PSB Heliport, Songkhla Town and Hat Yai Airport.



Excluding the organization of the blowout intervention team, the most complicated and typically overlooked components of implementing an emergency project are the logistics of required services and equipment. Many of these services are very specialized and may not be available in the immediate region or area. Also, knowledge of many of these services and the companies which provide such services may be unknown to the typical oil company engineer who has minimal experience with an intervention project.

An expensive and time consuming learning curve, with sometimes disastrous results, has been evidenced in many projects which utilized standard services beyond their capabilities and overlooked details which became insurmountable. There are methods to reduce the associated problems with good logistics practices for any project. The primary one is planning for what will be required and how it can be obtained.

10.1.2 Drilling Rigs

PTTEP is currently operating jack-up drilling rigs and tender assist barge for support exploration and development campaign.

10.1.3 Location and Distances

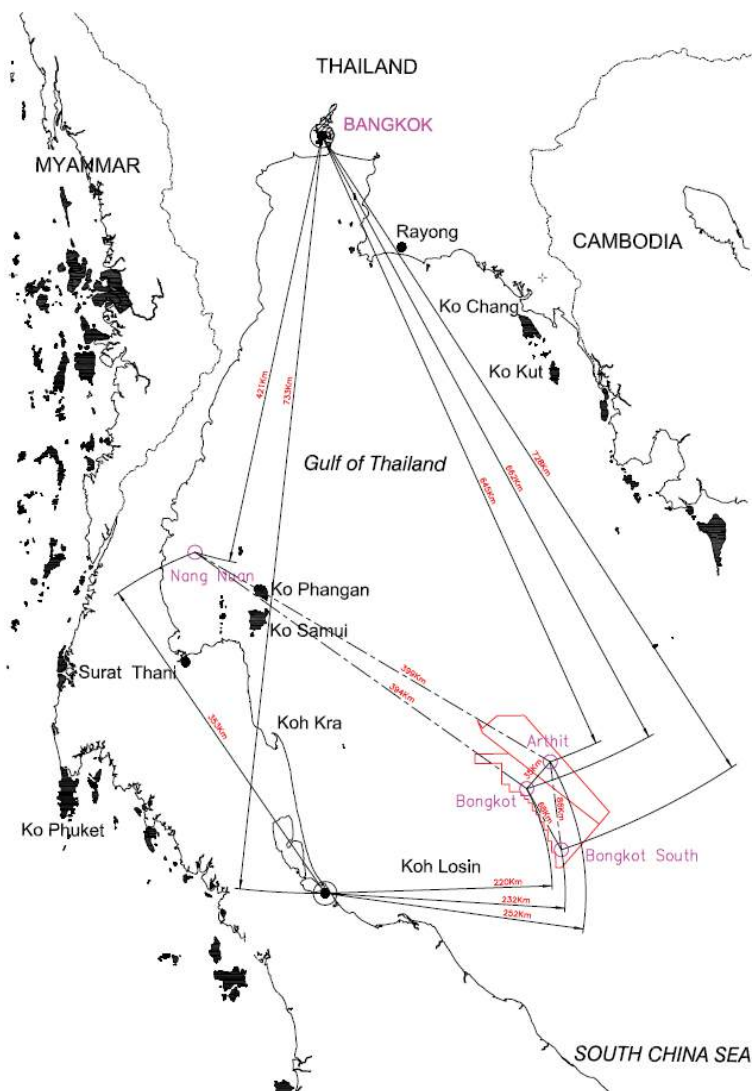
Distances and ETA

Point of Reference		Approximate Distance	ETA	By Mean		
From	To			Trailer Truck	Air	Sea
Singapore	Logistic Base in Songkhla	900 km	10 hrs	X		
		900 km	2 hrs		X	
Songkhla	Nang Nuan	195 nm	20 hrs			X
		361 km	1.5 hrs		X	
Songkhla	Bongkot	110 nm	12 hrs			X
		204 km	50 min		X	
Songkhla	Arthit	132 nm	14 hrs			X
		244 km	1 hr		X	

Petroleum Development Support Base (PSB) Coordinates and Addresses

07° 14' N 100° 34" E

PTTEP Offices in Bangkok
Energy Complex Building A Floors 6, 19-36
555/1 Vibhavadi Rangsit Road, Chatuchak, Bangkok 10900, Thailand
P: +66(0) 2537-4000
F: +66 (0) 2537-4444



10.1.4 Met-Ocean Information (Gulf of Thailand)

The Gulf of Thailand is bordered by [Cambodia](#), [Thailand](#) and [Vietnam](#). The northern tip of the gulf is the [Bay of Bangkok](#) at the mouth of the [Chao Phraya River](#). The gulf covers roughly 320,000 [km²](#). The boundary of the gulf is defined by the line from [Cape Bai Bung](#) in southern Vietnam (just south of the mouth of the [Mekong](#) river) to the city [Kota Baru](#) on the Malayan coast. At the height of the last [ice age](#) the Gulf of Thailand did not exist, due to the lower sea level, the location being part of the Chao Phraya river valley.

The Gulf of Thailand is relatively shallow: its mean depth is 45 [m](#), and the maximum depth only 80 [m](#). This makes water exchange slow, and the strong water inflow from the rivers make the Gulf low in [salinity](#) (3.05-3.25%) and rich in [sediments](#). Only at the greater depths does water with a higher salinity (3.4%) flow into the gulf from the [South China sea](#) and fills the central depression below a depth of 50 [m](#). The main rivers which empty into the gulf are the Chao Phraya (including its tributary [Tha Chin River](#)), [Mae Klong](#) and [Bang Pakong](#) Rivers at the [Bay of Bangkok](#), and to a lesser degree the [Tapi River](#) into [Bandon Bay](#) in the southwest of the gulf.

< <http://www.answers.com/topic/gulf-of-thailand#ixzz114vU8VbT> >

10.1.5 Petroleum Development Support Base (PSB) Jetty Facilities.

In the event additional heavy equipment should need to be transported from Singapore or Houston, it would arrive at Hat Yai International Airport.

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complete set of firefighting equipment and associated equipment for a major fire in a single load and unloading itself. No other commercially available aircraft has this capability.

Nose-load 747 cargo aircraft can also be used to haul all firefighting equipment. The large pipe rack unit and the 20' containers are the most difficult to load in a 747 cargo aircraft. Special cargo handling equipment is required to unload this type of aircraft. Any emergency air cargo charter flight will have to work with Thailand's transport agencies.

Heavylift Aircraft would land at the Hat Yai International Airport where the runway length can accommodate the Antonov 124 or 747-400.

10.1.8 PTTEP Marine Vessels Sheet

10.1.7 Heavy Airfreight

The Russian 124 Antonov aircraft brokered by Heavylift Air Cargo Ltd., Standsfield, U.K. can be made available (24 hour operations center phone number is 44-279-680611. This aircraft is capable of hauling 120 metric tons of oddly proportioned equipment and capable of hauling a

10.1.9 Incident Response Challenges at PTTEP offshore Locations

Personnel, equipment, and supplies during an incident will be flown to the installations or the drilling rigs (Level III) by helicopter or supply vessel (approximately 1 to 1.5 hours by helicopter and 12 to 20 hours by supply vessel). The main obstacles are:

- Distance from the Onshore Base.
- Transportation of Equipment, Supplies and Personnel
 - Any additional equipment, supplies and personnel will have to be mobilized via helicopter or supply boat. All heavy equipment and machinery will have to be transported by supply boat only.
- The limitations in working area and space typical of an offshore drilling facility.
 - Limits the ability to place additional well control auxiliary equipment.
- Any major incident will require evacuating all non-essential personnel from the drilling unit.
- Offshore operations represent a challenge.
- High seas that impede mobilization of equipment and personnel.

10.1.10 Role of a Rig Contractor

The key to successful blowout control is fast and efficient mobilization of the required support. The following list is not complete but can be used as a reference as to what may be required. The greatest key team member if a blowout is experienced will be the rig contractor, especially if they are experienced in how to acquire local available services, equipment and materials. The rig crew may be needed to assist the well control specialists. PTTEP should hold a pre-planning meeting with the rig contractor and discuss these and any additional points:

- Third party billing and purchase order system
- Cash flow assistance (must maintain good credit with local vendors)
- Increased rig crew pay for hazard duty (triple time is not uncommon)
- Added staff from rig contractor to handle logistical duties
- Spare equipment sources (ex: BOPs & choke manifolds)
- Welding/fabrication sources
- Oilfield supply sources
- Implementation of the fire water system

10.1.11 Minimum Recommended Firefighting Equipment

10.1.12 Specialized Firefighting Equipment

Quantity	Mobilized	Description
2		Fire pumps, minimum 4000 gpm @150 psi
1		Pipe rack, complete with suction & discharge hoses, water monitors, pipe nipples, fittings, butterfly valves, flanges, hammer unions, aluminium pipe, high temperature cloth, etc. necessary in rigging up fire pumps (see pipe rack inventory)
1		Job Box, complete with hand tools, hammer wrenches, brass hammers, air impact wrenches w/sockets, pipe wrenches, air grinders etc. (see job box inventory)
30		4" x 20" aluminum pipe w/indusco fittings
4		8" x 20' oil, suction and discharge hose complete with figure 100 hammer union
12		4" x 10' discharge hose complete w/ fig. 100 hammer Union
6		4" x 10' discharge hose complete w/ fig. 100 hammer union/male aluminium adapter
6		4" x 10' discharge hose complete w/ fig. 100 hammer union/female aluminium adapter
2		4" Stang monitors complete w/ nozzle & base
1		2" – 5" Porta-Lathe cutter
1		3" – 6" Porta-Lathe cutter
1		6" – 9" Porta-Lathe cutter
1		9" – 14" Porta-Lathe cutter
1		14" – 16" Porta-Lathe cutter
1		18" – 20" Porta-Lathe cutter
1 Lot		Miscellaneous spare parts for Porta-Lathe cutter
20		Double edge cutter blades for Porta-Lathe cutter
1		Halliburton Abrasive Jet Cutter
1		Spare parts for fire pumps
1		Junk shot Manifold complete w/rope, rubber, steel balls, golf balls and other plugging material



10.1.13 Rental Equipment

Quantity	Mobilized	Description
1		185 cfm air compressor
4		Light plants, trailer mounted
1		Generator
2		Pressure Washers

10.1.14 Metal for Fabricating Support Equipment

Quantity	Mobilized	Description
250 Sheets		3' x 8' sheets corrugated tin
1000 ft.		Large diameter pipe for fire water supply line (12" – 16")
1 sheet		2" steel plate
2 sheets		1" steel plate
2 sheets		½" – 5/8" steel plate
1500 ft.		2" x 2" x ¼" angle iron (heat shields for bulldozers)
50 sheets		3/16" or ¼" diamond plate, expanded metal or floor grating (flooring for monitor sheds, cutting sheds, etc.)
2000 ft.		2 3/8" or 2 7/8 " junk tubing (structural for building monitor sheds, sheds and heat shield)
1 Lot		Casing for diverter lines

10.1.15 General Oilfield Supplies

Quantity	Mobilized	Description
6		8" Figure 100 hammer unions
6		6" figure 100 hammer unions
12		4" figure 100 hammer unions
6		8" x 12" pipe nipples, threaded both ends
12		6" x 12" pipe nipples, threaded both ends
12		4" x 12" pipe nipples, threaded both ends
6		4" wafer type butterfly valves
12		4" 150# R.F. threaded flange
50		5/8" x 6 1/4 " studs w/nuts both ends
10 rolls		Tie wire
20		3/8" x 15' high test chain w/grab hooks
40		2" shackles, pinned
40		1 ¾" shackles, pinned
40		1 ½" shackles, pinned
40		1 ¼" shackles, pinned
40		1" shackles, pinned
40		¾" shackles, pinned
1-roll		½" manila rope
1 roll		¾" manila rope
4		200 psi liquid filled gauges
4		600 psi liquid filled gauges
4		1000 psi liquid filled gauges
4		3000 psi liquid filled gauges
4		5000 psi liquid filled gauges
4		10000 psi liquid filled gauges
2 Boxes		Shop Rags
2		Snatch blocks for 1 1/8" cable, shackled not hooked
		Structural lumber (2 x 4's) for heat shields



10.1.16 Specialized Oilfield Supplies

Quantity	Mobilized	Description
10 min.		Tanks for fire water or mud supply
2		Large volume diesel driven water transfer pumps (3000 gpm min.)
2		Mud charging pumps (to feed pumping equipment and tanks)
1		Mud system – complete with mixing and circulating capabilities
1000 ft.		High pressure tubing, for pumping or cutting operation (to maintain good distance between well and pumping equipment) size to be determined per requirement
1		Coil tubing unit
1		Snubbing Unit

10.1.17 Explosives and Associated Supplies

Quantity	Mobilized	Description
1000 lbs.		Explosives, 90 – 100%, general oilfield type
		Dry chemical
		Blasting caps for explosives
4		55 gallon drums
2000 ft.		auge wire, 2 wire minimum

10.1.18 Cables, Slings and Clamps

Quantity	Mobilized	Description
2000 ft.		1 1/8" 6 x 36 soft lay cable (for rig removal)
1000 ft.		¼" 6 x 36 soft lay (slings for debris removal)
1000 ft.		5/8" 6 x 36 soft lay cable (slings for debris removal)
100		11/8" cable clamps
100		¾" cable clamps
100		5/8" cable clamps
10		1 ½" x 10' wire rope slings 6 x 36 soft lay cable
20		1 ¼" x 10' wire rope slings 6 x 36 soft lay cable
20		1 ¼" x 20' wire rope slings 6 x 36 soft lay cable
20		1" x 10' wire rope slings, 6 x 36 soft lay cable
20		1" x 20' wire rope slings, 6 x 36 soft lay cable
40		3/4 " x 10' wire rope slings, 6 x 36 soft lay cable
40		¾" x 20' wire rope slings, 6 x 36 soft lay cable
40		5/8" x 10' wire rope slings, 6 x 36 soft lay cable
40		5/8" x 20' wire rope slings, 6 x 36 soft lay cable

10.1.19 Welders and Associated Equipment

Quantity	Mobilized	Description
6		Structural welders with helper and equipment
1		Certified Welder with Helper and equipment
4		Cutting torch complete with large supply of oxygen, acetylene and accessories, 250 ft. of hose per torch, strikers, tip cleaners and spare tips
2		Long reach cutting torch, complete with large supply of oxygen, acetylene and accessories, 250 ft. of hose per torch, strikers, tip

		cleaners and spare tips
--	--	-------------------------

10.1.20 Personal Protective Equipment (PPE), Personnel and Equipment

Quantity	Mobilized	Description
1		Decontamination area for personnel with change room
1		Decontamination area for equipment
2		Wind socks
		Flagging tape
6 min.		Two way radios with headsets
1 lot		Work gloves, ear plugs for work force
1		Weather forecast updated regularly
		Living accommodations for crew
		Meals for all work force
1 lot		H ₂ S equipment (if necessary)
1 lot		Drinking water with water cooler and cups
1 lot		Rain suits
1 lot		Rubber boots, work gloves and ear plugs for work force

10.1.21 Wellhead and Capping Equipment

Quantity	Mobilized	Description
1		Replacement wellhead for blowout well
1		Capping stack
1		Choke manifold
1		Choke house
1 lot		Spacer spools
1 lot		Diverter spools
1 lot		Spare flanges for diverter lines
1 lot		Spare parts for capping equipment (ring gaskets, studs, etc.
1		Extension tube for capping BOPS
1		Wellcat tool box
1		Mud/Gas Separator
1		Bowl/Slips
1 lot		Chicksan Iron Basket (loops, swings, straights, tees)
		Plug valves
		TIW valve w/handle
1		Drillpipe tree

10.2 LOGISTICAL CONSIDERATIONS FOR ONSHORE AND MAJOR RESPONSE - IMPORTANT

Prior knowledge of what will be required and how it can be obtained will be extremely important. This precisely what this Document will outline and discuss. One of the very first assignments of the incident Manager should be to designate the Logistics Coordinator to locate and define the availability of equipment and services required to respond to a major blowout.

In the event of a major blowout, efficient mobilization of the necessary equipment will depend on knowledge of what equipment is needed. This section provides guidance on such logistical considerations.

A listing of the equipment Boots & Coots typically requires for a large surface blowout is outlined below. In Thailand, much of this type of equipment is available and possibly be procured in country. If this equipment is unavailable, Boots and Coots has specialized firefighting equipment in Singapore and Houston and this equipment could be mobilized from there.

10.2.1 Logistics

The logistic base supporting PTTEP Thailand's onshore operations (S-1 and Ratana Fields) is located in the S-1 block about 400 km North of Bangkok. The Ratana field is about 400 km east of the S-1 logistic base, with a trucking time of about 8 hrs between the two locations.

In an emergency large cargo would move from Singapore or Houston to either Phitsanulok Airport (80 km from Ratana). An alternative would be trucking the equipment if coming from Singapore, which would require about two days of travel time.


10.2.2 Regional Perspective



10.2.3 Transport

In the event additional heavy equipment should need to be transported from Singapore or Houston, it would arrive at Phitsanulok Airport (80 km from S-1) or Khon Kaen Airport (80 km from Ratana).

Phitsanulok Airport			
<div><div></div><div><div></div><div>IATA: PHS – ICAO: VTTP</div></div></div>			
Summary			
Airport type	Public		
Operator	Government		
Serves	Phitsanulok, Thailand		
Elevation AMSL	154 ft / 47 m		
Coordinates	<div><div><div></div><div>Coordinates</div></div><div><div>16°46′23″N 100°16′56″E﻿•﻿16.77306°N 100.28222°E</div></div></div>		
Runways			
Direction	Length		Surface
	m	ft	
14/32	3,000	9,843	Asphalt
Source: DAFIF ^{[1]2]}			

Khon Kaen Airport			
IATA: KKC – ICAO: VTUK			
Summary			
Airport type	Military/Public		
Operator	Military		
Location	Khon Kaen		
Elevation AMSL	670 ft / 204 m		
Coordinates	<div>Coordinates</div> <div>16°27′59.86″N 102°47′01.18″E﻿ / ﻿16.4666278°N 102.7836611°E﻿ / </div>		
Runways			
Direction	Length		Surface
	ft	m	
03/21	10,007	3,050	Asphalt

10.2.4 Heavy Airfreight

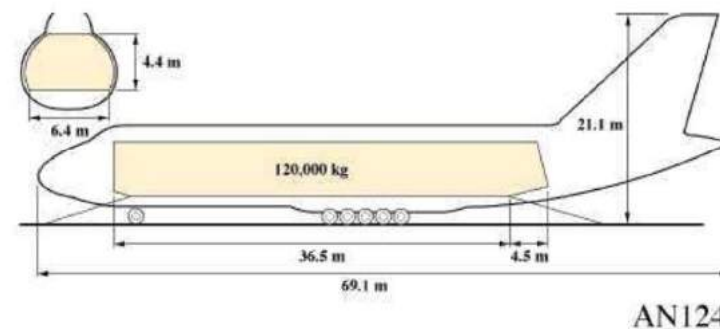
The Russian 124 Antonov aircraft brokered by Heavylift Air Cargo Ltd., Standsfield, U.K. can be made available (24 hour operations centre phone number is 44=279-680611. This aircraft is capable of hauling 120 metric tons of oddly proportioned equipment and capable of hauling a complete set of firefighting equipment and associated equipment for a major fire in a single load and unloading itself. No other commercially available aircraft has this capability.

Nose-load 747 cargo aircraft can also be used to haul all firefighting equipment. The large pipe rack unit and the 20' containers are the most difficult to load in a 747 cargo aircraft. Special cargo handling equipment is required to unload this type of aircraft. Any emergency air cargo charter flight will have to work with Kurdish transport agencies.

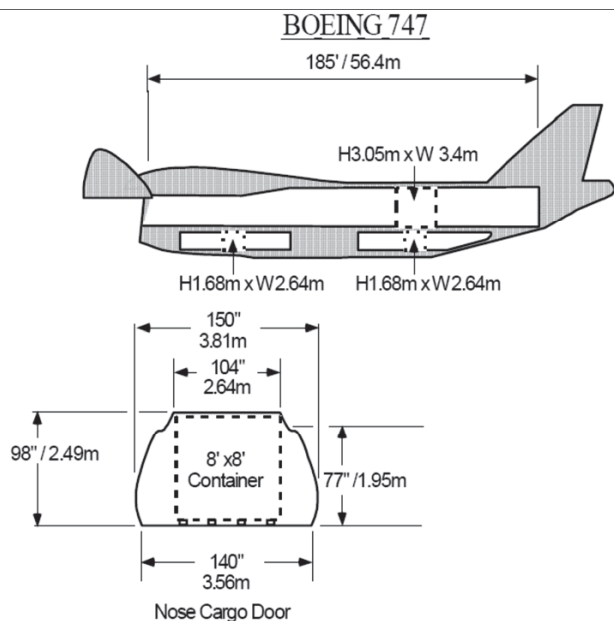
Heavylift Aircraft would most likely land in Khon Kaen or Phitsanulok where runway lengths can accommodate the Antonov 124 or 747-400.

List below are some data on air craft commonly for hire for air cargo.

Aircraft	Payload	Cargo Cabin		
		Length	Height	Width
Antonov 124	120,000 Kgs	36.5 metres	4.4 metres	6.4 metres
Antonov 22	55,000 Kgs	26 metres	4.4 metres	
Antonov 12	15,000 Kgs	23.5 metres	2.4 metres	
Llyushin 76	48,000 Kgs	20 metres	3.4 metres	
Belfast	25,000 Kgs	19.76 metres	3.65 metres	
Begula	74,000 Kgs	37.7 metres	7.10 metres	
Airbus A300 B4	45,000 Kgs	20 x P1 pallets, 20 LD3 containers		
Hercules L100-30	23,136 Kgs	17.07 metres.	2.74 metres	3.12 metres
S-64 E Helicopter	9,071 Kgs	Limited only by payload		
S-64 F Helicopter	11,339 Kgs	Limited only by payload		



Antonov AN-124	Metric	USA/Europe Moderate	Imperial	USA/Asia Long
Maximum Net Payload	150,000 kg	165 Ton	330,693 lbs	100 T
Main Cabin Floor Limitation	10,000 kg/m ²		2048 lbs/ft ²	
Max. Vol. Upper Deck	750 m ³		26,486 ft ³	
Uld / Pallet Capacity	10 x 6 m - 150 Containers			
Ht. of main cargo door sill from ground	218 – 300 cm			86 – 118 in.



Boeing 747 – 200 F	Metric	USA/Europe Moderate	Imperial	USA/Asia Long
Maximum Net Payload	123,184 kg	165 Ton	271574 lbs	100 T
Main Cabin Floor Limitation	976.5 kg/m ²		200 lbs/ft ²	
Max. Vol. Upper Deck	853.4 m ³		30,135 ft ³	
Max. Vol. Lower Deck	206.7 m ³		7,298 ft ³	
Uld / Pallet Capacity	9 x LD-7 or Equivalent			
Ht. of main cargo door sill from ground	Nose Door	4.72 – 5.18 M	86 – 204 in.	
	Side Door	4.90 – 6.10 M	193 – 240 in.	



C-130J-30	Metric	USA/Europe Moderate	Imperial	USA/Asia Long
Maximum Net Payload	19,090 kg	20 Ton	42000 lbs	20 T
Main Cabin Floor Limitation	976.5 kg/m ²		200 lbs/ft ²	
Max. Vol. Upper Deck	105.24 m ³		570 ft ³	
Uld / Pallet Capacity	8 pallets or 97 litters or 24 CDS bundles			
Ht. of main cargo door sill from ground	Rear Door	3.12 M	123 in.	

10.2.5 PTTEP Thailand Regional Perspective

Excluding the organization of the blowout intervention team, the most complicated and typically overlooked components of implementing an emergency project are the logistics of required services and equipment. Many of these services are very specialized and may not be available in the immediate region or area. Also, knowledge of many of these services and the companies which provide such services may be unknown to the typical oil company engineer who has minimal experience with an intervention project.

10.2.6 Incident Response Challenges at PTTEP Onshore Locations

- Remote field location
- Supply of water at high rates at the remote location
- Potential H₂S presence
- Limitedness and/or difficulty of access to the location during the rainy season
- Difficulty of drenching reserve pits at the Ratana location due to the hard nature of the surface.

10.2.7 Establishing a Water Supply

Probably the most important step when controlling a Level III incident is establishing a water supply that will be plentiful and consistent. The plan will be to set up two (2) 4000 or 6000 gpm pumps to supply water. Also, it will be necessary to use a 14-20 inch pipeline from the fire pumps to the fire main manifold which will be placed on the upwind edge of the location. This would enable us to use the water supplied at 153 psi discharge to reach the fire main and the monitor sheds with proper pressure.



10.2.8 Water Supply Storage



10.2.9 Water Supply Calculations

A blowout on fire requires a tremendous volume of water. For example, the following calculations show how fast a 1,000,000 (24,000 bbl) pit would be emptied using various capacity fire pumps.

$$1,000,000 \text{ gallons} / (6,000 \text{ GPM} + 6,000 \text{ GPM}) = 83 \text{ minutes}$$

$$1,000,000 \text{ gallons} / (6,000 \text{ GPM} + 4,000 \text{ GPM}) = 100 \text{ minutes}$$

$$1,000,000 \text{ gallons} / (4,000 \text{ GPM} + 4,000 \text{ GPM}) = 125 \text{ minutes...or 2 hours and 5 minutes}$$

In reality, the output of a 4,000 GPM pump is about 3,200 GPM.

NOTE: Some of the calculations below have been rounded.

Using 23,200 GPM the water usage is 6,400 GPM.

$$100,000 \text{ gal} / 6,400 \text{ GPM} = 156 \text{ minutes}$$

$$156 \text{ minutes} / 60 \text{ min per hour} = 2.5 \text{ hours water supply}$$

A 30% recovery rate extends the water supply to just over 3 hours

$$2.5 \times 1.3 > 3 \text{ hours}$$

If 1,000,000 gal is used in 3 hours, then 3,000,000 gal is used in a 9 hour work day.



The average water well in the S1 field produces about 190 bbls/hour

$190 \text{ bbls/hour} \times 42 \text{ gal/bbl} = 7,980 \text{ gal/hr.}$

With the pit full (1,000,000 gal) in the morning 2,000,000 additional gallons would need to be produced in a 9 hour period.

$2,000,000 \text{ gal/9 hours} = 220,000 \text{ gal/hour needed production}$

$(220,000 \text{ gal/hr}) / (7,980 \text{ gal/hr/well}) = 27 \text{ water wells.}$

The alternative would be to construct 21,000,000 gallon pits.

On hand supply would then be 6 hours with the need to replenish 1,000,000 gallons in 9 hours.

$1,000,000 \text{ gal/9 hours} = 110,000 \text{ gal/hr replenish rate}$

$(110,000 \text{ gal/hr}) / (7,980 \text{ gal/hr/well}) = 14 \text{ water wells.}$

To replenish the dry pits over night the water volume would be as follows:

$24 \text{ hours} - 9 \text{ hours} = 15 \text{ hours to replenish the pits}$

$2,000,000 \text{ gal} / 15 \text{ hours} = 130,000 \text{ gal/hr}$

$(130,000 \text{ gal/hr}) / (7,980 \text{ gal/hr/well}) = 16 \text{ wells.}$

NOTE: If necessary, water wells could be augmented by water tankers. Drilling for water wells and constructing water storage pits is expected to be difficult within the Ratana field due to the hardness of the surface. Water supply within the Ratana field will most likely be from one of the reservoirs in the area.

NOTE: if the above minimums prove to be logistically unfeasible, then operations would necessarily have to be planned around the water supply that IS available.

10.2.10 Civil Works Equipment

A critical point for any major onshore blowout is having the adequate heavy civil works equipment available. If the well is on fire, a D8 bulldozer (or larger) with a Cat Model 57 or Hyster D89C winch is typically used.

The civil works equipment (dozers, cranes, front end loaders etc.) and trucking must be locally obtained. Normally the main civil works equipment problem is the lack of large dozers equipped with a winch. Equipment will need to be maintained and have a working equipment inventory. It may be necessary to mobilize a skilled heavy equipment mechanic with the fire fighters to help keep the equipment running.

Machine shop services needed from custom capping equipment (ex: stingers, crossovers, custom flanges) should be identified and located. The Incident Manager should assign someone to locate these providers.

PTTEP Thailand will need dedicated support personnel working in the areas of transport, material acquisition, logistics, contracting, accounting and communications if a major blowout occurs.

It will be wise, at some point, to gather up the blowout task force and run a test drill on response to a blowout emergency scenario. Minute by minute well reports can be generated to simulate the type of information received from the field to the task force. The response steps are taken including vendor call ups. After the simulation is completed, the exercise is criticized and then edited based on the results of the simulation.



10.2.11 Role of a Rig Contractor

The key to successful blowout control is fast and efficient mobilization of the required support. The following list is not complete but can be used as a reference as to what may be required. The greatest key team member if a blowout is experienced will be the rig contractor, especially if they are experienced in how to acquire local available services, equipment and materials. The rig crew may be needed to assist the well capping specialists. PTTEP Thailand should hold a pre-planning meeting with the rig contractor and discuss these and any additional points:

- Third party billing and purchase order system
- Cash flow assistance (must maintain good credit with local vendors)
- Increased rig crew pay for hazard duty (triple time is not uncommon)
- Added staff from rig contractor to handle logistical duties
- Increase camp space options.
- Spare equipment sources (ex: BOPs & choke manifolds)
- Welding/fabrication sources
- Oilfield supply sources
- Implementation of the fire water system (water wells, pits and pipelines)

10.2.12 Typical Dimensions of Major Firefighting Components

- ATHEY WAGON: three pieces as follows: carriage 26.5' x 8' x 5.5' (15000 lbs), long boom 41' x 4.5' x 2.5' (3000 lbs) short boom 25' x 3' x 2.5' (1500 lbs). Two athey wagons required for a major rig fire.
- FIRE PUMP: integrated on skid (pump capable of 4000 GPM w/425 feet of head): 13' x 7' x 7.5' (10000 lbs). Two pumps required for a major rig fire.
- TRANSFER PUMP: integrated on skid (pump capable of 4750 GPM w/100 feet of head): 13' x 7' x 7' (9000 lbs). Two pumps required for a major rig fire.
- PIPE RACK UNIT: discharge piping and suction lines for pumps: 33' x 7' x 7' (20,000 lbs). One unit required.
- AIR COMPRESSOR UNIT: integrated on skid with priming pump to start fire pumps: 10' x 6' x 4.5' (3000 lbs).

10.2.13 Example Equipment List

The following is an example listing of the equipment and materials that will be required for major blowout scenarios. Not all of these items will be required nor is it a complete list as all blowouts are different and not all needs can be anticipated.

Worst Case Underground Blowout

- The major items that may be required are as follows:
- Cement pump and cementing lines
- Cementing batch mixer or additional mud mixing tank
- Cased hole wireline unit
- Pressure / temperature log, perforators, drill collar severing tool, gyro

- Possible additional stimulation pumps (higher rates and/or pressures required)
- Centrifugal pumps (mud transfer and circulation)
- Suction hoses and mud transfer lines (additional mud tanks and water pit)
- Sack cement and pure bentonite for bentonite – cement – diesel oil – plug
- Medium & coarse LCM materials (KwickSeal, mica, nut plug, ground CaCO₃)
- Additional mud products for quick mix mud (gel, water, caustic, barite, lignosulfonate).
- Additional water supply (possible additional water wells and water storage pit)
- New seismic to map gas flood front (sustained high rate gas flow).
- Re-survey surface location from fixed reference point (severe gas flow)
- Rate gyro run on drill pipe for better relief well target (severe gas flow)
- Initiate relief well planning (severe gas flow, potential loss of surface access).
- Additional mud storage tanks.
- Snubbing unit and tools (drill pipe off bottom, drill pipe plugged, hole in casing).
- Inflatable packer (unable to dynamically kill, due to a hole in casing)
- Handheld radios for site communication

Surface Blowout without Fire or Rig Removal

The major items that may be required are as follows:

- H₂S/Paramedic services: detection equipment, breathing air equipment
- Major civil works contractor to provide: 2 dozers (Cat D7), excavator, front end loader, compactor, 150 ton tracked crane (w/hook & bucket), probable 100 ton hydraulic crane, lube/fuel support, forklifts equivalent to a cat 950 and associated support personnel and skilled operators.
- Welding/fabrication contractor: to provide welders, welding supplies and equipment, nearby fabrication shop
- In country delivery/barge services
- Machine shop: to provide custom toll fabrication and modification
- Pumping/cementing services: to provide cementing unit, batch mixer/blender, spare tanks, pump lines, possible additional horsepower units.
- Medical evacuation services
- Well capping specialists
- Fire pumps and associated equipment
- Blowout technical advisor
- Two air compressors (185 CFM 150 psi) for air tools and engine starting
- Replacement valves, wellheads or BOPs. Additional ram blocks and packers, associated studs, nuts and ring gaskets.
- 75 kg wheel mounted fire extinguishers, additional smaller fire extinguishers

- Fabrication steel including (1/2" – 3/4" round stock, 1" steel plate, H-Beams)
- Dry ice and insulated transport box
- Teflon tape and thread lubricant
- Epoxy thread locking kits
- Cotton Rags
- Bottled drinking water
- Rest location for well capping specialists
- Flare pistol or rifle with flares
- Video and still photographer to record operations
- Location security and location access control of non-essential personnel
- Evacuation of local villagers, livestock
- Water well driller, casing and pumps (additional water supply requirement)
- Portable generators and light plants
- Misc. common oil field supplies and tools
- Ten handheld radios
- Diesel powered centrifugal pumps for fire protection, water transfer
- One reel of 1" to 1-1/8" (25 to 28 mm) soft lay steel cable for tie-downs, snub down lines and winches.

Major Rig Fire

The following services will be required:

- All of the above equipment (1.5.1 and 1.5.2)
- Support mats for pumps and equipment
- Four D8 equivalent dozers (prefer low ground pressure D8N dozers with cat Model 57 winches)
- Two cat Model 57 winches or those compatible with the dozers on location with power forward/reverse and no neutral (free spool) position
- Large walking crane > 150 ton with large boom, hook and bucket
- Two large cat 235 excavators
- Two cat 950 or 966E front end loaders with bucket and forks
- 2", 3" and 4" A36 steel plate (1m square)
- Structural steel: channel iron, box tubing, H beams, round tubing
- Air conditioned rest and paramedic stations
- River rock and gravel for location stabilization
- 6" pipeline pipe and 8-5/8" – 9-5/8" 8RD casing
- Water pumps for pipeline
- Light plants and generators

- Carpentry crews and materials (plywood, boards, nails, etc.)
- 50 ton rough terrain crane w/slides for assembling firefighting and capping tools
- Pipeline welding machines
- Anchor setting machine and anchors (auger type)
- Construction concrete and rebar
- UPS power supply for operations center
- 100000 psi discharge lines from Halliburton, Schlumberger or BJ (steel or Coflex)
- Additional horsepower from Halliburton, Schlumberger or BJ
- Over 50 handheld radios with extra batteries and multiple rechargers
- Over 5 long range mobile units
- Two international phone lines as the on-scene command center
- 1", 3/4" and 1/2" wire rope and cable clamps for slings
- Centrifugal trash pumps to pump out sumps, excavations and cellars

Normal Oilfield Services

Other considerations include such services and supplies as are normally used in oilfield operations.

The following is a partial list of the types of services or materials which may be needed.

- Oilfield Services and Materials:
- Mud Supplies and Mixing Equipment
- Civil Works (earth moving)
- Water Tanks
- Environmental
- Rental Tools
- Communications
- Cementing Stimulation Services
- Slick Line
- Open hole E-Line
- Cased Hole E-Line
- Well Testing
- Wellhead Maintenance
- Hot Tapping

Other Requirements

BOP and well control equipment will likely be rented locally but it may be necessary to bring in a specialized capping stack from Houston (Weatherford).

10.3 BLOWOUT SCENARIOS AND COMMENTARY

10.3.1 Underground Blowouts

Underground blowouts are the most common type of blowout. These blowouts generally occur when loss of circulation is experienced while circulating out a kick.

10.3.2 Basic Control Procedures

It is common for field personnel to fail to recognize that an underground blowout is occurring since many times they are focused on curing loss circulation. The following are signs of underground flow:

- Initial drill pipe and casing pressure increase followed by decrease. Typically, drill pipe pressure will drop to zero and then increase and casing pressure may not change very much.
- Gas, oil or salt water to surface on drill pipe caused mud jetted out of drill pipe by flow and replaced with blowout fluids (no float).
- Unable to get mud returns with blowout fluids at surface in annulus. Mud carried out in loss zone by mud.
- Able to strip up or down with no change in annulus pressure. Controlling pressure is fracture pressure or pore pressure at the loss zone.
- Thermal anomalies seen in temperature log. Higher temperatures seen opposite shallower loss zone (flow from bottom). Lower temperatures seen opposite loss zone (flow from top rare).
- No direct indication of pressure communication between drill pipe and annulus.

Underground flow begins when normal drill pipe circulation pressure is lost. It is common for this to occur when the leading edge of a gas kick is circulated past the last casing shoe or hits surface (choke line restriction). After underground blowout gas flow starts, mud is quickly jetted out of the well bore. If pumps are shut down the drill pipe pressure will stabilize slightly above the annulus pressure. This difference results from flowing frictional pressure drop in the annulus and/or the hydrostatic of gas lifted water. The greater this difference the higher the annulus friction or fluid density will be. If the bit is significantly off bottom and the drill pipe string is free, the drill string should be stripped through annular to bottom to facilitate the control. This is easily done, as no mud needs to be led out of the well when stripping into an underground flow. This is facilitated if there is a drill string float. If a DP float is not installed, BPV can be installed to allow making up connections, however, BPV in the string will limit wireline work and should be avoided if possible.

In the underground blowout it is often necessary to run logs in the DP so obstructions should be avoided.

When underground flow occurs, run a pressure/temperature log in the drill pipe to locate the loss zone and define flowing bottomhole pressure. Blow nozzles out of bit to minimize pressure drop and risk of nozzle plugging with loss circulation materials. If not possible, consider perforating or severing the drill collars. However, perforations in DC are at best difficult to accomplish as the bore limits the size tool that can be run via wireline. Consider running a rate gyro for a better relief well target or in case the well is sidetracked after control is gained.

Mobilize additional mud storage tanks if necessary. Mobilize cementing batch mixer if available. Mix and store at least one additional hole volume of mud on location. While mixing mud, bullhead water down the annulus to loss zone to minimize annulus surface pressure and keep possible H₂S off of casing, wellhead and BOPs. This will assist in interpreting the temperature log by defining a



temperature gradient at loss zone. Fracture extension pressure can be estimated from surface injection pressure over water hydrostatic to loss zone.

Slow the annulus rate and continue annular water injection with cementing pump. Pump down drill string at 90% of maximum possible rate using rig pumps with water until pressure stabilizes. Record stabilized pressure and rate. Increase the pump rate to maximum and record stabilized pressure and rate. The stabilized pressure on drill pipe is a function of the annulus two-phase flow hydrostatic and friction. If single flow can be achieved in the annulus, the well can be dynamically killed with the rig pumps. The drill pressure for single phase water flow can be accurately determined. If this pressure is nearly achieved during the test, the well can be easily killed using kill weight mud instead of water. Loss circulation materials can be added to the mud to help get a static kill after the pumps are shut down. If a dynamic kill with mud or water is not achieved, the recorded stabilized two phase flow pressure developed during the attempted kill in combination with the results of the pressure/temperature log can be analysed to determine what would be required. Gunk squeezes (diesel oil-bentonite-cement) or high density pills (barite pills) could also be used depending on the results.

10.3.3 Surface Blowout/Not on Fire

During drilling, a kick must be taken before the well can blowout. Generally, all surface blowouts are a result of equipment or operational failure of the BOP system, wellhead equipment or near surface tubular during a kick. Some blowouts are a result of an underground blowout breaching to surface. Surface breaching generally eliminates surface access making a relief well the only viable option. Surface intervention of a breached well is only possible if the breached is stable and downwind of the well. And flow rate is low. A surface blowout that is not on fire would be either in the BOP equipment, wellhead equipment, through the drill pipe or during testing. These are the four surface blowout scenarios that will be evaluated.

Likely Surface Blowout Scenarios

Flow may not ignite if low heat content gas is produced (low C_1 fraction, N_2 and CO_2) and particularly if free water is produced with the gas. Dry gas production makes ignition of a blowout very likely. High internal corrosion/erosion rates (combination of high velocity, CO_2 and free water) can complicate control. H_2S and CO_2 may be present in very low concentrations.

Annular Blowout Flow

If the annular blowout flow is occurring above the wellhead, then a failure is at the BOP flanges, bonnet seals, ram packer, steam packing or outlets has occurred. Generally, the failures are not catastrophic but start as leaks that cut-out the affected BOP area and become blowouts. Quick detection and proper response can keep the problem from getting any worse. The first option is to isolate the leak if possible by closing the lower rams. Leaks can then be plugged by pumping plugging materials through the kill lines. In some limited cases, gas hydrates form a temporary plug, then melts, and the leak restarts, and then hydrates re-form. This cycle of leakage and the formation of hydrates, most probably will cause the leak to worsen due to erosion. The application of water ice (better) or dry ice (solid CO_2) at the leak can help hydrates form or reform and keep them from melting. Pressure can be temporarily relieved down the choke line while preparing to fix the leak and/or re-torque flanges. In all these cases response time is limited. Action must be taken at the well site immediately. Ultimately, severe cut out of equipment can eliminate all of these options. Removal and replacement of cutout equipment would be required. This could require removal of the drilling rig and would require a well capping specialist.

A minor leak at or below the wellhead could also be controlled, as discussed before, with plugging materials or dry ice induced hydrates.



Drill Pipe Blowout Flow

Most drill pipe blowouts occur either while tripping into swabbed in gas or from failure of surface safety valves and pump in lines. It can be impossible to close a ball type safety valve against strong flow. Drill pipe blowouts can be prevented by using drill string float valves. An Oil Base Mud will increase the risk of a drill pipe blowout.

Tripping into oil mud saturated with gas leads to drill pipe blowouts if a float valve is not used. Immediate well site control could be accomplished by stabbing a safety valve. Leaks in threads could be hydrated off with dry ice or plugged with junk shots.

A method used to control drill pipe flow is by stabbing a double ram BOP with inverted slip ram under inverted pipe ram, drilling spool, single blind ram, 2 m long bell nipple.

- Tool joint is spaced out between the rams, diverter and pump in lines are hooked up to the spool.
- The inverted slip ram is closed.
- The inverted pipe ram is closed
- The diverter line opened and the blind ram is closed
- The diverter line is choked back and control is accomplished conventionally through the pump in line.

Small BOPs (7-1/16") have been successfully used to cap drill pipe flow in this manner with drill pipe suspended in rotary or BOP. A hydraulic crane has been used to place the BOPs over the drill pipe with the rig in place. With are on space out, the drilling spool can be eliminated by using the outlets on the upper BOP. BOP equipment as small as 4 1/16" have been used successfully on small drill pipe and tubing blowouts. On lower pressure blowouts the inverted slip ram can be dropped as the inverted pipe ram that will catch on the upset or collar.

If the well breaches to surface, it is imperative that wellbore pressure be released before the rig is cratered. Rigs have been lost because the location was abandoned with the BOP still shut in on the annulus with the well broached to the surface. The first step to take is to open the choke line directly to a flare line. If the flow in the broach is not impacted, then opening the BOP stack and letting the well blow vertically must be considered. Ideally, the rotary slips and bushings should be removed and drill string slacked off nearly totally on bottom with a tool joint rested against a ram. Remove all loose tools away from rotary and drop the travelling block out the V-door or pull up high in derrick. Shut down all sources of ignition, evacuate rig and open all rams from BOP remote station to let well flow vertically and drop the drill pipe. This will likely result in the well bore bridging. Most open hole blowouts end from natural formation bridging. Bridging can be induced if wellbore pressure is suddenly lowered and annulus is partially filled with helically buckled drill string. Many cratered rig blowouts requiring relief well control have been controlled in this manner by the wellsite crew.

Whenever there is a gas risk at surface, firefighting equipment should be positioned and manned (example: well testing). The rig fire main should be charged and fire hoses in place and operated. The fire hoses need to be coupled away from the potential fire area and positioned upwind from the well head near the large wheel mounted fire extinguishers. Men operating the fire extinguishers can then go in toward the fire under protection from water spray from the fire hoses. Fire hoses and men will not burn if a water curtain is maintained between them and the fire. A water spray can prevent unwanted ignition. The large fire extinguishers can extinguish smaller well fires and used in combination with water from the fire hoses.



The key to successful use of the large fire extinguishers is to:

- Fully stretch out the discharge lines prior to operation.
- Work as close to the fire as possible on an upwind size.
- Start with water to cool area around fire prior to opening valve on extinguishers.
- After cooling the fire as much as possible with available water, open at least two extinguishers simultaneously and direct powder at base of flames.
- Fully discharge extinguishers and continue applying maximum available water to prevent re-ignition.
- If the fire does not extinguish or re-ignites, then there is insufficient water flow out the hoses. Larger pumps, more hoses or fire monitors are needed.

Ideally, the rig contractor should have a team with the assigned responsibility for this activity. At least two men are needed on each fire hose, two men on each extinguisher and one man in heat reflective asbestos dress as a rescue man. The other should wear normal safety equipment, long sleeve cotton coveralls and cotton gloves and be thoroughly soaked with water. A wet cotton towel stuffed around the head, neck and face and into the coverall will provide additional protection. Practice drills of firefighting team should be considered.

Capping & Control Procedure (most likely Blowout)

Major surface leaks during kick handling procedures in the BOP equipment should be the most likely type of surface blowout.

The use of junk shots to plug surface equipment leaks should be understood by wellsite supervisory personnel. Successful junk shot application is time dependent as the leak opening always grows. A junk shot is accomplished by removing the check valves (to prevent line plugging) and loading 1 to 2 meters of kill line with rope fiber and walnut hull. The best fibers are the Kevlar or polypropylene types (higher tensile strength than hemp or cotton). If rope is to be used, the rope pieces should be 6" long 3/8" diameter, and frayed with tight knot in the middle of the rope. The walnut hulls should be medium and coarse materials. Mud loaded with 10 ppb medium Kwick-seal should be used to displace the junk shot (Kwick seal is a blend of fiber, granular and flake material). The junk shot will bridge and seal the leak allowing conventional control operations to continue. Additional junk shots can be pumped at times to re-seal the leak. Large leaks have been controlled by pumping golf balls a head of the junk shots. A 5 gallon bucket of pre-cut rope and other bridging material can be kept on the rig to quickly inject a junk shot to seal a surface leak. Time is saved if this is done and a rig scavenger hunt for sealing materials is not required.

Leaks can be worked on or stabilized until a fix is possible by relieving pressure. Flow out wide open chokes down the flare line should be considered. It is better to open the well up on flare line than to allow pressure containing equipment to cut-out.

The ram blocks of Cameron type "U" preventers can be replaced by well capping specialists while the well is blowing out vertically. Steps taken involve opening all BOPs to eliminate any back pressure, applying water deluge, hydraulically opening the bonnets and replacing ram blocks. This is possible as the high velocity gas flow produces a vacuum from a Venturi effect in the BOP and the bell nipple located above the BOP to be repaired. (The bonnets can be remotely hydraulically operated and quickly opened. The Venturi effect draws air into the BOP and very little gas escapes.)



10.3.4 Surface Blowout/Well on Fire

A hot fire causes rig collapse within minutes. Melted steel and debris will cover the BOP and wellhead causing severe damage to the wellhead. If this happens, the well most probably will have to be capped on exposed casing. Blowout control operations can take weeks

10.4 CAPPING STRATEGY

10.5 SURFACE INTERVENTION, FIREFIGHTING & CAPPING STRATEGY

It is not possible to discuss every eventuality which may arise during an offshore blowout. However, a general discussion of the equipment and techniques typically used on a major offshore blowout/fire is needed. Appendix B offers a general discussion regarding capping operations. The following intervention techniques are those which may be employed after the initial mobilization and set-up of the primary support vessel has been completed.

10.5.1 Debris Removal

The initial phase of the intervention will involve clearing damaged or unnecessary equipment from the structure. This is done to provide working room as well as to remove valuable equipment from danger. The intervention team attempt to re-board the structure under the covering water spray from either a tie-in of the primary firewater ring or from the primary support vessel. Once on board, the intervention team will assess the situation and proceed accordingly. The crane on the support vessel can be used to remove all equipment which is accessible. In certain situations it may be possible to use the existing platform crane(s). This may not be feasible since the crane may be damaged beyond repair or it may not be practical to re-connect power to the crane.

10.5.2 Fire Control

To safely deal with an offshore blowout, the intervention team must have the capability to apply large volumes of water. This should be done to cool the area and allow wellhead access or to aid in the prevention of ignition while working in proximity to the flow. Portable monitors will be placed at the point where covering firewater is needed. There are three feasible sources of firewater. They are from:

- Existing firewater ring (provided it is operational)
- Firewater pumps on standby boats or barges (vessels of opportunity) or
- Portable firewater pumps (from well control vendor or others)

During the intervention project, usually following debris removal, attempts will be made to place firefighting monitors (outlets) on the structure at points that will be determined by the incident, per Figure below. If possible, attempts may be made to utilize the existing deluge piping on the structure. This has been accomplished on platform fires and blowouts in the past and has proven very beneficial to the project. If the existing firewater ring is not energized from the pumps on the platform, an external tie-in of portable pumps at the splash zone (boat landing) is recommended. This is best accomplished if a vertical riser is in place beforehand. However, this can be installed in by the intervention team if necessary.

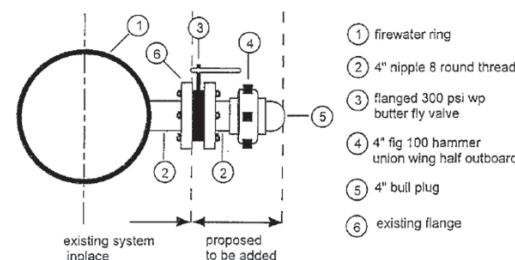


Figure Example of a tie-in to the firewater ring for portable monitors

Portable firewater monitors (type rated at 1,200 gpm) placed on the structure will provide precise placement of water for cover and cooling purposes. If the firewater ring cannot be utilized, an alternate will be to install temporary conduits such as large, low pressure hoses from the support vessel to the monitors on the structure. If space and conditions allow, portable firewater pumps can be placed on the structure and their suctions charged by the pumps on the support vessel.

Firewater application from standby boats is a viable option and has certain advantages and disadvantages. One advantage is that the boat can be mobilized to the site and used if the platform is abandoned. Therefore a re-start of engines and re-boarding of the facility may not be necessary. Firewater supply from a barge or boat necessitates that the boat come alongside the burning or blowing well platform. This places the boat and the crew closer to the problem and increases the potential for injury and damage if proper procedures are not employed. Firewater support from floating platforms is controlled by the wind and seas. Precise application is required to protect the intervention personnel, and wave action (greater than ½ to ¾ m) may prevent the boat from applying the water stream onto the point of interest with sufficient reliability. Therefore this method may require more stringent weather windows for close work by the intervention team.

Portable pumps and marine manifolds can also be deployed to provide firewater for the intervention efforts. This equipment will have to be flown in from the USA or sourced in the local market. Mobilization and rig up takes time. While this is underway the situation can worsen (structural damage, wellhead leaks, etc.). This pumping equipment and specially designed marine manifolds will be used for the purpose of applying firewater for prevention of subsequent damage and to cover the intervention efforts. If the primary support vessel has no firefighting capabilities, these pumps can be used exclusively. If other firefighting capabilities are available, they can be used in conjunction with the onboard pumps.

10.5.3 Moving Onto the Structure

Once sufficient working space is made an available on the structure, operations will be undertaken on the structure. The initial and supporting approaches with the MSV or crane barge will generally be determined by wind and tide direction.

Water monitors will be placed at the working area for more precise water application and protection of the crews and equipment. All operations near the wellhead must be done with a protective and/or cooling water spray cover. In some instances, portable cranes will be assembled on the deck of the structure. This will in turn be used for further debris removal, precise equipment placement and eventually for capping the well. In previous operations it has been possible to place a large tracked crane (80 ton) onto the deck of the well platform.



10.5.4 Gaining Wellhead Access

With operations established on the structure, final debris removal can begin which will allow wellhead access. This may require more cutting which can be done by one of the methods previously mentioned. If the well is on fire, all heated metal debris must be removed before the fire can be extinguished. A Venturi tube may be placed over the well flow to raise the ignition point and consolidate the flow. This will allow better access to the wellhead and provide a means to cool the surrounding structural steel components. Fires which cause major structural damage sometimes require extensive fabrication projects to re-build a working platform around the wellhead.

10.5.5 Extinguishing the Fire

Once clear access to the wellhead has been established, efforts will be made to configure the flow into a single vertical stream (if not so already). Many fires can be extinguished using water alone. Unless obviously unsuitable, this technique will be attempted first. The Venturi tube may be used in conjunction with the water application to improve the chances of success. If these attempts fail, explosives may be used to extinguish the fire (this is a rare occurrence in offshore operations however). Unless major structural damage is imminent the fire may be left burning until all preparations have been made for capping. This is done as a pollution control measure.

10.5.6 Wellhead, Tree and BOP Removal

With the fire either extinguished or directed through a Venture tube, closer inspection of the wellhead equipment can be made. This inspection will determine whether the existing equipment can be used to attach capping devices or if all or part of it will need to be removed. If nothing can be salvaged, the entire wellhead and all casing strings can be cut off. More detail can be found in Appendix b: Capping Operations.

10.5.7 Control Operations

Control operations usually fall into one of two general categories; shut-in or divert. If for some reason the well cannot be shut-in, it is common practice to divert the well and utilize a snubbing unit to either fish the tubing/drillpipe or to snub in a kill work string (e.g. place a tubing string on bottom for kill operations).

Depending on the severity of damage, extensive structural repair may be necessary before this type of work can proceed. If the well is to be diverted, flow lines and choke manifolds can be set in place allowing safe operations for construction while the well is on diversion.

There are infinite scenarios for kill operations so detail is not possible in this section. Kill operations will fall into board categories as follows;

- Bullhead after shut in.
- Dynamic kill through a work string.
- Circulate out after shut-in.

The circumstances of the event will guide the intervention team to the solution that best fits the conditions at hand. Much work may be needed to be in a position to kill the well. Careful evaluation of the integrity of the wellhead equipment on the well and the downhole equipment is a must. It is often the case that judgment is the only means to guide the kill operation. A general rule for kill operations is that the stresses induced in the kill should be kept to a minimum if there are any doubts with the pressure control equipment on or in the well.

Auxiliary vessels such as pump boats and fluid handling vessels may be required if the structure will not support or accommodate such equipment. If snubbing equipment or other wellhead



supported equipment of significant weight is to be utilized, additional fabrication may be necessary to insure structural integrity.

10.5.8 Support: MSV, Goods and Material Services

PRIMARY SUPPORT VESSEL: The primary support vessel is the platform from which the intervention effort will be directed. Conventionally moored derrick/pipelay barges are generally the vessel of choice for primary support. This type vessel possesses several features that are beneficial to the overall success of the project.

These barges are available with adequate open deck space to support even the most complex projects. Simultaneous projects such as fabrication, modifications and repairs can all be undertaken on deck. This significantly reduces the logistics of monitoring and supervision of these tasks.

Most derrick/pipelay barges are equipped with "jet" pumps mounted below deck. These pumps, normally used for pipe laying operations, are typically rated at 3,000-5,000 GPM @ 400-600 psi. Some barges have modifications that allow these pumps to be used for firefighting purposes. If not, the modifications must be made quickly. Where elevated structures are involved, these pumps can be used to supply water to other pumps mounted on the structure itself

The cranes on these type vessels are essential for debris removal and equipment/personnel movement to and from the structure. It is not unusual for crane lifting capabilities to far exceed actual needs. The heaviest lifts likely to be encountered are the removal of a complete drilling package from the platform. However, barges with lifting capabilities of 500 to 700 tons are sometimes required to ensure adequate boom length and deck space. A 300' boom length may be required to reach the uppermost portions of the structure while allowing a safe horizontal offset distance. A typical crane barge with a 300' boom offset 150' from the structure is only capable of lifting approximately 25% of its maximum rating to a height of 240'. Barge with larger dimensions also provide added stability which will allow work to proceed during moderately rough seas.

The additional expense of the larger barge is justified given the limited availability of this type vessel. If a smaller barge is contracted and conditions develop that make it inadequate, a larger vessel may not be immediately available. These are obviously very undesirable circumstances. Another benefit of the moored barge is its ability to be removed from proximity to the well in an emergency. This is often necessary due to changing well or weather conditions. Adequate towing capabilities (tugs) should be at hand to assist if needed. The derrick/pipelay barge should be mobilized to the location immediately. Firewater pumps and accessory equipment can be mobilized on a utility boat if required. Once on location, anchors can be set for the barge, the equipment can be off loaded from the utility boat and assembled prior to moving close to the structure.

SECONDARY VESSELS: In addition to the primary support vessel and pollution containment vessels, at least two crew boats and one utility (work) boat will be needed.

FABRICATION PERSONNEL AND EQUIPMENT: A minimum of two certified welders will be needed for various fabrication projects. Each should be fully supplied with necessary equipment such as welding machines, cutting torches, grinders, chipping hammers, wire brushes, etc. An adequate supply of safety equipment ordinarily used during fabrication projects such as goggles and face shields will be required.

ROUSTABOUTS: A roustabout crew will be needed for various tasks such as fabrication and rig-up of pumps and lines. A crew consisting of one supervisor and five roustabouts should be contracted.

MATERIAL: A considerable amount of fabrication material will be needed for various tasks. The material in the following list will generally provide an adequate amount for the initial requirements:

- 200 sheets – 2' x 8' galvanized corrugated tin (10 gauge or thicker)

- 150 lb. of bailing wire (soft wire for attaching fire shields)
- 30 joints – 2-3/8" tubing (junk)
- 12 pieces (500 ft²) – expanded metal grating
- 750 ft – 2" x 2" x 1/4" angle iron
- 500 ft – 3" x 3" x 1/4" angle iron
- 2 sheets – 4' x 8' x 1/4" steel plate
- 1 sheet – 4' x 8' x 1" steel plate
- 500 feet – 1/2" softlay cable (6 x 36) with 50 clamps
- 500 feet – 3/4" softlay cable (6 x 36) with 50 clamps
- 500 feet – 1" softlay cable (6 x 36) with 50 clamps
- 500 feet – 1-1/8" softlay cable (6 x 36) with 50 clamps
- 250 feet – 1/2" cold rolled bar

AIR COMPRESSOR: Two 255 CFM, 125 psi air compressor each with 300 ft of 2" 200 psi WP hose and spare end connections. These will be required to supply air for starting pumps and operating other pneumatic tools later in the project. Available through local specialty rental companies or may be available on the primary support vessel.

LIGHT TOWERS: Self-contained diesel powered light towers should be ordered to facilitate fabrication projects which may extend into the night, available from specialty rental companies. Primary support vessel may have adequate lighting.

ABRASIVE CUTTERS: Ultra-high pressure (30,000 + psi) cutters which use abrasive material such as frac sand, slag or crushed garnet. Used for debris wellhead and casing cutting in explosive atmospheres, available from Halliburton (Duncan, OK).

LATHE CUTTERS: Portable lathe type dye cutters may be required for circumferential cuts on casing strings.

EXPLOSIVES: Explosives may be necessary for debris removal and possibly for extinguishing the fire. NOTE: Since Abrasive Jet Cutters have been introduced explosives have been rarely used, therefore this is mentioned as a contingency only.

TRASH PUMPS: Portable air operated diaphragm type pumps may be needed for various fluid transfer tasks on the structure. Small pumps such as Wilden 3" are preferred since they provide the necessary mobility, available from specialty rental tool companies.

PORTABLE CRANES: it may become necessary to install a portable crane on the structure for capping and/or debris removal, available through various marine crane rental companies.

PNEUMATIC WINCHES: Large pneumatic winches, or "air tuggers", may be needed for capping and/or debris removal, available through specialty rental companies.

PNEUMATIC TOOLS: Impact wrenches, drills, grinders, pneumatic hacksaws along with hoses, sockets, bits and various other accessory pieces. These are available from most oilfield supply outlets.

HYDRAULIC TOOLS: Torque wrenches, nut splitters and portable power jacks. These are available from pressure testing companies and specialty rental companies.

SURFACE EQUIPEMNT: BOPS's, chokes/manifolds, closing units, chicksan lines etc. Available from oilfield rental tool companies.

10.5.9 Personnel Safety and Medical Services

The highest possible standards must be maintained with regard to personnel safety at all times. The well control intervention team will constantly strive to insure the safest possible working environment based on their previous experience with similar situations. However, risks will inevitably be involved with some operations. The well control team must work with TOTAL to properly manage and minimize these risks.

EMERGENCY MEDICAL EQUIPMENT: There should be trained medical personnel on location with equipment to treat trauma. Their expertise should cover burn treatment in addition to typical oil-field related injuries. Certified EMT, personnel are available through some oil-field safety companies such as CAMCO, SABER, etc.

MEDIVAC SERVICES: A medical evacuation helicopter should be on alert at all times to transport seriously injured personnel to near-by medical facilities for treatment. This service should be able to provide advanced life support during transit.

10.5.10 Communications

Efficient communication is essential to the success and safety of the project. A central dispatching system must be arranged to control the movement of equipment and personnel (existing system or installed after the incident occurs). This is best handled by a central base station operation where a radio operator continually monitors and dispatches necessary services in conjunction with the TOTAL project control procedures and purchasing specifications.

An independent communication link should be established between the location and the coordinating TOTAL office. Voice and data transfer capabilities will be necessary.

On-site communications are vital. Portable radios should be provided with a dedicated frequency to be used by the personnel at the location.

10.5.11 Fabrication

If a major fabrication project becomes necessary, the most expedient method may be to have it undertaken onshore. In some cases the offshore construction barge or MSV may be able to handle the job. An evaluation should be conducted to assess the need for major fabrication projects as soon as feasible and make the decision to fabrication onshore or offshore. Regardless of the choice, a competent fabrication shop should be contracted to begin the projects(s) immediately.

10.5.12 Machine Shop Services

There may be occasion to construct or repair precision components of various pieces of equipment used in the well control effort. It is recommended that a full service machine shop be available on a 24 hour basis during the project.

10.5.13 General Support

There should be a pool of resources that cover labor and transportation as well as procurement and expediting to support the well control effort. One should not lose sight of the fact that, in the end, all costs will have to be accounted for and justified. Tracking of material and documentation of purchasing will be essential tasks that can best be done at the time of procurement rather than after the fact.

10.5.14 Weather Monitoring

A recognized weather reporting/forecasting service should be employed. Daily weather reports should be made available to the TOTAL coordinating office and the personnel on location. Prior knowledge of impending weather changes can be a valuable tool for operational planning and safety.

10.5.15 Personnel Quarters

If adequate facilities are not present on the primary support vessel, arrangements will have to be made for housing and feeding of the personnel on location. A 24 hour galley may be necessary as fabrication and repair projects will likely be on-going around the clock. Laundry services will be needed for personnel staying on location. It is expected that these needs will be met by contracting a "floatel" or by using adjacent TOTAL facilities.

10.5.16 Firefighting Equipment

The major well control vendors have an inventory of specialized tools and equipment ready for immediate mobilization 24 hours a day. The following is a partial listing including a brief description;

- Fire pumps – Driven by diesel engines with centrifugal high volume low pressure firewater pump. (Example: Detroit Diesel 8V-91, 540 HP turbo charged engine with centrifugal pump delivering 4 to 5,000 GPM @ 200 psi) Each pump is mounted on an oilfield skid with protective roll cage and single lift attachment point, forklift attachment and loading hitch for rolling tailboard transport.
- Suction manifolds, suction and discharge hoses.
- Marine manifold for installation on marine vessel deck. The main components of the marine manifold are.
 - 1 ea., 10" x 20' steel fire monitor manifold w/ 4 ea. 4" flanged outlets, 1 ea., 10" flanged inlet, 4 ea. 4" butterfly valves, 4 ea. 4" Fig. 100 hammer unions.
 - 3 ea., 10" x 21' flanged supply line sections
 - 1 ea., 10" x 16' flanged supply line section
 - 1 ea., 10" x 6" 90° flanged elbow
 - 4 ea., 6" x 4' steel pipe extensions w/90° ells for use with suction hoses
 - 4 ea., 1000 GPM water cannons
- Fire monitors: 2,000 to 6,000 GPM.
- Casing clamps: for use in various capping procedures.
- Venturi tube: to consolidate and raise the flow and/or ignition point.
- Portable toolhouse – containing complete set of hand tools from 1/4" end wrench to 48" pipe wrench for maintenance and repair. Complete set of hammer wrenches and brass hammers.
- Portable Lathe Type Cutters – Used for making circumferential cuts on casing strings.
- Explosives – All necessary equipment for demolition. A fully-licensed explosives expert will be required.
- Nomex Protective Clothing – For use by personnel working in proximity to the combustible flow or fire.

- Communications – Hand held radios for use by personnel on location
- Foam/Dispersant Application – For fire extinguishing or protection

10.6 CAPPING OPERATIONS

Capping operations are an integral part of most blowout intervention projects. In many instances, capping of the blowout well is the primary objective, the first major step in regaining control of the well.

The term “capping” is sometimes loosely used to refer to the whole process of surface intervention. The more precise definition, used here, is the placement of a competent pressure control device onto the blowout well under flowing conditions. Once the new control device (BOP, valve, etc.) is positioned over the well, there must be a means of attaching the device so that pressure integrity can be regained.

Regardless of its components, the control device is typically referred to as the capping stack or capping assembly. The magnitude of the pressure which the control device will be expected to withstand is the Maximum Anticipated Surface Pressure (MASP). For capping operations, the MASP is the maximum shut-in wellhead pressure plus externally applied pressure (e.g., pressures exerted while bullheading) multiplied by a safety factor (e.g., 1.25). The MASP with appropriate safety factor should be compared to the working pressure of the equipment. Temperature can be a consideration, as the BOP may need to be de-rated for the flowing wellhead temperature. This is especially true for HTHP wells. Capping operations also include preparing the wellhead for placement of the capping stack. This sometimes involves removal of part or all of the existing wellhead/BOP stack.

Important factors to consider in planning a capping operation include:

- Forces exerted on the capping stack as it is brought into the flow.
- Best method to insure full control of the movement of the capping stack when it enters the flow (prevention of turning and swinging).
- Measures to minimize the potential for ignition during the capping operation and contingencies for ignition if it does occur.
- Through bore size (ID) of the capping stack sufficient to allow subsequent work.
- Functions required of the capping stack (e.g., outlets needed for diverting the flow, pumping into the well, pressure monitoring and snubbing operations).
- Best attachment method for securing the capping stack to the well.
- Pressure and temperature ratings required to control the well throughout all phases of the well control operation.
- Forces exerted on the capping stack during the post capping operations such as snubbing and bullheading.

Proper planning of a capping operation must take into account the mass flow rate, combustible nature of the flow, wellbore geometry and operations to be undertaken in the ensuring post-capping phase of the project. The methods used for capping can generally be divided into three techniques:

- Capping to a flange.
- Capping to a stub by first installing a wellhead.
- Capping to a stub by swallowing the stub.

This chapter provides an overview of the steps necessary to safely accomplish capping operations using these three techniques.

10.6.1 GAINING ACCESS WITH THE ACV

Before the actual capping process can begin, well access is necessary. Direct access is usually denied because of structural damage to the drilling structure or platform. Debris, which may include melted masses of metal, must be removed before the intervention at the wellhead can begin. The All-Purpose Capping Vehicle (ACV) was developed for the purposes of working on blowing wells that can also be on fire. ACV applications include:

- Removing debris using hooks and rakes.
- Conveying special tools, such as abrasive jet cutters, Venturi tubes and stingers.
- Placing explosives at a “safe” distance for severing or extinguishing the fire.
- Hoisting and stabbing-on capping assemblies.
-

Figures F.1 and F.2 illustrate the two main types of ACV's Figure F.3 shows end attachments often used in well control operations.

In the early years of the well control business, Athey wagons were employed to drag damaged equipment from the well. They were generally used to remove debris and only rarely to convey tools to the wellhead. The name 'Athey' is in fact a misnomer, as it actually refers to the leading manufacturer of a certain type of steel track used for rig moves, or for moving heavy lifts in rough terrain, though the older name is still commonly used by capping companies. All-Purpose Capping Vehicle or ACV better describes the capabilities of the modern vehicles.

There are two basic versions of the ACV: conventional and hydraulic. The conventional unit relies on the power of a bulldozer and its tail winch to move and position the boom. Figure F.1 shows the conventional ACV hooked up to a bulldozer. The tail winch articulates the boom while the dozer is used to position the wagon.

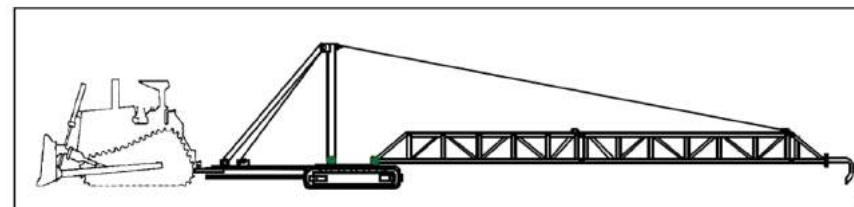


Figure F.1 Conventional ACV with End Hook Attachment

The hydraulic version of the ACV was developed primarily for the purpose of stabbing-on BOP and conveying tools that require precise positioning, such as the abrasive jet cutter. In these applications, hydraulic winches provide fine control of the boom articulation. Wild Well Control, Inc. has developed a hydraulic ACV that is secured by a bulldozer, which provides movement, hydraulic winches to control the boom angle and a set of winches at the front of the vehicle for pulling or snubbing on BOPs. One drawback of the hydraulic ACV is the requirement of a power pack to operate the hydraulic winches, and this increases the overall air shipping weight and volume. However, all components break down into small lifts that will fit on almost all commercial cargo planes. Figure F.2 illustrates the hydraulic model of the ACV equipped for a stab-on manoeuvre.

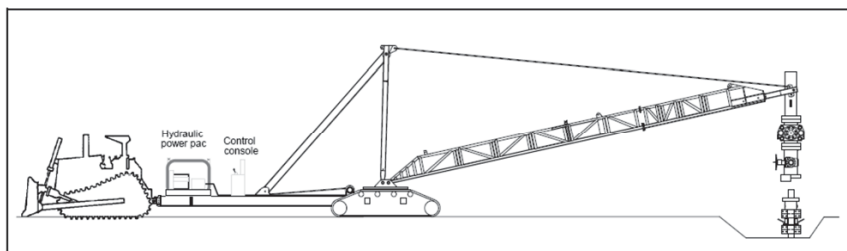


Figure F.2 Hydraulic ACV Stabbing-on a BOP

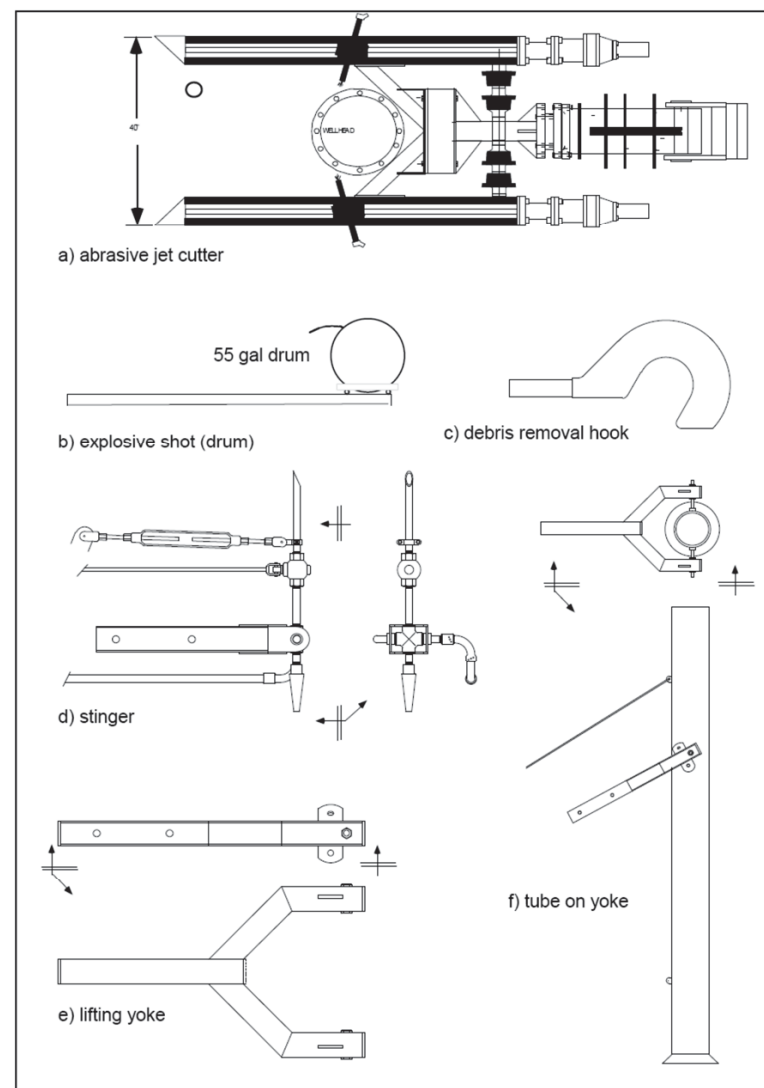


Figure F.3 Typical ACV End Attachments

10.6.2 Wellhead and BOP Removal

With the fire either extinguished or directed through a Venturi tube, close inspection of the wellhead equipment can be made and work can be performed at the wellhead. The inspection will determine whether the existing equipment can be used to attach capping devices or if all or part of it will need to be removed.

Caution! Reusing wellhead components that have been involved in a blowout can be hazardous and must be thoroughly evaluated. If nothing can be salvaged, the entire wellhead and all casing strings will need to be cut off and new equipment installed.

Wellhead or BOP components must be removed when they have suffered structural damage. Falling debris can cause mechanical damage and fire can weaken the integrity of most elastomer seals.

A typical technique for removing wellhead or BOP components is to install clamps on the flange to allow the removal of all bolts. A crane is attached to the component and snub lines are installed through the bolt holes. With the snub lines tight, the clamps are removed and the component can be taken off in a controlled manner. Other removal methods have included explosives, cables, and even hand-operated hacksaws. Some operators have resorted to tearing the wellhead off with brute force, which often caused additional damage and prolonged capping work to repair the casing.

Explosives have proved to be a highly precise and reliable method for removing wellhead equipment or sections of casing at the surface. This technology requires very specialized expertise and highly experienced personnel.

Shaped charges can be constructed to accomplish a variety of tasks, from severing the entire wellhead to removing casing valves or strings. If properly applied, shaped charges can remove an outer string of casing without damaging the next inner string. Figure F.4 shows a typical shaped charge configuration with a focused bias for removing a single outer casing string.

By contrast, the cable method is a crude type of friction cut. It is now considered outdated technology. Wire rope or cable is wrapped around the wellhead or casing and each end is connected to a swabbing unit. The cable is then dragged back and forth until it severs the casing. The cable method works, but often takes several days. Depending on the number of casing strings and the presence of cement, the job could take from two to five days of continuous cutting. There are other disadvantages to this method. The cut is difficult to re-enter if the cable is pulled out of the groove. Cable replacement is often necessary due to wear, overheating, breakage or when the operation is shut down for darkness. Cable cutting can cause the casing to become egged, further hindering the capping operation.

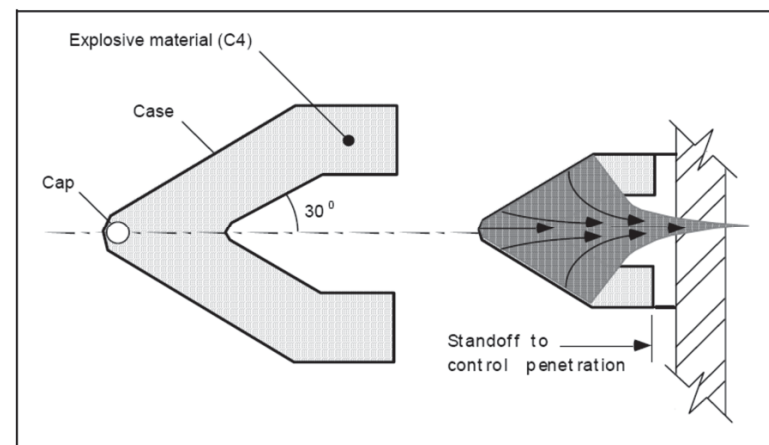


Figure F.4 Shaped Charge Diagram

The Kuwait oil fires proved the perfect testing ground for the abrasive jet cutter, a newer and more efficient cutting method. This equipment performed well in the removal of damaged wellhead components and trees. It was one of the most important innovations responsible for increasing the speed of capping operations in Kuwait. Two types of cutting services were used there: the Hydro-Jet (by Halliburton) and the Ultra-High-Pressure (UHP) abrasive particles to erode away metal and cement, but they are very different tools.

The UHP equipment is an ultra-high pressure, trailer mounted, self-contained system capable of quick mobilization and easy rig up. Rig-up consists of attaching a split-type track with hydraulic advancing tractor to the wellhead above or below the area to be cut off. This is typically done by two men without a crane. The tractor and nozzle are then positioned on the track and attached to the water, abrasive and hydraulic lines.

A high pressure, low volume stream of water and abrasive slurry is pumped through the jet at the area to be cut, and a circumferential cut is performed. The device works very much like an automatic track torch used to bevel pipe. The water leaves the jet nozzle with a pressure in excess of 30,000 psi. Generally, the nozzle used is a 0.75 mm diameter, man-made ruby. The calculated nozzle velocity at a typical pump rate of 4 gpm is 2,007 ft/sec (roughly equivalent to Mach 2⁺). The abrasive material is conveyed to the jet body through a separate line with compressed air. The abrasive enters the jet through a siphon port by Venturi effect and is discharged through the nozzle. Excess abrasive returns to the hopper through a hose. In Kuwait, the abrasive used was granulated garnet with a hardness of 7.5 as compared to steel at 6.0

The jet can be configured in different ways to meet specific cutting requirements. In several instances in Kuwait, it made circular cuts through as many as seven cemented strings of casing, with one or more blowing, to remove a damaged wellhead. The average time spent on this type of circular cut was between one and two hours with many done in less than one hour.

To cut off a wellhead completely, the jet nozzle is pointed directly at the casing, perpendicular to its axis. The jet circumnavigates the casing on the track, making a complete 360 degree cut. The jet stream usually penetrates 15 to 18 inches. Depth of penetration is highly dependent on the tracking speed.

Sometimes it is necessary to leave the inner string or production casing intact and peel back the outside strings. This is done by setting the jet at an angle where the abrasive stream never penetrates deeper than the thickness of the outer string. In either case, the cut is remotely controlled by the operator and no personnel are required close to the wellhead during the cutting operation.

The UHP jet cutter is not limited to circular casing cuts. For example, the track can be attached to the wellhead, allowing cuts to be made under damaged valves or between flanges. One unique application of the tool is for cutting bolts and other small diameter sections. In this case, the jet cutter is mounted on a tripod stand (see Figure F.5) and the operator can cut the nuts off the top or bottom of the flange in short order. The time required to cut a single API 11" 3M stud ranges from 45 seconds to 8 minutes. Sometimes the bolts can even be cut between the flanges, depending on the severity of the damage.

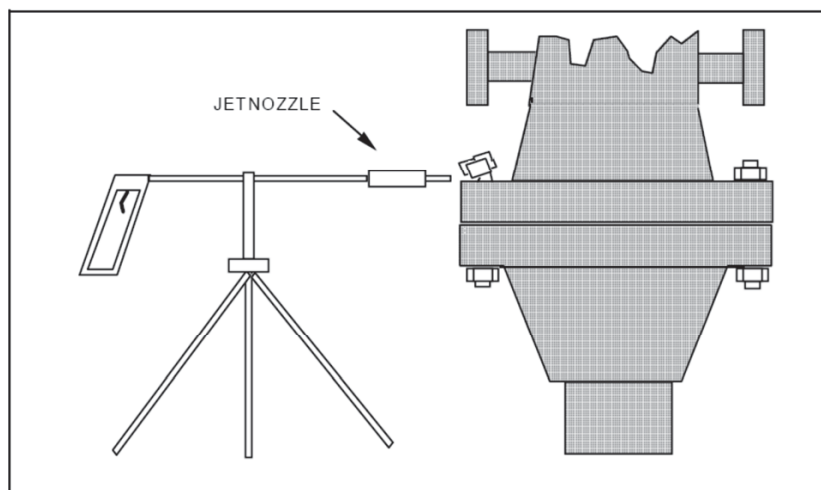
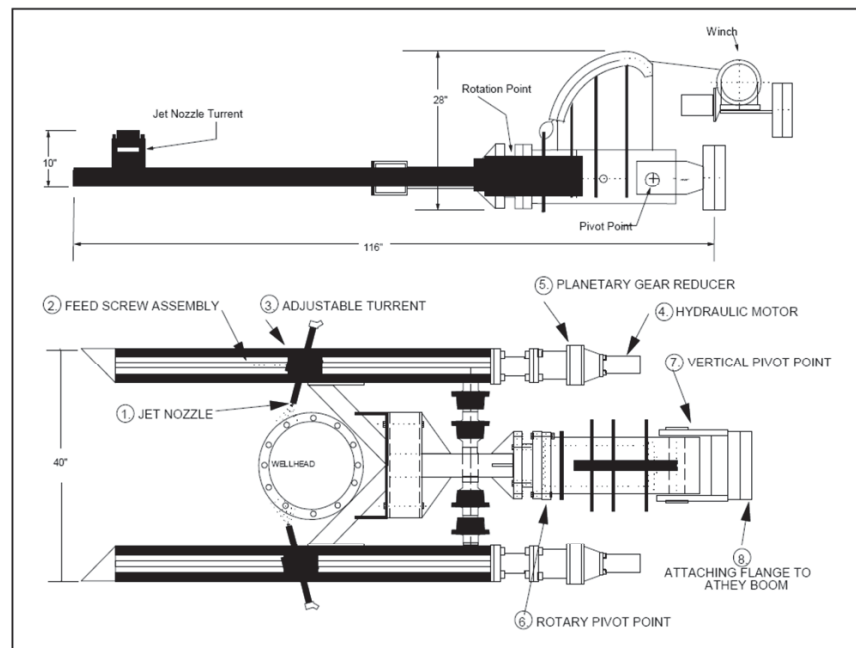


Figure F.5 Bolt Cutting with a Hand-Held Gun and Tripod

The ultra-high pressure cutting tool does have some limitations. The operator must physically attach the tractor band to the wellhead or casing, and when there is lateral flow this is virtually impossible to do. The cut is jagged and often irregular, perhaps because of the light construction of the tracking frame. But despite these minor limitations, the UHP jet cutter is a valuable asset to the capping operation.

Halliburton's HYDRA-JET cutter was adapted for use in Kuwait by the creation of a specialized carrier, allowing it to be conveyed to the wellhead using a conventional ACV boom. Two different carriers were employed in Kuwait. One was a vertical cutter with a single nozzle. The other was a horizontal carrier with a U-shaped yoke and two opposing jet nozzles (see Figure F.6). In both versions, a small hydraulic motor drives long worm screws to advance the cutters along the length of the yoke. To make the cut, a slurry of gelled water and 1ppg sand is pumped at 150 gpm to each 3/16" nozzle, a much higher flow-rate than the UHP device, and at a lower pressure of approximately 11,000 psi. The abrasive stream of high pressure slurry erodes away the casing or wellhead, tracking laterally much like a hacksaw blade passing through a piece of pipe.

The jet cutter requires considerably more rig-up time and equipment than the UHP unit. However, the jet cutter can cut off a wellhead that is on fire or has limited access due to lateral flow, because it can be conveyed at the end of the ACV boom. It can be cooled and shielded from the fire by a water spray. Its hydraulic control lines are protected in an arrangement that resembles a tube-and-shell heat exchanger. The lines run inside the tube and water is circulated around them to cool the system.



Halliburton Horizontal Cutter With Yoke Attachment
(Courtesy of Halliburton Energy Services, Duncan OK)

Figure F.6 Halliburton Horizontal Cutter with Yoke Attachment

Table F.1 Comparison of High-Pressure (Hydro-Jet) and Ultra-High Pressure (UHP) Cutting Techniques

	Ultra-High-Pressure	Hydra-Jet Cutter
Pump Pressure	30,000 psi	10-12,000 psi
Discharge Rate	3 - 4 gpm	84 gpm – one nozzle 170 gpm – two nozzles
Nozzles	0.5 to 0.7 mm man-made ruby	3/16" tungsten carbide
Pump Unit	1 – single unit Self-contained	1 hydraulic hose/power unit 2 cement/frac trucks
Cutting Track	Circular ± 200 lbs	U-yoke and vertical types ± 1,800 lbs
Rig-Up	No crane required attaches by hand with screw clamps ±1 hr.	Crane and AVC boom required boom refit (if required) ± 6 hrs
Well Conditions	Fire extinguished personnel access required.	Well can be on fire no close personnel access required
Fire Protection	None available	Shielded and water cooled
Support Protection	50 bbls distilled water truck with filter	1 sand bulk truck 2 gelled water trucks
Feed Water	Drinking quality with tank	Semi-clean/brackish
Consumables	Crushed garnet	40 mesh frac sand, 1 ppg
Personnel	4	± 6

The vertical cutter has a single arm jet holder. It can be used to cut off wing valves or flowlines when necessary. The vertical cutting time of 50-80 minutes is comparable to the UHP, if rig-up time is not considered. In either vertical or horizontal position, the finished cut is clean and smooth.

Using the HYDRA-JET cutter does create some special logistical considerations. The higher cutting-fluid volume requires the use of tank trucks (or frac tanks offshore) to supply the fluid, and a bulk truck (or skid) to supply the sand. The high pressure, high volume fluid discharges also require more horsepower, resulting in a large equipment spread. On a small location extra dirt work may be required to accommodate all the equipment. The ACV boom must be retrofit to accommodate the carrier (unless special provisions are already built-in). The rig-up time of several hours should be taken into consideration for daylight-only operations. Based on the Kuwait experience, Halliburton has made substantial improvements to the jet cutter, reducing the amount of equipment required.

Even with their individual disadvantages, these tools far outperform previous methods for removing damaged components on blowing or burning wells. They represent a significant advance in wild well control technique.

Both cutters worked well in Kuwait and, between the two, almost any conceivable cutting job can be accomplished. It would be unfair to say that one was better than the other because both fit into useful niches. Table F.1 shows a comparison of the two cutters.

Following the cut-off, circumferential cuts must be made on the casing strings prior to capping. These cuts can be made with an abrasive jet cutter or a portable lathe die cutter. The lathe cutter utilizes a track, air or hydraulic motor and a hardened cutting blade similar to those used on commercial lathes. The lathe cutter can be split and wrapped around the casing so it can be mounted without entering the flow. The resulting cuts have beveled machine-quality edges. The casing strings are cut at different lengths to expose an adequate amount of the innermost string for capping purposes. If necessary, these cuts can be made with the well on fire.

10.6.3 Capping to a Flange

In large violent flows of high velocity, the snub-on technique is recommended for installation of a capping stack to an existing flange. This is not a hard and fast rule, but generally the idea is to control the movement of the capping stack along its three axes by the use of hoist, tag and snub lines. This method, illustrated in Figure F.7, involves the following steps:

- Rig up a capping assembly with a mating flange, and proper pressure, temperature and service ratings. Track weld the ring gasket to the bottom of the capping assembly flange.
- Hold a final safety and coordination meeting to insure that all personnel understand the safety procedures to be followed and the operational plans, including the contingency plan for a flash fire or explosion.
- Snub the capping assembly into the flow. Center and lower the capping assembly and mate the flanges.
- Install bolts and tighten to energize ring gasket seal.
- Connect hydraulic lines between the closing unit and capping assembly.
- Install diverter lines and kill lines as necessary, then continue with the chosen course of action, e.g., pump to kill, divert, or rig-up to snub.

Similar procedures are used whether the capping assembly consists of a valve arrangement or a BOP stack. Torque wrenches should be available to speed the installation and insure a proper seal since pressure testing is often impossible.

10.6.4 Capping to a Stub by Installing a Wellhead

This procedure is an option when the entire wellhead has been removed, leaving only a casing stub. After cutting back the outer strings of casing to expose the capping string, a standard slip-on weld type head is modified by adding pad eyes for attaching the snub lines. For ease of installation, this wellhead should be at least one size larger than the casing stub to be swallowed, for example, a 9-5/8" head would be used to cap 7" casing.

As an option, a plate can be tack welded onto the side of the head to deflect the flow and improve visibility as the spool is placed into the flow over the casing stub. This plate will have to be removed before installation of the casing clamps. Snatch blocks are secured to the base of the casing with a bolt-on clamp (see Figure F.8). Cables are threaded through the snatch blocks and attached to the head to facilitate the snub-on operation.

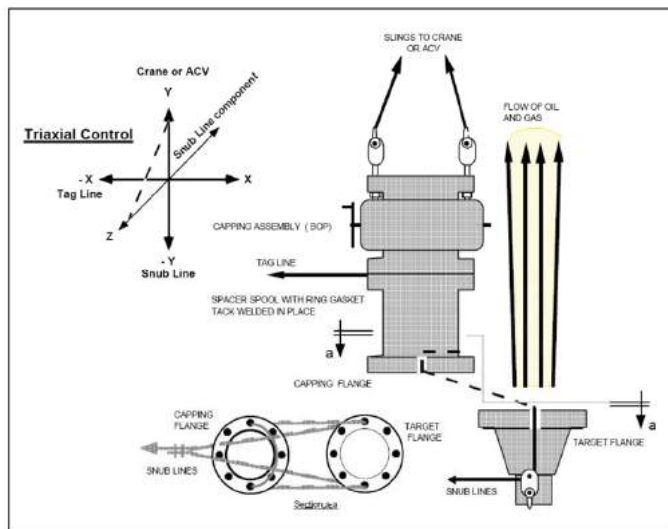


Figure F.7 Capping to a Flange via Snub lines

Once the head has been positioned over the casing stub, the blocks and snub line are removed. A second clamp is installed, but not tightened, between the existing clamp and the head. Hydraulic jacks are positioned between the two clamps (bottom clamp is secure, top clamp is loose). A standard set of split type casing slips are placed in the bowl and engaged by using the hydraulic jacks. After the slips are in place and the pack-off is energized, the top clamp is secured under the head to hold it in place when the hydraulic jacks are released. The sequence is illustrated in Figure F.9

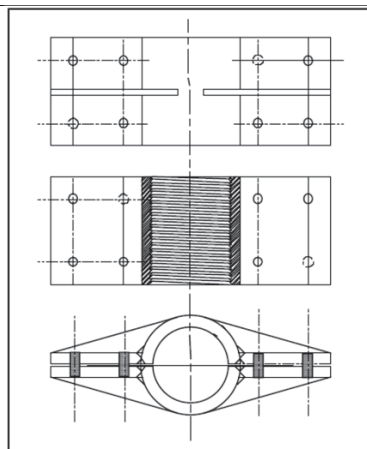


Figure F.8 Casing Clamp
(Courtesy of Blowout Tools, Inc., Lafayette, LA)

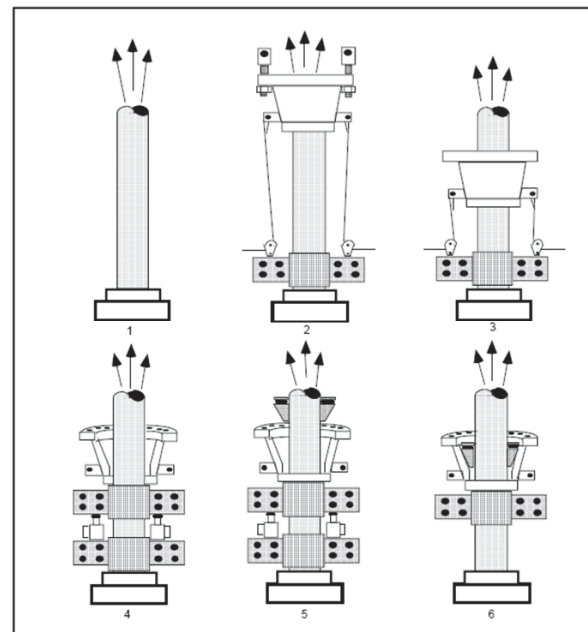


Figure F.9 Emergency Wellhead Installation

To calculate the jacking force required to fix the wellhead onto the casing stub, all subsequent operations should be considered, including.

- Rig deal loads (e.g. BOPE, snubbing equipment)
- Dynamic loading:
 - Pull from snubbing jack
 - Running casing
 - Applied pressure (e.g., shut-in bullheading)

A minimum of two calculations should be made based on the worst case scenarios for forces acting in the upward and downward directions, as illustrated in Example F.1

Example

Given:

SIWHP = 6500 psi

Casing Capped – 7-5/8" in., 47.1 lbs/ft, N-80 (0.8 F_y = 880 kbf, 80% Burst = 8,392 psi)

Snubbing jack weight – 22,000 lbs

BOPE Weight – 40,000 lbs

Snubbing String – 3-1/2" in. 15.5 lbs/ft S-135 DP (80% F_y = 464.8 kbf)

Measured Total Depth (MD) – 15,000 ft

Determine: a) Maximum upward & b) downward forces on wellhead (Fig F.10)

F_{ew}=Equipment dead weight (weight of snubbing jack, BOPs, etc.)

F_p=Pipe weight [ppf * pipe depth (ft)]

F_{p-a}=Pressure area effect (internal pressure* cross-sectional area casing I.D)

Worst Case – Upward Forces:

Bullheading at 80% burst pressure of casing with no pipe in hole.

$$\Sigma F = F_p + F_{ew} + F_t$$

$$F_p = 0$$

$$F_{ew} = 62,000 \text{ lbf}$$

$$F_{tw} = \frac{\pi (6.375^2)}{4} (8,392 \text{ psi}) \Rightarrow +267,865 \text{ lbf}$$

Therefore:

$$\Sigma F = F_p + F_{ew} + F_t$$

$$\Sigma F = 0 - 62,000 + 267,865$$

$$\Sigma F = 205,865 \text{ lbf} \uparrow$$

Worst Case – Downward Forces:

Pipe on bottom (stuck) with wellhead pressure @ 0 psi. Pull 80% F_y of work string.

$$F_p = 0.8 F_y \text{ work string} = -464,800 \text{ lbf}$$

$$F_{ew} = 62,000 \text{ lbf}$$

$$F_t = 0 \text{ lbf}$$

Therefore:

$$\Sigma F = F_p + F_{ew} + F_t$$

$$\Sigma F = 464,800 - 62,000 + 0$$

$$\Sigma F = -526,800 \text{ lbf} \downarrow$$

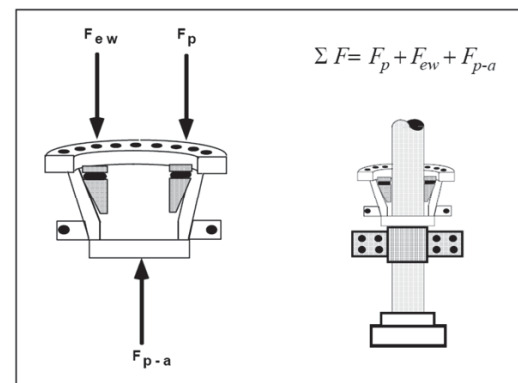


Figure F.10 Diagram of Wellhead Forces

Note that the net upward forces are transferred to the casing slips. These forces should not be allowed to exceed 80% of the casing tensile strength. Since the casing slips are incapable of imparting a downward force, all net downward forces are transferred to the casing via the casing clamp. Maximum unsupported bucking length associated with the worst case scenarios exceed 50% of the maximum tensile stress, bi-axial (axial and hoop stresses) calculations should be performed to evaluate the safety of the rig up.

10.6.5 Capping by Swallowing the Stub

Capping by swallowing the stub is an alternative when the entire wellhead has been removed. This procedure can also be used for capping drillpipe or tubing.

The typical capping assembly for this procedure (see Figure F.11) is a BOP stack. The stack is dressed out with (bottom to top):

- Slip rams
- Inverted pipe rams
- Drilling spool with one each manual and hydraulic valve on each outlet
- Blind rams

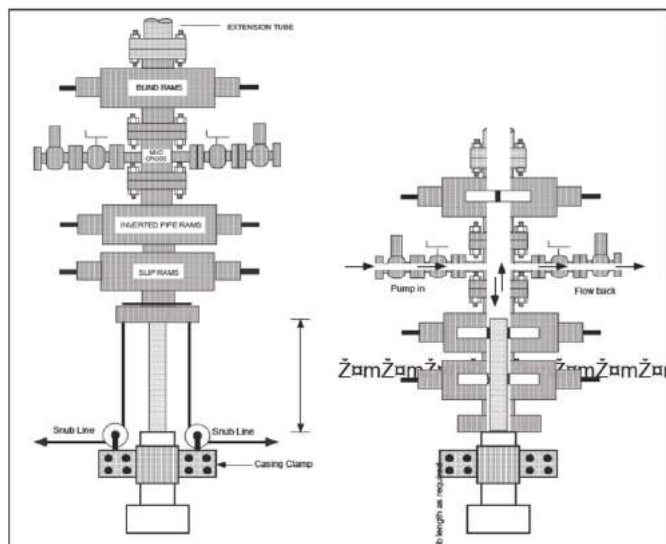


Figure F.11 Typical BOP Stack for Swallowing Casing Stub

Unlike pipe and blind rams, slip rams are not pressure sealing devices. They provide a mechanical grip only which is used to fix the BOP to the casing stub. Figure F.12 shows a diagram of a slip ram insert for a Cameron Type U preventer.

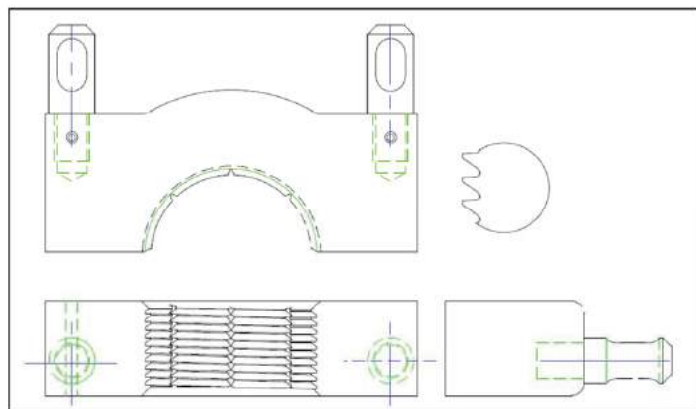


Figure F.12 Slip Ram Inserts (Courtesy of Blowout Tools, Inc. Lafayette, LA)

Once the proper amount of casing is exposed, a casing clamp is installed on the outer casing stub. This clamp is then used to connect the snatch blocks and the snub lines. The BOP stack is lifted with the crane and controlled with the snub and tag lines while being placed over the casing stub. With the BOP assembly safely over the casing stub, the hydraulic lines are connected from the closing unit. The rams are closed in the following sequence:

- Slip rams – to fix the BOP stack onto the casing stub. Note that the BOP must be laterally supported to prevent casing damage from bending forces.
- Inverted pipe rams – to contain the pressure exerted from the top.
- Blind rams – to shut-off the flow, or direct the flow through the side outlet valves for diverting.

The BOP stack can be stabilized with hydraulic jacks and casing clamps if further rig-up is required, such as snubbing or coiled tubing equipment.

10.6.6 Spin On Technique

Spinning a valve or BOP into a flow is a viable option for capping of a flow. The technique is illustrated in Fig F.13. The procedure is simple and has been in use since the 1930's. Very large flows can be handled this way in a safe and efficient manner.

Once feature is that this can be done and requires no special materials or fabrication. Valves and BOPs can be removed as well as installed using this method. As in any capping operation the potential for ignition cannot be eliminated, so firewater protection for the capping crews must be maintained during this and all capping manoeuvres. One drawback is the close proximity of the capping crew to the flow. This aspect must be carefully evaluated. The procedures for installation to an existing flange are as follows:

- Install a hinge bolt (one longer bolt flange).
- Install a lever arm to the capping assembly and sling the assembly for lifting.
- Lift and position the capping assembly onto the hinge bolt at 180 degrees (see 'a-a' of Figure B.13)
- Position crane hook at centerline of the flow/flange to be capped.
- Cover the work area with fire water.
- Manually spin the valve into the flow and align capping and mating flanges.
- Drop in bolts and torque up to effect seal.

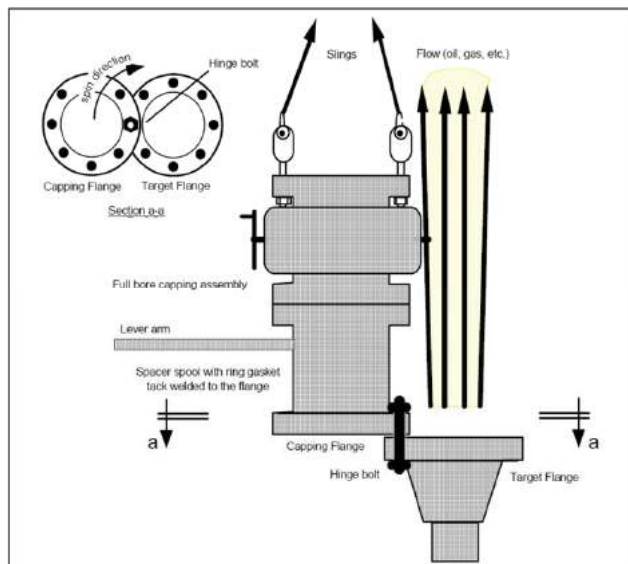


Figure F.13 Spin-on Technique

10.6.7 Forces Encountered during capping operations

The forces imparted on the capping assembly as it is brought into the flow stream can be substantial. A conservative approach is usually taken with regard to the size cables used for the snub lines. However it is sometimes useful to estimate the magnitude of the forces to be encountered. This is done by calculating the momentum flux through a control volume surface which is taken to be the area of the flow stream. This provides a conservative margin since only part of the flow should actually impact onto the capping assembly.

Equation

$$F_{mg} = \frac{S Q_g^2}{1.715 (10^{10}) z D_c^2}$$

Where:

F_{mg} = momentum force of gas, lb force

S = gas specific gravity (Air = 1.0, natural gas use 0.6 to 0.7)

Q_g = volume rate of gas flow, scf/day

z = average gas compressibility factor

D_c = diameter of flow (casing ID), inches

Equation F.2

$$F_{ml} = \frac{\rho Q_l^2}{2.6785 D_c^2}$$

Where:

F_{ml} = momentum force of the liquid, lbs force

ρ = fluid density, lbm/gal

Q = liquid flow rate, bbl/min

D_c = diameter of flow (casing ID), inches

Example

Given :

A gas flow rate = 50,000,000 scf/day (used to yield conservative result).

Casing size = 5-1/2 – in. O.D., 5.0-in. I.D.

Gas specific gravity = 0.7

Z factor = 0.95

Associated liquid of 28,000 bbls/day of 9.3 ppg salt water

$$F_{mg} = \frac{(0.7)(50,000,000)^2}{1.715 (10^{10})(0.95)(5^2)} \Rightarrow 4296.5 \text{ lbf}$$

Second, calculate liquid momentum:

$$F_{ml} = \frac{(9.3) \left(\frac{28000}{24 \times 60} \right)^2}{2.6785 (5)^2} \Rightarrow 52.5 \text{ lbf}$$

The total force possible will be 4296.6 + 52.5 = 4349 lbf or say 4500 lbf. Therefore the cables or boom must be able to withstand a live load force of about 4500 lbf. If a cable system is to be used a minimum safety factor of 4 should be used (4.0 is the preferred design safety factor recommended for this very critical component). Thus the design load will be 4 x 4500 or 18,000 lbs force.

10.6.8 Capping on Fire

Emphasis on environment and personnel safety has caused certain wells to be capped on fire. From an environmental viewpoint, leaving a well on fire can reduce the amount of pollution, provided the well is burning clean. One must realize that capping operations may take longer to complete if the well is left on fire throughout the entire operation. If the well is not burning cleanly then a judgment is needed to determine if less pollution will be caused if the fire is extinguished and thereby allow quicker capping operations.

Capping on fire is also justified if toxic gases are being produced, such as H_2S . Leaving the well on fire may be the solution to personnel hazards for the escaping gases. Regardless of whether the well is on fire or not, the work should proceed carefully taking necessary precautions for H_2S hazards while taking care to guard the intervention team from burns.

An ACV can be used to cap a well on fire. In this particular instance the main reason to leave the well on fire was to prevent pollution from running off into a creek. This creek fed directly into a

drinking water supply reservoir. For this reason it was imperative to avoid polluting the creek at all possible costs.

10.6.9 Stinging to Kill

The stinging operation is technique that can be used to kill a blowing well while it is on fire or simply blowing, provided certain well conditions prevail. Stinging to kill the well is the placement of a "stinger" in the throat of a blowing well in such a way that it functions as a temporary valve. The stinger has a hollow bore that will enable a kill fluid to be pumped into the well by bullheading. It may be the most expedient means to control the well provided wellhead and downhole conditions are favorable. In offshore operations, extra fabrication is sometimes necessary. Some means of placing the stinger at the wellhead will have to be fabricated based on the conditions of the well and structure. The conditions necessary for a successful stinging operations are:

- Shut-in wellhead pressure will be less than 1000 psi.
- Cross sectional flow area must also be fairly small (max 6.5" I.D.)
- There is an unobstructed access to the flow area.
- Ovality of the flow area must be less than 5%
- Downhole conditions are conducive for a bullhead kill.
- Pressure area effect must be less than 30,000 lbs force.

IF the SIWHP is greater than 1000 psi it may be difficulty to create a seal with bridging agents. Common bridging agents are hard rubber, gel, barite, nylon rope or other lost circulation material. These are mixed as a slurry and pumped ahead in a pill. They should be graded in size from 2 mm up to 20 mm (1/16" to 3/4"). Strips of rubber from tire inner tubes are an excellent bridging agent for stinging operations, however almost any type of lost circulation material will suffice. If the shut in pressure will produce more than 16 metric tons (35,200 lbs) of upward thrust from the pressure area effect, it may not be possible to provide rigging or tie downs that will prevent pump-out (ejection) of the stinger (which is assumed to be 99% round) is less than 5 mm (3/16 inch). If this gap is small the bridging agents can seal the leak, per the diagram shown in Figure F.14.

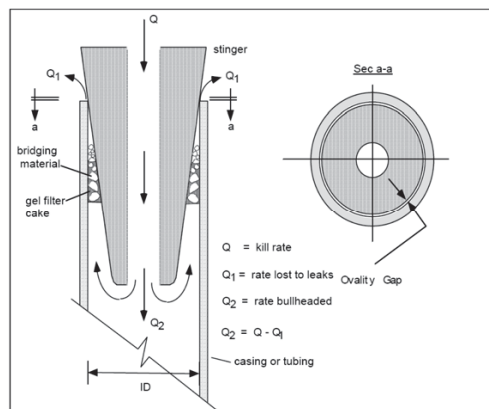


Figure F.14 Stinger Diagram

Example Given:

A flow from 7" (6.24 inch I.D.) to be stung

Determine:

The maximum wellhead pressure to limit pressure area effect to 30,000 lbs force.

$$30000 = (\pi) \frac{(6.25)^2}{4} \cdot WHP$$

$$WHP = \left(\frac{30000}{30.67} \right)$$

$$WHP = 977.8 \text{ psi}$$

Downhole conditions must be conducive for a bullhead kill for the stinging operation. Although a pump and bleed (volumetric kill) procedure will in theory be possible, the general idea is to sting in, pump the bridging agents to seal the leaks and then bullhead the well dead.

Once the well is killed, the objective will be to secure the well. The stinger and its bridging agent seal cannot in any way be considered a permanent barrier. There are several options available. Install a:

- Slip-on weld type head (if productive string is weldable material).
- Temporary wellhead or
- Capping assembly (swallow stub) and/or permanent wellhead and re-tension casing strings.

10.6.10 Conclusions

In recent years there have been great advances in the techniques for capping and controlling blowouts. Equipment and techniques continue to improve due to cooperative efforts by both the capping vendors and the oil operators. This chapter has spoken to a few of the principles of the capping operation. There are many topics concerning capping that were not discussed here. We caution the reader that capping is an "experience-intensive" activity and absolutely nothing can replace the sound judgment that has been gained from years of doing the job. Although procedures have been offered, they are in no way complete. They have not been given for the purpose of guiding the inexperienced to become a capping crew, but for general information to aid all concerned with these types of operations.

Capping operations depend greatly on the situation. However, the three major types of capping operations – capping to a flange, capping by installing a wellhead and capping to a casing stub - cover a vast majority of all well control jobs. Although typically regarded as a somewhat "unscientific" undertaking, certain calculations can and should be made to insure that the end result will allow the subsequent operations to proceed safely.

Advances in explosive and abrasive cutting technology have resulted in improved methods for removing damaged equipment and preparing wellheads for capping operations. This technology should be used to its fullest extent to maximize the safety and efficiency of the capping job.

Stinging operations are applicable where certain conditions prevail. Where the circumstances will allow the use of the stinger technique, it should be considered, since it is a safe and effective means to control a blowing well.

10.7 RELIEF WELL INTERVENTIONS

Implementation of a relief well as a well control technique basically involves establishing direct communication with the problem well by directional drilling of a hole to a specific down hole location in very close proximity to the problem well and at a depth sufficient that will allow overcoming the blowout flow. The interception of the wellbore should be adequate enough to communicate with the blowout flow of the problem well. This would be considered a direct interception allowing a more effective control of the blowout flow. Alternatively, the relief well can be designed to communicate to the blowing reservoir with intentions to alter the reservoir properties with a matrix flood using water or polymers. Regardless of the objective, the relief well must make a close pass or interception of the blowing well to be successful. If possible and as a precaution, the interception should be planned and positioned to intercept within the plane of the maximum principal stresses of the formation rock. This will improve the chances to effectively communicate with the blowing well via the matrix or an induced hydraulic fracture when a direct interception fails. When a proper communication is established, it should be possible to pump kill fluid at designed rates to kill the well.

10.7.1 Kill Well Techniques review

In attempting to classify kill techniques, it is convenient to consider those which can be implemented directly over the blowing well (direct kills), and those that require the drilling of one or several relief wells.

Blowout control methods include some 'pumping', whether directly through the top of the blowing well or at depth via a relief well. The four basic pumping techniques that blowout 'specialists' usually refer to are:

- Overbalance kill
- Dynamic kill
- Momentum kill
- Matrix kill or flood kill

The best practice, once it is obvious that a 'simple kill' of the hydrostatic nature for instance will be ineffectual, is to prepare and spud a relief well concurrently with eventual surface kill preparations. If the surface kill fails, much time will have been gained.

The situation of the blowout will dictate the objectives of the relief well. The reservoir data and geological model will determine the type of kill required and the number of relief wells to consider. Once this has been established, quantity estimates and the availability of the following can be made.

- personnel,
- equipment,
- supplies,
- services, and

When making these estimates, the tendency is to look only to the worst possible case. While this is advisable in a contingency plan, a moderate or most likely scenario should also be investigated. Having alternative plans other than the worst case event will help eliminate "overkill" and waste and allow the operator to move quickly in response to the emergency.

The further the surface location of the relief well is from drilled well, and the greater the depth to the intercept target, the greater the degree of precision required in directional control. The depth of the blowout has a major effect on how the well is killed. If relatively shallow (less than 3000 ft) it

will require a shallow kick-off depth which can complicate directional control. The softer clays encountered while trying to obtain the high build and drop rates and high drift angles necessary just add to the directional control problems. Later under reaming or hole opening operations are also more difficult in such soft and often unconsolidated formations.

As the point of intersection becomes deeper, drilling times increase. However, the longer drilling time will allow orderly planning and mobilization of special equipment, supplies, and kill personnel. On the other hand, the deeper horizons are typically at a higher pressure and, up to a point, more prolific. The special equipment must therefore be sized upwards to meet the higher pressure and volume requirements. The deeper horizons and added drilling depths impact negatively on navigation as the ellipse of uncertainty increases. It might require many passes and re-drills before the blowing well is cleanly intercepted.

The planned trajectory is merely a general guideline and not an absolute rule. The relief well is drilled in three major phases.

- Phase I: Drill directionally to a point in space that converges near the blowing well's casing or BHA, within range of wireline proximity logs.
- Phase II: Locate the relative position of the relief well to the blowing well using proximity logging techniques and sound judgment.
- Phase III: Converge with the blowout well at the desired interception point (or a very close pass by) to establish the necessary communication to kill the flow.

In reality, the plan for the well can only take the relief well to the start of Phase II. After the well is located using proximity techniques, the final trajectory design will take place.

10.7.2 Positioning the Relief Well

Positioning the relief well involves a number of objective and subjective considerations. Listed below are the general factors taken into account while positioning relief wells for a typical exploration well:

- Direction of the prevailing winds as defined by the regional wind roses.
- Direction and dispersion of oil by the offshore currents.
- Safety perimeter around the well surface location (350m ± 10m) based on minimum pollution levels at the surface location and heat radiation of a 120 mmscf/d gas fire.
- The blowout's targeted bottom hole location and position uncertainty.
- The subsurface location of other wellbores.
- The presence of sea bed obstacles or installations such as pipelines
- Minimizing the distance and time to drill the relief well.
- Natural offshore characteristics which influence directional control
- The desired approach angle and direction in converging to the target.
- Degree of confidence in achieving a trajectory to interception.
- The depth at which interception must occur.
- Range and ability of proximity tools to detect casing or BHA (60 meters for induction tools / 50 meters passive magnetic).
- Maintaining as simple as possible trajectory and minimum dogleg severity; upper acceptable dogleg for planning purposes has been 2.0 deg/100 ft [667 deg/10 meters].

The position of the relief well is always more critical in an offshore location. Consideration needs to be given to current and wave behavior in the vicinity of the PTTEP location. The prevalent wind direction also dictates the location of the relief well.

Some of the factors in positioning the well include local regulatory and environmental considerations, the influence of the underwriters, the state of the seas and winds (current speed, direction, velocity, frequency), water depth, mudline conditions (debris, pipelines, sediments, obstacles, other wells), and the situation at the blowout site (size of the plume, type of well effluent, fires, surface cratering, state of the BOPE). There does not appear to be any minimum distance, except as dictated by specific conditions. Other factors relate to the well to be drilled, such as where the original well will be intercepted and the intercept trajectory. A site selected without due consideration of all relevant factors can result in increased difficulty and cost in reaching the desired objective. The location of the relief well for each blowout should be chosen based on its own merits.

More importantly, the relief drilling site and the relief well trajectory must not be compromised by any existing platform, wells, or well paths. It is difficult to conceive of a more extreme situation than a blowout at or near a producing platform, where numerous wells converge to the platform. The nearby wells interfere with ranging techniques and enhance the ellipse of uncertainty. These conditions might suggest that the blowing well be intersected as deep and as far away from the congested area as possible, even though the ellipse of uncertainty is greater. The platform scenario becomes more complex when multiple wells are blowing out, requiring multiple simultaneous relief well drilling operations. Every effort must be given to avoid any mooring pattern from overlapping other mooring patterns.

The general factors listed establish the preferred relief well location for a typical exploration well. An S-shaped trajectory for the relief well will usually suffice. This is the absolute shortest drilling distance that meets the objectives of the relief well and the 350 meter exclusion zone criteria. It represents an aggressive drilling trajectory with directional control, but compared to a simple J-shape that will require multiple plug backs, it is considered to be the most direct and efficient of all the possibilities. For a typical exploration well, a single relief location that is a sufficient distance from the well, but close enough that an aggressive drilling program is possible, is usually recommended. However, each case is unique.

10.7.3 Relief Well Target

In considering the relief well target, there are two distinct possibilities in the blowing well. The first is that the drillstring is on bottom and the other that the drill string is out of the hole, or pulled up inside the casing shoe (as in the string hung off before shearing the drillpipe). It is essential that there be metal (casing or drill string) in the blowing well for all types of proximity logs to function. If the target interception point is an open hole interval, the drill string must be across the target zone. If this is not the case, the target will be the deepest casing shoe. If the drill string is on bottom, the target can be where the blowing well penetrates the flowing reservoir. However, for planning purposes, the last casing shoe set is a target that is known to exist and therefore the most advantageous target as the primary initial target in Phase II. Should a blowout occur, the directional plan can be altered for deeper horizon targets when conditions justify such a change.

The Phase II objective will be converge to the blowing well at the estimated location of the deepest casing shoe. The relief well must be between 50 to 60 meters of horizontal distance from the blowout wellbore, and be approximately lined up (within 7 to 10 degrees in combined inclination and azimuth) when the end of phase II is reached.

Phase II begins when calculations show that the relief well has come within 50 to 60 meters of horizontal distance to the blowing well. (Note that the proximity logs measure distance between the two wells in a plane perpendicular to the well to be ranged to, therefore high angle wells may need adjustment of these criteria. At the depth of interest, the trajectory of the target wells in this

plan is vertical (or near vertical). Thus, the horizontal distance of 50-60 meters is valid without adjustment for inclination.

The first proximity survey can be made at the 50 to 60 meter range. However, one should not expect to receive definitive information until the distance between wells is 15 to 30 meters, and the most reliable information becomes available in the 1 to 15 meter range. Course corrections should not be made unless data from the proximity logs is in the 10 to 20 meter range, and confidence in the data collected is high.

Phase III, drilling to interception, is the most critical stage of the relief well project. Once the blowing well trajectory is determined, a precise trajectory can be determined for an interception. Given that confidence in the ranging data is attained, Phase III can begin.

The intercept point where the relief well and the flowing well are designed to come together is most usually at the bottom of the flowing well. This is normally where the flowing zone is found, except when serious pressure reversals exist. It is also the place where the kill fluid, when placed in the flowing well, has the greatest influence due to its having access to the entire drilled wellbore. An off bottom kill would require a higher kill mud weight to achieve a similar hydrostatic kill pressure. The bottom kill uses the lowest possible kill mud weight. However, bottom kill is not always the best approach. Lessons learned from the past tell us that in high permeability reservoirs (8 darcies, Ixtoc 1, June 1979) a bottom kill will never work.

The ellipse of uncertainty increases with depth so that more passes might be required before the flowing well can be hit with certainty. The deeper the well, the longer the drilling time. Temperature also increases with depth, so mud treatment becomes more complex. Ranging surveys and logging services also require more sophisticated methods at elevated temperatures. These effects, individually and collectively, increase operational costs. However, if the blowout well has several zones flowing, it might be necessary to consider a bottom kill *and* an off bottom kill.

Once the well is intercepted, the task will be to communicate directly with the blowing well. This communication will most likely occur by a breakthrough from the relief well to the blowout well when the wellbores are within 0.2 to 1 meter apart. This will depend on the flowing bottom hole pressure of the blowing well and the formation rock mechanics. In this case, the communication link should establish itself very quickly. It should become physically quite large (5 to 20 mm) and offer little if any flow restriction.

Once communication has been established, the objective shifts to pumping a sufficient volume of kill fluid into the blowing well, at an adequate rate to overcome and kill the hydrocarbon flow from the producing interval. Once control is achieved during the initial kill operation, both wells need to remain stable until abandonment or workover operations can take place. In no case should the kill operation expose the well to additional risk of unmanageable problems brought on by a worsening control situation. Reasonable judgment and practices should be taken in pursuing the kill operation. The kill should not be irreversible, nor should it unduly eliminate reasonable kill alternatives if the initial attempts fail. An example of an irreversible operation would be attempting to kill the well with cement rather than drilling mud. The overall plan should take this philosophy into account.

There is a remote possibility that in spite of best efforts, the relief well will miss the blowing well and make a close pass, perhaps 1 to 2 meters away. If a direct communication is not possible, it may be necessary to plugback to intercept. Depending upon the distance between wellbores, an acid job in carbonate rock may be considered to establish communication. This will work best if the relief well bore is in the pressure draw-down of the deepest producing zone. If this is the case, the acid will travel naturally through the matrix of the producing zone and into the blowing wellbore. A worm hole path will be created and the net result will be the creation of a direct communication between the two wellbores. This option should be carefully studied before implementation as there are many acid treatment designs using gels, retarders and concentrations to consider. Direct communication established through interception is better than relying on an acid job to create a

worm hole. Fracturing the rock matrix should be avoided, but if fracturing is to be attempted, then rock stresses will dictate the direction of the fracture path. If the intercept is not in the plane of the maximum rock stresses then the fracture will never intercept the blowing wellbore. Other options are perforating or milling techniques, if communication is to a cased hole.

10.7.4 Casing Design and Seat Selection

The relief well casing design and seat selection must meet both the requirements of the kill operation and the normal regional drilling conditions. The ultimate objective of the relief well is to overcome and kill the flowing well. The conditions imposed by this objective are additional requirements beyond the normal casing design.

Casing strings should be designed against the following conditions:

Regulatory agencies may set the minimum-design conditions they expect to see in wells drilled in their jurisdiction, relating to whether or not the well must contain the full pressure at the surface, the safety factor for collapse, and so forth. Typically, they will dictate the maximum setting depth for the surface string to protect any ground water supplies.

These conditions could be pressures during kick operations such as shutting in the well, circulating out the kick, or the pressures that could build if the pipe is sheared.

However, additional factors might need to be taken into account as the direct result of the blowout. If too little casing is set, there is the real problem of loss of circulation or worse, or even stuck pipe if differential pressures become extreme. If too much casing is set, you can run out of hole as the resultant hole size becomes too small to handle the large kill flow rates required.

- What is the impact on well design by the reservoir?
- Will the casing be of sufficient capacity to allow the high volume pumping required for the kill operation?
- Will the casing design allow for a back-up string in the event an additional string is required?
- Are any shallow zones pressure charged? Is the reservoir expected to be depleted in the vicinity of the wellbore?

These unique conditions that occur in the relief well are not common to ordinary wells. In an underground blowout, for example, there can be charging of upper formations or depletion of deeper formations. This may significantly alter previously observed conditions and present new problems during the drilling process. Additional factors have been considered and evaluated in addressing the relief well design:

- Effects of well casing configuration on the friction and flow rates required during the kill operation.
- Implications of setting an additional casing string to combat downhole problems encountered during drilling, i.e. can the objective still be attained if a further reduction in hole size is required or additional strings set.
- Realistic possibility of individual zones being artificially pressured or depleted and there is information to support this position.

Besides the above, certain questions should be reviewed before spudding the relief well, to take advantage of the most current information:

- Has the target location changed significantly since the relief well plan was developed?

- Were there complications encountered in the original blowing well during the up hole sections which could threaten the success of the relief well? How will these be averted?
- Will the casing schedule have to be modified to meet the directional drilling objectives required to intercept the blowing well?
- Was there an unanticipated presence of a corrosive or toxic fluid such as CO₂ or H₂S requiring special consideration?

If the relief well is to be considered as a replacement well for the blowing well then future requirements for production and stimulation must also be taken into consideration in the overall design. These details have not been covered by this study because it is thought that stimulation or productive casing loads are not to be applied to a relief well casing string. In other words, the relief well is thought of as a sole purpose well and not a producing well. The casings as detailed for a typical developmental and exploration well have been reviewed, and are adequate for all relief well loadings and conditions. Open hole and casing loads imposed by the kill operation have also been considered.

10.7.5 Ellipsoid of Uncertainty

The primary objective is to intersect the blowing well at some predetermined subsurface point (in this case the top of the producing formation). It must be realized that various factors detract from the ability to reach that point with pin point accuracy. The influence of the various factors is frequently described as the "cone of uncertainty." Normal directional well targets are usually a two dimensional circle or rectangle in the horizontal projection. The relief well must view the producing well's trajectory in a three dimensional perspective. Consideration is given to possible inaccuracies in, or lack of, survey data. As a result, rather than having a specific point for the target for the relief well, it becomes in reality an ellipse which is commonly referred to as the "ellipsoid of uncertainty".

While some would argue that an ellipsoid applies only to outdated directional survey tools, such as the single shot or multi-shot (not the EMS), it is still considered a standard to think of wellbore uncertainty as an ellipsoidal shape. High accuracy tools, such as the North seeking gyro, have equal accuracy in azimuth as they do in inclination, and therefore the ellipsoid would truly be a sphere.

The factors which influence the relationship of uncertainty in a relief well situation can be summarized as:

- Accuracy of the survey on the surface location (2 meters).
- Type of directional survey equipment employed and their inherent inaccuracies.
- Ability to confirm the well trajectory using different methods of measurement.

The following criteria are a guideline for the preparation of this relief well contingency plan:

- Initial spotting of the rig on the relief well location must be accurate to within 5 meters of the desired position. Surveys must be recalculated through interactive measurements until the accuracy is within 2 meters by the time the kickoff point is reached.
- Three types of survey tools will be used, the MWD, EMS and a North Seeking Gyro. Although not a directional tool the proximity tools will influence the degree of uncertainty. The tools will be supplied by the local directional or surveying vendors.

- The use of the three types of survey equipment in both open and cased hole will serve to verify the accuracy and repeatability of the surveys. Proximity tools will determine the relative position of the wells to each other once the wellbores converge within the tool's range. Details on the survey program will be provided under the topic "Directional Control."

The reliability of a relief well plan depends not only on the ability to accurately measure the hole position, but also on the prescribed directional program. On paper, a wide variety of relief well trajectories are possible, but in practice only a few are practical. The selection of a relief well location and the planned trajectory go hand-in-hand. As discussed earlier, a great number of considerations are involved in the selection of the relief well location. The weighting of the various considerations relative to this plan has been biased by:

- Desire to minimize the necessary drilling time by picking a kickoff point as deep as possible and planning a trajectory which minimizes survey requirements, eliminates additional motor runs and doesn't automatically require plugback operations.
- Avoidance of difficult directional maneuvers or approaches to minimize the possibility for failure.
- Availability of reasonably accurate survey data on the blowout wells makes it sensible to plan a relief well trajectory with a fairly deep initial crossing point for wellbore location.

10.7.6 Directional Control and Surveying Requirements

Maintaining a high degree of accuracy in the relief well directional control is essential for success. A successful relief well can be assured if stringent directional control is maintained.

- The relief well intersect of a blowing well is contingent on the ability to accurately map the blowing well's path from the surface to the bottom of the hole.
- A consistent directional survey program is the key to this goal.
- Inconsistencies in the directional data should be backed up by additional surveys resolve the differences.

10.7.7 Surveying Requirements for the Relief Well

The relief well directional program will follow a trajectory from the selected surface location to a point in close proximity to the wellbore of the blowing well. At that point proximity tools will detect the casing in the target wellbore. Once the target wellbore is located, the existing blowout directional surveys are tied into the proximity tool's results to guide the relief well to interception.

Survey data obtained in the relief well should maintain a high degree of accuracy in order to reach the interception objective. The survey policy for a typical exploration well is adequate for the depth of the wells, considering the range of the proximity logs. Full-time use of MWDs should now commence. Run a North seeking gyro to confirm the location below the kickoff point in the relief well before running surface and protective casings. Use the same vendor's downhole survey tools as were used in the blowout well, in order to limit tool characteristic variables. Duplication of data accuracy between wells is best achieved if any variance in tool characteristics is minimized.

Avoid collision except at the point of interest. When the relief well comes into the vicinity of any wellbore, it may be necessary to run proximity tools to verify that a premature collision will not occur. Note that Phase II of the drilling of the relief well begins when the calculated distance between the wells is about 60 meters. Proximity logs are used to avoid an early collision. If a collision is eminent, course corrections may be required to guide the relief well safely past the wellbore to the intended target.

10.7.8 Converging to a Blowing Well

Provided the directional surveys for the blowing well are reasonably accurate, it should be possible for the relief well to drill directly to the vicinity of the deepest casing shoe or the BHA left in the blowing well. The convergence path of the relief well presented in this plan should have a combined difference in both azimuth and inclination of less than 10 degrees from that of the target well. If the target well is to achieve this path, the relative position of the relief well to target well must be established at considerable distance from the crossing point. The radius of uncertainty can create a situation where it is very unlikely that an interception could be achieved using directional techniques alone (e.g. drill to a point in space without ranging to the target).

In essence, the proximity tool reduces the ellipse of uncertainty. For relief well plans, there are two primary types of proximity tools. One derives its ability to detect an adjacent well through an induced electrical field, while the other measures the magnetic flux between the tool and the casing or bottomhole assembly in the target well. Regardless of the tool used, metal (iron for the passive tool) in the BHA or casing of the relief well is required for these tools to work. If there is cased wellbore nearby, the interpretation can be difficult. Both proximity tools have unique sets of strengths and weaknesses so use both to take advantage of each tool's strengths.

10.7.9 Induction Tool

The induction tool makes use of an induced electromagnetic process which effectively, allows detection of a well within 50 to 90 feet. The inductive electromagnetic process requires the tool to be run in open hole. If the emitting electrode cannot be placed in open hole, the range is reduced to about 30 to 40%. For best results with the electric process range, the induction tool should be run in at least 100 meters of open hole. Open hole logging can be a major drawback if hole conditions are not optimal. A method used to overcome this problem has been to run open-ended drill pipe to just above the depth near the point of investigation. The tool is then run inside the drillpipe and allowed to exit into the open hole.

10.7.10 Passive Magnetic Surveys

The passive magnetic tool has detected casing at 150 feet. This process isn't strongly influenced by being run inside a non-magnetic drill collar, and is the preferred method of making the survey. The ability to run inside the string saves valuable rig time by eliminating trips. Although used to detect pipe at a distance of 150 feet, the accuracy of the passive tool is generally better within a 40 to 60 foot range of the target wellbore.

10.7.11 Intercepting and Establishing Communication

Under the conditions presented by a typical exploration well, direct interception of the blowing well in the open hole, at or below the top of the producing interval, should be the primary objective. If the well is cased, the objective will be to pass near the top perforation. The ideal point for the relief well to intercept the target well is at the top of the main reservoir, where kill weight fluid will be injected directly into the flow at its source. It is possible that a direct intercept cannot be accomplished, but adequate communication can be established between the wells. Since the reservoir is limestone, the communication can be through the rock matrix. Acid may be used to remove mud damage and open up the permeability if required.

If the target well is not intercepted, and acid fails to open up a sufficient flow path, more drastic methods may be required to establish communication with the well. The options will vary depending on the individual situation, but may include such operations as fracturing between wells or perforating the formation with a tubing conveyed shaped charge, oriented toward the target wellbore. However this option is considered a remote possibility because the confidence for making a wellbore interception is very high.



Despite the means necessary to establish communication, all preparations to perform the kill operation must be in place before drilling the final segment of the relief well. If an intercept is attained, there will be no option but to immediately commence the kill operation.



10.8 RELIEF WELL PLANNING

The purpose of this Appendix is to provide a generalized guideline for drilling a relief well. Information that is common to relief well planning and implementation is contained in this section. This Appendix does not address fully site specific issues for any particular reservoir or field.

It is important to remember that every blowout has a unique set of circumstances from which the majority of the planning process is directed. However, the strategy applied here is acceptable since the primary purpose of this appendix is to familiarize local personnel with some of the special techniques and services associated with planning a HTHP relief well. If an actual emergency were to occur, this planning process would have already been established and would save valuable time in a real intervention situation.

10.8.1 General Commentary on Relief Wells

The primary purpose of drilling a relief well is to kill an uncontrolled flow from a blowing well that cannot be reliably controlled at the wellhead by capping operations. One such example is when the well has cratered and there is no access to the wellhead leaving the relief well as the only feasible alternative. Another case is deep water wells where an offset re-entry kill is not possible. However, if the wellhead is accessible, capping operations are successful in controlling the well more than 97% of the time (making relief wells low probability options). While relief wells have been responsible for controlling only a minor number of all blowouts, they are an important part of well control capabilities.

The relief well is a special type of directional well. It is drilled from a surface location in as close a proximity to the surface well as possible. Its purpose is to provide a conduit, down which a kill mud of adequate weight can be pumped in sufficient quantities to arrest the blowout. The kill procedures might include the momentum kill, the dynamic kill, or flooding the reservoir. In practice, the trajectory of the kill well is designed to intersect the blowing well just above and as close to the inflow zone as possible. Casing or drillpipe is then set as close to this point as possible, prior to any attempt to kill.

Uncontrolled flows fall into two general categories: underground and surface blowouts. Subsea blowouts where the exit point is to the seabed are also classified as surface blowouts. Regardless of the exit point of the flow, the relief well will have the objective of a very close pass by, or an intercept of, the wellbore of the blowing well if it is to be successful (see Figure A.1). This will be at depth sufficient to kill the flow by pumping a kill fluid from the relief well into the blowing well. The interception of the wellbore should also communicate to the blowing well and create a viable flow path for the kill fluid from the relief wellbore. Alternatively, the relief well can communicate to the blowing reservoir to perform a matrix flood of the reservoir to control the well.

The situation of the well dictates the objectives of the relief well. In the preplanning phase, it is necessary to make educated guesses based on several likely scenarios. Much information is needed to describe the reservoir, such as its pressure, permeability, porosity, reservoir limits, and most importantly, the reservoir deliverability. This information is then used to determine the type of kill most likely to achieve the desired objective, the number of relief wells likely to be required, an estimate of the personnel, equipment, supplies, and services needed, and a timetable for the event.

When making these estimates, the tendency is to look only to the worst possible case. While this is advisable in a contingency plan, a moderate or most likely scenario should also be investigated. Having alternative plans other than the worst case event will help eliminate "overkill" and allow the oil operator to move quickly in response to the emergency.

Several case histories offer valuable insights into contingency planning for relief wells. Beginning with a Texas panhandle event in 1982, there have been three major events where the operator planned complicated kill operations from relief wells. These blowouts were all 'engineered' as

large volume, massive horsepower kill operations. At the end of the day, the exotic and costly kill operations were not required and therefore only served to fulfil the perceived design requirement.

In a 1989 North Sea control operation, preparations were made for a high horsepower, large volume pump job designed for what was perceived to be a worst case scenario. About 9,600 HHP was rigged up and kept on a constant state of readiness for 6 months. Upon interception of the blowing borehole with the relief well, the fluid in the relief well U-tubed by gravity into the blowout well, killing in 1 a few minutes, and none of the high pressure horsepower pumping spread was employed to kill the well. Pumping requirements were limited to keeping the relief well hole full, which was accomplished with a single cement pump unit carried on board as part of the basic rig components. These wells are examples of "overkill" in the pumping requirements and the failure of the designers to account for the drawdown of the blowing well. On the contrary, if the reservoir is very strong (little depletion) large pump pressure and horsepower kill operations will be required. Another source of overkill in a relief well plan is excessive use of safety factors. If the reservoir parameters, leakoff losses, kill requirements, frictional pressures and pumping output all have safety factors applied individually, the overall result will be massive pumping spreads and volumes.

In the USA, there were two deep, high pressure wells which blew out in 1982 and 1985. Both wells were controlled by relief wells. The plans again called for high pressure/volume pumping kill operations. In both cases the kill volumes and pressures necessary were much less than anticipated. In these cases, as in the previously described North Sea operation, fluid in the relief well U-tubed into the blowing well on interception without assist from applied HHP from the surface. This again made the kill operation merely "keeping the relief well hole full". Minimal assistance from the surface pumping equipment rigged up specifically for the kill operation was required, and in the opinion of the author, not justified. All wells were controlled by keeping the relief well full, at average pumping rates of less than 10 bbls per minute, until about one hole volume U-tubed into the blowing well. Thereafter, the wells were under control and circulation established.

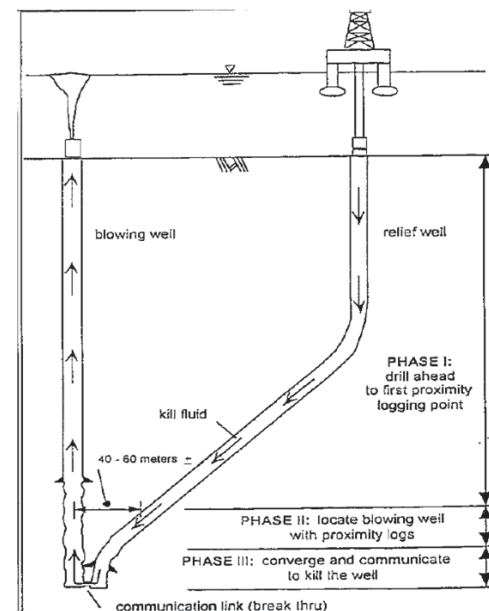
The point to be taken from these case histories is that there may well be a scenario where the blowout can be killed with conventional equipment, resources found in normal drilling operations, and may not require massive pumping spreads. However, there are situations in which a significant amount of hydraulic horsepower and kill volume is required. A concerted effort to offer both the worst case possible and a reasonable kill plan for a dynamic kill from a relief well is necessary.

10.8.2 General Trajectory and Objectives of the Relief Well

In simple terms, the relief well is a directional well that unlike the common directional well has a small, well defined target. Otherwise, the attributes are the same as a common directional well. The main objective will be to establish a direct communication with the blowing wellbore. This communication is the single most critical element in the success of the relief well. The accuracy of present technology for locating blowing wells with wireline proximity logs enables an interception or 'hit' of the blowing well to establish a direct communication link. The confidence for an interception is very high. In the last ten years, every relief well that has been drilled to objective with an interception in mind has been successful in achieving that goal.

To a large extent, the greater the depth of water the more the water will act as a buffer or choke to restrict the effluent flow. Gas will not escape as readily. Gases such as methane and hydrogen sulfide partially dissolve in the water, so their effects are lessened. Gases normally will not adversely affect operations where water depths exceed 1200 feet. The deeper the water, the less the reservoir drawdown, so kill pressures are higher. In some cases, reservoir conditions might cause localized depletion around the wellbore so kill pressures are lower. The further the surface location of the relief well is from drilled well, and the greater the depth to the intercept target, the greater the degree of precision required in directional control. For deeper water operations, the

offset well might be drilled in close proximity to the original well and track that well until close to the planned point of interception.



Relief Well Drilling Phases

The depth of the blowout has a major effect on how the well is killed. If relatively shallow (less than 3000 ft) it will require a shallow kick-off depth which can complicate directional control. The softer gumbo-type clays encountered while trying to obtain the high build and drop rates and high drift angles necessary just add to the directional control problems. Later under-reaming or hole-opening operations are also more difficult in such soft and often unconsolidated formations.

As the point of intersection becomes deeper, drilling times increase. On the one hand, the longer drilling time allows more orderly planning and mobilization of special equipment, supplies, and kills personnel. On the other hand, the deeper horizons are typically at a higher pressure and, up to a point, more prolific. The special equipment must therefore be sized upwards to meet the higher pressure and volume requirements. The deeper horizons and added drilling depths impact negatively on navigation as the ellipse of uncertainty increases. It might require several passes and re-drills before the blowing well is cleanly intercepted.

Besides establishing a communication link to the blowout well, the relief well hole must be maintained in such a state that the drillstring can be easily tripped in and out. The hole must be maintained for logging casing running and cementing operations, and most importantly, for well killing operations. Whenever possible, hole problems such as loss of circulation and sticking must be solved so that continuing progress can be made. If downhole drilling problems are not resolved, the well may not reach its objective. Progress cannot sacrifice these essential parameters. For example, the hole will be useless if proximity logs cannot be run without causing a fishing job.

The major differences between relief well and ordinary directional wells are that the target is much smaller and fluid injection rather than production will be the prime concern. In some cases, the target may be only inches wide, as in the Texas Panhandle well, Apache Key #1-11, where the objective was to hit a 5" liner at 16,080 feet (4902 m) TVD. In other cases, the target can be quite large as in matrix kill operations (Aramco Berri #34, 1979, where horizontal separation was approximately 40 feet). In this case the formation characteristics allowed the relief well to converge to a near passby of the target wellbore rather than an interception. Regardless of the type of kill operation desired, the ability to drill to a well-defined target will enhance the chance of success for the kill operation. Bearing in mind the small size of the target and the limited range (50-60 meters maximum) of the proximity tools, a relief well must be drilled with consideration for necessary course corrections.

The planned trajectory is merely a general guideline and not an absolute rule. The relief well is drilled in three major phases as illustrated in Figure H.1:

- Well's casing or BHA, within range of wireline proximity logs.
- Phase II: Locate the relative position of the relief well to the blowing well using proximity logging technique and sound judgment
- Phase III: Converge with the blowout well at the desired interception point (or a very close passby)

In reality, the plan for the well can only take the relief well to the start of Phase II. After the well is located using proximity techniques, the final trajectory design will take place.

10.8.3 Positioning the Relief Well

Positioning the relief well involves a number of objective and subjective considerations. Safety considerations are more straightforward and require prudent decisions. The trajectory required for interception strongly influences well placement, and involves more complex decisions based on the anticipated ability to achieve the prescribed directional drilling program. Listed below are the general factors taken into account while positioning relief wells:

- Direction of the prevailing winds as defined by the regional wind roses.
- Direction and dispersion of oil by the currents.
- Safety perimeter around the well surface location (as required) based on minimum pollution levels at the surface location and heat radiation.
- The blowout's targeted bottom hole location and position uncertainty.
- The proximity of other surface facilities or wells.
- The subsurface location of other wellbores.
- The presence of sea bed obstacles or installations such as pipelines.
- Minimizing the distance and time to drill the relief well/
- Natural regional characteristics which influence directional control.
- The desired approach angle and direction in converging to the target.
- Degree of confidence in achieving a trajectory to interception.
- The depth at which interception must occur.
- Range and ability of proximity tools to detect casing or BHA (60 meters for induction tools/ 50 meters passive magnetic).

- Maintaining as simple as possible trajectory and minimum dogleg severity; upper acceptable dogleg for planning purposes has been 2.0 deg/100 ft. [0.667 deg/10 meters].

The position of the relief well is most critical in an offshore location. Figure H.2 is excerpted from a Blowout Contingency Plan where factors listed above have been considered.

Most likely, the casing will be detected before a crossing occurs, and a mid-course correction made for an interception at the producing interval. However, if casing is not detected by the time that the deepest casing target point is reached, the relief well will drill ahead, holding angle and direction, until casing is located or total depth of approximately 20 meters above the reservoir is reached. If casing is still not located, the well must be plugged back and turned to a new target. Care must be taken to not penetrate the reservoir before protective casing is set. Once casing has been detected with proximity logs, the relief well will be turned and guided to make an interception at or near the reservoir penetration. The deepest casing point was chosen as the Phase II target because, unlike the drill string, it will always be in place. It is at sufficient distance up hole from the interception target that course corrections are possible to carry through an interception of the blowing wellbore.

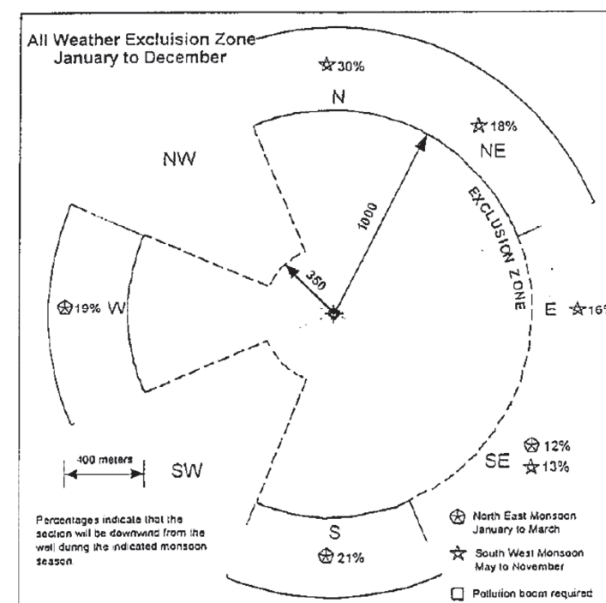


Figure H.2 Exclusion Zone Example for An Offshore Relief Well.

Phase I should be drilled in a manner similar to that of any other development well. The drill site for the relief well must be chosen with care. Particular attention must be paid to the surface location of the well, and to accurate directional control. The surface location must be accurate to within 5 meters when moving the rig onto the desired location. Thereafter, the surface location of both the blowout and the relief well should be resolved to within plus or minus 1 meter accuracy.

The relief well site will often be a compromise based on several conflicting or complimentary factors. Some factors will point to a specific direction and location while others will point to contrary directions or locations.

Some of the factors in positioning the well include local regulatory and environmental considerations, the influence of the underwriters, the state of the seas and winds (current speed, direction, velocity, frequency), water depth, mud-line conditions (debris, pipelines, sediments, obstacles, other wells), and the situation at the blowout site (size of the plume, type of well effluent, fires, surface cratering, state of the BOPE). There does not appear to be any minimum distance, except as dictated by specific conditions. For example, the intensity of the fire, if present, might require the relief well be situated a thousand feet or so away from the heat source. Other factors relate to the well to be drilled, such as where the original well will be intercepted and the intercept trajectory. A site selected without due consideration of all relevant factors can result in increased difficulty and cost in reaching the desired objective. A single site can rarely be optimally located to serve multiple blowouts. The location of the relief well for each blowout should be chosen based on its own merits.

More importantly, the relief drilling site and the relief well trajectory must not be compromised by any existing platform, wells, or well paths. It is difficult to conceive of a more extreme situation than a blowout at or near a producing platform, where numerous wells converge to the platform. The nearby wells interfere with ranging techniques and enhance the ellipse of uncertainty. These conditions might suggest that the blowing well be intersected as deep and as far away from the congested area as possible, even though the ellipse of uncertainty is greater. The platform scenario becomes more complex when multiple wells are blowing out, requiring multiple simultaneous relief well drilling operations. Every effort must be given to avoid any mooring pattern from overlapping other mooring patterns.

The general factors listed establish the preferred relief well location for a typical exploration well. An S-shaped trajectory for the relief well will usually suffice. This is the absolute shortest drilling distance that meets the objectives of the relief well and the 350 meter exclusion zone criteria. It represents an aggressive drilling trajectory with directional control, but compared to a simple J-shape that will require multiple plug backs, it is considered to be the most direct and efficient of all the possibilities. For a typical exploration well, a single relief location that is a sufficient distance from the well not to create a hazard for the drilling crew, but close enough that an aggressive drilling program is possible, is usually recommended. However, each case is unique.

10.8.4 Discussion of Relief Well Targets

In considering the relief well target, there are two distinct possibilities in the blowing well. The first is that the drillstring is on bottom and the other that the drill string is out of the hole, or pulled up inside the casing shoe (as in the string hung off before shearing the drillpipe). It is essential that there be metal (casing or drill string) in the blowing well for all types of proximity logs to function. If the target interception point is an open hole interval, the drill string must be across the target zone. If this is not the case, the target will be the deepest casing shoe. If the drill string is on bottom, the target can be where the blowing well penetrates the flowing reservoir. However, for planning purposes, the last casing shoe set is a target that is known to exist and therefore the most advantageous target as the primary initial target in Phase II. Should a blowout occur, the directional plan can be altered for deeper horizon targets when conditions justify such a change.

The Phase II objective will be to converge to the blowing well at the estimated location of the deepest casing shoe. The relief well must be within 50 to 60 meters of horizontal distance from the blowout wellbore, and be approximately lined up (within 7 to 10 degrees in combined inclination and azimuth) when the end of phase II is reached.

Phase II begins when calculations show that the relief well has come within 50 to 60 meters of horizontal distance to the blowing well. (Note that the proximity logs measure distance between the two wells in a plane perpendicular to the well to be ranged to, therefore high angle wells may need

adjustment of these criteria. At the depth of interest, the trajectory of the target wells in this plan is vertical (or near vertical). Thus, the horizontal distance of 50-60 meters is valid without adjustment for inclination.

The first proximity survey can be made at the 50 to 60 meter range. However, one should not expect to receive definitive information until the distance between wells is 15 to 30 meters, and the most reliable information becomes available in the 1 to 15 meter range. Course corrections should not be made unless data from the proximity logs is in the 10 to 20 meter range, and confidence in the data collected is high. Figure H.3 shows how the first proximity log run can be calculated. This is of course based on the survey accuracy of the tools used.

Phase III, drilling to interception, is the most critical stage of the relief well project. Once the blowing well trajectory is determined, a precise trajectory can be determined for an interception. Given that confidence in the ranging data is attained, Phase III can begin.

The intercept point where the relief well and the flowing well are designed to come together is most usually at the bottom of the flowing well. This is normally where the flowing zone is found, except when serious pressure reversals exist. It is also the place where the kill fluid, when placed in the flowing well, has the greatest influence due to its having an access to the entire drilled wellbore. An off-bottom kill would require a higher kill mud weight to achieve a similar hydrostatic kill pressure. The bottom kill uses the lowest possible kill mud weight.

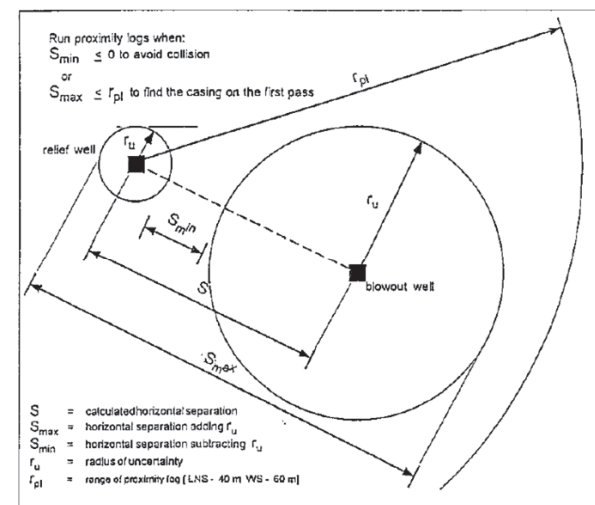


Figure H.3 Radius of Uncertainty Defined

The ellipse of uncertainty increases with depth so the more passes might be required before the flowing well can be hit with certainty, the deeper the well, the longer the drilling time. Temperature also increases with depth, so mud treatment becomes more complex. Ranging surveys and logging services also require more sophisticated methods at elevated temperatures. These effects, individually and collectively, increase operational costs. However, if the blowout well has several zones flowing, it might be necessary to consider a bottom kill and an off-bottom kill.

Once the well is intercepted, the task will be to communicate directly with the blowing well. This communication will most likely occur by a breakthrough from the relief well to the blowout well when the wellbores are within 0.2 to 1 meter apart. This will depend on the flowing bottom hole pressure of the blowing well and the formation rock mechanics. In this case, the communication link should establish itself very quickly. It should become physically quite large (5 to 20 mm) and offer little if any flow restriction.

Once communication has been established, the objective shifts to pumping a sufficient volume of kill fluid into the blowing well, at an adequate rate to overcome and kill the hydrocarbon flow from the producing interval. Once control is achieved during the initial kill operation, both wells need to remain stable until abandonment or workover operations can take place. In no case should the kill operation expose the well to additional risk of unmanageable problems brought on by a worsening control situation. Reasonable judgment and practices should be taken in pursuing the kill operation. The kill should not be irreversible, nor should it unduly eliminate reasonable kill alternatives if the initial attempts fail. An example of an irreversible operation would be attempting to kill the well with cement rather than drilling mud. The overall plan should take this philosophy into account.

There is a remote possibility that in spite of best efforts, the relief well will miss the blowing well and make a close pass, perhaps 1 to 2 meters away. If a direct communication is not possible, it may be necessary to plugback to intercept. Depending upon the distance between wellbores, an acid job may be considered to establish communication. This will work best if the relief well bore is in the pressure draw-down of the deepest producing zone. If this is the case, the acid will travel naturally through the matrix of the producing zone and into the blowing wellbore. A worm hole path will be created and the net result will be the creation of a direct communication between the two wellbores. This option should be carefully studied before implementation. Direct communication established through interception is better than relying on an acid job to create a worm hole. Fracturing the rock matrix should be avoided. Other options are perforating or milling techniques, if communication is to a cased hole.

In many old gas storage wells, the casing has become so corroded that conventional workover tools cannot enter the lower section of the hole. Techniques have been developed to mill a window from the outside of the casing from a relief well. The precision of this technique has allowed liners to be run into the lower section to tie it back to the original wellbore. If necessary, tubing-conveyed perforations can be used to make the communication. However, the authors are confident that milling can be used to cut a window in casing from the outside, if the blowout target is cased and a direct communication is needed.

10.8.5 HPHT or High Volume – Bottom Supported Operations

The following guide outlines the non-routine steps that would be considered in planning an actual high pressure high temperature (HPHT) relief well drilled in an offshore environment.

Define Objectives

The first step in this procedure is to establish the kill principle. Due to high pressures and temperatures, blowout flowrates, depths, reservoir characteristics, relief well casings and other factors the only practical method for controlling a HPHT blowout, that is not severely choked, is by direct intersection with the blowout wellbore followed by a dynamic injection of kill fluid.

Several hydraulic methods should be investigated, such as; dynamic kill with sea-water followed by mud, dynamic kill with brine followed by mud and mud as the only kill fluid. The method utilized would be dictated by the circumstances at the time of kill.

With this principle established, a primary objective will be to determine the relief well(s) placement, depth and proximity to the blowout to hydraulically regain its control. This information is required to arrive at a suitable well geometry.

Secondary objective is planning the hydraulic design. This information is necessary to design the casing program, to determine the number of required relief wells, and to specify the necessary surface and special equipment, rig requirements. Support vessels, etc.

Establish Kill Point

The kill point will usually be either at the last casing string set, along the drillstring or below the bit. The driving factors are; the bottom hole temperature at the reservoir, which will affect precision directional drilling and the kill rates required at the last casing shoe and the fracture gradients or potential weak zones affected by the kill.

Other elements to be considered are;

- Status of the blowout casing / wellhead
- Reservoir inflow performance and characteristics
- Blowout flow path and tubing performance
- Blowout fluid and kill fluid properties
- Formation drill ability
- Surface and special equipment required
- Risk analysis and probability of success.

Kill Program Design

Once the hydraulic kill principle, the kill depth, and proximity to the blowout wellbore is established, detailed planning can begin. The following steps are evaluated in this process;

Hydraulic Design

The hydraulic requirements for a kill on a HPHT well are complicated and require a two-phase time transient analysis to design the relief well casing, surface pumping plant, kill fluid volumes, final kill mud weight and pumping schedules to avoid fracturing the formation. Hydraulic planning process is an iterative process that may require several loops to arrive at an acceptable solution. The relief well kill simulations can be generated using "OLGA-Well-Kill", a dynamic-multiphase-hydraulic computer simulator, maintained by Well Flow Dynamics a/s.

Surface Kill Equipment

The kill hydraulics for a HPHT blowout, depending on the circumstances, can be immense. This will require a significant kill pumping plant, large mud storage and mud transfer capacities, and

monitoring capability. Other special equipment will be a high pressure two-four outlet kill spool with a 10,000+ rating and long steel flexhoses to connect to the subsea wellhead if a floater is being used to drill the well. If possible a large jack-up would make the best relief well and killing platform for a HPHT blowout, assuming shallow gas charging is not a problem.

Casing Design

While conventional casing design criteria are employed when designing a HPHT relief well, several additional considerations must be investigated. The first is to design the kill string diameter to assure that the control fluids can be pumped at the required rate without excessive surface pressure. The second is to allow for at least one additional, emergency casing string to assure the required kill string diameter can be set. A third is to establish strength requirements for the casing strings that might be exposed to higher than normal burst and collapse forces during kill pumping, well control or complete loss of circulation. A fourth is environmental considerations, such as hydrogen embrittlement on high strength casing and connections, casing wear, high dogleg considerations for bending stresses, thermal loading and temperature effects during kill operation (e.g. cold fluid being pumped down a hot well at high rates will cause high thermal tensile stresses).

Rig % Surface Equipment

After the kill hydraulics and relief well casing program has been established, rig and surface equipment requirement can be investigated. This is again an iterative step, requiring an analysis of equipment and available rig specifications, their ability to achieve the initial design goals and then repeating the process until a successful outcome is expected.

Surface Equipment

- High and low pressure pumps
- High and low pressure manifolds
- Mud tanks and mixing equipment
- Water, mud and diesel supplies
- Mud supply vessels and transfer equipment
- Stimulation vessels

Rig(s) Selection

- Rig specifications
- Deck layout for kill equipment
- Special kill equipment
- Kill spools
- Long co-flexip hoses
- High pressure riser, etc.

Relative position uncertainty

One of the first steps in relief well geometry planning is to estimate the relative position uncertainty for the blowout and the proposed relief well(s). This is essential for determining the initial magnetic search depth, the number of relief wells required, and the angle of approach. Both the uncertainty in the surface positions and the borehole trajectory must be analysed.

Surface Uncertainty

More than one relief well has missed its intended target do to errors in, or misunderstanding, the surface coordinates and azimuth reference system of the two wells. To avoid this costly mistake, redundant surveys should be taken between the blowout and the relief well wellheads using different measuring techniques.

The main objective is to assure that no gross errors exist in the primary positioning system. The secondary objective is to fix the relative distance and true north bearing between the two surface locations to an uncertainty of +/- 1m, with a high degree of confidence.

For relief well drilling purposes only the relative position of the two wells is important (as opposed to UTM coordinates or Latitude/Longitude). Additionally, it is important to assure that a common azimuth and depth reference system is being used. This has caused many directional drilling problems in the past, particularly when switching between grid systems and magnetic / true north reference systems. Normally three independent measurements are sufficient to assure reasonable confidence in relative positioning, one using geodetic surveying techniques and sun-shots for true north reference if possible, to eliminate any grid errors.

Borehole Uncertainty

This step is essential in determining the initial magnetic search depth, the number of relief wells to start, and the angle of approach. This can be a complicated and confusing task. Reliance on position uncertainty models without analysis of the actual data is not adequate. The following items should be investigated by a borehole surveying specialist in conjunction with the service contractor supplying the instrument;

- Type of instrument
- Geographic location, borehole attitude
- Instrument uncertainty model
- Calibration data
- Field quality control
- Field data analysis
- Survey comparisons

Number of Relief Wells

Several factors must be considered when planning the number of relief wells to start. Technical and economic considerations are influenced by the required hydraulics to regain control of the blowout, high relative position uncertainty between the wells, and a high probability of encountering time delay problems during the course of the project.

These factors may technically require more than one well, or it may be an economic risk decision. That is, will the increased cost of a second well out-weight the risk of possible long delays or the complete loss of a single relief well?

Historically, the execution of two redundant, simultaneous and independent intervention projects has normally proven sufficient. If a surface intervention is undertaken, and has a reasonable chance of success, then a single relief well may be adequate. If serious pollution or other environmental damage is being caused by the blowout, two relief wells might be considered regardless of the surface intervention plans.

Initial Casing Search Depth

The items normally evaluated in establishing this point are;

- Type of search instrument

- Blowout tubular and sidetracked fish
- Formation characteristics
- Type of drilling fluid
- Relative position uncertainty
- Formation drill ability near detection point
- Well control considerations
- Well path and dogleg considerations

Relief Well Geometry

With the kill point, casing search and cross point, and surface location fixed, detailed directional planning can commence. The following items are normally considered in the relief well geometry.

- KOP, build, drop, and turn rates
- Formation consideration
- Well control/lost circulation
- Casing detection considerations
- Survey accuracy considerations
- Torque, drag, and casing wear
- Hole sizes and casing points
- Kill point approach angle.

Documentation and Audit Trail

If the blowout intervention operation develops into a major project with many people and organizations involved, both within and outside the company, control of critical documents can be very important.

This information will be required later by the insurance companies, regulatory bodies, upper management, and auditors, etc., not to mention future value as a training tool. It is even more important during the project to assure all well data is transferred properly, important operational steps are not omitted, engineering work is checked, written communication is properly distributed, confidential material is protected, and the meeting minutes are properly documented.

Under these circumstances, it is recommended to assign someone full-time to manage this task. This should be assigned to someone, preferably an engineer, who understands what is taking place, and should not arbitrarily be assigned to a secretary.

NON-STEERABLE DRILLING TOOLS

The drilling tools required to drill the relief well may vary somewhat depending on the exact requirements and availability at the time. Listed in Tables A.1, A.2 and A.3 are general listings to be used as a guide in preparation for drilling the relief well when using non-steerable systems (which may not be available in the region).

Table A.1: 17-1/2" Phase, Non-Steerable Directional Drilling Tools

Item	Qty	Size	Description	Connections (Up x Down)
1	2	9-5/8"	Down Hole Motor	7-5/8" Reg B x 7-5/8" Reg B
2	2	9-1/2"	Short Drill Collar (0.50m)	7-5/8" Reg B x 7-5/8" Reg P
3	1	9-1/2"	Short Drill Collar (0.90m)	7-5/8" Reg B x 7-5/8" Reg P
4	1	9-1/2"	Short Drill Collar (1.50m)	7-5/8" Reg B x 7-5/8" Reg P
5	1	9-1/2"	Short Drill Collar (2.0m)	7-5/8" Reg B x 7-5/8" Reg P
6	1	9-1/2"	Short Drill Collar (4.0m)	7-5/8" Reg B x 7-5/8" Reg P
7	1	9-1/2"	Short Drill Collar (6.0m)	7-5/8" Reg B x 7-5/8" Reg P
8	2	17-1/2"	Integral Blade Near Bit Stabilizer	7-5/8" Reg B x 7-5/8" Reg P
9	3	17-1/2"	Integral Blade String Stabilizer	7-5/8" Reg B x 7-5/8" Reg P
10	2	17-1/4"	Integral Blade String Stabilizer	7-5/8" Reg B x 7-5/8" Reg P
11	1	17"	Integral Blade String Stabilizer	7-5/8" Reg B x 7-5/8" Reg P
12	1	9-1/2"	Bent Sub – 2-1/2 degree	7-5/8" Reg B x 7-5/8" Reg P
13	1	9-1/2"	Bent Sub – 2-1/4 degree	7-5/8" Reg B x 7-5/8" Reg P
14	1	9-1/2"	Bent Sub – 2 degree	7-5/8" Reg B x 7-5/8" Reg P
15	1	9-1/2"	Bent Sub – 1-3/4 degree	7-5/8" Reg B x 7-5/8" Reg P
16	2	9-1/2"	Circulating Sub	7-5/8" Reg B x 7-5/8" Reg P
17	2	9-1/2"	Float Sub	7-5/8" Reg B x 7-5/8" Reg P
18	2	9-1/2"	MWD	7-5/8" Reg B x 7-5/8" Reg P
19	2	9-1/2"	UBHO Sub	7-5/8" Reg B x 7-5/8" Reg P
20	1	17"	Melon Stabilizer	7-5/8" Reg B x 7-5/8" Reg P
21	2	9-1/2"	Mandrel String Stabilizer	7-5/8" Reg P x 7-5/8" Reg P
22	5	Assort.	Sleeves	7-5/8" Reg B x 7-5/8" Reg P

Table A.2: 12-1/4" Phase, Non-Steerable Directional Drilling Tools

Item	Qty	Size	Description	Connections (Up x Down)
1	2	9-5/8"	Down Hole Motor	7-5/8" Reg B x 7-5/8" Reg B
2	2	9-5/8"	9-5/8" XO PDM	6-5/8" Reg B x 7-5/8" Reg P
3	1	8"	Down Hole Motor	6-5/8" Reg B x 6-5/8" Reg B
4	2	8"	Short Drill Collar (0.50m)	6-5/8" Reg B x 6-5/8" Reg P
5	1	8"	Short Drill Collar (0.90m)	6-5/8" Reg B x 7-5/8" Reg P
6	1	8"	Short Drill Collar (1.50m)	6-5/8" Reg B x 6-5/8" Reg P
7	1	8"	Short Drill Collar (2.0m)	6-5/8" Reg B x 7-5/8" Reg P
8	1	8"	Short Drill Collar (4.0m)	6-5/8" Reg B x 6-5/8" Reg P
9	1	8"	Short Drill Collar (6.0m)	6-5/8" Reg B x 7-5/8" Reg P
10	2	12-1/4"	Integral Blade Near Bit Stabilizer	6-5/8" Reg B x 6-5/8" Reg B
11	4	12-1/4"	Integral Blade String Stabilizer	6-5/8" Reg B x 7-5/8" Reg P
12	2	12"	Integral Blade String Stabilizer	6-5/8" Reg B x 6-5/8" Reg P
13	1	11-3/4"	Integral Blade String Stabilizer	6-5/8" Reg B x 7-5/8" Reg P
14	1	11-7/8"	Melon Stabilizer	6-5/8" Reg B x 6-5/8" Reg P
15	1	11-3/4"	Melon Stabilizer	6-5/8" Reg B x 7-5/8" Reg P
16	1	8"	Bent Sub – 2-1/2 degree	6-5/8" Reg B x 6-5/8" Reg P
17	1	8"	Bent Sub – 2 degree	6-5/8" Reg B x 7-5/8" Reg P
18	1	8"	Bent Sub – 1-3/4 degree	6-5/8" Reg B x 6-5/8" Reg P
19	1	8"	Bent Sub – 1-1/2 degree	6-5/8" Reg B x 7-5/8" Reg P
20	1	8"	Bent Sub – 1-1/4 degree	6-5/8" Reg B x 6-5/8" Reg P
21	2	8"	Circulating Sub	6-5/8" Reg B x 7-5/8" Reg P
22	2	8"	Float Sub	6-5/8" Reg B x 6-5/8" Reg P
23	2	8-1/8"	MWD	6-5/8" Reg B x 7-5/8" Reg P
24	2	8"	UBHO Sub	6-5/8" Reg B x 6-5/8" Reg P

Table A.3 : 8-1/2" Phase, Non-Steerable Directional Drilling Tools

Item	Qty	Size	Description	Connections (Up x Down)
1	2	6-1/2"	Down Hole Motor	4" IF B x 4" IF P
2	2	6-1/2"	Short Drill Collar (0.50m)	4" IF B x 4" IF P
3	1	6-1/2"	Short Drill Collar (0.90m)	4" IF B x 4" IF P
4	1	6-1/2"	Short Drill Collar (1.50m)	4" IF B x 4" IF P
5	1	6-1/2"	Short Drill Collar (2.0m)	4" IF B x 4" IF P
6	1	6-1/2"	Short Drill Collar (4.0m)	4" IF B x 4" IF P
7	1	6-1/2"	Short Drill Collar (6.0m)	4" IF B x 4" IF P
8	2	8-1/2"	Integral Blade Near Bit Stabilizer	4" IF B x 4-1/2" Reg B
9	4	8-1/2"	Integral Blade String Stabilizer	4" IF B x 4" IF P
10	1	8-1/4"	Integral Blade String Stabilizer	4" IF B x 4" IF P
11	1	8"	Integral Blade String Stabilizer	4" IF B x 4" IF P
12	1	6-1/2"	Bent Sub – 2-1/2 degree	4" IF B x 4" IF P
13	1	6-1/2"	Bent Sub – 2 degree	4" IF B x 4" IF P

14	1	6-1/2"	Bent Sub – 1-3/4 degree	4" IF B x 4" IF P
15	1	6-1/2"	Bent Sub – 1-1/2 degree	4" IF B x 4" IF P
16	2	6-1/2"	Circulating Sub	4" IF B x 4" IF P
17	2	6-1/2"	Float Sub	4" IF B x 4" IF P
18	2	6-1/2"	MWD	4" IF B x 4" IF P
19	2	6-1/2"	UBHO Sub	4" IF B x 4" IF P
20	1		Portable Computer	4" IF B x 4" IF P

10.8.6 Steerable Drilling Tools

The drilling tools required to drill the relief well may vary somewhat depending on the exact requirements and availability at the time. List in Tables A.4, A.5 and A.6 are general listings to be used as a guide in preparation for drilling the relief well when using steerable systems (which may not be available in the region).

Table A.4 : 17-1/2" Phase, Steerable System Tools, 5° – 6° /100'

Item	Qty	Size	Description	Connections (Up x Down)
1	2	9-5/8"	Steerable Motor, 0-3° Adjustable	7-5/8" Reg B x 7-5/8" Reg B
2	2	9-1/2"	Non-magnetic Drill Collars (10.0m)	7-5/8" Reg B x 7-5/8" Reg P
3	3	9-1/2"	Drill Collars (10.0m)	7-5/8" Reg B x 7-5/8" Reg P
4	2	9-1/2"	Short Non-magnetic Drill Collars (3.0m)	7-5/8" Reg B x 7-5/8" Reg P
5	2	17-1/2"	Integral Blade Near Bit Stabilizer	7-5/8" Reg B x 7-5/8" Reg B
6	4	17-1/4"	Integral Blade String Stabilizer	7-5/8" Reg B x 7-5/8" Reg P
7	1	17-1/4"	Integral Blade String Stabilizer	7-5/8" Reg B x 7-5/8" Reg P
8	1	17"	Monel Integral Blade String Stabilizer	7-5/8" Reg B x 7-5/8" Reg P
9	2	9-1/2"	Circulating Sub	7-5/8" Reg B x 7-5/8" Reg P
10	2	9-1/2"	Float Sub	7-5/8" Reg B x 7-5/8" Reg P
11	2	9-1/2"	MWD	7-5/8" Reg B x 7-5/8" Reg P
12	2	9-1/2"	UBHO Sub	7-5/8" Reg B x 7-5/8" Reg P
13	1	17"	Melon Stabilizer	7-5/8" Reg B x 7-5/8" Reg P
14	2	9-1/2"	Mandrel String Stabilizer	7-5/8" Reg P x 7-5/8" Reg P
15	5	Assort.	Sleeves	7-5/8" Reg B x 7-5/8" Reg P

Table A.5 : 12-1/4" Phase, Steerable System Tools, 11° – 12° /100'

Item	Qty	Size	Description	Connections (Up x Down)
1	2	9-5/8"	Steerable Motor, 0-3° Adjustable	7-5/8" Reg B x 7-5/8" Reg B
2	2	9-5/8"	9-5/8" XO PDM	6-5/8" Reg B x 7-5/8" Reg P
3	1	8"	Steerable Motor, 0-3° Adjustable	6-5/8" Reg B x 6-5/8" Reg B
4	2	8"	Non-magnetic Drill Collars (10.0m)	6-5/8" Reg B x 6-5/8" Reg P
5	2	8"	Non-magnetic Drill Collars (3.0m)	6-5/8" Reg B x 7-5/8" Reg P
6	3	8"	Drill Collars (10.0m)	6-5/8" Reg B x 6-5/8" Reg P
7	1	8"	Short Non-magnetic Drill Collars (3.0m)	6-5/8" Reg B x 7-5/8" Reg P
8	2	12-1/4"	Integral Blade Near Bit Stabilizer	6-5/8" Reg B x 6-5/8" Reg P
9	4	12-1/4"	Integral Blade String Stabilizer	6-5/8" Reg B x 7-5/8" Reg P
10	2	12"	Integral Blade String Stabilizer	6-5/8" Reg B x 6-5/8" Reg B
11	1	11-3/4"	Monel Integral Blade String Stabilizer	6-5/8" Reg B x 7-5/8" Reg P
12	1	11-7/8"	Melon Stabilizer	6-5/8" Reg B x 6-5/8" Reg P
13	1	11-3/4"	Melon Stabilizer	6-5/8" Reg B x 7-5/8" Reg P
14	2	8"	Circulating Sub	6-5/8" Reg B x 6-5/8" Reg P
15	2	8"	Float Sub	6-5/8" Reg B x 7-5/8" Reg P
16	2	8-1/8"	MWD	6-5/8" Reg B x 6-5/8" Reg P
17	2	8"	UBHO Sub	6-5/8" Reg B x 7-5/8" Reg P

Table A.6 : 8-1/2" Phase, Steerable System Tools

Item	Qty	Size	Description	Connections (Up x Down)
1	2	6-1/2"	Steerable Motor, 0-3° Adjustable	4" IF B x 4" IF B
2	2	6-1/2"	Non-magnetic Drill Collars (10.0m)	4" IF B x 4" IF P
3	3	6-1/2"	Drill Collars (10.0m)	4" IF B x 4" IF P
4	2	6-1/2"	Drill Collars (3.0m)	4" IF B x 4" IF P
5	1	6-1/2"	Short Non-magnetic Drill Collars (3.0m)	4" IF B x 4" IF P
6	2	8-1/2"	Integral Blade Near Bit Stabilizer	4" IF B x 4-1/2" Reg B
7	4	8-1/2"	Integral Blade String Stabilizer	4" IF B x 4" IF P
8	1	8"	Monel Integral Blade String Stabilizer	4" IF B x 4" IF P
9	2	6-1/2"	Circulating Sub	4" IF B x 4" IF P
10	3	6-1/2"	Float Sub	4" IF B x 4" IF P
11	2	6-1/2"	MWD	4" IF B x 4" IF P
12	2	6-1/2"	UBHO Sub	4" IF B x 4" IF P
13	1		Portable Computer	

10.8.7 Pumping Speeds

The worst horsepower case must be determined from the runs made with the dynamic two-phase flow simulator for a surface blowout flow, assuming that the design rate is 57.3 barrels per minute at 740 psi surface pumping pressure. The piping and discharge pressure specification for kill equipment shall be 5,000 psi. The 5000 psi rating is chosen because this is the minimum rating to be considered for any relief well pump job and secondly it is minimum rating commonly available

from pumping vendors. Horsepower is determined by rating of units rather than equating horsepower alone. The recommended method is per Equation A.1 shown below. Example A.1 shows that a minimum safety factor or 1.5 for pumping is recommended. Therefore, if a discharge of 750 psi is anticipated the required horsepower would be 8 units or 612 HP each for a total of 4896 HP (612 HP is the 100% rating for an HT-400 used in the example). If one were to use a simplified approach where HP is merely pump discharge pressure time rate the calculations would yield only a minimum of 1040 horsepower without SF and 1560 HP with a 1.5 SF. There is significant difference in these calculations, because pure horsepower calculation does not take into account the pump limitations (liner rating, strokes per minute limits, etc.). Some cases may require more pump rate, but these are usually accompanied with low flowing bottom hole pressures. This condition required less hydraulic horsepower. For safety and reliability, it is recommended that external stand-alone, independent drive pumps (DS Schlumberger, Halliburton, etc.) be provided in all cases. For purposes of discussion in this report Halliburton pump specifications have been used (not as a recommended vendor for these services although they are very capable, but because the author is more familiar with their equipment). If competing vendors are chosen, their equipment will be comparable and little modification except review of pressure-volume characteristics will be required. Figure H.4. shows this pumping spread for 8 each 600+ HP pumps.

The methods for specifying the hydraulic horsepower and numbers of units required to achieve the required injection pressure use the predicted pressure and pumping volumes from a two-phase flow model (for example DYN-X). Rather than applying a multitude of safety factors to each individual input value that affects the pumping requirements, the maximum theoretical values are used. Allowances are made for leakoff of fluid to the open hole (for example 10%) and calculations should be made to determine the numbers of units required for a given scenario. All these calculations should be done without applying safety factors and then an overall safety factor applied. The basis for calculating the required pumps follow;

Equation A.1

$$N_p = \frac{Q_k}{(1 - LO)} \frac{SF}{Q_u}$$

Where:

N_p =number of pump units (round to integer)

Q_k =design kill rate, [bpm]

SF=safety factory [*]

Q_u =max. Flow per unit, [bpm per unit] from manufacturer's data for 100% performance at anticipated discharge pressure (see Fig. H.5)

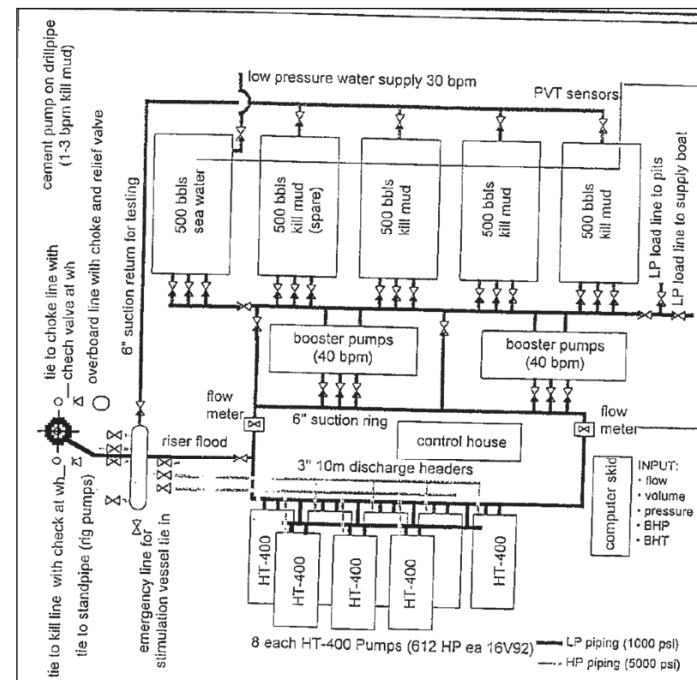


Figure H.4 Example Relief Well Pump Spread (Offshore)

Example

For Exploration type wells analysed using a two-phase dynamic kill model, 57.3 BPM kill rate was determined (maximum for 12-1/4" drilling phase). The maximum discharge from the pressure loss model is 740 psi (rounded to nearest 10 psi). From Figure H.5 the PVC discharge yields maximum available rate per unit, Q_u , of 12.5 barrels per minute per unit if maximum horse power is expended. Assuming 10% leakoff to the formation during the kill operation, LO becomes 0.10 given that the overall safety factor, SF, is 1.50. For this scenario, the required number of pumps will be;

$$N_p = 57.3 / (1 - 0.2) \times 1.5 / 12.5$$

$$N_p = 7.64 \text{ say } 8 \text{ units rounded to the nearest integer}$$

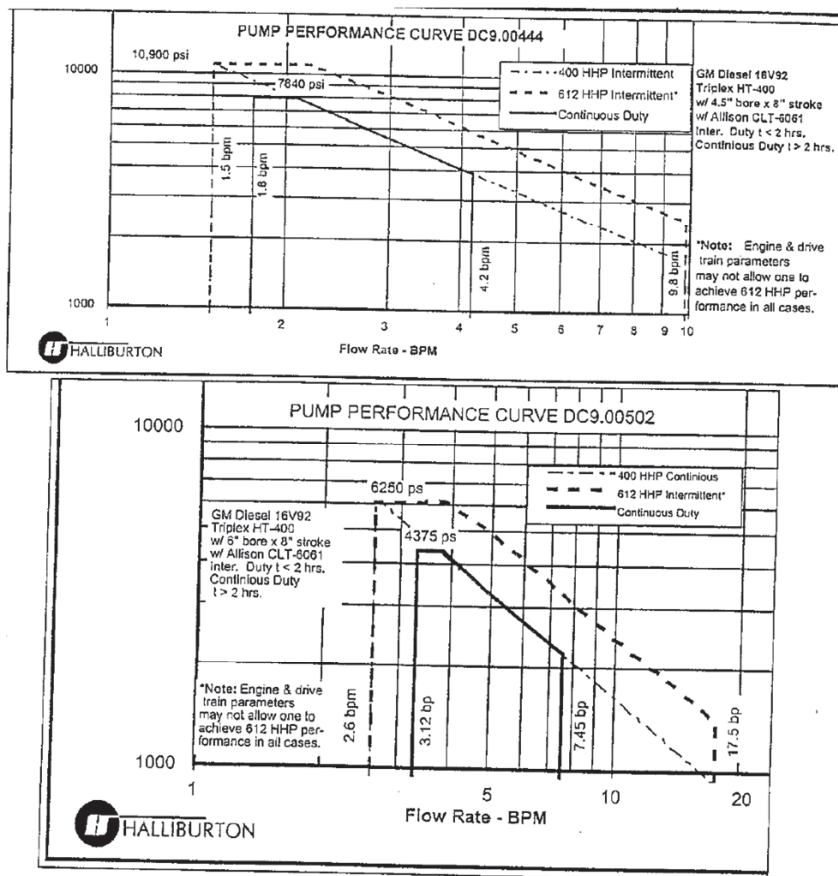


Figure H.5 Pressure Volume Curve
(Courtesy of Halliburton Energy Services, Duncan, OK)

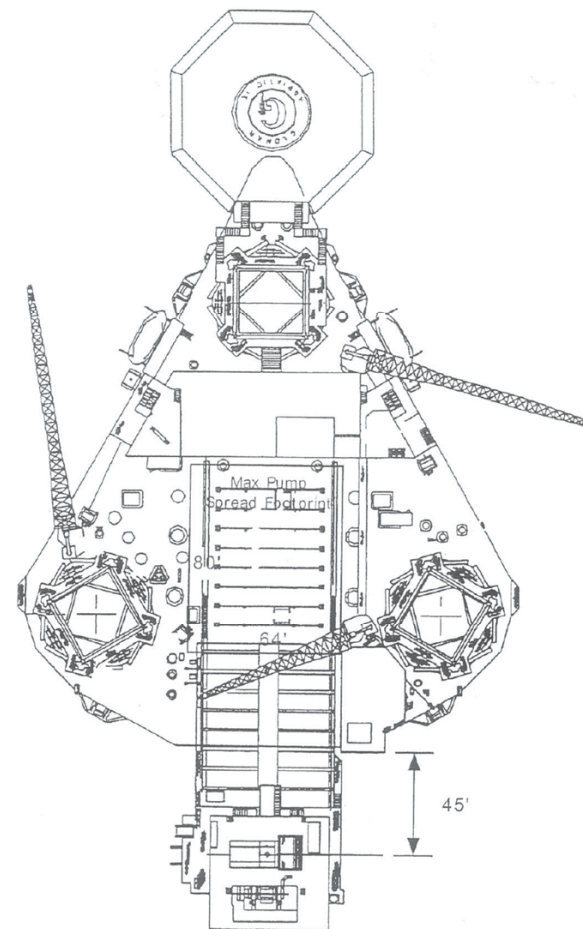


Figure H.6

10.8.8 CONCLUSION

The conclusion to be drawn is that the relief well can in fact be drilled to an interception of the blowout well with great confidence. Further, the directional and proximity drilling technology has advanced so that a wellbore interception is now the rule instead of the exception. While a relief well is necessary to control only a minor portion of blowout wells, it is a viable option in those situations where surface intervention is not a workable alternative.

10.9 RELIEF WELL STRATEGY

This discussion provides site specific details necessary for drilling a relief well in the Gulf of Thailand. It assumes the blowout is from a well that has penetrated the main producing interval of a development, delineation or exploration well. This section contains site specific relief well details while Appendix D contains the generic guidelines. (Note: Appendix D can be found in Volume II). Relief wells are not usually considered for the solution of shallow gas blowouts therefore this is not addressed in this plan.

10.9.1 Relief Well Target

The relief well will be aimed for an intercept of the blowout well as near to the source of the blowout as possible. For planning purposes in this report the target used to design trajectories is the top perforation in development wells and the top of the producing interval in drilling wells.

If the drill string is not in the hole or across the primary interval, an upper target must be selected based on the location of pipe or casing in the well. The worst case would be an interception target in the open hole that is void of pipe (casing or drill pipe). This would require the relief well to be aimed at the last casing shoe set, the 13-3/8" or 9-5/8" casing shoes for the 12-1/4" or 8-1/2" phases.

For this report the coordinate system at the surface is referenced to the surface location of the target well and UTM coordinates.

10.9.2 Positioning the Relief Well

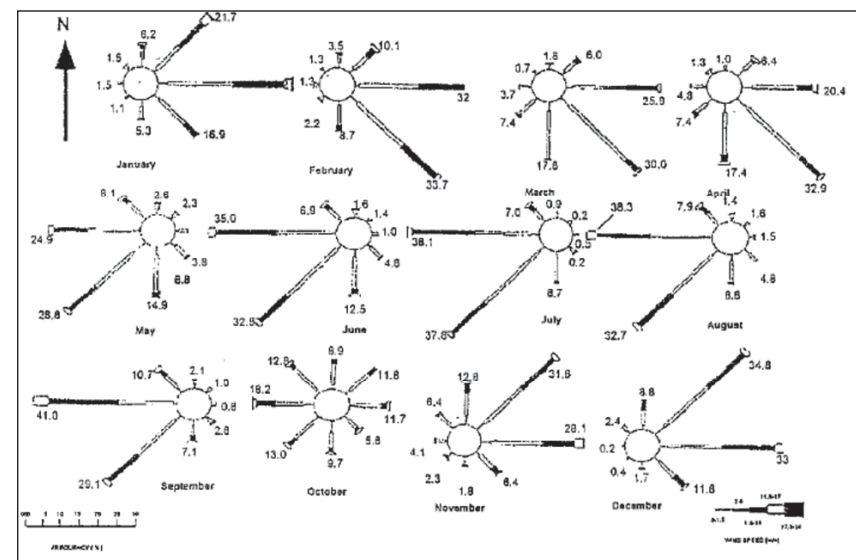
Positioning the relief well involves a number of objective and subjective considerations. Listed below are the factors taken into account for safe positioning of a relief well:

- Maintain at least a 300 m clearance from the blowout well surface location if the relief well is located in the SE quadrant (see figure 1.3).
- Maintain a 600 m clearance from the blowout well surface location if the relief well is located in any quadrant other than the SE.
- Avoid the current gas dispersion streams by positioning the relief well where the Lower Explosive Limits 'LEL' of 5% by volume are within acceptable limits at every possible wind condition.
- Avoid seafloor obstructions in area; anchor pattern to leave 50 m of clearance from any obstruction (pipelines, flowlines, umbilicals, etc.).
- Avoid shallow gas zones that can be drilling hazards per the discussion of Section C.4 also see hazard map and relief well position for Bongkot platforms according to shallow gas hazard in Section 8).
- A position that accounts for favorable winds so that the relief well is upwind most of time. The major factors are the time of year and the time that will be required to drill the well Note: This will have to be determined on the fly and is not specifically addressed in this report.

The SE quadrant shown in Figure 1.3 is the preferred all weather relief well position relative to the blowout. This is chosen as the position that is most likely to be upwind the majority of the time. The exception is the month of October when the winds are light and variable. Gas dispersion modelling has been done which indicates that the 300 meter distance is acceptable for the October wind conditions. IF necessary the relief well can be positioned downwind, but distance from the blowout must be increased to 600 m. The basis for this is taken from gas dispersion modelling where the blowout rates were used to determine LEL for the worst case wind conditions (slight

breeze and a subtropical inversion reducing natural mixing of the air). More detail of the gas dispersion analysis can be found in Section G.5. Figures I.1 and I.2 show the wind roses used to make this determination and the result of the gas dispersion analysis.

If may be possible to position a well inside the exclusion zone, but this will need to be based on actual conditions (e.g. air quality monitoring). Choosing a location not meeting the above conditions can only be done if conditions at the blowout location do not jeopardize the drilling crew or equipment safety. If the risk is excessive, then the alternative profiles (Double-S to vertical shapes) should be chosen for the relief wells.



(Figure Wind Rose Data (1987-1992))

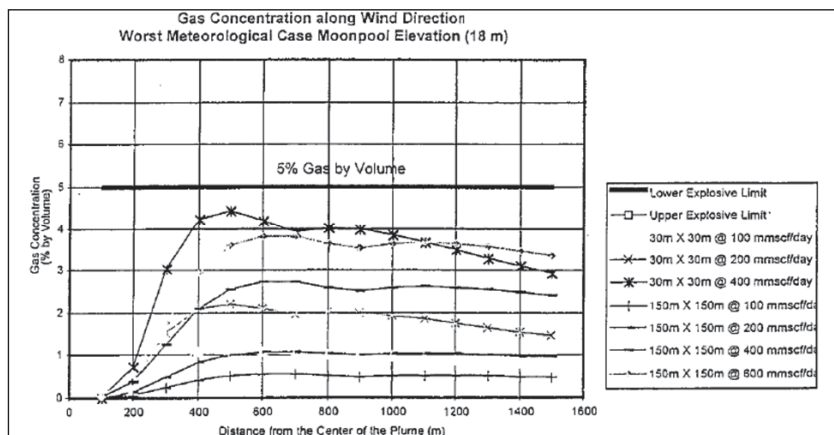


Figure 2 Gas Dispersion Analysis Summary

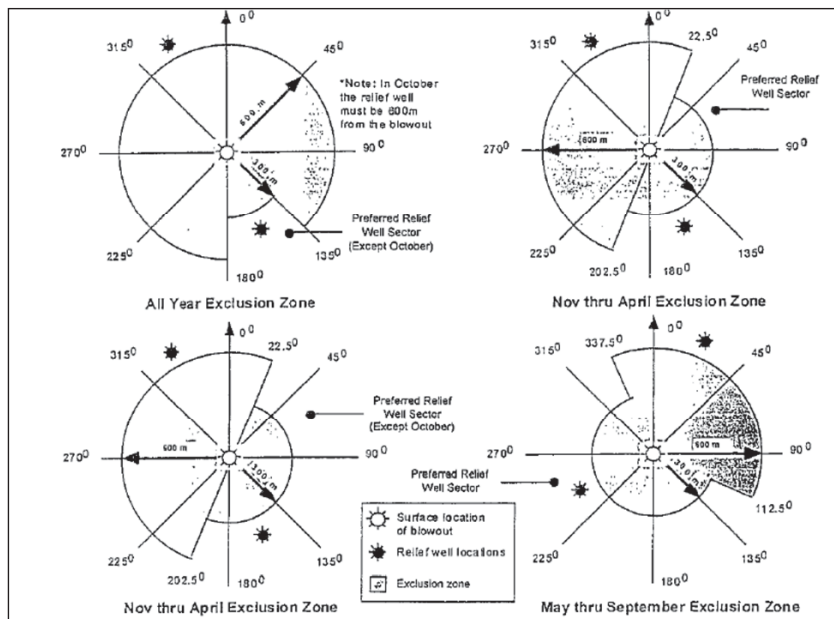


Figure 1.3 Exclusion Zone for Relief Well Placement

10.9.3 Relief Well Trajectory

The relief wells are designed to have the relief well lined up at least 100 m before reaching the target and to have no more than 10 degrees of combined azimuth and inclination difference from the blowing well at the intercept point. The relief wells should come within the effective range of the proximity tools (25 to 50 m displacement) at the first detection point and approximately 150 m before drilling to the target (e.g. reservoir penetration or last casing shoe). When within this range, the proximity tools will be run to locate the target and direct the relief well to this revised target. The azimuth direction will be approximately the same as the blowing well. A slight lead to the left is preferred in order to allow the well to turn to the right and drop angle as the final corrections are made to the target (about 5 to 10 degrees will be adequate to meet this criteria). For purposes of design and to account for some right-hand walk a 6 degree lead angle has been chosen for planning purposes.

The simplest and shortest drilling distance for the relief well was chosen whenever possible. This is a simple build and hold (J-curve) trajectory. For a J-curve, the surface location is placed for the minimum required displacement, therefore minimum lineal drilling distance. This is the chosen relief well plan for the intercept. The first detection target is the blowout well at a point approximately at the reservoir penetration.

The logic for presenting these minimum displacement locations is to have the option to minimize the relief well drilling effort should a blowout occurs during a period of the year when historic wind conditions are favorable. Also, if the well is blowing out underground and no slick was anticipated or being generated the distance to blowout surface location may not be factor.

J-curve (build and hold) and S-curve

Relief well trajectories designed for this project were put into three (3) categories and are summarized below:

- Relief Well A – J curve build and hold positioned at least 600 m from the blowout platform location.
- Relief Well B-S-curve to vertical positioned 300 or 600 m from the blowout bottom hole location. These would be the relief wells needed for a vertical well blowing out on a platform or a floating rig. Two cases are considered for a development well and an exploration well.
- Relief Well C-A vertical well positioned at least 600 m from the blowout platform location. This would cover the relief well needs of wells BK-4-D, F, G and L along with BK-6-A and D. These wells are S-curve wells with the bottom hole portion of the well at least 600 m from the platform. The wells are assumed to be close to vertical at the top of reservoir, which would allow a vertical relief well to be drilled.

Table I.1 gives the surveying data and ties for the relief wells mentioned above.

Well	Top Perf m TVD	Top Perf UTM N	Location UTM E	Angle deg	Azimuth deg	Displ to plat	Direction from plat	Relief Plan	Well Displ	RW UTM N	Sur Loc UTM E	RW Displ to Plat	No te
BK-1-B	1308	889,175	865,859	38.76	323.95	267	358.13	37	176	889,279	865,803	479	
BK-1-C	1415	889,592	865,041	49.55	355.57	851	22.53	5E	248	889,511	865,050	876	
BK-1-E	2040	888,632	865,516	32.25	58.52	250	231.34	30	127	888,544	865,408	402	
BK-1-D	1493	888,516	865,783	25.41	109.04	1111	105.14	25	95	888,427	865,692	1053	
BK-1-F	1502	888,862	865,574	31.65	294.24	147	291.51	30	127	888,978	865,690	171	
BK-1-G	1423	887,985	865,700	45.82	184.21	823	180.77	6E	248	888,003	865,718	805	
BK-1-H	1458	888,953	865,871	43.65	82.59	1169	82.87	6E	248	888,707	865,825	920	
BK-1-K	1769	888,109	865,237	5.82	98.35	845	214.14	Vert	0	888,109	865,237	845	
BK-1-L	1369	888,356	866,123	18.52	89.98	512	137.71	13	37	888,318	866,086	517	
BK-1-M	953	887,814	866,023	58.88	164.00	1042	152.57	5C	494	887,678	865,887	1144	
BK-2-A	1531	885,137	868,324	55.70	304.10	1241	340.71	6B	332	885,412	868,599	1453	
BK-2-B	1532	884,091	867,821	52.74	271.73	921	277.82	6B	332	884,423	868,153	738	
BK-2-C	1418	883,900	869,352	35.53	195.00	822	95.07	30	127	883,935	869,387	554	
BK-2-D	1454	883,989	869,604	52.14	86.99	870	88.47	5E	248	883,741	869,356	652	
BK-2-E	1290	883,428	868,208	40.13	224.39	752	224.36	37	176	883,551	868,331	578	
BK-2-F	1318	883,255	868,175	43.45	206.92	902	217.58	37	176	883,335	868,259	790	
BK-2-G	1515	882,782	869,324	54.54	177.02	1323	153.50	6B	332	882,768	869,307	1331	
BK-2-H	1279	883,285	869,381	53.68	139.26	935	135.45	6B	332	883,058	869,154	995	
BK-2-K	1519	883,184	869,040	39.15	157.04	839	158.52	37	176	883,115	868,971	883	
BK-2-J	1478	884,028	866,508	49.88	269.65	2227	271.55	6E	248	884,274	866,756	2002	
BK-2-L	1343	884,127	867,417	58.20	277.28	1327	275.96	6B	332	884,456	867,746	1103	
BK-2-M	1365	882,951	867,319	51.82	236.15	1741	234.35	6E	248	883,157	867,525	1455	
BK-3-A	1515	887,976	867,055	57.15	288.29	1277	266.08	6B	332	888,291	867,390	965	
BK-3-B	1529	888,334	867,528	39.01	281.51	854	288.43	37	176	888,506	867,700	777	
BK-3-C	1549	888,941	868,837	37.21	48.51	763	40.81	37	176	886,509	868,705	577	
BK-3-D	1551	888,877	869,585	58.73	55.83	1498	55.88	6B	332	888,569	869,307	1107	
BK-3-E	1490	887,511	867,228	49.73	258.13	1241	243.54	6E	248	887,754	867,471	922	
BK-3-F	1446	887,757	867,819	24.92	241.79	804	239.49	25	95	887,842	867,903	489	
BK-3-G	1453	887,919	868,092	13.72	328.39	285	238.58	13	37	887,938	868,111	360	
BK-3-K	1436	887,192	867,501	58.74	264.50	975	265.85	6B	332	887,330	868,039	793	
BK-4-D	1542	895,099	863,153	48.54	52.39	951	52.00	6E	248	894,903	862,557	566	
BK-4-H	1459	894,465	863,041	38.99	90.38	647	93.76	37	176	894,239	862,865	518	
BK-4-G	958	894,399	862,615	45.75	123.88	265	124.11	6E	248	894,153	862,409	355	
BK-4-F	1407	895,026	861,767	18.27	309.53	815	309.51	13	37	895,054	861,795	812	
BK-4-K	1581	893,714	861,535	46.69	194.99	1171	227.33	6E	248	893,778	861,589	1080	
BK-4-L	934	894,178	862,595	60.38	147.17	387	148.87	6B	332	893,996	862,416	512	

Well	Top Perf m TVD	Top Perf UTM N	Location UTM E	Angle deg	Azimuth deg	Displ to plat	Direction from plat	Relief Plan	Well Displ	RW UTM N	Sur Loc UTM E	RW Displ to Plat	No te
BK-5-B	2041	888,437	861,957	60.2	341.81	2,275	345.9	50	519	887,960	862,151	6552	
BK-5-C	1534	887,141	864,894	83.1	57.60	2,404	87.5	63	560	886,884	864,198	7834	
BK-5-D	2120	885,385	864,325	54.97	112.73	2,031	114.3	6E	448	885,249	863,999	9379	
BK-5-E	1329	886,761	862,184	40.34	5.02	612	28.2	40	269	886,492	862,179	5019	
BK-5-F	1584.7	884,993	862,426	50.34	159.23	1,229	2.2	5E	394	884,638	862,255	9970	
BK-5-G	1518.9	886,159	862,559	31.95	125.87	108	61.5	32	183	886,075	862,412	8432	
BK-5-H	940	888,055	862,982	80.92	104.85	535	108.1	5B	529	885,955	862,461	8543	
BK-5-J	1320	886,198	862,311	38.89	51.72	164	8.0	38	253	886,140	862,065	8374	
BK-5-K	2032	885,039	862,790	47.97	164.29	1,224	166.0	6E	358	884,704	862,563	9907	
BK-5-L	1624	883,710	862,406	60.79	178.00	2,512	178.5	6B	527	883,187	862,342	11320	
BK-5-M	2229	884,755	864,048	37.27	125.44	2,144	132.8	37	236	884,645	863,844	9968	
BK-6-A	1591	878,428	870,511	52.64	232.29	1097	233.15	6E	248	879,624	870,707	1423	
BK-6-B	1432	880,703	870,864	55.07	283.48	1037	284.37	6B	332	881,026	871,187	895	
BK-6-C	1214	881,825	871,141	58.33	328.46	1560	332.19	6C	494	882,083	871,399	1704	
BK-6-D	1375	881,102	872,217	30.47	30.50	743	27.56	30	127	881,038	872,153	657	
BK-6-E	1395	879,605	871,306	42.98	214.05	795	216.46	6E	248	879,945	871,535	802	
BK-6-F	1568	880,465	871,475	38.97	273.11	364	272.97	37	176	880,642	871,651	293	
BK-6-G	1353	880,290	872,438	47.95	106.20	560	105.28	6E	248	880,052	872,200	515	
BK-6-H	1458	880,282	871,771	33.65	223.79	191	210.82	30	127	880,370	871,859	78	
BK-6-J	1835	881,285	870,828	44.94	237.20	1337	308.89	6E	248	881,522	871,065	1343	
BK-6-M	971	879,571	872,089	48.18	154.04	523	155.09	6E	248	879,852	871,983	594	
BK-7-B	1857.4	885,264	874,780	60	323.77	2,306	301.54	60	516	887,075	875,121	1819	
BK-7-E	2331.3	887,218	874,516	44.91	271.82	1,751	327.71	6E	321	887,538	874,499	1955	
BK-7-F	2036.6	885,292	875,355	39.91	269.61	542	399.12	6E	264	886,055	875,330	721	
BK-7-G	1511.5	885,240	875,946	12	227.20	66	230.50	vert	40	885,266	875,916	300	
BK-7-H	1650	885,199	876,120	39.73	123.90	149	124.07	6E	262	885,369	875,994	313	
BK-7-L	1581.2	884,720	876,079	60.21	213.38	1,554	183.00	6B	519	884,967	875,622	1367	
BK-6	Later												
BK-9	Later												
BK-10	Later												
Platform	Location	North	East							North	East		
WP1		888,808.00	865,711.00							WP6	880,445.60	871,858.60	
WP2		883,965.70	868,733.90							WP7	886,282	875,997	
WP3		888,063.80	868,338.60							WP8	888,931	873,025	
WP4		894,507.43	862,395.85							WP9			
WP5		888,221	862,473.7							WP10			

Note: Special consideration may be required for these locations due to the time of year and the wind patterns at that time of year.

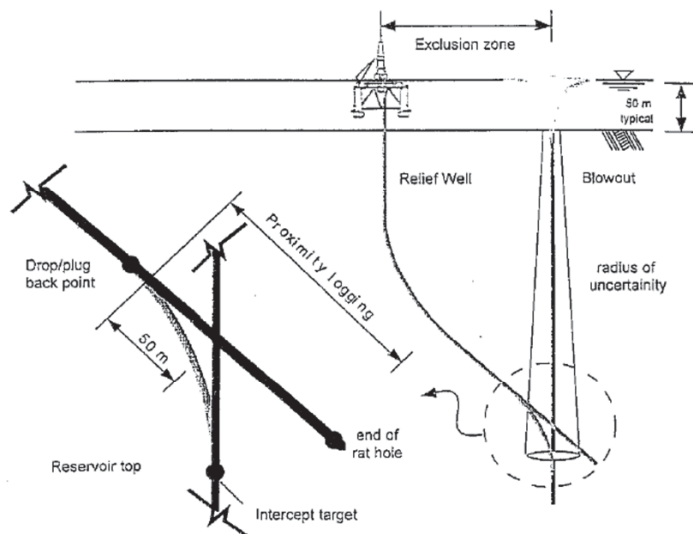


Figure I.4 Type A Relief Wells

10.9.4 Shallow Gas Discussion

As of April 97 the hazard maps for shallow gas for the Bongkot Field and surrounding area is not complete. The mapping done to date has been for the platform areas only. Therefore the choice of locations for the relief wells has ignored the fact that there may be a shallow gas hazard at the optimum location. The optimum location is that position that will yield the minimum lineal footage to reach the target. For example, for high angle wells the relief well location was moved out to a position near the reservoir target. It may well be that these locations are over shallow gas drilling hazards, therefore an investigation must be undertaken before a rig, especially a jack up is moved to drill a relief well. The options for addressing these problems are summarized below:

- If a semi rig is available (either on the market or under contract to PTTEP for exploration during the 1998 exploration campaign), a pilot hole could be drilled riserless to test for the presence of shallow gas.
- Seismic interpretations can be performed for each relief well location (from available data 3-D seismic survey data). This can be done now for all locations chosen for relief wells (perhaps cost prohibitive) or done on a crash program while the rig is being prepared to move onto the relief well location. If the interpretations show a hazard then it can be tested with a pilot hole or an alternative location chosen. Waiting is not seen to have an impact on the timeline to drill the relief well as one can be doing the interpretation while the rig is under tow and other equipment made ready to spud the well. However the window for moving on to the relief well after being given the approval to proceed is approximately 6 days (given there is a rig in the area that can be moved to the Bangkok area). If the interpretation takes more than 6 days it will impact the relief well drilling spud date.

These operational parameters will have to be reviewed if relief well projects become a reality to choose the most expeditious means to drill the relief well given the potential for shallow gas hazard.

10.9.5 Casing Design and Seat Selection

The relief well casing design is the same for a development or exploration type well. This will meet the pumping requirements for the dynamic kill. Additional factors have been considered and evaluated in addressing the relief well design and they are the;

- Effects of well casing configuration on the friction and flow rates required during the kill operation.
- Implications of setting an additional casing string to combat downhole problems encountered during drilling, i.e. can the objective still be attained if a further reduction in hole size is required or addition strings set?
- Realistic possibilities of individual zones being artificially pressured or depleted and is there information to support this position.

In addition to the above, certain questions should be reviewed prior to spudding the relief well to take advantage of the most current information, and these are;

- Has the target location changed significantly since the relief well plan was developed?
- Were there complications encountered in the original blowing well during the up hole sections which could threaten the success of the relief well? How will these be averted?
- Will the casing scheduled have to be modified to meet the directional drilling objectives required to intercept the blowing well?
- Was there an unanticipated presence of a corrosive or toxic fluid such as H₂S that requires special consideration?

Casing Program

The casing program for a development or exploration relief well has taken the above list of considerations into account. The result was basically the same casing program used in the well with one exception; a larger surface casing was used to provide for any contingencies requiring that an additional casing string be run due to hole problems or mechanical difficulties. This is not to say that extenuating circumstances such as an underground flow may require re-evaluation. If unanticipated pressuring of a shallow interval occurs, additional casing may be required. For the purposes of this report, subsurface charging has not been considered because it is believed that the relief well can be spudded and drilled to objective TVD before time dependent charging can become a factor in the shallow horizons. Also, the likelihood of shallow charging is dependent upon having a shallow casing leak, which is a low probability scenario, but should be considered if a relief well becomes a reality.

CAUTION Charging of subsurface zones must be reviewed prior to spudding the relief well to make assurance that it does not represent a drilling hazard.

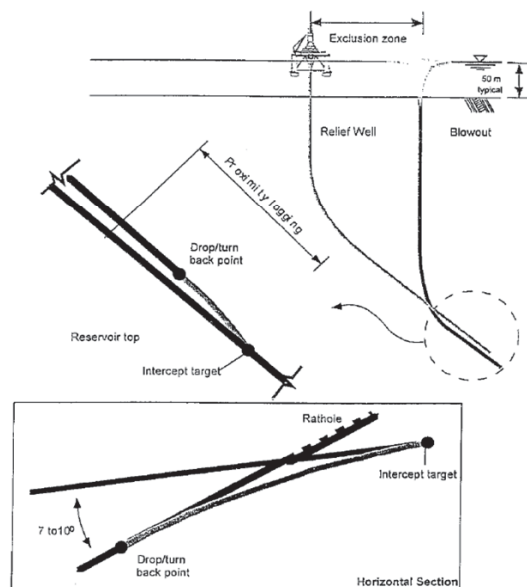


Figure I.5 Relief Wells for Inclined Targets

A 7" liner would not be required under most circumstances unless hole conditions require its use. The author saw no reason to program the 7" liner and 6" open hole to target PTTEP depth, but leaves this as a contingency should it be needed to accomplish the interception. This option would have to be thoroughly evaluated because with its use would come a host of additional problems and limitations. With the 7" liner in place it will be difficult or impossible to plugback the relief well to make directional corrections. Thus the 7" liner will induce additional risks to the relief well should interception or pumping to kill fail in the initial attempts. Table 5.2 shows the recommended casing program for all relief wells.

CAUTION Setting a 7" liner must be done only as a last resort and then only after very careful review. Note that this will certainly limit any future directional correction and severely restrict the flow during the kill operation.

Table I.2 : Relief Well Casing Program

Casing Size	Casing point objective	Casing description	Drift ID. (inches)	Internal Yield
30"	Approx. 60 m. below sea floor	1.5"Wall LYNX-HD		
13-3/8"	Approx. 450 m.	68 ppf N80 Buttress	12.26	5018 psi
9-5/8"	Approx. 1060 m TVD	53.5 ppf 95 grade New Vam	8.525	9410 psi
7" Liner*	To be set only if hole conditions dictate to reach objective	32 ppf 95 grade 0 VAM	5.969	10760 psi

*Note: Only if required by hole conditions.

Well Control Considerations

The blowing well may introduce new pressure environments in the formations through which the relief well must drill. This may be characterized by over pressured or depleted zones.

When considering a surface blowout after the 9-5/8" casing has been set above the reservoir, it is assumed that the integrity of the 9-5/8" casing and casing shoe are maintained and no underground flow has or can occur. Under this scenario, no unusual or abnormal pressures should be encountered above the 9-5/8" casing setting depth in the blowing well. It is believed that drilling of the relief well should proceed according to the program to the 9-5/8" casing point (approximately 1060 m TVD) without major concern.

Before reaching the 9-5/8" shoe all the BOP equipment should be completely tested to the maximum rated pressure and the entire compliment of fully tested kill equipment and kill weight mud should be on hand. From that point forward, precaution must be exercised to control any possible influx. The increased trips necessitated by the directional work will require close control of tripping practices.

Should hole conditions in the relief well deteriorate to the point that progress cannot be made without casing the open hole section, a 7" liner may be set to provide the necessary protection. This should be avoided if possible because it:

- Limits the options for directional correction
- Restricts the use of some directional equipment
- Increases the duration of drilling activity and
- Adds additional friction restrictions for the kill operation.

Should the 7" liner be required, a packoff liner hanger should be installed, and the liner lap dry tested and pressure tested before drilling new open hole.

Subsurface Charging

An underground blowout can cause subsurface charging that can create a drilling hazard for the relief well. If this is the case, careful reservoir modelling will need to be undertaken to determine at what distance the relief well can approach the thief zone without encountering a well kick. Since the relief well target will be the producing zone, this may not be of concern, however careful study is warranted.

The reason for penetrating the blowout reservoir before setting the 9-5/8" casing must be carefully studied before commencing the relief well. Factors such as a thinning of overlying formations or faulting must also be taken into consideration in drilling the relief well.

Before drilling into each zone containing possible abnormal pressures, kill weight mud must be available to control an influx. Tripping practices must be closely monitored with an emphasis on minimal off bottom time. Excessive logging or wiper trips may potentially cause problems (reason for specifying proximity logs to be run inside the drill string rather than in open hole). IF extended periods of logging are required, strong consideration should be given to hole conditioning trips between runs.

Under this scenario, the greatest probability of problems on the relief well would be expected between the 9-5/8" shoe and the interception point. The presence of a high volume underground flow could create a situation that could require the 7" liner. The same complications discussed earlier would be further exacerbated by the requirement for a high rate kill operation.



Operational Comments

As the relief well converges on the blowing well, it is often difficult to anticipate at what point the relief well may begin losing fluids to the blowing wellbore. With this in mind, it must be possible to immediately switch the relief well from drilling to the kill operation at any given time during the final approach to the target wellbore. Therefore, it is imperative that prior to the final approach, all preparations for the kill operation must be complete. In this case, the point at which preparations for the kill operation must be fully completed is before reaching 9-5/8" casing setting depth. Once full wellbore communication is established, the kill operation can continue according to plan.

After locating the target wellbore and before drilling the final segment to interception under either scenario, a trip should be made to remove all unnecessary restrictions, i.e., drill collars, heavy-weight drill collars, subs, etc., from the drill string. In this manner the friction losses inside and outside the drill string will be minimized during the kill operation.

10.9.6 Tool Specifications

Directional Survey Tools

Listed below is the directional survey program recommended for the exploration and delineation type wells

42" Hole Section	Check verticality teledrift
Inside 30" Casing	None
17-1/2" Hole Section	Single shot in the middle of the phase and 1 single shot per trip and one battery tool gyro at the end of the phase
Inside 13-3/8" Casing	None
12-1/4" Hole Section	Single shot in the middle of the phase and 1 single shot per trip and one battery tool gyro at the end of the phase
Inside 9-5/8" Casing	None
8-1/2" Hole Section	Magnetic multishot
Inside 7" Casing	No survey

The directional survey program for the relief well follows the basic plan of the program for the producing wells, except for the additional equipment needed in the event a 7" liner must be set, and 5-7/8" hole must be drilled to interception. Listed below is the recommended program:

42" Hole Section	Check verticality with the MWD at the casing point.
Inside 30" Casing	No survey
12-1/4" Hole Section	Drill with an MWD taking data while circulating after drilling each stand
Inside 9-5/8" Casing	Run a North seeking gyro at 10 m stations to 9-5/8" shoe
8-1/2" Hole Section	Drill with an MWD taking data while circulating after drilling 10 m or use of a proximity steering tool
Inside 7" Liner	If a 7" liner is required run a North seeking gyro at 10 m stations to 300 m above the liner top and tie survey data back to the survey inside the 9-5/8" casing
6" Hole Section	Drill with MWD taking data while circulating at intervals dictated by situation or proximity steering tool.



Drilling Tools: The drilling tools required to drill the relief well may vary somewhat depending on the exact requirements and availability at the time. Please see Appendices: Relief Well Planning for a list of equipment recommended.

10.9.7 Modelling Criteria

For this project the DYN-X computer model was employed to describe the relief well and blowout well scenarios. This model considered two-phase steady state gas and oil flow for various pumping rates. The model took into account the geometry of the well, the inflow performance of the reservoir, reservoir fluids and its non-Newtonian behavior and the rheology of the kill fluid. Both sonic (theoretical maximum) and sub-sonic exit conditions were analysed. The models were developed by Dr. Adam. T. Bourgoyne of Louisiana State University on a consulting basis to ABEL Engineering. The models take into account experimentation at LSU where the exit conditions for gas in large diameter pipes have been observed and mathematical descriptions of the pressure relationships developed. The computer models and the equations used are documented in the text Firefighting and Blowout Control by L. William Abel et al. The model is Microsoft Excel™ spreadsheet (runs on the Mac in Version 5.0 and on a PC in Windows Excel™ Version 5.0).

DYN-X was used to investigate several scenarios of blowout conditions and to establish the kill pumping criteria. In addition to kill requirements, the model was used to predict a gas flow rate based on certain assumptions regarding reservoir parameters.

10.9.8 Blowout Scenarios

There are quite literally an infinite number of scenarios for loss of control of a well, however for planning purposes two general categories were considered:

- an underground blowout or
- a surface blowout (e.g. a leak at the BOP level)

All the investigations undertaken were subsets of these two general categories. Some were run to established boundary conditions. The more reasonable or likely situations are noted. Full reservoir potentials were considered for three scenarios. The geometry variations included drillpipe and drill collars in the hole and out of the hole. For each scenario, the wellbore with the shortest path was considered. For some cases, the wellbore with the longest path was used for comparison. In conjunction with this approach, only those scenarios that are both reasonable and feasible were reported and used for designing the pumping requirements. The results are not considered final and adjustment of the kill requirements is anticipated if an actual relief well project becomes a reality.

From the reasoning above the following scenarios were considered for development and exploration wells:

SCENARIO I:

Well is blowing out through a leak in the BOP stack during the 8-1/2" drilling phase. The flow is from the target reservoir at full reservoir potential. There are no leaks in the open hole or cased interval. The drill string is in the hole as per Figure I.6.

SCENARIO II:

Well is blowing out underground from the reservoir to the shoe to the 13-3/8" casing during the 12-1/4" drilling phase. The flow is from the target reservoir at reduced reservoir potential. The drill string is in the hole per Figure I.7

These scenarios are considered to cover the worst case and likely well conditions if the well does blowout. They are **not** a risk assessment that a blowout is likely to occur. A blowout is considered

a very unlikely probability in the first place, but this probability cannot be reduced to zero, therefore a set of “likely” scenarios has been examined.

Scenarios Commentary

An abbreviated system has been chosen for the description of the various scenarios. This is exhibited in the above scenario descriptions. A Roman numeral system describes the physical geometry and exit condition where I, II and A are the three basic physical geometry's scenarios:

I: 9-5/8" casing set, reservoir penetrated with open hole, BOP leaking, casing holding (not ruptured) and no underground flow.

II: 13-3/8" casing set, reservoir penetrated with open hole, underground flow, BOP and casing holding.

A: Designation means that the drill string is in the hole.

B: Designation means that no drill string is in the hole.

xx mD: Designation means that “xx” millidarcies were considered for the strength of the reservoir.

yy Nm: Designation means that “yy” meters of reservoir penetration were considered.

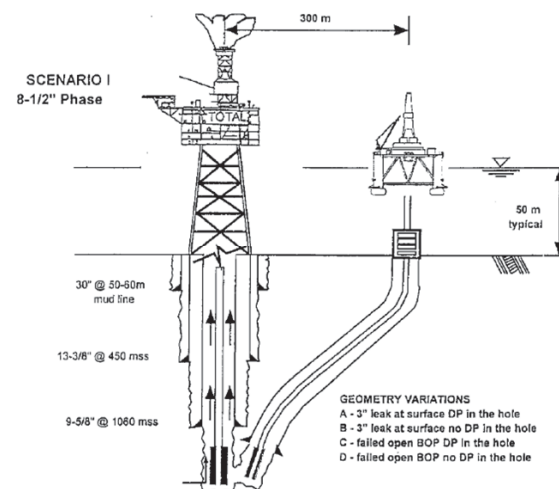


Figure I.6: Scenario I

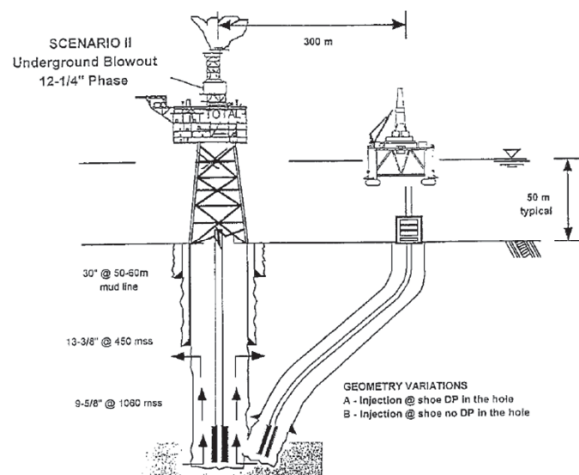


Figure I.7 Scenario II

10.9.9 Kill Fluid Design

Kill Fluid

This report used experience and computer simulations to determine that the most logistically sound kill fluid is a water based drilling mud similar in density to what was used to drill the well. The objective is to slightly overbalance the reservoir pressure, but not fracture the open hole interval during the kill procedure. Note that the kill pump rates calculated will certainly produce an equivalent circulation density that will exceed fracture gradient if not mixed with gas in the wellbore. Therefore, it will be necessary to reduce the pumping rates as the well comes under control to avoid fracturing and leak off of the fluid. Procedural recommendations are contained in a latter section of this report. The kill rheology chosen for the relief well kill operation and computer modelling follows:

Development

- SG = 1.2
- 8-1/2" Hole
- PV = 8 YP = 17
- Fann 600 = 25 Fann 300 = 33

Exploration

- SG = 1.4
- 8-1/2 Hole"
- PV = 10 YP = 14

- Fann 600 = 24 Fann 300 = 34

The important factor for the kill fluid rheology is that it has sufficient density to slightly overbalance the reservoir when static but still remain "thin" enough to be pumped at the necessary rates. The properties stated above are not absolute values but reasonable estimates for modelling purposes and estimation of horsepower requirements. These values were taken from the chart shown in Figure C.8. Should a relief well become a reality, the pumping requirements must be reviewed carefully to insure that the actual properties do not exceed the above values by more than 20% as the frictional losses could be significantly larger. Hydraulic calculations for each scenario considered are contained in Appendix E, Section E.3.

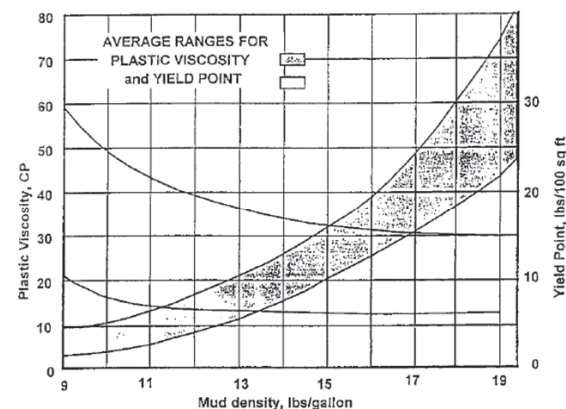


Figure I.8

Fracture Avoidance / Leak Off

During the kill operation when fluid is placed in the blowing well, the objective will be to overcome flowing bottom hole pressure. Thereafter the bottom hole pressure exerted must then slightly overbalance the static reservoir pressure. In no case should the pressure profile in the open hole interval (reservoir to the last casing shoe in the blowing well) be allowed to exceed fracture gradient. If massive fracturing is allowed, the majority of the kill fluid will be lost to the fracture and it is doubtful the well will be killed.

Some leak off will most likely occur during the initial stages of the pump to kill operation. For this report, leak off has been estimated to be 10% of the volume being pumped. Adjustments of the pumping rate have been increased accordingly. For example if the computer model says that 42 barrels per minute is required to kill the well, then 46.2 barrels are modelled for the frictional model.

Fracture avoidance may be very difficult to maintain, but never-the-less it is the most logical and prudent procedure to follow during the kill operation. To this end, the pressure profiles for various pumping rates of kill fluid have been reviewed to see that fracture gradient is not exceeded at the recommended pumping rates. A procedure will need to be developed to prevent fracture of the open hole during the kill operation. DYN-T transient analysis is recommended to the guide actual operation.

10.9.10 Pumping Requirements

Of the scenarios considered, scenario I-A and II-A are more likely to present themselves than scenarios I-B and II-B. Table C.6 contains summaries of the computer investigations. All the computer results are contained in the appendix of this report should more detail be needed.

All other scenarios are considered to be subsets of the above. For kill rates determined to be greater than 50 barrels per minute the scenario were reviewed carefully and all were considered to be either unreasonable or boundary condition and unlikely to occur. In the event that a blowout does occur that matches these models for gas rates and pump rates greater than 50 barrels per minute, multiple relief wells may be needed.

(Kill Pump rates, Pump Spread, FBHP and Blowout Flowrates)

DYN-X		CALCULATED PARAMETERS													
Qgas mmscfd	Coil sid/d	FBHP* psi	Mud Hydro	System Losses	Pump Press	Min HHP	BPM w/LO	SF	Assm'd LO	BBL/S Pump	HHP/ pump	Num pumps	actual HHP	Case	
218.7	4374.2	3065.9	-1188	325	1858	1461	31.91	1.5	10%	8	612	6	3672	Dev 3" leak DP	
308.9	6177	2746	-1188	682	1558	1838	48.14	1.5	10%	8	612	9	5506	Dev 3" leak NDP	
364.5	3243	5528	-2155	488	3373	2537	30.68	1.5	10%	8	612	6	3672	Exp 3" leak DP	
583.6	5193	5048	-2155	1099	2892	3413	48.16	1.5	10%	8	612	9	5506	Exp 3" leak DP	
47.9	959	955	-2313	874	-1348	n/a	41.11	1.5	10%	12	612	5	3060	UGBO Dev Norm	
66.1	595	5374	-2155	670	3218	n/a	20.00	1.5	10%	12	612	4	2448	UGBO 9m pen	
254.5	5288	94	-1188	345	-1094	n/a	33.03	1.5	10%	8	612	6	3672	Dev 3" leak DP Horiz	
417.8	8356	149	-1188	730	-1039	n/a	49.99	1.5	10%	8	612	9	5506	Dev 3" leak NDP Horiz	

Table I.3 DYN-X SIMULATION SUMMARY

- *Note: Qgas is the maximum rate possible given the input wellbore geometry, as calculated from DYN-X runs.
- *Note: Negative pump pressure means that the relief well will go on a vacuum when interception is made.

The wellbore geometry along with the contract drilling equipment was modelled in a frictional model. Pressure loss equations were per Preston L. Moore "Drilling Practices where Fann data is used to determine friction at a fluid shear rate. Flowing bottom hole pressures were taken from the computer models described earlier. The kill rate plus a percentage to account for leak off was modelled for flow down the relief well annulus, with the drillpipe held for pressure observations. The design horsepower requirements have a 1.5 safety factor applied. Note that the rates used in the frictional model were increased 10% for leak off. Therefore the gross factor of safety for horsepower is 1.65 times the theoretical values. This safety factor is reasonable when considerations are given to unknown factors, like equipment failures etc. The horsepower requirements are summarized in Table I.3.

The volume anticipated for the kill operation is two hole volumes of the blowout well or about 1500 barrels. This was determined from the computer model and experience. Note that if a relief well is drilled, a transient analysis, DYN-XT, will be needed to refine the pumping requirements for the kill operation. This was not done in this report because it was not part of the scope of work and not necessary.

10.9.11 Equipment Specifications

For safety and reliability, it is recommended that the external pumps (DS Schlumberger, BJ, etc.) be provided in all cases. For purposes of discussion in this report Halliburton pump specifications shall be used (not as a recommended vendor for these services, but because the author is more

familiar with this equipment than others). If a vendor other than Halliburton is chosen, their equipment will be comparable and little modification necessary except a review of pump-volume characteristics.

To follow the kill procedures, and in particular to maintain control of bottom hole pressure in all downhole conditions and in all-weather environments, a surface pumping spread per Figure I.10 will be necessary. Table I.3 shows the maximum recommended pumping spread where 10 each 612 HP pumps are provided. The lesser cases will require fewer pumps, but all the supporting booster pumps and holding tanks will remain the same.

Having a stimulation vessel provide the pumping requirements was considered; at first, it seemed to be a viable choice. However, upon review, certain factors ruled out the stimulation vessel as the primary pumping source. The major reasons were availability and possible conflicts with existing long term contracts with other area operators. The main reason is that these vessels are not equipped to handle a weighted fluid for extended periods of time. For safety reasons, the overall plan calls for kill weight fluid to be on standby ready to pump at a moment's notice. Thus the kill operation must be rigged up and kept on 24 hour notice during all of Phase III drilling. To use a stimulation vessel to provide pumping capacity, kill fluids must be transferred to the vessel on the fly making a complex hook up for both suction and discharge requirements. This cannot be considered 100% reliable in all weather and light conditions. Therefore installation of all pumping equipment on the main deck of the drilling rig is the most viable option.

Mixing

Mixing of the kill mud will be done by the drilling rig. The kill fluid should be transferred to 500 barrel top deck storage tanks sea fastened to the main deck of the drilling rig.

Suction Supply

Booster pumps will provide suction pressure for the high pressure pumping spread. These booster pumps shall feed into a 6" discharge ring that is fully manifolded to feed the high pressure pumps and return fluid to the pit area for conditioning if required. A tie in for a supply boat transfer of mud shall also be provided. A fluid transfer system shall also be supplied to move mud from the pit room to the main deck at 10 bpm rates. The booster system and/or the high pressure pumps shall be used to roll the fluid in the deck holding tanks, thereby assisting in maintenance of rheological properties. Densometers and flowmeters shall be installed at convenient locations in the suction supply system.

Discharge System

A 3" 10M working pressure distribution manifold will connect all high pressure pumps to a central manifold connected to the kill and choke line of the drilling rig. The central manifold shall have provisions for a tie to a stimulation boat, high volume return line to the holding tanks (for testing the system) and a relief-dump line overboard. Check valves will be required on the lines that connect the choke and kill lines. Tie in to the kill lines shall be in the moon pool area, bypassing the standpipe and choke manifold. Both high pressure and volume pumping will be required of this system.

Pumping Equipment

The pumping equipment shall be high pressure fracture treatment pumps. They shall be skid mounted in a protective frame acceptable to offshore operations. Due to limited deck space these frames must be so configured that it is permissible to stack the pump on top of one another. They shall be independently driven by diesel powered engines with normal controls, spark arrestors, and air shut offs. Discharge pressure shall be 10,000 psi working pressure. For pump unit calculation the capacity of a Halliburton HT-400 pump (4-1/2" liner with 8 inch stroke) powered by a GM Diesel 16V92 with 612 input horsepower is used. The pump pressure relationship, pressure volume

curve, has been used as supplied by Halliburton, Duncan, Oklahoma. This particular PVC is shown in Fig. I.9

Rather than applying a multitude of factors to each of the inputs to the pumping requirement. The author has chosen to use the maximum values and then apply an overall safety factor, therefore when predicting the number of pumping units required the calculated discharge pressure determines maximum unit discharge rather than applying factors of safety to each individual parameter.

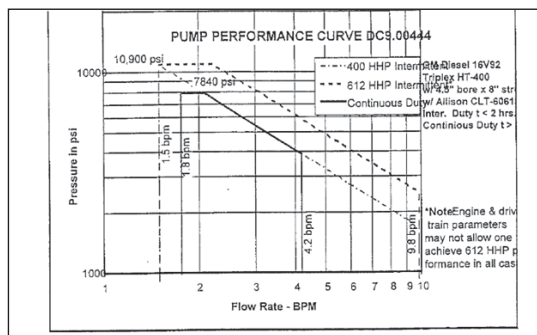


Figure I.9 Pressure Volume Curve

(Courtesy of Halliburton Energy Services, Duncan, OK)

The basis for calculating the required pumps follows:

$$N_p = Q_k / (1 - LO) \times SF / Q_m$$

Where :

N_p = number of pump units (round to integer)

Q_k = design kill rate, (bpm)

SF = safety factory (*)

LO = per cent leak off in decimal form, (*)

Q_m = max flow per unit, (bpm per unit) from manufacturer's data for 100% performance at anticipated discharge pressure, P_m

Example: For a given Scenario, the maximum discharge from the pressure loss model is 1600 psi (rounded to nearest 100 psi). From Figure C.9 the PVC discharge yields maximum available rate per unit, Q_m of 10.0 barrels per minute per unit if maximum horse power is expended. Assuming 10% leak off to the formation during the kill operation, LO becomes 0.10. The recommended overall safety factor, SF , is 1.50. Thus for this scenario the required number of pumps will be:

$$N_p = 47.52 \times 1.5 / (1 - 0.1) \times 10 = 7.92 \text{ or } 8 \text{ rounded up.}$$

Table I.3 presents the design conditions for pumping units if Halliburton HT-400 16V92 powered units with 4-1/2" liners (162 max hp each unit) are chosen as the primary pump unit.

Control System

Control of all high pressure pumps shall be by remote control from a single unit so that one person can control all the pumps in the spread. Constant communication with the command center

(computer skid) shall be necessary. Pump and bottom hole pressure as well as volume pumped shall be electronically recorded. Digital displays of discharge pressure, cumulative pumping rate, density of discharge fluid and cumulative volume shall be displayed. The control and recording devices shall be housed in a single module that has space for the pumping vendor technicians as well as 4 company's representatives.

Safety System

Safety systems shall be provided so that the technicians can monitor:

- critical engine functions on pumps and boosters
- fluid levels in holding tanks
- communications from rig command center
- Bottom hole pressure and temperature from a surface read out wireline conveyed pressure gauges located in the relief well.

A relief valve in the overboard line shall be installed. This shall have automatic reset. Check valves shall be installed in the discharge line and at critical points in the discharge piping system.

Testing / Training

Testing of the pumping system should be done with sea water and with weighted fluid. The discharge system has a return and overboard line for this purpose. The pumping of 2000 barrels should take less than one hour at design rates; however the final stages of the kill may have very low rates. Therefore the pumps should be tested to see that they can deliver the design rate and horsepower (with safety factor) by pumping against a choke with sea water for 30 minutes at 3300 psi. Intermittent (10 minutes) pump test at 7,000 psi with all pumps on line will test that all available horsepower can be delivered through a range of working pressures. This will ensure flexibility of the operation should it become necessary to alter the job specifications.

A weighted fluid pumping test should be performed to insure that the suction and discharge systems provided are adequate at the design rates. The actual frictional losses in the system from the discharge, deck lines, manifolding and kill line to the BOP should be determined by circulation. This test should be done with weighted fluid and with sea water while waiting on cement after setting 9-5/8" casing or earlier if possible.

An important aspect of the kill procedure will be the coordination of all service company personnel and company representative. It will be critical that information flow freely to the onsite management team. The trial runs to test the pumping system should include a full test of all monitoring systems and personnel involved.

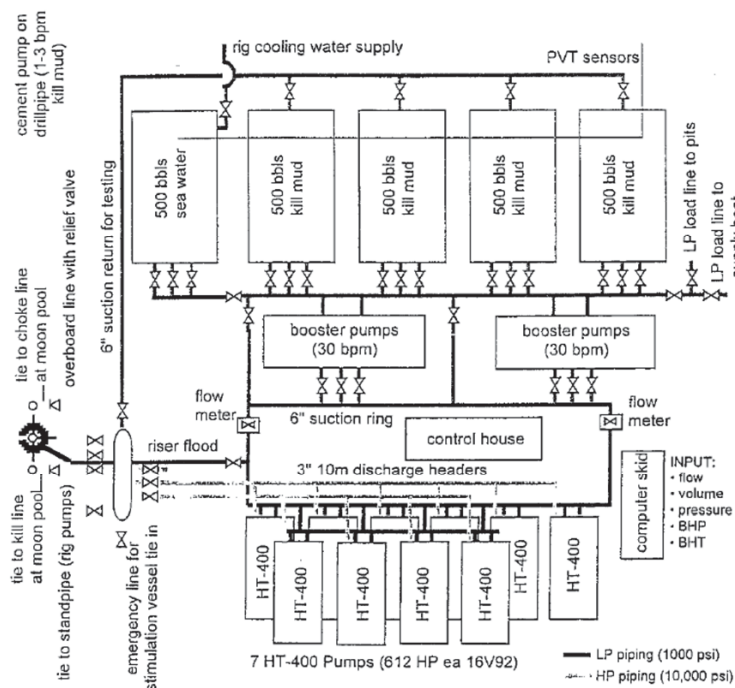


Figure I-10

10.10 SURFACE CONTROL SPECIAL SERVICES

10.10.1 Hot Tapping and Valve Drilling

Hot tapping and valve drilling equipment has been used on blowouts to allow pumping into wellheads, tubulars or fire frozen valves. This equipment is available from most major blowout specialist companies as part of their service capabilities.

In a hot tap, a saddle clamp is installed around the tubular and a pack off is energized. Within the lubricator a drill bit cuts through the tubular with pressure held slightly higher on the outside than on the inside so positive indication that a hole has been made is seen. After the hole is cut, it can be reamed out up to 1". Valve drilling machines are available to drill out frozen gates. Up to 3" holes have been drilled with larger hole sizes milled out.

These services are available from Boots & Coots, Cudd, Halliburton, HWC and others. Pipeline companies use hot tap equipment and may be adaptable to certain applications. Saddle clamp sizes should be investigated. A specialist should be utilized in any case for safety.

10.10.2 Freezing

Freezing is used to place an ice plug within shut in wells (within pipe, wellheads or annulus) to allow removal, repairs or replacement of wellhead equipment. Freezing has not been used to control a high volume blowing well.

Some inventors attempted to market devices using liquid nitrogen to freeze off blowing wells in Kuwait, but simpler control methods were available. Difficulties were seen in maintaining the freeze plug of frozen oil and brine while making extensive surface repairs to blown up wellhead equipment.

Freezing techniques usually use dry ice to freeze water or fresh water-bentonite slurries. Methanol can be used with dry ice to get a lower temperature. A 75% methanol/water mixture has a freeze temperature of <-200° F. Methanol water mixtures could be potentially cooled by liquid nitrogen and the cold methanol/water mixture circulated around the area to be frozen.

This would allow control of the applied temperature to the steel. Problems with low fracture toughness in super cooled steels have been observed in nitrogen pumping service when pump rates exceeded heater capabilities and liquid nitrogen was pumped into wells.

Freezing services are available from Boots & Coots, Cudd, Halliburton, HWC and others.

10.10.3 Pneumatic Casing Cutters

Pneumatic cold cutters are used to strip away outer casing strings to expose inner casing strings for well capping. ABB Vetco Gray has equipment available to make vertical stripping cuts to split casing strings. The pneumatic cold cutters are commonly used in the pipeline business. Common sources are ABB Vetco Gray, Boots & Coots, Enterra Wellcat, Porta-lathe and others.

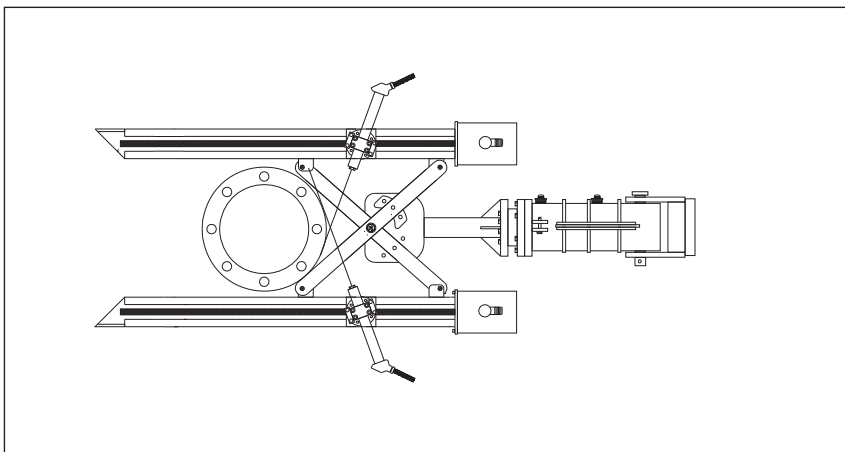
10.10.4 Abrasive Jet Cutters

The Halliburton abrasive jet cutter was developed to deal with the aftermath of the Arabian Gulf War. Because of the extensive number of wells that were burning, Halliburton developed a way to rig up quickly, cut from a remote location and rig down quickly to move to another well. This cutter was designed to cut the casing below the braden head, which cuts all the casing strings, cement between casing strings and tubing in the center.

The abrasive jet cutter incorporates two jet nozzles opposing each other. A hydraulic motor turns a linear screw that moves the nozzles either in a forward or reverse direction. The cutter is positioned on each side of the wellhead and pressure from the pumping equipment is established

at 10,000 psi at approximately 4 bbls/min. Sand is added to the blender and the sand slurry is delivered to each nozzle. The nozzles are then tracked forward cutting everything between the two nozzles.

All hydraulic lines are encased in a water jacket due to the intense radiant heat associated with a blowout. Also as an added feature the cutter can be rotated clockwise to counter-clockwise and raised up or down. This simplifies trying to cut on a leaning or damaged wellhead.



This is controlled by a small hydraulic power pack that is incorporated into the skid that houses the cutter during shipping. This power pack and control system can be placed up to 250 feet from the actual cutter assembly. From this safe distance the well control specialist can control the movement of the cutting jets.

The abrasive jet cutter has cut a forty eight inch diameter flange the largest to date. The average cut usually made with the cutter is between twenty four inches to eighteen inches in diameter. With a cutting pressure of 10,000 psi, a pump rate of four barrels per minute and a pound per gallon sand concentration the cutting time is less than one hour for these applications.

10.10.5 Requirements for the Halliburton Abrasive Jet Cutter

- Two thousand hydraulic horsepower (2,000 hhp) – that has been horsepower tested for at least twenty minutes at 10,000 psi and 4 bbls/min. If 2,000 hhp is not available, contact Halliburton Well Control in Duncan.
- Pumping iron – This depends on each individual blowout location. Usually five hundred feet of straight two inch 1502 with an assortment of style 50 angle wing chiksans and tees to wye the pumping equipment together. Suction hoses to hook up pumps.
- Sand Requirements – 20/40 Ottawa frac sand is preferred but 20/40 Brady, 20/40 inter-prop or 20/40 bauxite can be used if the Ottawa is not available. Amount per hour of cutting = 12,500 pounds.

Halliburton Well Control will supply the blender and in most cases a centrifugal pump to mix the sand and water together.

10.10.6 Explosive Jet Cutter

Shaped charges can be made in the field using raw C4 plastic explosive in fabricated holders. Point cuts, linear cuts and circular cuts can be fabricated by firefighting explosive experts. Manufactured cutting charges are stocked by explosive manufacturers in some regions, but cannot be custom configured to the application. These are generally the same companies that make oil well perforating charges (GOEX and JRC).

10.10.7 Hydraulic Simulator

Hydraulic modelling software and specialists will be required to help perform blowout scenario diagnostics and kill simulations.

Planning the kill strategy for a 1989 underground blowout in the North Sea required development of an improved flow simulator. The hydraulic kill simulator was based on the industry standard, two phase pipe flow model, OLGA. After the project, the planning team realized that they gained considerable advantage from using a transient two phase flow simulator for comparing various kill scenarios. Since then, the OLGA-WELL-KILL simulator has been used successfully for a number of intervention design plans.

The ability to analyse hydraulic kill scenarios quickly and find their effect on the rest of the intervention operation is critical to project success. A specialized need was therefore identified for a multiphase, time transient, flow simulator designed for easy blowout kill analysis. This need was the driver that motivated the continued modification of the pipeline code for well flow and kill simulations.

During a blowout kill, up to six fluids can be present simultaneously in the well reservoir; oil, gas and water; kill water, intermediate and final kill mud. Conventional kill models cannot easily evaluate multiphase flow where heavy kill muds are used.

Simulations handle this by first simulating the dynamics of a liquid/gas biphasic flow regime, then comparing this to a simulation using averaged properties in a light weight liquid phase. The kill phase is then introduced and a dynamic two phase simulation is performed until a steady state condition is reached. Afterwards, the next phase can be introduced and the simulations can be restarted at any time.

Modelling is accomplished using a number of controllers set to contain the simulation within the physical constraint of the real blowout. The controllers can, for example, be set on the following parameters:

- Pump rate.
- Pump horsepower.
- Formation collapse pressure.
- Casing burst pressure.
- Surface injection pressure.
- Bottom hole pressure (min/max).
- The simulation modeling includes
 - Pump performance
 - Non-Newtonian fluid flow (for mud)
 - Fluid temperature and pressure response
 - Inflow modelling (multiple if needed)
 - Leaks (multiple if needed)
 - Back pressure (outflow conditions)

- Several reservoir inflow models
- Variable reservoir pressure
- Path chokes (critical and sub critical)

In practical use, the modelling is usually taken through a number of steps starting with a PVT fluid characterization of the reservoir fluids. The blowout is then modelled to match all available data.

The next step is to set up a constant rate kill simulation to work out the range for the simulation of the actual dynamic kill. This is also useful in evaluating allowance for losses between wells (for relief well kills) as well as for the kill fluid density, and for velocity and pressures at critical points in the blowout path. The fully dynamic simulations can then incorporate all the actual constraints in the kill such as casing pressure ratings, fracture pressures, inflow performance and reservoir pressure (dynamically versus time, if necessary), pumping plant and mud properties.

The simulation yields an actual pump schedule vs. time (with rates and pressures at any chosen point in the flow path). If needed, a number of sensitivities can be developed to evaluate kill effectiveness during the actual pumping. This later step can often prove useful when there are unknowns in the kill (such as communication between relief well and blowout well, actual blowout flow path or reservoir performance.)

Applications include the following:

- Kill with different mud densities in the well.
- Partial losses during kill.
- Multiple blowout paths, cross flows and leaks.
- Multiple relief wells pumping at different rates.
- Underground blowouts from a drilling rig.
- Simultaneous bullheading and dynamic kill.
- Off bottom or momentum kills, shallow gas blowouts.
- Horizontal well flow analysis.
- Slugging in long reach production wells.
- Rates required to circulate out a kick in horizontal wells.
- Alternating gas and water injection.
- Sensitivity analysis by varying parameters.

10.11 EMERGENCY CONTACT LISTS

Refer to current contact lists provided by the various department managers.

Use this link to find everyone in the oil field

<https://www.oildex.com/resources/directory/>



บริษัท ปตท.สผ. สยาม จำกัด

รายงานผลการปฏิบัติตามมาตรการป้องกันและแก้ไขผลกระทบสิ่งแวดล้อม และมาตรการติดตามตรวจสอบผลกระทบสิ่งแวดล้อม
โครงการในพื้นที่จังหวัดกำแพงเพชร
ฉบับเดือนมกราคม - ธันวาคม พ.ศ. 2566

ภาคผนวกที่ 36
นโยบายความปลอดภัย มั่นคง อาชีวอนามัย
และสิ่งแวดล้อม



นโยบายความปลอดภัย มั่นคง อาชีวอนามัย และสิ่งแวดล้อม

ปตท. สผ. ยึดถือความปลอดภัย ความมั่นคง อาชีวอนามัย และสิ่งแวดล้อม เป็นพื้นฐานในการดำเนินธุรกิจ ดังนั้น เพื่อให้บรรลุและคงไว้ซึ่งความเป็นเลิศในการปฏิบัติงานตามเป้าหมายการพัฒนาที่ยั่งยืน ปตท.สผ. ได้กำหนดให้มีระบบการบริหารจัดการด้านความปลอดภัยฯ และยึดถือปฏิบัติอย่างมีประสิทธิภาพ โดยสร้างความมั่นใจด้านความปลอดภัยและสุขภาพของบุคลากรทุกคน รวมถึงชุมชนรอบพื้นที่ปฏิบัติงาน ปกป้องสิ่งแวดล้อม รวมทั้งความมั่นคงปลอดภัยของบุคลากรและทรัพย์สิน

ปตท.สผ. มีนโยบายเพื่อให้บรรลุวิสัยทัศน์ของการเป็นองค์กรที่ปราศจากอุบัติเหตุ ดังนี้

- มุ่งมั่นที่จะสร้างวัฒนธรรมความปลอดภัยฯ ในระดับสูงสุด โดยเน้นภาวะผู้นำด้านความปลอดภัยฯ และการมีส่วนร่วมของพนักงานและผู้รับเหมาทุกคน
- กำหนดวัตถุประสงค์ ตัวชี้วัด เป้าหมายและแผนงานด้านความปลอดภัยฯ เพื่อพัฒนาการจัดการด้านความปลอดภัยฯ อย่างต่อเนื่องและเป็นไปตามเป้าหมายของการมีผลการดำเนินงานด้านความปลอดภัยฯ ในระดับชั้นนำ โดยผู้บังคับบัญชาตามสายงานมีภาระหน้าที่รับผิดชอบต่อผลการปฏิบัติงานที่เกิดขึ้น
- ปฏิบัติงานภายใต้กฎหมาย ระเบียบ ข้อบังคับหรือมาตรฐานที่เกี่ยวข้องกับการดำเนินงานด้านความปลอดภัยฯ ทั้งในระดับประเทศและระดับสากลอย่างเคร่งครัด
- บริหารจัดการความเสี่ยงด้านความปลอดภัยฯ ให้อยู่ในระดับต่ำที่สุดเท่าที่สามารถปฏิบัติได้ ตลอดวัฏจักรของธุรกิจ และเมื่อมีการเปลี่ยนแปลงในการดำเนินงาน
- ส่งเสริมการสร้างระบบการจัดการสุขภาพที่มีประสิทธิภาพ และเข้มงวดเรื่องการปฏิบัติงานโดยปราศจากสารเสพติดและแอลกอฮอล์ในสถานที่ปฏิบัติงาน
- ลดการดำเนินกิจกรรมที่ส่งผลกระทบต่อสิ่งแวดล้อมให้สอดคล้องกับหลักการของแนวทางสู่องค์กรคาร์บอนต่ำ การใช้ทรัพยากรหมุนเวียน และการสร้างคุณค่าเชิงบวกด้านความหลากหลายทางชีวภาพและบริการจากระบบนิเวศ
- ปกป้องพนักงานและองค์กรจากการระบาดของโรคติดต่อ ภัยพิบัติ ภัยคุกคามและช่องโหว่ด้านความมั่นคงปลอดภัย ผ่านกระบวนการจัดการเหตุการณ์ฉุกเฉิน เหตุการณ์วิกฤติ และความต่อเนื่องในการดำเนินธุรกิจที่มีประสิทธิภาพ
- ให้อำนาจทุกคนในองค์กรใช้สิทธิในการหยุดปฏิบัติงานภายใต้สถานะที่ไม่ปลอดภัย
- มุ่งมั่นพัฒนาและปรับปรุงประสิทธิภาพการจัดการด้านความปลอดภัยฯ อย่างต่อเนื่อง ผ่านการฝึกอบรม โปรแกรมการมีส่วนร่วมของผู้มีส่วนได้เสีย และการปรับปรุงพัฒนาระบบและเครื่องมือที่เกี่ยวข้องด้วยเทคโนโลยี

ทั้งนี้ เพื่อให้การนำนโยบายความปลอดภัย มั่นคง อาชีวอนามัย และสิ่งแวดล้อม ไปใช้ให้เกิดประสิทธิผลสูงสุด บุคลากรของ ปตท.สผ. ตั้งแต่ระดับผู้บริหารสูงสุดจนถึงระดับพนักงานในพื้นที่ปฏิบัติการ รวมทั้งผู้รับเหมาทุกคนต้องมีความมุ่งมั่นร่วมกันและมีสติในทุกครั้งที่ลงมือปฏิบัติงาน

ประธานเจ้าหน้าที่บริหาร

วันที่ 13.04.25



บริษัท ปตท.สผ. สยาม จำกัด

รายงานผลการปฏิบัติตามมาตรการป้องกันและแก้ไขผลกระทบสิ่งแวดล้อม และมาตรการติดตามตรวจสอบผลกระทบสิ่งแวดล้อม
โครงการในพื้นที่จังหวัดกำแพงเพชร
ฉบับเดือนมกราคม - ธันวาคม พ.ศ. 2566

ภาคผนวกที่ 37
ผลการตรวจวัดคุณภาพอากาศ

ព្រះរាជាណាចក្រកម្ពុជា

ព្រះបរមរាជវាំង

ភ្នំពេញ

ថ្ងៃទី ០១ ខែ ០១ ឆ្នាំ ២០២០

លេខ ០១/២០២០

ស្តីពី

ការ

អនុញ្ញាត

ឲ្យ

ស្ថាប័ន

ពាក់ព័ន្ធ

នឹង

ការ

អនុវត្ត

ក្នុង

វិស័យ

សេវា

សាធារណៈ

ប្រកាស

នេះ

មាន

សុពលភាព

ចាប់ពី

ថ្ងៃចេញ

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตซีเมนต์เสริมแรงในบ่อบำบัดน้ำเสีย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตในบ่อบำบัด-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Ambient Air Quality
Sampling Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลวง หมู่ที่ 5 ตำบลโนนพลวง อำเภอสามโก้ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589993 E, 1832898 N
Sampling Date : January 11-14, 2024
Sampling Time : 09:00
Sampling Method : U.S. EPA 40 CFR Part 50
Sampling By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.

Quotation No. : 2023-01037
Folder No. : 2024-AA095
Received Date : January 15, 2024
Analytical Date : January 15-18, 2024
Report No. : 2024-RAAB198
Report Date : January 18, 2024


Parameter	Unit	Method of Analysis	Result			Standard ¹⁾
			Jan 11-12, 24	Jan 12-13, 24	Jan 13-14, 24	
Total Suspended Particulate (TSP) 24 Hours Average	mg/m ³	High-Volume, Gravimetric	0.157	0.147	0.095	0.330
Particulate Size Less Than 10 Micron (PM10) 24 Hours Average	mg/m ³	PM10 Size Selective, High-Volume, Gravimetric	0.094	0.080	0.056	0.120

Remark : ¹⁾ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995) and Notification No.24, B.E.2547 (2004), published in the Royal Government Gazette No.121 Special Part 104D dated September 22, B.E.2547 (2004), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



[REDACTED]

Laboratory Reviewer



[REDACTED]

Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตซีเมนต์เสริมแรงในบ่อบำบัดน้ำเสีย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตในบ่อบำบัด-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Ambient Air Quality
Sampling Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลานกระบือ อำเภอสามโก้ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Sampling Date : January 11-14, 2024
Sampling Time : 09:30
Sampling Method : U.S. EPA 40 CFR Part 50
Sampling By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.

Quotation No. : 2023-01037
Folder No. : 2024-AA095
Received Date : January 15, 2024
Analytical Date : January 15-18, 2024
Report No. : 2024-RAAB199
Report Date : January 18, 2024


Parameter	Unit	Method of Analysis	Result			Standard ¹⁾
			Jan 11-12, 24	Jan 12-13, 24	Jan 13-14, 24	
Total Suspended Particulate (TSP) 24 Hours Average	mg/m ³	High-Volume, Gravimetric	0.164	0.137	0.120	0.330
Particulate Size Less Than 10 Micron (PM10) 24 Hours Average	mg/m ³	PM10 Size Selective, High-Volume, Gravimetric	0.098	0.082	0.065	0.120

Remark : ¹⁾ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995) and Notification No.24, B.E.2547 (2004), published in the Royal Government Gazette No.121 Special Part 104D dated September 22, B.E.2547 (2004), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



[REDACTED]

Laboratory Reviewer



[REDACTED]

Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตไฟฟ้าโดยพลังงานแสงอาทิตย์ในแปลงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานข้อมูลผลิตในแปลง-5 (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลาญ หมู่ที่ 5 ตำบลโนนพลาญ อำเภอสามโก้ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589993 E, 1832898 N
Measured Date : January 11-14, 2024
Measured By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : NOx Chemiluminescence Analyzer Horiba Model APNA-370 Serial Number M4286F23

Quotation No. : 2023-01037
Analysis No. : 2024-AA095-001
Report No. : 2024-RAAB281
Report Date : January 20, 2024

Interval Time	Result (ppm)									Standard ¹⁾
	Jan 11-12, 24			Jan 12-13, 24			Jan 13-14, 24			
	NO	NO ₂	NO _x	NO	NO ₂	NO _x	NO	NO ₂	NO _x	
09:00-10:00	0.0029	0.0084	0.0113	0.0033	0.0090	0.0123	0.0066	0.0131	0.0197	0.17
10:00-11:00	0.0035	0.0104	0.0139	0.0026	0.0084	0.0110	0.0030	0.0080	0.0110	
11:00-12:00	0.0037	0.0104	0.0141	0.0042	0.0111	0.0153	0.0048	0.0122	0.0170	
12:00-13:00	0.0031	0.0091	0.0122	0.0047	0.0145	0.0192	0.0034	0.0092	0.0126	
13:00-14:00	0.0030	0.0085	0.0115	0.0032	0.0096	0.0128	0.0032	0.0085	0.0117	
14:00-15:00	0.0027	0.0082	0.0109	0.0024	0.0077	0.0101	0.0026	0.0080	0.0106	
15:00-16:00	0.0024	0.0079	0.0103	0.0023	0.0073	0.0096	0.0022	0.0075	0.0097	
16:00-17:00	0.0023	0.0076	0.0099	0.0022	0.0078	0.0100	0.0022	0.0074	0.0096	
17:00-18:00	0.0023	0.0093	0.0116	0.0022	0.0085	0.0107	0.0022	0.0075	0.0097	
18:00-19:00	0.0023	0.0113	0.0136	0.0023	0.0112	0.0135	0.0022	0.0086	0.0108	
19:00-20:00	0.0025	0.0152	0.0177	0.0026	0.0165	0.0191	0.0024	0.0142	0.0166	
20:00-21:00	0.0028	0.0209	0.0237	0.0024	0.0131	0.0155	0.0026	0.0178	0.0204	
21:00-22:00	0.0026	0.0166	0.0192	0.0023	0.0131	0.0154	0.0028	0.0138	0.0166	
22:00-23:00	0.0024	0.0120	0.0144	0.0022	0.0104	0.0126	0.0031	0.0178	0.0209	
23:00-00:00	0.0037	0.0194	0.0231	0.0023	0.0099	0.0122	0.0024	0.0114	0.0138	
00:00-01:00	0.0024	0.0122	0.0146	0.0023	0.0086	0.0109	0.0022	0.0067	0.0089	
01:00-02:00	0.0024	0.0109	0.0133	0.0022	0.0079	0.0101	0.0021	0.0059	0.0080	
02:00-03:00	0.0022	0.0086	0.0108	0.0024	0.0115	0.0139	0.0021	0.0055	0.0076	
03:00-04:00	0.0028	0.0098	0.0126	0.0023	0.0089	0.0112	0.0022	0.0055	0.0077	
04:00-05:00	0.0025	0.0091	0.0116	0.0023	0.0076	0.0099	0.0022	0.0054	0.0076	
05:00-06:00	0.0023	0.0077	0.0100	0.0029	0.0105	0.0134	0.0025	0.0060	0.0085	
06:00-07:00	0.0026	0.0074	0.0100	0.0031	0.0104	0.0135	0.0023	0.0079	0.0102	
07:00-08:00	0.0097	0.0135	0.0232	0.0027	0.0116	0.0143	0.0022	0.0067	0.0089	
08:00-09:00	0.0100	0.0129	0.0225	0.0038	0.0114	0.0152	0.0117	0.0058	0.0175	
24 Hours Average	0.0033	0.0111	0.0144	0.0027	0.0103	0.0130	0.0031	0.0092	0.0123	-
1 Hour Maximum	0.0100	0.0209	0.0237	0.0047	0.0165	0.0192	0.0117	0.0178	0.0209	0.17

Remark : ¹⁾ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995), Notification No.28, B.E.2550 (2007), published in the Royal Government Gazette No.114 Special Part 58D dated May 14, B.E.2550 (2007) and Notification No.33, B.E.2552 (2009), published in the Royal Government Gazette No.126 Special Part 114D dated August 14, B.E.2552 (2009), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตไฟฟ้าโดยพลังงานแสงอาทิตย์ในแปลงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานข้อมูลผลิตในแปลง-5 (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลาญ หมู่ที่ 5 ตำบลโนนพลาญ อำเภอสามโก้ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589993 E, 1832898 N
Measured Date : January 11-14, 2024
Measured By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : SO₂ UV-Fluorescence Analyzer Thermo Model 43C Serial Number 0611116460

Quotation No. : 2023-01037
Analysis No. : 2024-AA095-001
Report No. : 2024-RAAB282
Report Date : January 20, 2024

Interval Time	Result SO ₂ (ppm)			Standard
	Jan 11-12, 24	Jan 12-13, 24	Jan 13-14, 24	
09:00-10:00	0.0014	0.0020	0.0019	0.12 ¹⁾
10:00-11:00	0.0015	0.0020	0.0019	
11:00-12:00	0.0015	0.0021	0.0021	
12:00-13:00	0.0016	0.0021	0.0021	
13:00-14:00	0.0016	0.0021	0.0020	
14:00-15:00	0.0017	0.0022	0.0021	
15:00-16:00	0.0017	0.0021	0.0020	
16:00-17:00	0.0017	0.0021	0.0021	
17:00-18:00	0.0019	0.0022	0.0020	
18:00-19:00	0.0018	0.0021	0.0020	
19:00-20:00	0.0018	0.0021	0.0021	
20:00-21:00	0.0019	0.0020	0.0020	
21:00-22:00	0.0018	0.0021	0.0019	
22:00-23:00	0.0017	0.0021	0.0020	
23:00-00:00	0.0018	0.0020	0.0020	
00:00-01:00	0.0019	0.0021	0.0020	
01:00-02:00	0.0018	0.0020	0.0019	
02:00-03:00	0.0018	0.0020	0.0019	
03:00-04:00	0.0018	0.0019	0.0020	
04:00-05:00	0.0019	0.0021	0.0020	
05:00-06:00	0.0019	0.0021	0.0019	
06:00-07:00	0.0019	0.0021	0.0019	
07:00-08:00	0.0018	0.0021	0.0020	
08:00-09:00	0.0019	0.0021	0.0021	
24 Hours Average	0.0018	0.0021	0.0020	0.12 ¹⁾
1 Hour Maximum	0.0019	0.0022	0.0021	0.30 ²⁾

Remark : ¹⁾ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995) and Notification No.24, B.E.2547 (2004), published in the Royal Government Gazette No.121 Special Part 104D dated September 22, B.E.2547 (2004), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).
²⁾ Notification of National Environmental Board, No.12, B.E.2538 (1995), published in the Royal Government Gazette No.112 Special Part 27D dated July 13, B.E.2538 (1995) and Notification No.21, B.E.2544 (2001), published in the Royal Government Gazette No.118 Special Part 39D dated April 30, B.E.2544 (2001), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโบนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโบนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโบนหลวง หมู่ที่ 5 ตำบลโบนหลวง อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589953 E, 1832898 N
Measured Date : January 11-14, 2024
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : CO NDIR Analyzer Horiba Model APMA-370 Serial Number 4N02XP27

Quotation No. : 2023-01037
Analysis No. : 2024-AA095-001
Report No. : 2024-RAAB283
Report Date : January 20, 2024

Interval Time	Result CO (ppm)						Standard ^{1*}
	Jan 11-12, 24		Jan 12-13, 24		Jan 13-14, 24		
	1 hr Avg	8 hr Avg	1 hr Avg	8 hr Avg	1 hr Avg	8 hr Avg	
09:00-10:00	0.6	-	0.7	0.8	0.6	0.6	
10:00-11:00	0.6	-	0.6	0.7	0.5	0.6	
11:00-12:00	0.7	-	0.6	0.7	0.4	0.6	
12:00-13:00	0.6	-	0.6	0.7	0.4	0.6	
13:00-14:00	0.6	-	0.5	0.7	0.4	0.6	
14:00-15:00	0.5	-	0.5	0.7	0.4	0.5	
15:00-16:00	0.5	-	0.5	0.6	0.4	0.5	
16:00-17:00	0.5	0.5	0.4	0.6	0.4	0.4	
17:00-18:00	0.5	0.5	0.4	0.5	0.4	0.4	
18:00-19:00	0.5	0.5	0.5	0.5	0.4	0.4	
19:00-20:00	0.7	0.5	0.6	0.5	0.5	0.4	
20:00-21:00	0.9	0.5	0.6	0.5	0.7	0.4	
21:00-22:00	1.0	0.5	0.6	0.5	0.7	0.5	
22:00-23:00	0.9	0.7	0.6	0.5	0.7	0.5	
23:00-00:00	0.8	0.7	0.6	0.5	0.6	0.6	
00:00-01:00	0.7	0.8	0.6	0.6	0.4	0.6	
01:00-02:00	0.7	0.8	0.6	0.6	0.5	0.6	
02:00-03:00	0.7	0.8	0.6	0.6	0.5	0.6	
03:00-04:00	0.7	0.8	0.6	0.6	0.4	0.6	
04:00-05:00	0.7	0.8	0.5	0.6	0.4	0.5	
05:00-06:00	0.6	0.7	0.5	0.6	0.4	0.5	
06:00-07:00	0.6	0.7	0.7	0.6	0.5	0.5	
07:00-08:00	1.0	0.7	0.7	0.6	0.5	0.4	
08:00-09:00	1.0	0.8	0.7	0.6	0.5	0.5	
24 Hours Average	0.7	-	0.6	-	0.5	-	-
1 Hour Maximum	1.0	-	0.7	-	0.7	-	30
8 Hours Maximum	-	0.8	-	0.8	-	0.6	9

Remark : ^{1*} Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโบนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโบนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโบนหลวง หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : January 11-14, 2024
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : NOx Chemiluminescence Analyzer Horiba Model APNA-370 Serial Number YCPL4HTM

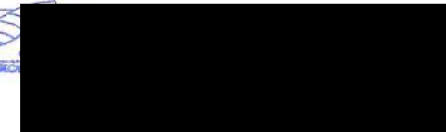
Quotation No. : 2023-01037
Analysis No. : 2024-AA095-004
Report No. : 2024-RAAB284
Report Date : January 20, 2024

Interval Time	Result (ppm)									Standard ¹
	Jan 11-12, 24			Jan 12-13, 24			Jan 13-14, 24			
	NO	NO ₂	NO _x	NO	NO ₂	NO _x	NO	NO ₂	NO _x	
10:00-11:00	0.0043	0.0132	0.0175	0.0067	0.0111	0.0178	0.0036	0.0065	0.0101	-
11:00-12:00	0.0051	0.0147	0.0198	0.0044	0.0103	0.0147	0.0035	0.0065	0.0100	
12:00-13:00	0.0053	0.0143	0.0196	0.0040	0.0087	0.0127	0.0051	0.0105	0.0156	
13:00-14:00	0.0049	0.0106	0.0155	0.0074	0.0115	0.0189	0.0045	0.0134	0.0179	
14:00-15:00	0.0038	0.0101	0.0139	0.0036	0.0068	0.0104	0.0038	0.0090	0.0128	
15:00-16:00	0.0037	0.0099	0.0136	0.0033	0.0060	0.0093	0.0034	0.0082	0.0116	
16:00-17:00	0.0036	0.0098	0.0134	0.0038	0.0077	0.0115	0.0034	0.0083	0.0117	
17:00-18:00	0.0036	0.0096	0.0132	0.0050	0.0091	0.0141	0.0036	0.0103	0.0139	
18:00-19:00	0.0034	0.0127	0.0161	0.0034	0.0087	0.0121	0.0034	0.0154	0.0188	
19:00-20:00	0.0033	0.0131	0.0164	0.0032	0.0085	0.0117	0.0034	0.0257	0.0291	
20:00-21:00	0.0039	0.0138	0.0177	0.0032	0.0080	0.0112	0.0037	0.0202	0.0239	
21:00-22:00	0.0045	0.0153	0.0198	0.0034	0.0136	0.0170	0.0075	0.0266	0.0341	
22:00-23:00	0.0048	0.0163	0.0211	0.0034	0.0116	0.0150	0.0039	0.0186	0.0225	
23:00-00:00	0.0047	0.0146	0.0193	0.0034	0.0107	0.0141	0.0037	0.0123	0.0160	
00:00-01:00	0.0042	0.0128	0.0170	0.0034	0.0127	0.0161	0.0035	0.0107	0.0142	
01:00-02:00	0.0052	0.0162	0.0214	0.0034	0.0120	0.0154	0.0035	0.0102	0.0137	
02:00-03:00	0.0064	0.0130	0.0194	0.0033	0.0096	0.0129	0.0041	0.0109	0.0150	
03:00-04:00	0.0060	0.0101	0.0161	0.0036	0.0082	0.0118	0.0035	0.0098	0.0133	
04:00-05:00	0.0047	0.0089	0.0136	0.0044	0.0087	0.0131	0.0110	0.0120	0.0230	
05:00-06:00	0.0054	0.0087	0.0141	0.0073	0.0121	0.0194	0.0060	0.0110	0.0170	
06:00-07:00	0.0064	0.0095	0.0159	0.0049	0.0099	0.0148	0.0035	0.0085	0.0121	
07:00-08:00	0.0064	0.0083	0.0147	0.0048	0.0094	0.0142	0.0035	0.0070	0.0105	
08:00-09:00	0.0156	0.0100	0.0256	0.0043	0.0103	0.0146	0.0039	0.0077	0.0116	
09:00-10:00	0.0147	0.0104	0.0251	0.0064	0.0087	0.0151	0.0045	0.0079	0.0124	
24 Hours Average	0.0056	0.0119	0.0175	0.0043	0.0097	0.0140	0.0043	0.0120	0.0163	
1 Hour Maximum	0.0156	0.0163	0.0256	0.0074	0.0136	0.0194	0.0110	0.0266	0.0341	

Remark : ^{1*} Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995), Notification No.28, B.E.2550 (2007), published in the Royal Government Gazette No.124 Special Part 58D dated May 14, B.E.2550 (2007) and Notification No.33, B.E.2552 (2009), published in the Royal Government Gazette No.125 Special Part 114D dated August 14, B.E.2552 (2009), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



Laboratory Supervisor

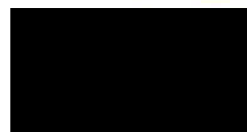
ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : January 11-14, 2024
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : SO₂ UV-Fluorescence Analyzer Horiba Model AP5A-370 Serial Number E5KBWB08

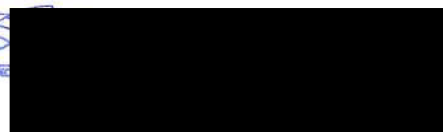
Quotation No. : 2023-01037
Analysis No. : 2024-AA095-004
Report No. : 2024-RAAB285
Report Date : January 20, 2024

Interval Time	Result SO ₂ (ppm)			Standard
	Jan 11-12, 24	Jan 12-13, 24	Jan 13-14, 24	
10:00-11:00	0.0027	0.0027	0.0027	0.12 ^{1*} 0.30 ^{2*}
11:00-12:00	0.0029	0.0027	0.0028	
12:00-13:00	0.0026	0.0025	0.0027	
13:00-14:00	0.0021	0.0027	0.0025	
14:00-15:00	0.0027	0.0026	0.0031	
15:00-16:00	0.0027	0.0025	0.0032	
16:00-17:00	0.0025	0.0024	0.0033	
17:00-18:00	0.0026	0.0025	0.0031	
18:00-19:00	0.0027	0.0024	0.0027	
19:00-20:00	0.0022	0.0022	0.0026	
20:00-21:00	0.0025	0.0021	0.0025	
21:00-22:00	0.0021	0.0018	0.0029	
22:00-23:00	0.0015	0.0014	0.0025	
23:00-00:00	0.0013	0.0013	0.0021	
00:00-01:00	0.0012	0.0011	0.0028	
01:00-02:00	0.0019	0.0014	0.0027	
02:00-03:00	0.0013	0.0013	0.0021	
03:00-04:00	0.0011	0.0025	0.0027	
04:00-05:00	0.0011	0.0022	0.0030	
05:00-06:00	0.0019	0.0023	0.0030	
06:00-07:00	0.0024	0.0033	0.0031	
07:00-08:00	0.0025	0.0033	0.0031	
08:00-09:00	0.0024	0.0020	0.0031	
09:00-10:00	0.0025	0.0031	0.0032	
24 Hours Average	0.0021	0.0023	0.0028	0.12^{1*}
1 Hour Maximum	0.0029	0.0033	0.0033	0.30^{2*}

Remark : ^{1*} Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995) and Notification No.24, B.E.2547 (2004), published in the Royal Government Gazette No.121 Special Part 104D dated September 22, B.E.2547 (2004), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).
^{2*} Notification of National Environmental Board, No.12, B.E.2538 (1995), published in the Royal Government Gazette No.112 Special Part 27D dated July 13, B.E.2538 (1995) and Notification No.21, B.E.2544 (2001), published in the Royal Government Gazette No.118 Special Part 35D dated April 30, B.E.2544 (2001), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : January 11-14, 2024
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : CO NDIR Analyzer Horiba Model APMA-370 Serial Number SFB4TS99

Quotation No. : 2023-01037
Analysis No. : 2024-AA095-004
Report No. : 2024-RAAB285
Report Date : January 20, 2024

Interval Time	Result CO (ppm)						Standard ^{1*}
	Jan 11-12, 24		Jan 12-13, 24		Jan 13-14, 24		
	1 hr Avg	8 hr Avg	1 hr Avg	8 hr Avg	1 hr Avg	8 hr Avg	
10:00-11:00	0.6	-	0.6	0.7	0.5	0.5	0.12 ^{1*} 0.30 ^{2*}
11:00-12:00	0.6	-	0.6	0.7	0.4	0.5	
12:00-13:00	0.5	-	0.5	0.6	0.4	0.5	
13:00-14:00	0.5	-	0.5	0.6	0.3	0.5	
14:00-15:00	0.5	-	0.5	0.6	0.4	0.4	
15:00-16:00	0.4	-	0.5	0.6	0.4	0.4	
16:00-17:00	0.5	-	0.4	0.5	0.4	0.4	
17:00-18:00	0.4	0.5	0.4	0.5	0.4	0.4	
18:00-19:00	0.5	0.5	0.5	0.5	0.4	0.4	
19:00-20:00	0.5	0.5	0.5	0.5	0.5	0.4	
20:00-21:00	0.7	0.5	0.5	0.5	0.6	0.4	
21:00-22:00	0.8	0.5	0.5	0.5	0.6	0.5	
22:00-23:00	0.8	0.6	0.5	0.5	0.6	0.5	
23:00-00:00	0.7	0.6	0.7	0.5	0.7	0.5	
00:00-01:00	0.7	0.6	0.6	0.5	0.4	0.5	
01:00-02:00	0.7	0.7	0.5	0.5	0.4	0.5	
02:00-03:00	0.7	0.7	0.5	0.5	0.4	0.5	
03:00-04:00	0.7	0.7	0.5	0.5	0.4	0.5	
04:00-05:00	0.7	0.7	0.5	0.5	0.4	0.5	
05:00-06:00	0.7	0.7	0.5	0.5	0.4	0.5	
06:00-07:00	0.7	0.7	0.6	0.6	0.4	0.4	
07:00-08:00	0.6	0.7	0.6	0.5	0.4	0.4	
08:00-09:00	0.7	0.7	0.4	0.5	0.5	0.4	
09:00-10:00	0.7	0.7	0.5	0.5	0.5	0.4	
24 Hours Average	0.6	-	0.5	-	0.5	-	-
1 Hour Maximum	0.8	-	0.7	-	0.7	-	30
8 Hours Maximum	-	0.7	-	0.7	-	0.5	9

Remark : ^{1*} Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



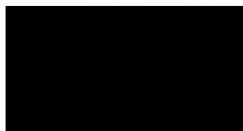
Laboratory Supervisor

ANALYSIS REPORT

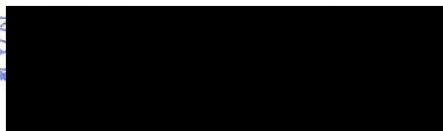
Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลวง หมู่ที่ 5 ตำบลโนนพลวง อำเภอลานกระบี่ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589993 E, 1832896 N
Measured Date : January 11-14, 2024
Measured By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Quotation No. : 2023-01037
Analysis No. : 2024-AA095-001 - 003
Report No. : 2024-RAAB221
Report Date : January 20, 2024

Data/Time	Jan 11-12, 24		Jan 12-13, 24		Jan 13-14, 24	
	WS	WD	WS	WD	WS	WD
09:00-10:00	0.4	N	0.4	SE	0.4	ENE
10:00-11:00	1.3	SSE	1.3	SSE	2.2	SE
11:00-12:00	1.8	SSE	1.3	SSW	3.1	SSE
12:00-13:00	2.2	SSE	1.8	SE	2.7	SSE
13:00-14:00	2.2	SSE	1.8	S	2.7	SSE
14:00-15:00	2.7	SSE	2.2	SE	2.2	SSE
15:00-16:00	2.7	SE	2.2	SE	2.2	SSE
16:00-17:00	2.2	SSE	2.2	SE	1.8	SSE
17:00-18:00	2.2	SSE	1.3	ESE	1.8	SE
18:00-19:00	1.3	SE	0.9	ESE	1.3	SE
19:00-20:00	0.4	SE	<0.4	Calm	0.4	SE
20:00-21:00	0.9	SE	<0.4	Calm	<0.4	Calm
21:00-22:00	<0.4	Calm	0.4	ENE	<0.4	Calm
22:00-23:00	<0.4	Calm	0.4	SSE	<0.4	Calm
23:00-00:00	0.4	N	0.4	N	0.9	E
00:00-01:00	0.4	WNW	0.4	W	2.2	SSW
01:00-02:00	0.9	SSE	0.4	WSW	1.8	S
02:00-03:00	0.4	N	0.4	ENE	1.8	SSE
03:00-04:00	0.4	SE	<0.4	Calm	0.4	W
04:00-05:00	0.9	SE	<0.4	Calm	0.4	SW
05:00-06:00	0.4	SSE	<0.4	Calm	0.4	SSW
06:00-07:00	0.4	NW	<0.4	Calm	0.4	E
07:00-08:00	<0.4	Calm	<0.4	Calm	0.4	ENE
08:00-09:00	<0.4	Calm	0.4	ENE	0.4	W

Remark : WS = Wind Speed (m/s)
WD = Wind Direction
Height of wind vane and anemometer above ground 10 meters.



Laboratory Reviewer



Laboratory Supervisor

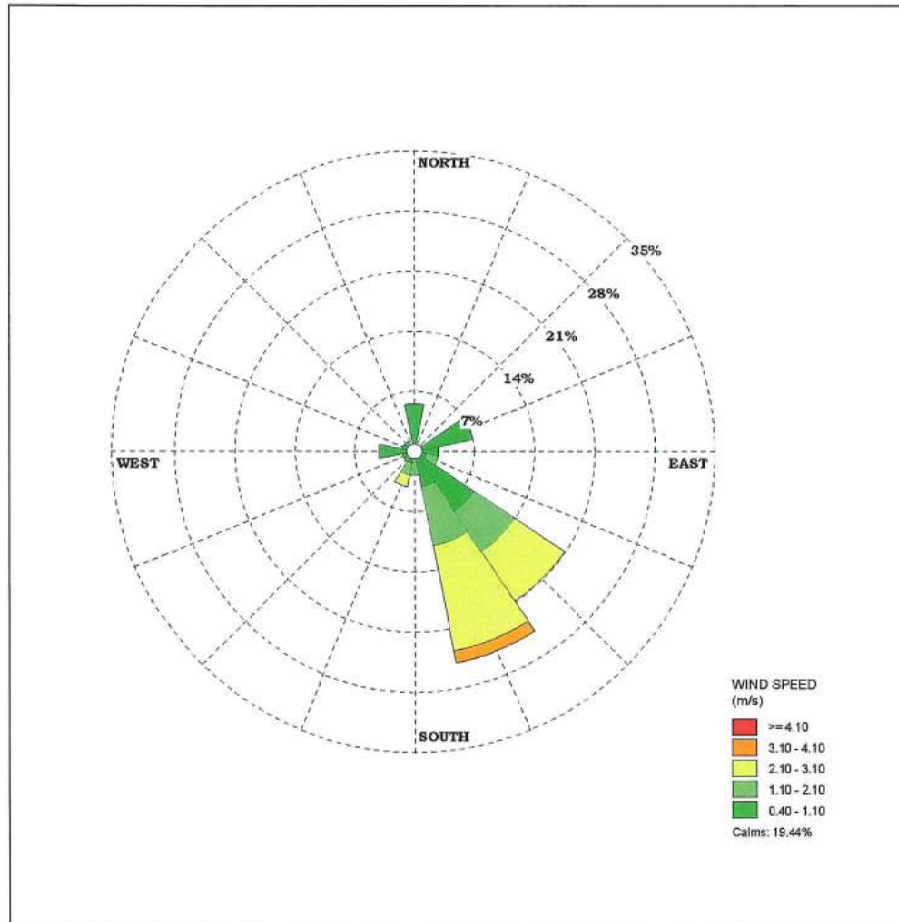
ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลวง หมู่ที่ 5 ตำบลโนนพลวง อำเภอลานกระบี่ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589993 E, 1832896 N
Measured Date : January 11-14, 2024
Measured By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Quotation No. : 2023-01037
Analysis No. : 2024-AA095-001 - 003
Report No. : 2024-RAAB221
Report Date : January 20, 2024

Wind Direction	Percentage frequency of wind in each speed and direction					Total
	0.4-1.1	1.1-2.1	2.1-3.1	3.1-4.1	≥4.1	
N	5.55556	0.00000	0.00000	0.00000	0.00000	5.55556
NNE	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NE	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
ENE	6.94444	0.00000	0.00000	0.00000	0.00000	6.94444
E	2.77778	0.00000	0.00000	0.00000	0.00000	2.77778
ESE	1.38889	1.38889	0.00000	0.00000	0.00000	2.77778
SE	8.33333	5.55556	6.94444	0.00000	0.00000	20.83333
SSE	4.16667	6.94444	12.50000	1.38889	0.00000	25.00000
S	0.00000	2.77778	0.00000	0.00000	0.00000	2.77778
SSW	1.38889	1.38889	1.38889	0.00000	0.00000	4.16667
SW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
WSW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
W	4.16667	0.00000	0.00000	0.00000	0.00000	4.16667
WNW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
NW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
NNW	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
Calm	19.44440					

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลองส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลอง-อี (NPG-E))
Measured Point : บริเวณบ้านเลขที่ 25/1 ป่านโนนพลอง หมู่ที่ 5 ตำบลโนนพลอง อำเภอลานกระบือ จังหวัดกำแพงเพชร
Measured Date : January 11-14, 2024
Report No. : 2024-RAAB221



ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลองส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลอง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 ป่านโนนพลอง หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : January 11-14, 2024
Measured By : [Redacted]
Analyzed By : Environment Research & Technology Co., Ltd.

Quotation No. : 2023-01037
Analysis No. : 2024-AA095-004 - 005
Report No. : 2024-RAAB222
Report Date : January 20, 2024

Date/Time	Jan 11-12, 24		Jan 12-13, 24		Jan 13-14, 24	
	WS	WD	WS	WD	WS	WD
10:00-11:00	1.3	SSE	0.9	SSE	1.8	SE
11:00-12:00	1.8	SSE	0.9	SSW	2.7	SE
12:00-13:00	1.8	SSE	1.3	SSW	2.2	SE
13:00-14:00	2.2	SSE	1.8	SSW	2.2	SSE
14:00-15:00	2.2	SSE	1.8	SSE	1.8	S
15:00-16:00	2.2	SE	1.8	SE	2.2	ESE
16:00-17:00	1.8	S	1.8	SSE	1.8	SE
17:00-18:00	1.8	SE	1.8	ESE	1.8	SE
18:00-19:00	1.3	SE	0.9	ESE	0.9	ESE
19:00-20:00	0.4	ESE	<0.4	Calm	0.4	ESE
20:00-21:00	0.4	ESE	0.9	ENE	<0.4	Calm
21:00-22:00	<0.4	Calm	<0.4	Calm	0.4	ENE
22:00-23:00	<0.4	Calm	<0.4	Calm	<0.4	Calm
23:00-00:00	<0.4	Calm	<0.4	Calm	0.4	ENE
00:00-01:00	<0.4	Calm	0.4	WNW	1.3	SSW
01:00-02:00	0.4	SE	<0.4	Calm	1.8	S
02:00-03:00	<0.4	Calm	0.4	NW	1.3	SE
03:00-04:00	<0.4	Calm	<0.4	Calm	<0.4	Calm
04:00-05:00	0.4	SE	<0.4	Calm	<0.4	Calm
05:00-06:00	<0.4	Calm	<0.4	Calm	<0.4	Calm
06:00-07:00	<0.4	Calm	<0.4	Calm	0.4	ENE
07:00-08:00	<0.4	Calm	<0.4	Calm	<0.4	Calm
08:00-09:00	<0.4	Calm	0.4	ENE	<0.4	Calm
09:00-10:00	0.4	WSW	0.4	ENE	<0.4	Calm

Remark : WS = Wind Speed (m/s)
WD = Wind Direction
Height of wind vane and anemometer above ground 10 meters.

[Redacted Signature]

Laboratory Reviewer

[Redacted Signature]

Laboratory Supervisor

ANALYSIS REPORT

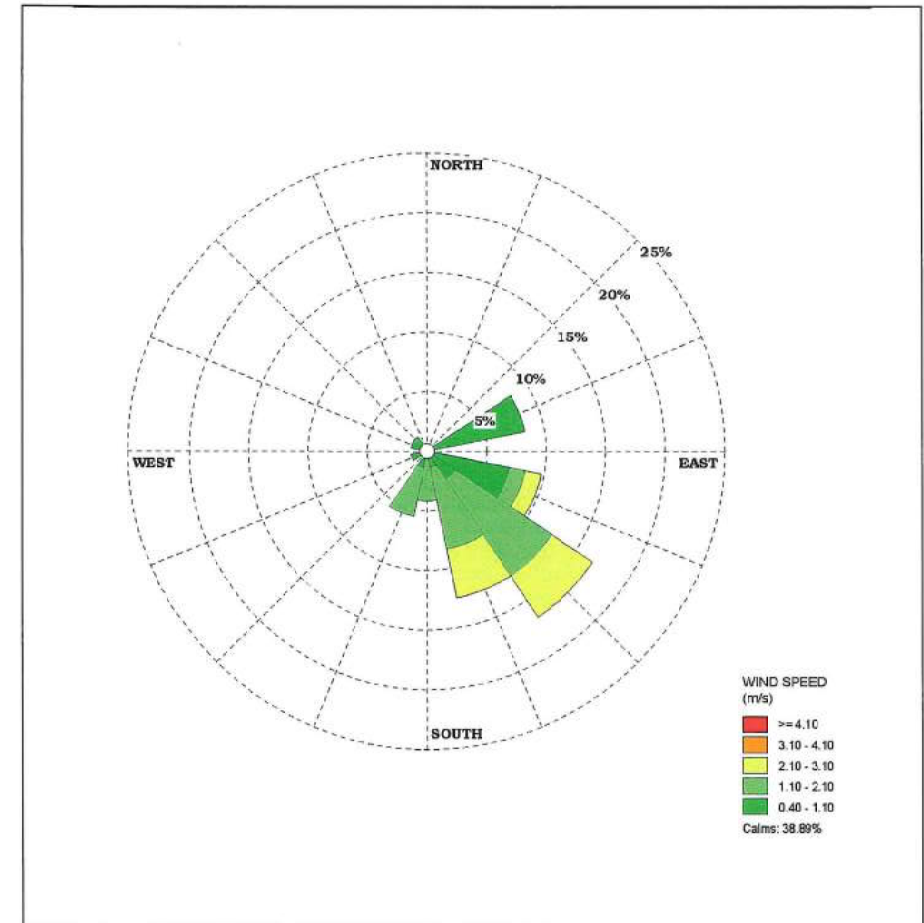
Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งในหลวงส่วนขยาย แปลงเลข 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตในหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : January 11-14, 2024
Measured By : 
Analyzed By : Environment Research & Technology Co., Ltd.

Quotation No. : 2023-01037
Analysis No. : 2024-AAC95-004 - 006
Report No. : 2024-RAAB222
Report Date : January 20, 2024

Wind Direction	Percentage frequency of wind in each speed and direction					Total
	0.4-1.1	1.1-2.1	2.1-3.1	3.1-4.1	≥4.1	
N	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NNE	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NE	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
ENE	8.33333	0.00000	0.00000	0.00000	0.00000	8.33333
E	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
ESE	6.94444	1.38889	1.38889	0.00000	0.00000	9.72222
SE	2.77778	9.72222	4.16667	0.00000	0.00000	16.66657
SSE	1.38889	6.94444	4.16667	0.00000	0.00000	12.50000
S	0.00000	4.16667	0.00000	0.00000	0.00000	4.16667
SSW	1.38889	4.16667	0.00000	0.00000	0.00000	5.55556
SW	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
WSW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
W	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
WNW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
NW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
NNW	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
Calm	38.88890					

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Project Name : โครงการผลิตปิโตรเลียมแหล่งในหลวงส่วนขยาย แปลงเลข 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตในหลวง-อี (NPG-E))
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
Measured Date : January 11-14, 2024
Report No. : 2024-RAAB222



ฤดูฝน

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งในพลาญส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตในพลาญ-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Ambient Air Quality
Sampling Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลาญ หมู่ที่ 5 ตำบลโนนพลาญ อำเภอสามโก้ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589993 E, 1832898 N
Sampling Date : August 6-9, 2023
Sampling Time : 07:55
Sampling Method : U.S. EPA 40 CFR Part 50
Sampling By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.

Quotation No. : 2023-01005
Folder No. : 2023-AD376
Received Date : August 11, 2023
Analytical Date : August 11-18, 2023
Report No. : 2023-RAAP843
Report Date : August 21, 2023

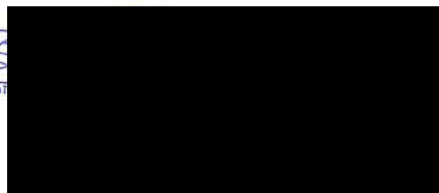
Parameter	Unit	Method of Analysis	Result			Standard ¹⁾
			Aug 6-7, 23	Aug 7-8, 23	Aug 8-9, 23	
Total Suspended Particulate (TSP) 24 Hours Average	mg/m ³	High-Volume, Gravimetric	0.064	0.051	0.058	0.330
Particulate Size Less Than 10 Micron (PM10) 24 Hours Average	mg/m ³	PM10 Size Selective, High-Volume, Gravimetric	0.030	0.023	0.024	0.120

Remark : ¹⁾ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995) and Notification No.24, B.E.2547 (2004), published in the Royal Government Gazette No.121 Special Part: 104D dated September 22, B.E.2547 (2004), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



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ENVIRONMENT RESEARCH & TECHNOLOGY CO., LTD.

Laboratory Reviewer



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ENVIRONMENT RESEARCH & TECHNOLOGY CO., LTD.

Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งในพลาญส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตในพลาญ-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Ambient Air Quality
Sampling Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนพลาญ หมู่ที่ 6 ตำบลลานกระบือ อำเภอสามโก้ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Sampling Date : August 6-9, 2023
Sampling Time : 08:55
Sampling Method : U.S. EPA 40 CFR Part 50
Sampling By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.

Quotation No. : 2023-01005
Folder No. : 2023-AD376
Received Date : August 11, 2023
Analytical Date : August 11-18, 2023
Report No. : 2023-RAAP844
Report Date : August 21, 2023

Parameter	Unit	Method of Analysis	Result			Standard ¹⁾
			Aug 6-7, 23	Aug 7-8, 23	Aug 8-9, 23	
Total Suspended Particulate (TSP) 24 Hours Average	mg/m ³	High-Volume, Gravimetric	0.052	0.030	0.035	0.330
Particulate Size Less Than 10 Micron (PM10) 24 Hours Average	mg/m ³	PM10 Size Selective, High-Volume, Gravimetric	0.028	0.016	0.019	0.120

Remark : ¹⁾ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 42D dated May 25, B.E.2538 (1995) and Notification No.24, B.E.2547 (2004), published in the Royal Government Gazette No.121 Special Part: 104D dated September 22, B.E.2547 (2004), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



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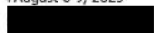
Laboratory Reviewer



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ENVIRONMENT RESEARCH & TECHNOLOGY CO., LTD.

Laboratory Supervisor

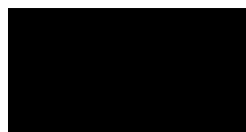
ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeaya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนหลวง หมู่ที่ 5 ตำบลโนนหลวง อำเภอสามโก้ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589993 E, 1832898 N
Measured Date : August 6-9, 2023
Measured By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : CO NDIR Analyzer Horiba Model APMA-370 Serial Number XRP3Y7LA

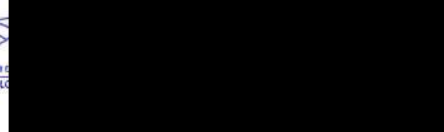
Quotation No. : 2023-01005
Analysis No. : 2023-AD375-001
Report No. : 2023-RAAQ755
Report Date : September 5, 2023

Interval Time	Result CO (ppm)						Standard ¹⁾
	Aug 6-7, 23		Aug 7-8, 23		Aug 8-9, 23		
	1 hr Avg	8 hr Avg	1 hr Avg	8 hr Avg	1 hr Avg	8 hr Avg	
08:00-09:00	0.4	-	0.4	0.3	0.4	0.3	-
09:00-10:00	0.4	-	0.4	0.3	0.4	0.3	
10:00-11:00	0.4	-	0.3	0.3	0.4	0.4	
11:00-12:00	0.5	-	0.4	0.3	0.5	0.4	
12:00-13:00	0.5	-	0.4	0.4	0.5	0.4	
13:00-14:00	0.5	-	0.3	0.4	0.4	0.4	
14:00-15:00	0.6	-	0.4	0.4	0.5	0.4	
15:00-16:00	0.6	0.5	0.4	0.4	0.5	0.4	
16:00-17:00	0.6	0.5	0.3	0.4	0.5	0.5	
17:00-18:00	0.4	0.5	0.4	0.4	0.6	0.5	
18:00-19:00	0.3	0.5	0.4	0.4	0.5	0.5	
19:00-20:00	0.2	0.5	0.3	0.4	0.4	0.5	
20:00-21:00	0.3	0.4	0.2	0.3	0.5	0.5	
21:00-22:00	0.3	0.4	0.3	0.3	0.4	0.5	
22:00-23:00	0.3	0.4	0.2	0.3	0.4	0.5	
23:00-00:00	0.3	0.3	0.3	0.3	0.3	0.4	
00:00-01:00	0.3	0.3	0.2	0.3	0.3	0.4	
01:00-02:00	0.2	0.3	0.3	0.3	0.2	0.4	
02:00-03:00	0.3	0.3	0.3	0.3	0.3	0.4	
03:00-04:00	0.3	0.3	0.4	0.3	0.3	0.3	
04:00-05:00	0.2	0.3	0.3	0.3	0.2	0.3	
05:00-06:00	0.3	0.3	0.3	0.3	0.2	0.3	
06:00-07:00	0.4	0.3	0.3	0.3	0.2	0.2	
07:00-08:00	0.3	0.3	0.3	0.3	0.3	0.2	
24 Hours Average	0.4	-	0.3	-	0.4	-	-
1 Hour Maximum	0.6	-	0.4	-	0.6	-	30
8 Hours Maximum	-	0.5	-	0.4	-	0.5	9

Remark : ¹⁾ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 420 dated May 25, B.E.2538 (1995), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).

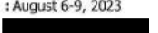


Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeaya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนหลวง หมู่ที่ 5 ตำบลโนนหลวง อำเภอสามโก้ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589993 E, 1832898 N
Measured Date : August 6-9, 2023
Measured By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : NOx Chemiluminescence Analyzer Horiba Model APNA-370 Serial Number KCDVY226

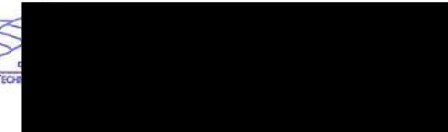
Quotation No. : 2023-01005
Analysis No. : 2023-AD376-001
Report No. : 2023-RAAQ766
Report Date : September 5, 2023

Interval Time	Result (ppm)									Standard ¹⁾
	Aug 6-7, 23			Aug 7-8, 23			Aug 8-9, 23			
	NO	NO ₂	NO _x	NO	NO ₂	NO _x	NO	NO ₂	NO _x	
08:00-09:00	0.0040	0.0070	0.0110	0.0027	0.0073	0.0100	0.0026	0.0093	0.0109	-
09:00-10:00	0.0030	0.0068	0.0098	0.0029	0.0075	0.0104	0.0034	0.0094	0.0118	
10:00-11:00	0.0043	0.0067	0.0110	0.0020	0.0075	0.0095	0.0021	0.0090	0.0101	
11:00-12:00	0.0099	0.0076	0.0175	0.0018	0.0075	0.0093	0.0023	0.0090	0.0108	
12:00-13:00	0.0043	0.0074	0.0117	0.0019	0.0079	0.0098	0.0023	0.0095	0.0108	
13:00-14:00	0.0024	0.0071	0.0095	0.0026	0.0077	0.0103	0.0023	0.0091	0.0101	
14:00-15:00	0.0023	0.0072	0.0095	0.0058	0.0081	0.0139	0.0015	0.0090	0.0096	
15:00-16:00	0.0019	0.0074	0.0093	0.0037	0.0082	0.0119	0.0019	0.0081	0.0099	
16:00-17:00	0.0020	0.0077	0.0097	0.0017	0.0078	0.0095	0.0015	0.0081	0.0096	
17:00-18:00	0.0019	0.0078	0.0097	0.0016	0.0080	0.0096	0.0014	0.0079	0.0093	
18:00-19:00	0.0023	0.0076	0.0099	0.0016	0.0082	0.0098	0.0017	0.0081	0.0098	
19:00-20:00	0.0021	0.0075	0.0096	0.0016	0.0083	0.0099	0.0018	0.0086	0.0104	
20:00-21:00	0.0021	0.0078	0.0099	0.0014	0.0088	0.0102	0.0018	0.0086	0.0104	
21:00-22:00	0.0026	0.0080	0.0106	0.0016	0.0086	0.0102	0.0016	0.0083	0.0099	
22:00-23:00	0.0025	0.0077	0.0102	0.0016	0.0085	0.0101	0.0014	0.0079	0.0093	
23:00-00:00	0.0023	0.0076	0.0099	0.0015	0.0087	0.0102	0.0016	0.0079	0.0095	
00:00-01:00	0.0024	0.0077	0.0101	0.0014	0.0088	0.0102	0.0015	0.0079	0.0094	
01:00-02:00	0.0025	0.0077	0.0103	0.0013	0.0083	0.0096	0.0013	0.0079	0.0092	
02:00-03:00	0.0024	0.0078	0.0102	0.0017	0.0083	0.0100	0.0015	0.0079	0.0094	
03:00-04:00	0.0022	0.0075	0.0097	0.0018	0.0083	0.0101	0.0015	0.0078	0.0093	
04:00-05:00	0.0024	0.0076	0.0100	0.0017	0.0084	0.0101	0.0014	0.0075	0.0089	
05:00-06:00	0.0024	0.0077	0.0101	0.0022	0.0085	0.0107	0.0014	0.0076	0.0090	
06:00-07:00	0.0025	0.0075	0.0100	0.0021	0.0086	0.0107	0.0019	0.0081	0.0100	
07:00-08:00	0.0021	0.0073	0.0094	0.0035	0.0087	0.0122	0.0024	0.0080	0.0104	
24 Hours Average	0.0029	0.0075	0.0104	0.0022	0.0082	0.0104	0.0018	0.0081	0.0099	-
1 Hour Maximum	0.0099	0.0080	0.0175	0.0058	0.0088	0.0139	0.0034	0.0086	0.0118	0.17

Remark : ¹⁾ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 420 dated May 25, B.E.2538 (1995), Notification No.28, B.E.2550 (2007), published in the Royal Government Gazette No.124 Special Part 560 dated May 14, B.E.2550 (2007), and Notification No.33, B.E.2552 (2009), published in the Royal Government Gazette No.126 Special Part 1140 dated August 14, B.E.2552 (2009), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการพัฒนาระบบบำบัดน้ำเสียชุมชนตำบลบางปลา อำเภอบางพลี จังหวัดนนทบุรี (ฐานหลุมฝังกลบหนอง-อี (NPG-E))
Project Location : จังหวัดนนทบุรี
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลาญ หมู่ที่ 5 ตำบลโนนพลาญ อำเภอสามโคก จังหวัดนนทบุรี
GPS. Coordinate : UTM (WGS84) 47Q 0589993 E, 1832898 N
Measured Date : August 6-9, 2023
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : SO₂ UV-Fluorescence Analyzer Thermo Model 43C Serial Number 0335804029

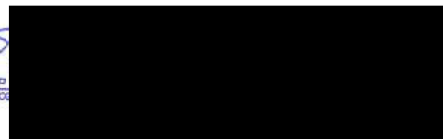
Quotation No. : 2023-C1005
Analysis No. : 2023-AD376-001
Report No. : 2023-RAAQ757
Report Date : September 5, 2023

Interval Time	Result SO ₂ (ppm)			Standard
	Aug 6-7, 23	Aug 7-8, 23	Aug 8-9, 23	
08:00-09:00	0.0013	0.0015	0.0016	
09:00-10:00	0.0014	0.0015	0.0016	
10:00-11:00	0.0013	0.0016	0.0015	
11:00-12:00	0.0012	0.0015	0.0016	
12:00-13:00	0.0011	0.0015	0.0015	
13:00-14:00	0.0011	0.0015	0.0016	
14:00-15:00	0.0011	0.0014	0.0015	
15:00-16:00	0.0011	0.0015	0.0014	
16:00-17:00	0.0011	0.0014	0.0015	
17:00-18:00	0.0012	0.0014	0.0014	
18:00-19:00	0.0013	0.0014	0.0014	
19:00-20:00	0.0012	0.0014	0.0014	
20:00-21:00	0.0014	0.0015	0.0015	
21:00-22:00	0.0013	0.0015	0.0014	
22:00-23:00	0.0014	0.0015	0.0014	
23:00-00:00	0.0014	0.0015	0.0015	
00:00-01:00	0.0015	0.0015	0.0016	
01:00-02:00	0.0015	0.0015	0.0014	
02:00-03:00	0.0015	0.0015	0.0014	
03:00-04:00	0.0015	0.0015	0.0015	
04:00-05:00	0.0015	0.0015	0.0015	
05:00-06:00	0.0015	0.0015	0.0014	
06:00-07:00	0.0015	0.0015	0.0014	
07:00-08:00	0.0015	0.0015	0.0014	
24 Hours Average	0.0013	0.0015	0.0015	0.12 ^{1*}
1 Hour Maximum	0.0015	0.0016	0.0016	0.30 ^{2*}

Remark : ^{1*} Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 420 dated May 25, B.E.2538 (1995) and Notification No.24, B.E.2547 (2004), published in the Royal Government Gazette No.121 Special Part 1040 dated September 22, B.E.2547 (2004), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).
^{2*} Notification of National Environmental Board, No.12, B.E.2538 (1995), published in the Royal Government Gazette No.112 Special Part 270 dated July 13, B.E.2538 (1995) and Notification No.21, B.E.2544 (2001), published in the Royal Government Gazette No.118 Special Part 390 dated April 30, B.E.2544 (2001), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการพัฒนาระบบบำบัดน้ำเสียชุมชนตำบลบางปลา อำเภอบางพลี จังหวัดนนทบุรี (ฐานหลุมฝังกลบหนอง-อี (NPG-E))
Project Location : จังหวัดนนทบุรี
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลำนกกระจิก อำเภอสามโคก จังหวัดนนทบุรี
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : August 6-9, 2023
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : CO NDIR Analyzer Horiba Model APMA-370 Serial Number Y05LRYAD

Quotation No. : 2023-01005
Analysis No. : 2023-AD376-004
Report No. : 2023-RAAQ768
Report Date : September 5, 2023

Interval Time	Result CO (ppm)						Standard ^{1*}
	Aug 6-7, 23		Aug 7-8, 23		Aug 8-9, 23		
	1 hr Avg	8 hr Avg	1 hr Avg	8 hr Avg	1 hr Avg	8 hr Avg	
09:00-10:00	0.5	-	0.4	0.4	0.4	0.4	
10:00-11:00	0.5	-	0.4	0.4	0.4	0.4	
11:00-12:00	0.5	-	0.4	0.4	0.4	0.4	
12:00-13:00	0.5	-	0.4	0.4	0.4	0.4	
13:00-14:00	0.4	-	0.4	0.4	0.4	0.4	
14:00-15:00	0.4	-	0.4	0.4	0.4	0.4	
15:00-16:00	0.4	-	0.4	0.4	0.4	0.4	
16:00-17:00	0.4	0.4	0.4	0.4	0.4	0.4	
17:00-18:00	0.4	0.4	0.4	0.4	0.4	0.4	
18:00-19:00	0.4	0.4	0.4	0.4	0.3	0.4	
19:00-20:00	0.3	0.4	0.4	0.4	0.4	0.4	
20:00-21:00	0.3	0.4	0.4	0.4	0.4	0.4	
21:00-22:00	0.3	0.4	0.4	0.4	0.4	0.4	
22:00-23:00	0.3	0.4	0.4	0.4	0.4	0.4	
23:00-00:00	0.5	0.4	0.4	0.4	0.3	0.4	
00:00-01:00	0.5	0.4	0.4	0.4	0.3	0.4	
01:00-02:00	0.5	0.4	0.4	0.4	0.3	0.4	
02:00-03:00	0.5	0.4	0.4	0.4	0.3	0.4	
03:00-04:00	0.5	0.4	0.4	0.4	0.3	0.3	
04:00-05:00	0.3	0.4	0.4	0.4	0.3	0.3	
05:00-06:00	0.4	0.4	0.4	0.4	0.3	0.3	
06:00-07:00	0.2	0.4	0.4	0.4	0.3	0.3	
07:00-08:00	0.3	0.4	0.4	0.4	0.3	0.3	
08:00-09:00	0.4	0.4	0.4	0.4	0.3	0.3	
24 Hours Average	0.4	-	0.4	-	0.4	-	-
1 Hour Maximum	0.5	-	0.4	-	0.4	-	30
8 Hours Maximum	-	0.4	-	0.4	-	0.4	9

Remark : ^{1*} Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 420 dated May 25, B.E.2538 (1995), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

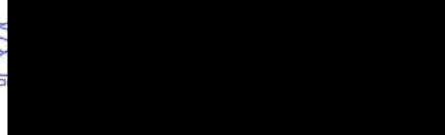
Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตไฟฟ้าโดยพลังงานแสงอาทิตย์ในฟาร์มหลวงสงขลานครินทร์ (NPG-E)
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : August 6-9, 2023
Measured By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : NOx Chemiluminescence Analyzer Horiba Model APNA-360CE Serial Number 8517870114

Interval Time	Result (ppm)									Standard ¹
	Aug 6-7, 23			Aug 7-8, 23			Aug 8-9, 23			
	NO	NO ₂	NO _x	NO	NO ₂	NO _x	NO	NO ₂	NO _x	
09:00-10:00	0.0035	0.0060	0.0095	0.0043	0.0053	0.0096	0.0044	0.0062	0.0106	-
10:00-11:00	0.0041	0.0062	0.0103	0.0040	0.0055	0.0095	0.0045	0.0067	0.0112	
11:00-12:00	0.0054	0.0064	0.0118	0.0039	0.0057	0.0096	0.0043	0.0060	0.0103	
12:00-13:00	0.0043	0.0055	0.0098	0.0044	0.0054	0.0098	0.0042	0.0060	0.0102	
13:00-14:00	0.0043	0.0052	0.0095	0.0042	0.0059	0.0101	0.0045	0.0071	0.0116	
14:00-15:00	0.0044	0.0059	0.0103	0.0041	0.0057	0.0098	0.0043	0.0073	0.0116	
15:00-16:00	0.0044	0.0055	0.0099	0.0038	0.0054	0.0092	0.0041	0.0062	0.0103	
15:00-17:00	0.0041	0.0051	0.0092	0.0042	0.0050	0.0092	0.0038	0.0058	0.0096	
17:00-18:00	0.0042	0.0055	0.0097	0.0040	0.0055	0.0095	0.0039	0.0056	0.0095	
18:00-19:00	0.0043	0.0062	0.0105	0.0042	0.0058	0.0100	0.0039	0.0061	0.0100	
19:00-20:00	0.0048	0.0076	0.0124	0.0044	0.0059	0.0113	0.0045	0.0072	0.0117	
20:00-21:00	0.0044	0.0072	0.0116	0.0049	0.0071	0.0120	0.0045	0.0077	0.0122	
21:00-22:00	0.0043	0.0059	0.0102	0.0043	0.0059	0.0102	0.0040	0.0066	0.0106	
22:00-23:00	0.0039	0.0056	0.0095	0.0041	0.0057	0.0098	0.0038	0.0059	0.0097	
23:00-00:00	0.0038	0.0050	0.0098	0.0040	0.0060	0.0100	0.0039	0.0065	0.0104	
00:00-01:00	0.0046	0.0064	0.0110	0.0042	0.0068	0.0110	0.0040	0.0066	0.0106	
01:00-02:00	0.0049	0.0069	0.0118	0.0049	0.0071	0.0120	0.0043	0.0072	0.0115	
02:00-03:00	0.0028	0.0050	0.0078	0.0049	0.0072	0.0121	0.0043	0.0082	0.0125	
03:00-04:00	0.0047	0.0070	0.0117	0.0044	0.0059	0.0103	0.0040	0.0062	0.0102	
04:00-05:00	0.0041	0.0059	0.0100	0.0041	0.0066	0.0107	0.0040	0.0056	0.0096	
05:00-06:00	0.0030	0.0044	0.0074	0.0040	0.0072	0.0112	0.0039	0.0057	0.0096	
06:00-07:00	0.0036	0.0061	0.0097	0.0043	0.0077	0.0120	0.0041	0.0065	0.0106	
07:00-08:00	0.0020	0.0040	0.0060	0.0047	0.0080	0.0127	0.0047	0.0068	0.0115	
08:00-09:00	0.0044	0.0066	0.0110	0.0052	0.0077	0.0129	0.0048	0.0072	0.0120	
24 Hours Average	0.0041	0.0059	0.0100	0.0043	0.0063	0.0106	0.0042	0.0065	0.0107	-
1 Hour Maximum	0.0054	0.0076	0.0124	0.0052	0.0080	0.0129	0.0048	0.0082	0.0125	0.17

Remark : ¹ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 420 dated May 25, B.E.2538 (1995), Notification No.28, B.E.2550 (2007), published in the Royal Government Gazette No.124 Special Part 580 dated May 14, B.E.2550 (2007) and Notification No.33, B.E.2551 (2009), published in the Royal Government Gazette No.126 Special Part 1140 dated August 14, B.E.2552 (2009), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).




Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

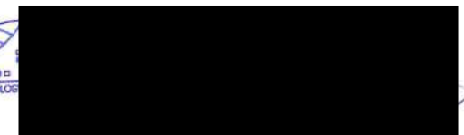
Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตไฟฟ้าโดยพลังงานแสงอาทิตย์ในฟาร์มหลวงสงขลานครินทร์ (NPG-E)
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : August 6-9, 2023
Measured By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : SO₂ UV-Fluorescence Analyzer Horiba Model APSA-370 Serial Number V4HC9062

Interval Time	Result SO ₂ (ppm)			Standard
	Aug 6-7, 23	Aug 7-8, 23	Aug 8-9, 23	
09:00-10:00	0.0011	0.0015	0.0013	-
10:00-11:00	0.0012	0.0015	0.0014	
11:00-12:00	0.0013	0.0015	0.0014	
12:00-13:00	0.0013	0.0012	0.0013	
13:00-14:00	0.0014	0.0011	0.0013	
14:00-15:00	0.0015	0.0011	0.0013	
15:00-16:00	0.0016	0.0013	0.0014	
16:00-17:00	0.0018	0.0012	0.0014	
17:00-18:00	0.0013	0.0012	0.0011	
18:00-19:00	0.0012	0.0011	0.0012	
19:00-20:00	0.0012	0.0014	0.0012	
20:00-21:00	0.0011	0.0014	0.0013	
21:00-22:00	0.0014	0.0014	0.0012	
22:00-23:00	0.0017	0.0015	0.0013	
23:00-00:00	0.0017	0.0013	0.0012	
00:00-01:00	0.0018	0.0014	0.0012	
01:00-02:00	0.0017	0.0014	0.0013	
02:00-03:00	0.0014	0.0015	0.0012	
03:00-04:00	0.0015	0.0014	0.0012	
04:00-05:00	0.0014	0.0014	0.0013	
05:00-06:00	0.0014	0.0014	0.0012	
06:00-07:00	0.0013	0.0014	0.0013	
07:00-08:00	0.0015	0.0013	0.0014	
08:00-09:00	0.0016	0.0012	0.0012	
24 Hours Average	0.0014	0.0013	0.0013	0.12 ¹
1 Hour Maximum	0.0018	0.0015	0.0014	0.30 ²

Remark : ¹ Notification of National Environmental Board, No.10, B.E.2538 (1995), published in the Royal Government Gazette No.112 Part 420 dated May 25, B.E.2538 (1995) and Notification No.24, B.E.2547 (2004), published in the Royal Government Gazette No.121 Special Part 1040 dated September 22, B.E.2547 (2004), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).
² Notification of National Environmental Board, No.12, B.E.2538 (1995), published in the Royal Government Gazette No.112 Special Part 270 dated July 13, B.E.2538 (1995) and Notification No.29, B.E.2544 (2001), published in the Royal Government Gazette No.116 Special Part 350 dated April 30, B.E.2544 (2001), under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนหลวง หมู่ที่ 5 ตำบลโนนหลวง อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589990 E, 1832894 N
Measured Date : August 6-9, 2023
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.

Quotation No. : 2023-01005
Analysis No. : 2023-AD376-001 - 003
Report No. : 2023-RAAP755
Report Date : August 22, 2023

Date/Time	Aug 6-7, 23		Aug 7-8, 23		Aug 8-9, 23	
	WS	WD	WS	WD	WS	WD
08:00-09:00	0.9	SSE	1.3	NE	<0.4	Calm
09:00-10:00	0.9	SSE	0.4	NE	<0.4	Calm
10:00-11:00	1.8	S	<0.4	Calm	<0.4	Calm
11:00-12:00	1.3	SE	<0.4	Calm	0.4	NNE
12:00-13:00	1.8	ESE	<0.4	Calm	0.4	NNE
13:00-14:00	1.3	ESE	<0.4	Calm	0.4	ENE
14:00-15:00	0.9	ESE	<0.4	Calm	<0.4	Calm
15:00-16:00	0.9	ENE	<0.4	Calm	0.4	N
16:00-17:00	0.4	ENE	<0.4	Calm	0.4	ESE
17:00-18:00	0.4	NNW	<0.4	Calm	0.4	SE
18:00-19:00	0.9	WNW	<0.4	Calm	0.4	E
19:00-20:00	0.9	SW	<0.4	Calm	<0.4	Calm
20:00-21:00	0.4	S	<0.4	Calm	<0.4	Calm
21:00-22:00	0.9	SSW	0.4	W	<0.4	Calm
22:00-23:00	0.4	S	<0.4	Calm	<0.4	Calm
23:00-00:00	0.9	SSE	<0.4	Calm	<0.4	Calm
00:00-01:00	<0.4	Calm	<0.4	Calm	<0.4	Calm
01:00-02:00	<0.4	Calm	<0.4	Calm	<0.4	Calm
02:00-03:00	<0.4	Calm	<0.4	Calm	0.4	SE
03:00-04:00	<0.4	Calm	<0.4	Calm	<0.4	Calm
04:00-05:00	<0.4	Calm	<0.4	Calm	0.9	ESE
05:00-06:00	0.4	NNE	<0.4	Calm	<0.4	Calm
06:00-07:00	0.9	NE	<0.4	Calm	<0.4	Calm
07:00-08:00	0.9	NE	<0.4	Calm	<0.4	Calm

Remark : WS = Wind Speed (m/s)
WD = Wind Direction
Height of wind vane and anemometer above ground 10 meters.

[REDACTED]

Laboratory Reviewer

[REDACTED]

Laboratory Supervisor

ANALYSIS REPORT

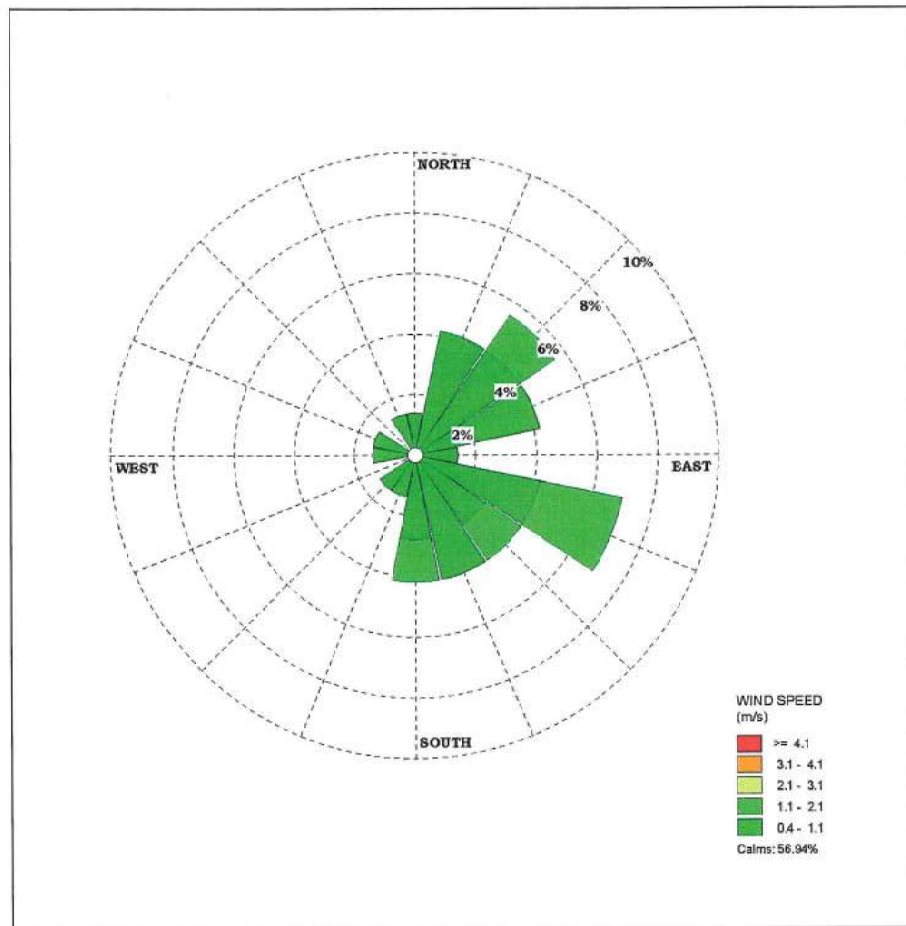
Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนหลวง หมู่ที่ 5 ตำบลโนนหลวง อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589990 E, 1832894 N
Measured Date : August 6-9, 2023
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.

Quotation No. : 2023-01005
Analysis No. : 2023-AD376-001 - 003
Report No. : 2023-RAAP755
Report Date : August 22, 2023

Wind Direction	Percentage frequency of wind in each speed and direction					Total
	0.4-1.1	1.1-2.1	2.1-3.1	3.1-4.1	≥4.1	
N	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
NNE	4.16667	0.00000	0.00000	0.00000	0.00000	4.16667
NE	4.16667	1.38889	0.00000	0.00000	0.00000	5.55556
ENE	4.16667	0.00000	0.00000	0.00000	0.00000	4.16667
E	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
ESE	4.16667	2.77778	0.00000	0.00000	0.00000	6.94445
SE	2.77778	1.38889	0.00000	0.00000	0.00000	4.16667
SSE	4.16667	0.00000	0.00000	0.00000	0.00000	4.16667
S	2.77778	1.38889	0.00000	0.00000	0.00000	4.16667
SSW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
SW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
WSW	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
W	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
WNW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
NW	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NNW	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
Calm	56.94440					

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลวง-อี (NPG-E))
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลวง หมู่ที่ 5 ตำบลโนนพลวง อำเภอลานกระบือ จังหวัดกำแพงเพชร
Measured Date : August 6-9, 2023
Report No. : 2023-RAAP755



ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนพลวง หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : August 6-9, 2023
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Quotation No. : 2023-01005
Analysis No. : 2023-AD376-004 - 006
Report No. : 2023-RAAP756
Report Date : August 22, 2023

Date/Time	Aug 6-7, 23		Aug 7-8, 23		Aug 8-9, 23	
	WS	WD	WS	WD	WS	WD
09:00-10:00	0.9	SSW	0.9	SSE	<0.4	Calm
10:00-11:00	0.9	SSW	1.3	SSE	<0.4	Calm
11:00-12:00	1.3	SSE	1.3	SSW	0.4	NE
12:00-13:00	1.3	SE	1.3	S	<0.4	Calm
13:00-14:00	1.3	SSE	1.3	S	0.4	ESE
14:00-15:00	0.9	SE	1.3	SSE	<0.4	Calm
15:00-16:00	0.4	E	1.8	SSE	<0.4	Calm
16:00-17:00	0.4	ENE	1.8	S	0.4	ESE
17:00-18:00	<0.4	Calm	1.3	S	0.4	S
18:00-19:00	<0.4	Calm	1.3	SSE	0.4	SSE
19:00-20:00	<0.4	Calm	0.4	S	0.4	SE
20:00-21:00	<0.4	Calm	<0.4	Calm	<0.4	Calm
21:00-22:00	0.4	SW	<0.4	Calm	<0.4	Calm
22:00-23:00	0.4	SW	<0.4	Calm	<0.4	Calm
23:00-00:00	0.4	S	<0.4	Calm	0.4	E
00:00-01:00	<0.4	Calm	0.9	E	0.4	E
01:00-02:00	<0.4	Calm	<0.4	Calm	0.4	E
02:00-03:00	<0.4	Calm	<0.4	Calm	0.4	SE
03:00-04:00	<0.4	Calm	<0.4	Calm	0.4	SSE
04:00-05:00	<0.4	Calm	0.4	ENE	0.4	SE
05:00-06:00	0.4	ESE	<0.4	Calm	0.4	SE
06:00-07:00	0.4	SSE	0.4	ENE	0.4	S
07:00-08:00	0.9	SSE	0.4	SE	<0.4	Calm
08:00-09:00	0.9	SE	<0.4	Calm	0.4	SSE

Remark : WS = Wind Speed (m/s)
WD = Wind Direction
Height of wind vane and anemometer above ground 10 meters.

[REDACTED]

Laboratory Reviewer

[REDACTED]

Laboratory Supervisor

ANALYSIS REPORT

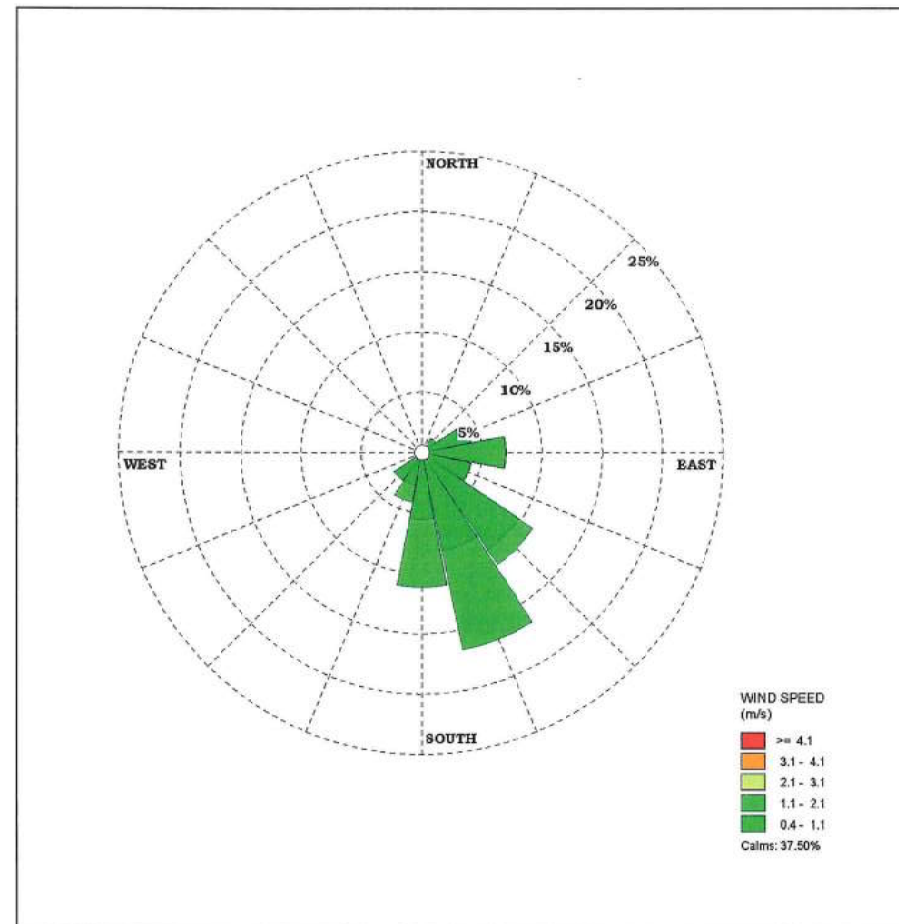
Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Air Quality
Measured Point : บริเวณบ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0589297 E, 1834331 N
Measured Date : August 6-9, 2023
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.

Quotation No. : 2023-01005
Analysis No. : 2023-AD375-004 - 006
Report No. : 2023-RAAP756
Report Date : August 22, 2023

Wind Direction	Percentage frequency of wind in each speed and direction					Total
	0.4-1.1	1.1-2.1	2.1-3.1	3.1-4.1	≥4.1	
N	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NNE	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NE	1.38889	0.00000	0.00000	0.00000	0.00000	1.38889
ENE	4.16667	0.00000	0.00000	0.00000	0.00000	4.16667
E	6.94444	0.00000	0.00000	0.00000	0.00000	6.94444
ESE	4.16667	0.00000	0.00000	0.00000	0.00000	4.16667
SE	9.72222	1.38889	0.00000	0.00000	0.00000	11.11111
SSE	8.33333	8.33333	0.00000	0.00000	0.00000	16.66666
S	5.55556	5.55556	0.00000	0.00000	0.00000	11.11112
SSW	2.77778	1.38889	0.00000	0.00000	0.00000	4.16667
SW	2.77778	0.00000	0.00000	0.00000	0.00000	2.77778
WSW	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
W	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
WNW	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NW	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NNW	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
Calm	37.50000					

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Measured Point : บ้านเลขที่ 250/1 บ้านโนนสมอ หมู่ที่ 6 ตำบลลานกระบือ อำเภอลานกระบือ จังหวัดกำแพงเพชร
Measured Date : August 6-9, 2023
Report No. : 2023-RAAP756





บริษัท ปตท.สผ. สยาม จำกัด

รายงานผลการปฏิบัติตามมาตรการป้องกันและแก้ไขผลกระทบสิ่งแวดล้อม และมาตรการติดตามตรวจสอบผลกระทบสิ่งแวดล้อม
โครงการในพื้นที่จังหวัดกำแพงเพชร
ฉบับเดือนมกราคม - ธันวาคม พ.ศ. 2566

ภาคผนวกที่ 38
ผลการตรวจวัดระดับเสียง

ព្រះឥសាន

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Noise
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนหลวง หมู่ที่ 5 ตำบลโนนหลวง อำเภอฉนวนกระวี จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0590013 E, 1832938 N
Measured Date : January 11-12, 2024
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : Integrating Sound Level Meter Scarlet Tech Model ST-11D Serial Number 820946

Quotation No. : 2023-01037
Analysis No. : 2024-AA095-007
Report No. : 2024-RAAB177
Report Date : January 20, 2024

Interval Time	Noise Level, dB(A)					
	Leq	Lmax	L5	L10	L50	L90
08:00-09:00	48.5	68.8	52.4	50.9	47.0	44.1
09:00-10:00	48.8	74.4	52.5	50.4	46.9	44.2
10:00-11:00	46.9	63.5	51.8	50.0	44.8	41.8
11:00-12:00	48.4	67.1	53.3	51.0	46.4	44.1
12:00-13:00	53.1	62.3	54.5	54.1	53.0	51.9
13:00-14:00	54.0	66.4	55.7	55.1	53.8	52.4
14:00-15:00	53.7	61.9	55.5	55.0	53.6	52.1
15:00-16:00	54.9	63.5	56.5	56.1	54.8	53.0
16:00-17:00	55.5	70.6	57.7	56.8	55.1	53.6
17:00-18:00	56.0	77.8	61.0	59.2	53.9	49.1
18:00-19:00	56.6	73.9	61.8	60.5	54.3	48.3
19:00-20:00	49.8	68.4	51.3	50.6	49.5	48.8
20:00-21:00	50.0	67.8	51.2	50.7	49.7	49.0
21:00-22:00	49.7	55.8	50.6	50.3	49.6	49.0
22:00-23:00	50.9	54.7	51.9	51.7	50.8	50.0
23:00-00:00	51.8	60.1	53.2	52.8	51.7	50.6
00:00-01:00	49.8	65.5	51.2	50.6	49.6	48.9
01:00-02:00	52.1	56.4	52.9	52.7	51.9	51.4
02:00-03:00	53.9	65.0	54.9	54.6	53.8	53.0
03:00-04:00	54.5	65.6	55.6	55.2	54.4	53.6
04:00-05:00	55.2	58.6	56.1	55.8	55.1	54.3
05:00-06:00	54.5	58.5	55.7	55.4	54.4	53.3
06:00-07:00	51.1	69.5	55.3	53.3	49.6	47.6
07:00-08:00	51.0	67.2	55.1	52.8	48.9	46.4
24 Hours Measurement	52.9	77.8	55.6	54.6	52.3	50.7
Standard¹⁾	70	115	-	-	-	-
Ldn	59.4	-	-	-	-	-

Remark : ¹⁾ Notification of National Environmental Board, No.15, B.E.2540 (1997) under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992), published in the Royal Government Gazette No.114 Part 270 dated April 3, B.E.2540 (1997).

(Ms.Supawan Suwannapa)
Laboratory Reviewer

(Ms.Thanida Bunrungrueang)
Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Noise
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนหลวง หมู่ที่ 5 ตำบลโนนหลวง อำเภอฉนวนกระวี จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0590013 E, 1832938 N
Measured Date : January 12-13, 2024
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : Integrating Sound Level Meter Scarlet Tech Model ST-11D Serial Number 820946

Quotation No. : 2023-01037
Analysis No. : 2024-AA095-007
Report No. : 2024-RAAB177
Report Date : January 20, 2024

Interval Time	Noise Level, dB(A)					
	Leq	Lmax	L5	L10	L50	L90
08:00-09:00	49.3	67.5	53.5	51.8	47.7	44.9
09:00-10:00	48.6	76.2	51.9	50.2	46.8	44.6
10:00-11:00	47.5	69.1	51.2	49.2	45.7	43.1
11:00-12:00	48.0	69.5	52.1	49.7	45.7	43.4
12:00-13:00	45.3	64.7	49.2	47.8	43.7	41.2
13:00-14:00	46.1	68.4	51.1	49.2	43.7	40.8
14:00-15:00	47.9	68.3	53.5	51.6	44.8	41.9
15:00-16:00	47.4	69.1	51.0	48.5	44.7	42.3
16:00-17:00	48.4	68.2	52.9	50.1	45.6	43.2
17:00-18:00	48.2	68.1	51.9	50.5	47.0	44.5
18:00-19:00	46.8	63.4	50.2	48.4	45.6	44.2
19:00-20:00	49.9	67.5	52.1	51.3	49.4	48.2
20:00-21:00	51.7	55.8	52.6	52.4	51.4	50.6
21:00-22:00	49.9	64.3	51.3	50.9	49.6	48.8
22:00-23:00	49.6	59.0	50.4	50.2	49.4	48.9
23:00-00:00	49.6	68.8	50.4	50.1	49.3	48.9
00:00-01:00	48.9	57.9	49.7	49.4	48.8	48.2
01:00-02:00	50.5	70.1	51.2	51.0	50.4	49.9
02:00-03:00	51.2	58.9	51.9	51.7	51.1	50.6
03:00-04:00	51.7	59.8	52.5	52.2	51.6	51.1
04:00-05:00	50.2	58.9	51.2	50.8	50.1	49.4
05:00-06:00	48.0	57.2	49.5	48.9	47.8	46.9
06:00-07:00	48.9	65.6	52.4	51.0	47.6	45.5
07:00-08:00	50.3	68.5	54.3	52.4	48.7	46.3
24 Hours Measurement	49.2	76.2	51.8	50.6	48.4	47.2
Standard¹⁾	70	115	-	-	-	-
Ldn	56.2	-	-	-	-	-

Remark : ¹⁾ Notification of National Environmental Board, No.15, B.E.2540 (1997) under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992), published in the Royal Government Gazette No.114 Part 270 dated April 3, B.E.2540 (1997).

(Ms.Supawan Suwannapa)
Laboratory Reviewer

(Ms.Thanida Bunrungrueang)
Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตมีโตรเคียมแหล่งโนนพลางส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลาง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Noise
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลาง หมู่ที่ 5 ตำบลโนนพลาง อำเภอลานกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0590013 E, 1832938 N
Measured Date : January 13-14, 2024
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : Integrating Sound Level Meter Scarlet Tech Model ST-11D Serial Number 820946

Quotation No. : 2023-01037
Analysis No. : 2024-AA095-007
Report No. : 2024-RAA8177
Report Date : January 20, 2024

Interval Time	Noise Level, dB(A)					
	Leq	Lmax	L5	L10	L50	L90
08:00-09:00	50.8	68.0	55.5	52.9	48.8	45.9
09:00-10:00	51.0	71.7	53.9	52.7	50.1	49.0
10:00-11:00	47.7	67.1	51.3	49.8	46.5	44.1
11:00-12:00	46.1	68.1	50.0	48.4	44.6	42.4
12:00-13:00	44.4	62.5	47.8	46.6	43.3	40.8
13:00-14:00	45.9	64.2	49.4	48.3	44.9	42.3
14:00-15:00	46.1	72.5	49.3	47.9	45.0	42.0
15:00-16:00	45.8	60.5	49.9	48.3	44.6	42.1
16:00-17:00	51.8	77.7	55.2	52.9	49.4	47.3
17:00-18:00	48.8	64.7	51.9	50.7	47.9	46.0
18:00-19:00	45.2	66.3	47.9	46.8	44.4	43.0
19:00-20:00	50.9	55.2	52.0	51.8	50.6	49.6
20:00-21:00	51.9	59.2	53.0	52.8	51.5	50.7
21:00-22:00	49.9	59.9	50.7	50.5	49.6	49.1
22:00-23:00	48.5	53.8	49.5	49.2	48.4	47.7
23:00-00:00	46.0	53.8	47.2	46.8	45.8	45.0
00:00-01:00	46.0	56.6	47.5	46.9	45.8	45.2
01:00-02:00	47.4	53.3	48.4	48.2	47.2	46.3
02:00-03:00	49.4	54.2	50.1	50.0	49.2	48.7
03:00-04:00	48.7	54.6	49.5	49.3	48.5	48.0
04:00-05:00	47.7	54.2	48.7	48.4	47.5	46.6
05:00-06:00	45.9	61.2	47.7	46.9	45.5	44.7
06:00-07:00	48.2	67.2	51.8	50.2	46.8	45.0
07:00-08:00	51.1	75.0	55.3	53.0	49.0	46.5
24 Hours Measurement	48.7	77.7	51.3	50.1	47.8	46.5
Standard ¹⁾	70	115	-	-	-	-
Ldn	54.4	-	-	-	-	-

Remark : ¹⁾ Notification of National Environmental Board, No.15, E.E.2540 (1997) under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992), published in the Royal Government Gazette No.114 Part 27D dated April 3, B.E.2540 (1997).



Laboratory Reviewer



Laboratory Supervisor



Environment Research & Technology Company Limited
25 / 114 Mu 6 Soi Chirakhet 1, Ngam Wong Wan Road,
Thung Song Hong, Lak Si, Bangkok 10210
Tel. 0-2954-7745-6 Fax 0-2954-7747
E-mail : envi@enviresearch.co.th
www.enviresearch.co.th

รายงานผลการตรวจวัดเสียงรบกวน

ข้อมูลทั่วไป
ที่ปรึกษา : บริษัท วิชั่น อี. คอนซัลตัน จำกัด
ที่ปรึกษา : เลขที่ 101/22 หมู่ที่ 2 ซอยแมนียาซอย 3, ซอยมา, เมืองนนทบุรี, นนทบุรี 11000
โครงการ : โครงการผลิตมีโตรเคียมแหล่งโนนพลางส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลาง-อี (NPG-E))
พื้นที่โครงการ : จังหวัดกำแพงเพชร
ประเภทของแหล่งกำเนิดเสียง : เสียงรบกวนกรณี 4 เครื่องจักรผลิตมีโตรเคียม
วัตถุประสงค์การวัดเสียงรบกวน : เพื่อประเมินค่าเสียงรบกวนจากแหล่งกำเนิดเสียงที่ 25/1 บ้านโนนพลาง หมู่ที่ 5 UTM (WGS84) 47Q 0590013 E, 1832938 N
บริเวณที่ต้องการวัดเสียงรบกวน : บริเวณจุดวัดเสียง UTM (WGS84) 47Q 0590296 E, 1833233 N
การวัดเสียง : บริษัท เอ็นไวรอนเม้นท์ รีเสิร์ช แอนด์ เทคโนโลยี จำกัด
เครื่องมือที่ใช้ในการวัด : เครื่องวัดระดับเสียง Scarlet Tech Model ST-11D Serial Number 820946, เครื่องวัดระดับเสียง Scarlet Tech Model ST-11D Serial Number 820941

นายวิชาญ วิเศษภักดี
นายวิชาญ วิเศษภักดี
นายวิชาญ วิเศษภักดี
วันที่รับงาน : 2023-01-03
วันที่ส่งงาน : 2024-AA095-007
วันที่รับงาน : 2024-RAA8178
วันที่รับงาน : 18 มกราคม 2567

ระดับเสียงขณะเกิดเสียงรบกวนแหล่งกำเนิด			ระดับเสียงขณะไม่มีการรบกวน				การคำนวณระดับเสียงรบกวน ²⁾			สรุป		
วันที่	ช่วงเวลา	ระดับเสียงขณะเกิดเสียงรบกวน (L _{max} , dB(A))	วันที่	ช่วงเวลา	ระดับเสียงขณะเกิดเสียงรบกวน 5 นาที (L _{max} , dB(A))	ระดับเสียงขณะไม่มีการรบกวน (L _{min} , dB(A))	ช่วงเวลาที่เสียงรบกวนเกิดขึ้น (T _{eq} นาที)	ระดับเสียงขณะเกิดเสียงรบกวน 4 นาที (L _{eq} , dB(A))	ระดับเสียงขณะไม่มีการรบกวน 5 นาที (L _{eq} , dB(A))			
12 ม.ค. 67	05:00-05:55	53.3	12 ม.ค. 67	05:45-05:50	50.9	48.4	5	49.6	52.6	4.2	≤10	ไม่มีเสียงรบกวน
13 ม.ค. 67	01:45-01:50	49.9	13 ม.ค. 67	01:50-01:55	47.7	46.8	5	45.9	48.9	2.1	≤10	ไม่มีเสียงรบกวน
14 ม.ค. 67	01:10-01:15	47.4	14 ม.ค. 67	01:40-01:45	45.9	44.5	5	42.1	45.1	0.6	≤10	ไม่มีเสียงรบกวน

หมายเหตุ : ¹⁾ วิธีการวัดระดับเสียงรบกวน : ใช้วิธีการวัดระดับเสียงรบกวนแบบไม่มีการรบกวน การวัดระดับเสียงรบกวนแบบไม่มีการรบกวน : การวัดระดับเสียงรบกวนแบบไม่มีการรบกวน : ไม่มีเสียงรบกวน

²⁾ วิธีการคำนวณระดับเสียงรบกวน : ใช้วิธีการคำนวณระดับเสียงรบกวนแบบไม่มีการรบกวน



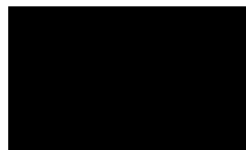
ฤดูฝน

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi ManeeYa Sol 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลวงส่วนขยาย แปลงเลข 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Noise
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลวง หมู่ที่ 5 ตำบลโนนพลวง อำเภอฉวางกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0590013 E, 1832938 N
Measured Date : August 6-7, 2023
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : Integrating Sound Level Meter Scarlet Tech Model ST-11D Serial Number 820801

Interval Time	Noise Level, dB(A)					
	Leq	Lmax	L5	L10	L50	L90
08:00-09:00	47.4	83.7	54.8	49.8	42.5	39.7
09:00-10:00	45.6	83.3	52.0	49.6	42.4	39.2
10:00-11:00	44.5	64.5	50.6	47.3	40.6	37.9
11:00-12:00	45.0	69.4	50.8	48.0	41.2	38.5
12:00-13:00	42.8	61.0	48.1	45.6	39.5	36.8
13:00-14:00	43.0	67.9	48.0	44.7	39.3	36.8
14:00-15:00	42.7	65.2	47.3	44.9	40.3	37.5
15:00-16:00	44.9	68.9	49.6	47.0	42.7	40.6
16:00-17:00	44.2	67.1	47.9	45.9	42.2	40.1
17:00-18:00	45.2	65.3	51.4	49.6	43.1	40.4
18:00-19:00	44.3	63.5	48.7	46.6	42.3	40.2
19:00-20:00	45.6	69.4	47.1	46.5	45.2	44.0
20:00-21:00	49.4	68.4	50.1	50.0	49.3	48.5
21:00-22:00	48.6	61.8	49.4	49.2	48.5	47.6
22:00-23:00	46.9	60.6	47.8	47.6	46.8	45.8
23:00-00:00	46.5	59.3	47.5	47.3	46.4	45.2
00:00-01:00	50.9	74.2	57.4	54.6	45.5	43.8
01:00-02:00	45.3	59.9	46.5	46.3	45.1	43.3
02:00-03:00	52.6	77.9	60.0	57.1	42.9	41.8
03:00-04:00	43.1	71.2	45.3	43.8	42.2	40.9
04:00-05:00	43.2	79.2	54.3	44.6	42.1	41.1
05:00-06:00	45.3	59.7	47.9	46.8	44.7	43.2
06:00-07:00	47.6	73.2	51.5	49.6	45.8	43.8
07:00-08:00	47.7	67.8	51.5	49.5	46.1	44.4
24 Hours Measurement	46.9	83.7	52.0	49.4	44.5	42.9
Standard ¹⁾	70	115	-	-	-	-
Ldn	54.2	-	-	-	-	-

Remark : ¹⁾ Notification of National Environmental Board, No.15, B.E.2540 (1997) under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992), published in the Royal Government Gazette No.114 Part 270 dated April 3, B.E.2540 (1997).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

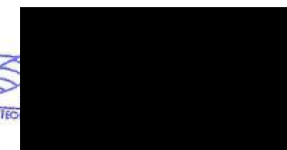
Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi ManeeYa Sol 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนพลวงส่วนขยาย แปลงเลข 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Measured Source : Ambient Noise
Measured Point : บริเวณบ้านเลขที่ 25/1 บ้านโนนพลวง หมู่ที่ 5 ตำบลโนนพลวง อำเภอฉวางกระบือ จังหวัดกำแพงเพชร
GPS. Coordinate : UTM (WGS84) 47Q 0590013 E, 1832938 N
Measured Date : August 7-8, 2023
Measured By : [REDACTED]
Analyzed By : Environment Research & Technology Co., Ltd.
Measured Instrument : Integrating Sound Level Meter Scarlet Tech Model ST-11D Serial Number 820801

Interval Time	Noise Level, dB(A)					
	Leq	Lmax	L5	L10	L50	L90
08:00-09:00	48.9	71.9	53.6	51.2	46.5	44.7
09:00-10:00	49.5	69.9	55.0	52.5	46.4	44.4
10:00-11:00	47.5	71.4	52.4	49.7	44.2	42.1
11:00-12:00	47.4	68.1	52.4	49.5	44.6	42.4
12:00-13:00	49.4	73.6	54.7	52.7	45.7	43.0
13:00-14:00	44.9	70.9	49.6	47.1	42.1	39.4
14:00-15:00	45.0	70.3	50.9	47.4	42.3	39.7
15:00-16:00	43.9	69.8	47.7	46.1	42.3	39.8
16:00-17:00	45.8	65.0	50.9	48.1	42.2	39.7
17:00-18:00	46.4	69.8	51.6	48.0	42.6	40.1
18:00-19:00	46.3	70.5	51.0	48.1	43.4	41.4
19:00-20:00	47.7	65.3	49.6	48.8	47.5	46.1
20:00-21:00	51.9	62.2	52.6	52.4	51.8	51.1
21:00-22:00	57.1	81.4	63.7	58.1	51.1	50.3
22:00-23:00	49.2	67.1	50.5	49.9	49.1	48.4
23:00-00:00	47.0	69.8	49.0	47.6	46.4	45.6
00:00-01:00	45.9	71.4	47.8	46.1	45.0	43.9
01:00-02:00	45.1	66.2	48.1	45.8	44.2	43.1
02:00-03:00	43.2	71.3	44.2	43.9	43.0	41.9
03:00-04:00	43.1	61.0	45.2	44.1	42.7	41.6
04:00-05:00	43.1	60.7	44.4	44.0	42.9	41.9
05:00-06:00	45.3	61.9	47.9	46.9	44.6	43.1
06:00-07:00	50.2	69.7	57.2	53.3	45.4	42.8
07:00-08:00	48.4	67.3	53.4	50.5	45.9	44.3
24 Hours Measurement	48.7	81.4	53.7	50.3	46.1	44.7
Standard ¹⁾	70	115	-	-	-	-
Ldn	53.5	-	-	-	-	-

Remark : ¹⁾ Notification of National Environmental Board, No.15, B.E.2540 (1997) under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992), published in the Royal Government Gazette No.114 Part 270 dated April 3, B.E.2540 (1997).



Laboratory Reviewer



Laboratory Supervisor

ANALYSIS REPORT

Customer Name	: Vision E. Consultants Co., Ltd.		
Address	: 101/22 Moo 2, Soi Maneeaya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000		
Project Name	: โครงการผลิตปิโตรเลียมแหล่งโนนพลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนพลวง-อี (NPG-E))		
Project Location	: จังหวัดกำแพงเพชร		
Measured Source	: Ambient Noise		
Measured Point	: บริเวณบ้านเลขที่ 25/1 บ้านโนนพลวง หมู่ที่ 5 ตำบลโนนพลวง อำเภอลานกระบือ จังหวัดกำแพงเพชร		
GPS. Coordinate	: UTM (WGS84) 47Q 0590013 E, 1832938 N	Quotation No. :	2023-01005
Measured Date	: August 8-9, 2023	Analysis No. :	2023-AJ376-007
Measured By	: [REDACTED]	Report No. :	2023-RAAP749
Analyzed By	: Environment Research & Technology Co., Ltd.	Report Date :	August 22, 2023
Measured Instrument	: Integrating Sound Level Meter Scarlet Tech Model ST-11D Serial Number 820801		

Interval/Time	Noise Level, dB(A)					
	Leq	Lmax	L5	L10	L50	L90
08:00-09:00	49.3	76.8	52.6	50.8	47.7	46.6
09:00-10:00	51.6	65.4	54.5	53.2	50.8	50.1
10:00-11:00	52.2	79.4	54.3	52.9	51.0	50.4
11:00-12:00	52.4	64.9	55.0	53.6	51.7	51.1
12:00-13:00	51.2	63.8	52.9	51.9	50.8	50.2
13:00-14:00	52.0	73.1	54.2	52.6	51.2	50.5
14:00-15:00	52.4	73.2	54.6	53.2	51.3	50.6
15:00-16:00	51.3	65.4	52.8	51.9	50.9	50.2
16:00-17:00	52.0	69.0	54.3	52.9	51.3	50.6
17:00-18:00	54.5	67.6	58.2	57.0	53.6	51.0
18:00-19:00	53.3	67.7	57.1	55.7	52.0	50.2
19:00-20:00	51.7	60.4	53.6	53.1	51.4	50.3
20:00-21:00	53.7	59.6	55.6	55.1	53.4	52.5
21:00-22:00	56.5	61.0	58.4	58.0	56.2	54.6
22:00-23:00	58.6	63.3	60.2	59.8	58.5	56.9
23:00-00:00	59.8	70.5	61.2	60.9	59.7	58.5
00:00-01:00	62.2	66.5	63.3	63.0	62.1	60.9
01:00-02:00	63.0	55.7	64.0	63.8	62.9	62.0
02:00-03:00	63.4	55.7	64.3	64.1	63.3	62.3
03:00-04:00	62.5	55.5	63.5	63.3	62.3	61.1
04:00-05:00	59.4	63.9	60.7	60.4	59.2	57.6
05:00-06:00	53.9	67.7	57.2	56.2	53.0	51.3
06:00-07:00	51.6	72.2	54.5	53.2	50.7	49.7
07:00-08:00	51.2	59.2	53.9	52.1	50.5	49.7
24 Hours Measurement	57.5	79.4	59.0	58.5	57.2	56.0
Standard ^{1/}	70	115	-	-	-	-
Ldn	66.5	-	-	-	-	-

Remark : ¹⁷ Notification of National Environmental Board, No.15, B.E.2540 (1997) under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992), published in the Royal Government Gazette No.114 Part 27D dated April 3, B.E.2540 (1997).

Laboratory Reviewer

Laboratory Supervisor

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REPORT ANALYSIS REFERS TO SUBMITTED SAMPLE (S) ONLY

Page 3/3

F-RP-008 Rev. 03, January 18, 2021



รายงานผลการตรวจประเมิน

๓. ผลลัพธ์
 ๔. ปัจจัยความสำเร็จ
 ๕. ข้อเสนอแนะ
 ๖. บทสรุป
 ๗. ภาคผนวก
 ๘. บรรณานุกรม
 ๙. ภาคผนวก
 ๑๐. ภาคผนวก

[illegible]

หมายเลขใบสมัครฯ	: 2023-01.005
หมายเลขปฏิทินฯ	: 2023-AD376-007
หมายเลขรายงานผล	: 2023-RAAP762
วันทำรายงานผล	: 22 สิงหาคม 2566

Environment Research & Technology Company Limited
25/113-114 Moo 6 Soi Chakret 1, Ngamwongwan Road,
Toungsongkhong, Laksh, Bangkok 10210
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[illegible]

หมายเหตุ : 1* ปรัชญาของเศรษฐกิจพอเพียงที่มุ่งเน้น เพื่อ ให้ประชาชนได้มีคุณภาพชีวิตที่ดีและมีความสุขในการดำรงชีวิต การดำรงชีวิตและมีความสุขนั้นจะต้องมีพื้นฐานที่มั่นคงและต้องไม่ขาดความก้าวหน้า การดำรงชีวิตและมีความสุขนั้นจะต้องมีพื้นฐานที่มั่นคงและต้องไม่ขาดความก้าวหน้า การดำรงชีวิตและมีความสุขนั้นจะต้องมีพื้นฐานที่มั่นคงและต้องไม่ขาดความก้าวหน้า

2* ปรัชญาของเศรษฐกิจพอเพียงที่มุ่งเน้น เพื่อ ให้ประชาชนได้มีคุณภาพชีวิตที่ดีและมีความสุขในการดำรงชีวิต การดำรงชีวิตและมีความสุขนั้นจะต้องมีพื้นฐานที่มั่นคงและต้องไม่ขาดความก้าวหน้า การดำรงชีวิตและมีความสุขนั้นจะต้องมีพื้นฐานที่มั่นคงและต้องไม่ขาดความก้าวหน้า การดำรงชีวิตและมีความสุขนั้นจะต้องมีพื้นฐานที่มั่นคงและต้องไม่ขาดความก้าวหน้า





บริษัท ปตท.สผ. สยาม จำกัด

รายงานผลการปฏิบัติตามมาตรการป้องกันและแก้ไขผลกระทบสิ่งแวดล้อม และมาตรการติดตามตรวจสอบผลกระทบสิ่งแวดล้อม
โครงการในพื้นที่จังหวัดกำแพงเพชร
ฉบับเดือนมกราคม - ธันวาคม พ.ศ. 2566

ภาคผนวกที่ 39
ผลการตรวจวัดคุณภาพน้ำผิวดิน

ព្រះឥសាន

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Surface Water Sampling
Sampling Point : บริเวณคลองหนองน้ำ ตำบลหนองหลวง อำเภอลานกระบี่ จังหวัดกำแพงเพชร (เหนือน้ำ)
GPS. Coordinate : UTM (WGS84) 47Q 0588314 E, 1833954 N
Sampling Date : January 13, 2024
Sampling Time : 10:15
Sampling Method : Grab
Sampling By :
Analyzed By : Environment Research & Technology Co., Ltd.
Physical Properties : Turbid, Light Yellow, Sediment, Odorless

Quotation No. : 2023-01037
Analysis No. : 2024-AA102-001
Received Date : January 15, 2024
Analytical Date : January 15-25, 2024
Report No. : 2024-RAAB037
Report Date : January 25, 2024

Parameter	Unit	Method of Analysis ^{1'}	MRL	Result	Standard ^{2'}	
					Class 3	Class 4
Temperature	°C	Certified Thermometer	-	26.0	n'	n'
pH	-	Electrometric	-	7.9	5.0-9.0	5.0-9.0
Dissolved Oxygen	mg/L	Azide Modification	1.0	2.2	≥4.0	≥2.0
Biochemical Oxygen Demand	mg/L	5-Day BOD Test, Membrane Electrode	1.0	2.8	2.0	4.0
Fecal Coliform Bacteria	MPN/100 mL	Most Probable Number	1.8	790	4,000	-
Copper	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	0.010	0.1	0.1
Nickel	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	0.005	0.1	0.1
Manganese	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	0.555	1.0	1.0
Zinc	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.01	0.02	1.0	1.0
Cadmium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.003	<0.033	0.005 ^{3'}	0.005 ^{3'}
Lead	mg/L	Digestion, Electrothermal Atomic Absorption Spectrometry	0.001	0.002	0.05	0.05
Mercury	mg/L	Digestion, Cold-Vapor Atomic Absorption Spectrometry	0.0005	<0.0005	0.002	0.002
Arsenic	mg/L	Digestion, Hydride Generation Atomic Absorption Spectrometry	0.0002	0.0002	0.01	0.01
Barium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.01	0.10	-	-
Iron	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.1	0.9	-	-
Selenium	mg/L	Digestion, Hydride Generation Atomic Absorption Spectrometry	0.0002	<0.0002	-	-
Total Chromium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	<0.005	-	-
Conductivity	µs/cm	Electrical Conductivity Meter	0.1	293	-	-
Salinity	ppt	Electrical Conductivity Meter	0.1	0.2	-	-
Total Dissolved Solids	mg/L	Dried at 180°C	50	155	-	-
Total Suspended Solids	mg/L	Dried at 103-105°C	5.0	27	-	-

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Surface Water Sampling
Sampling Point : บริเวณคลองหนองน้ำ ตำบลหนองหลวง อำเภอลานกระบี่ จังหวัดกำแพงเพชร (เหนือน้ำ)
GPS. Coordinate : UTM (WGS84) 47Q 0588314 E, 1833954 N
Sampling Date : January 13, 2024
Sampling Time : 10:15
Sampling Method : Grab
Sampling By :
Analyzed By : Environment Research & Technology Co., Ltd.
Physical Properties : Turbid, Light Yellow, Sediment, Odorless

Quotation No. : 2023-01037
Analysis No. : 2024-AA102-001
Received Date : January 15, 2024
Analytical Date : January 15-25, 2024
Report No. : 2024-RAAB037
Report Date : January 25, 2024

Parameter	Unit	Method of Analysis ^{1'}	MRL	Result	Standard ^{2'}	
					Class 3	Class 4
TPH (Gasoline Range Hydrocarbons; C ₆ -C ₉)	mg/L	Purge and Trap, Gas Chromatographic (GC-FID)	0.040	<0.040	-	-
TPH (Kerosene Range Hydrocarbons; C ₁₀ -C ₁₄)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	<0.020	-	-
TPH (Diesel Range Hydrocarbons; C ₁₅ -C ₂₄)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	<0.020	-	-
TPH (Heavy Oil Range Hydrocarbons; C ₂₅ -C ₃₄)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	<0.020	-	-


Remark : ^{1'} Standard Method for Examination of Water and Wastewater, 23rd Edition, 2017.

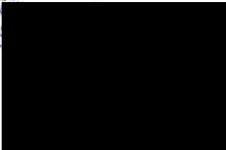
^{2'} Notification of the National Environment Board, No.6, B.E.2537 (1994), issued under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992).

published in the Royal Government Gazette No.111 Part 16, dated February 24, B.E.2537 (1994). (Standard Value of Surface Water for Class 3, 4)


^{3'} When water hardness not more than 100 mg/l as CaCO₃ (Hardness as CaCO₃ is 65 mg/l)

n' = naturally but changing not more than 3°C


Laboratory Reviewer


Laboratory Supervisor

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเลข 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Surface Water Sampling
Sampling Point : บริเวณคลองหนองบัว ตำบลโนนหลวง อำเภอลานกระบือ จังหวัดกำแพงเพชร (ห้วยน้ำ)
GPS. Coordinate : UTM (WGS84) 47Q 0589840 E, 1834008 N
Sampling Date : January 13, 2024
Sampling Time : 10:53
Sampling Method : Grab
Sampling By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Physical Properties : Turbid, Light Yellow, Sediment, Odorless

Quotation No. : 2023-01037
Analysis No. : 2024-AA102-002
Received Date : January 15, 2024
Analytical Date : January 15-25, 2024
Report No. : 2024-RAAB039
Report Date : January 25, 2024

Parameter	Unit	Method of Analysis ^{1'}	MRL	Result	Standard ^{2'}	
					Class 3	Class 4
Temperature	°C	Certified Thermometer	-	29.0	n ¹	n ¹
pH	-	Electrometric	-	7.8	5.0-9.0	5.0-9.0
Dissolved Oxygen	mg/L	Azide Modification	1.0	1.8	≥4.0	≥2.0
Biochemical Oxygen Demand	mg/L	5-Day BOD Test, Membrane Electrode	1.0	1.7	2.0	4.0
Fecal Coliform Bacteria	MPN/100 mL	Most Probable Number	1.8	490	4,000	-
Copper	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	0.009	0.1	0.1
Nickel	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	<0.005	0.1	0.1
Manganese	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	0.276	1.0	1.0
Zinc	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.01	0.03	1.0	1.0
Cadmium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.003	<0.003	0.005 ^{3'}	0.005 ^{3'}
Lead	mg/L	Digestion, Electrothermal Atomic Absorption Spectrometry	0.001	<0.001	0.05	0.05
Mercury	mg/L	Digestion, Cold-Vapor Atomic Absorption Spectrometry	0.0005	<0.0005	0.002	0.002
Arsenic	mg/L	Digestion, Hydride Generation Atomic Absorption Spectrometry	0.0002	0.0002	0.01	0.01
Barium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.01	0.07	-	-
Iron	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.1	0.5	-	-
Selenium	mg/L	Digestion, Hydride Generation Atomic Absorption Spectrometry	0.0002	<0.0002	-	-
Total Chromium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	<0.005	-	-
Conductivity	µs/cm	Electrical Conductivity Meter	0.1	216	-	-
Salinity	ppt	Electrical Conductivity Meter	0.1	0.1	-	-
Total Dissolved Solids	mg/L	Dried at 180°C	50	141	-	-
Total Suspended Solids	mg/L	Dried at 103-105°C	5.0	11	-	-

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเลข 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Surface Water Sampling
Sampling Point : บริเวณคลองหนองบัว ตำบลโนนหลวง อำเภอลานกระบือ จังหวัดกำแพงเพชร (ห้วยน้ำ)
GPS. Coordinate : UTM (WGS84) 47Q 0589840 E, 1834008 N
Sampling Date : January 13, 2024
Sampling Time : 10:53
Sampling Method : Grab
Sampling By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Physical Properties : Turbid, Light Yellow, Sediment, Odorless

Quotation No. : 2023-01037
Analysis No. : 2024-AA102-002
Received Date : January 15, 2024
Analytical Date : January 15-25, 2024
Report No. : 2024-RAAB039
Report Date : January 25, 2024

Parameter	Unit	Method of Analysis ^{1'}	MRL	Result	Standard ^{2'}	
					Class 3	Class 4
TPH (Gasoline Range Hydrocarbons; C6-C9)	mg/L	Purge and Trap, Gas Chromatographic (GC-FID)	0.040	<0.040	-	-
TPH (Kerosene Range Hydrocarbons; C10-C14)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	<0.020	-	-
TPH (Diesel Range Hydrocarbons; C15-C28)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	<0.020	-	-
TPH (Heavy Oil Range Hydrocarbons; C29-C35)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	<0.020	-	-

Remark : ^{1'} Standard Method for Examination of Water and Wastewater, 23rd Edition, 2017.
^{2'} Notification of the National Environment Board, No.8, B.E.2537 (1994), issued under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992), published in the Royal Government Gazette No.111 Part 16, dated February 24, B.E.2537 (1994). (Standard Value of Surface Water for Class 3, 4)
^{3'} When water hardness not more than 100 mg/l as CaCO₃ (Hardness as CaCO₃ is 76 mg/l)
n¹ = naturally but changing not more than 3°C


Laboratory Reviewer


Laboratory Supervisor

ฤดูฝน

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปุ๋ยอินทรีย์จากมูลสัตว์ปีกและเศษอาหาร มูลไก่ไข่ 1 จังหวัดกำแพงเพชร (ฐานผสมผลิตอินทผลัม-ดี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Surface Water Sampling
Sampling Point : บริเวณคลองหนองบัว ตำบลหนองหลวง อำเภอสามกระดี่ จังหวัดกำแพงเพชร (เหนือน้ำ)
GPS. Coordinate : UTM (WGS84) 47Q 0588314 E, 1833954 N
Sampling Date : August 8, 2023
Sampling Time : 15:00
Sampling Method : Grab
Sampling By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Physical Properties : Turbid, Light Yellow, Sediment, Odorless

Quotation No. : 2023-01005
Analysis No. : 2023-AD364-001
Received Date : August 11, 2023
Analytical Date : August 11-29, 2023
Report No. : 2023-RAAP566
Report Date : September 6, 2023

Parameter	Unit	Method of Analysis ^{1/}	MRL	Result	Standard ^{2/}	
					Class 3	Class 4
Temperature	°C	Certified Thermometer	-	28.0	n ^{3/}	n ^{3/}
pH	-	Electrometric	-	6.9	5.0-9.0	5.0-9.0
Dissolved Oxygen	mg/L	Aside Modification	1.0	4.1	≥4.0	≥2.0
Biochemical Oxygen Demand	mg/L	5-Day BOD Test, Membrane Electrode	1.0	2.7	2.0	4.0
Fecal Coliform Bacteria	MPN/100 mL	Most Probable Number	1.8	170	4,000	-
Copper	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	0.014	0.1	0.1
Nickel	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	0.005	0.1	0.1
Manganese	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	0.534	1.0	1.0
Zinc	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.01	0.02	1.0	1.0
Cadmium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.003	<0.003	0.005 ^{3/}	0.005 ^{3/}
Lead	mg/L	Digestion, Electrothermal Atomic Absorption Spectrometry	0.001	<0.001	0.05	0.05
Mercury	mg/L	Digestion, Cold-Vapor Atomic Absorption Spectrometry	0.0005	<0.0005	0.002	0.002
Arsenic	mg/L	Digestion, Hydride Generation Atomic Absorption Spectrometry	0.0002	0.0003	0.01	0.01
Barium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.01	0.10	-	-
Iron	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.1	3.1	-	-
Selenium	mg/L	Digestion, Hydride Generation Atomic Absorption Spectrometry	0.0002	<0.0002	-	-
Total Chromium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	<0.005	-	-
Conductivity	µs/cm	Electrical Conductivity Meter	0.1	369	-	-
Salinity	ppt	Electrical Conductivity Meter	0.1	0.2	-	-
Total Dissolved Solids	mg/L	Dried at 180°C	50	268	-	-
Total Suspended Solids	mg/L	Dried at 103-105°C	5.0	34	-	-

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปุ๋ยอินทรีย์จากมูลสัตว์ปีกและเศษอาหาร มูลไก่ไข่ 1 จังหวัดกำแพงเพชร (ฐานผสมผลิตอินทผลัม-ดี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Surface Water Sampling
Sampling Point : บริเวณคลองหนองบัว ตำบลหนองหลวง อำเภอสามกระดี่ จังหวัดกำแพงเพชร (เหนือน้ำ)
GPS. Coordinate : UTM (WGS84) 47Q 0588314 E, 1833954 N
Sampling Date : August 8, 2023
Sampling Time : 15:00
Sampling Method : Grab
Sampling By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Physical Properties : Turbid, Light Yellow, Sediment, Odorless

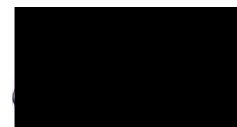
Quotation No. : 2023-01005
Analysis No. : 2023-AD364-001
Received Date : August 11, 2023
Analytical Date : August 11-29, 2023
Report No. : 2023-RAAP566
Report Date : September 6, 2023

Parameter	Unit	Method of Analysis ^{1/}	MRL	Result	Standard ^{2/}	
					Class 3	Class 4
TPH (Gasoline Range Hydrocarbons; C6-C9)	mg/L	Purge and Trap, Gas Chromatographic (GC-FID)	0.040	<0.040	-	-
TPH (Kerosene Range Hydrocarbons; C10-C14)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	<0.020	-	-
TPH (Diesel Range Hydrocarbons; C15-C28)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	0.065	-	-
TPH (Heavy Oil Range Hydrocarbons; C29-C36)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	<0.020	-	-

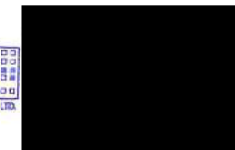
Remark : ^{1/} Standard Method for Examination of Water and Wastewater, 23rd Edition, 2017.

^{2/} Notification of the National Environment Board, No.8, 3.E.2537 (1994), issued under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992), published in the Royal Government Gazette No.111 Part 36, dated February 24, B.E.2537 (1994). (Standard Value of Surface Water for Class 3, 4)

^{3/} When water hardness not more than 100 mg/l as CaCO₃ (Hardness as CaCO₃ is 56 mg/l)
n^{3/} = naturally but changing not more than 3°C



Laboratory Reviewer



Laboratory Supervisor


ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Surface Water Sampling
Sampling Point : บริเวณคลองหนองบัว ตำบลโนนหลวง อำเภอลานกระบือ จังหวัดกำแพงเพชร (ท้ายน้ำ)
GPS. Coordinate : UTM (WGS84) 47Q 0589840 E, 1834008 N
Sampling Date : August 8, 2023
Sampling Time : 15:32
Sampling Method : Grab
Sampling By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Physical Properties : Turbid, Light Yellow, Sediment, Odorless

Quotation No. : 2023-01005
Analysis No. : 2023-AD364-002
Received Date : August 11, 2023
Analytical Date : August 11-September 6, 2023
Report No. : 2023-RAAP567
Report Date : September 6, 2023

Parameter	Unit	Method of Analysis ^{1*}	MRL	Result	Standard ^{2*}	
					Class 3	Class 4
Temperature	°C	Certified Thermometer	-	28.0	n ¹	n ¹
pH	-	Electrometric	-	6.8	5.0-9.0	5.0-9.0
Dissolved Oxygen	mg/L	Azide Modification	1.0	2.8	≥4.0	≥2.0
Biochemical Oxygen Demand	mg/L	5-Day BOD Test, Membrane Electrode	1.0	2.5	2.0	4.0
Fecal Coliform Bacteria	MPN/100 mL	Most Probable Number	1.8	16,000	4,000	-
Copper	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	<0.005	0.1	0.1
Nickel	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	<0.005	0.1	0.1
Manganese	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	1.0	1.0	1.0
Zinc	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.01	0.01	1.0	1.0
Cadmium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.003	<0.003	0.005 ^{3*}	0.005 ^{3*}
Lead	mg/L	Digestion, Electrothermal Atomic Absorption Spectrometry	0.001	<0.001	0.05	0.05
Mercury	mg/L	Digestion, Cold-Vapor Atomic Absorption Spectrometry	0.0005	<0.0005	0.002	0.002
Arsenic	mg/L	Digestion, Hydride Generation Atomic Absorption Spectrometry	0.0002	0.0005	0.01	0.01
Barium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.01	0.11	-	-
Iron	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.1	2.1	-	-
Selenium	mg/L	Digestion, Hydride Generation Atomic Absorption Spectrometry	0.0002	<0.0002	-	-
Total Chromium	mg/L	Digestion, Inductively Coupled Plasma (ICP-OES)	0.005	<0.005	-	-
Conductivity	µs/cm	Electrical Conductivity Meter	0.1	273	-	-
Salinity	ppt	Electrical Conductivity Meter	0.1	0.1	-	-
Total Dissolved Solids	mg/L	Dried at 180°C	50	176	-	-
Total Suspended Solids	mg/L	Dried at 103-105°C	5.0	25	-	-

ANALYSIS REPORT

Customer Name : Vision E. Consultants Co., Ltd.
Address : 101/22 Moo 2, Soi Maneeya Soi 3, Sai Ma, Mueang Nonthaburi, Nonthaburi 11000
Project Name : โครงการผลิตปิโตรเลียมแหล่งโนนหลวงส่วนขยาย แปลงเอส 1 จังหวัดกำแพงเพชร (ฐานหลุมผลิตโนนหลวง-อี (NPG-E))
Project Location : จังหวัดกำแพงเพชร
Sampling Source : Surface Water Sampling
Sampling Point : บริเวณคลองหนองบัว ตำบลโนนหลวง อำเภอลานกระบือ จังหวัดกำแพงเพชร (ท้ายน้ำ)
GPS. Coordinate : UTM (WGS84) 47Q 0589840 E, 1834008 N
Sampling Date : August 8, 2023
Sampling Time : 15:32
Sampling Method : Grab
Sampling By : 
Analyzed By : Environment Research & Technology Co., Ltd.
Physical Properties : Turbid, Light Yellow, Sediment, Odorless

Quotation No. : 2023-01005
Analysis No. : 2023-AD364-002
Received Date : August 11, 2023
Analytical Date : August 11-September 6, 2023
Report No. : 2023-RAAP567
Report Date : September 6, 2023


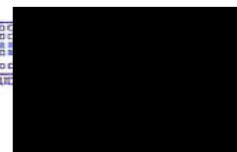
Parameter	Unit	Method of Analysis ^{1*}	MRL	Result	Standard ^{2*}	
					Class 3	Class 4
TPH (Gasoline Range Hydrocarbons; C ₆ -C ₉)	mg/L	Purge and Trap, Gas Chromatographic (GC-FID)	0.040	<0.040	-	-
TPH (Kerosene Range Hydrocarbons; C ₁₀ -C ₁₄)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	<0.020	-	-
TPH (Diesel Range Hydrocarbons; C ₁₅ -C ₂₈)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	0.114	-	-
TPH (Heavy Oil Range Hydrocarbons; C ₂₉ -C ₃₈)	mg/L	Liquid-Liquid Extraction, Gas Chromatographic (GC-FID)	0.020	0.096	-	-

Remark : ^{1*} Standard Method for Examination of Water and Wastewater, 23rd Edition, 2017.

^{2*} Modification of the National Environment Board, No.8, B.E.2537 (1994), issued under the Enhancement and Conservation of National Environmental Quality Act B.E.2535 (1992), published in the Royal Government Gazette No.111 Part 16, dated February 24, B.E.2537 (1994). (Standard Value of Surface Water for Class 3, 4)

^{3*} When water hardness not more than 100 mg/l as CaCO₃ (hardness as CaCO₃ is 83 mg/l)

n¹ = naturally but changing not more than 3°C

 Laboratory Reviewer
 Laboratory Supervisor